



**E.I. DUPONT DE NEMOURS
PONTCHARTRAIN SITE
NEOPRENE UNIT**

**APPLICATION FOR RENEWAL OF
PERMIT NUMBER 2249-V6**

**LAPLACE, LOUISIANA
ST. JOHN THE BAPTIST PARISH**

AGENCY INTEREST NUMBER 38806

DECEMBER 4, 2013



DuPont Performance Polymers
Pontchartrain Site
560 Highway 44
LaPlace, LA 70068-6908

December 4, 2013

Mr. Sanford Phillips
Assistant Secretary, Environmental Services
Department of Environmental Quality
602 N. Fifth Street
Baton Rouge, LA 70802

original to JOA
copy to Petro/G2/Taylor
PAME

Dear Mr. Phillips:

Re: Title V Permit Renewal Application, AI No. 38806 – Permit No. 2249-V6

Enclosed are three copies of the Title V permit renewal application for DuPont's Neoprene Unit located in LaPlace, Louisiana. This application includes revised emission calculations and the addition of four new sources.

The table below shows a summary of the permitted limits and the proposed limits due to the revisions and new sources.

| Pollutant | Current Permit (tpy) | Proposed Permit (tpy) | Change (tpy) |
|--------------|----------------------|-----------------------|--------------|
| Chloroprene | 173.48 | 174.3 | +0.82 |
| Toluene | 33.81 | 33.14 | -0.67 |
| VOC | 210.68 | 206.35 | -4.33 |
| Ammonia | 10.51 | 5.27 | -5.24 |
| Particulates | 0.15 | 0.19 | +0.04 |

Enclosed is a check for \$1,866.00 to cover the cost of the minor modification. If you need additional information or have any questions you can contact me at 985-536-5437 or at Doris.B.Gregory@usa.dupont.com.

Sincerely,

Doris B. Gregory

Doris B. Gregory, P.E.
Senior Environmental Consultant

Enclosures

cc: EPA Region VI

2013 DEC -5 AM 10:02

Thursday, December 05, 2013

12:29:01 PM

RECEIPT OF CHECK

Master AI #: 38806
Name on Check: El Dupont De Nemours & Company
Master File Name: E I DuPont de Nemours & Co - Pontchartrain Site
Check Received Date: 12/5/2013
Check Date: 11/20/2013
Check Number: 3000144100
Check Amount (\$): \$1,866.00
Staff Entry: SUNSHINEM
Date data entered: 12/5/2013
Media: AIR
Reason: Renewal w/a Mod.
Comments:



REG. U.S. PAT. TM OFF.

**E.I. DUPONT DE NEMOURS
PONTCHARTRAIN SITE
NEOPRENE UNIT**

**APPLICATION FOR RENEWAL OF
PERMIT NUMBER 2249-V6**

**LAPLACE, LOUISIANA
ST. JOHN THE BAPTIST PARISH**

AGENCY INTEREST NUMBER 38806

DECEMBER 4, 2013

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SECTION 1.0
INTRODUCTION

1.0 INTRODUCTION

E.I. DuPont de Nemours & Co., Inc. (DuPont) owns and operates a chemical manufacturing facility near LaPlace, Louisiana referred to as the Pontchartrain Site. The Site Location Map is provided in Figure 1.

Pontchartrain Site is a major source with respect to LAC 33:III.507 and 40 CFR 70 (i.e., a major source under the Part 70 Operating Permit program), a major stationary source with respect to LAC 33:III.509 and 40 CFR 51.166 (i.e., a major source under the Prevention of significant Deterioration [PSD] subprogram of the New Source Review [NSR] program) and a major source of toxic/hazardous air pollutants with respect to LAC 33:III.Chapter 51 and 40 CFR 63.

The site operates under several Part 70 operating permits for the following units: Neoprene Unit, Chloroprene Unit, HCl Recovery Unit, Diamines Unit and the Power Unit. The Neoprene Unit is permitted under permit number 2249-V6. This permit expires on June 16, 2014 unless a *timely and complete renewal application* has been submitted six months prior to expiration. This application is being submitted for the purpose of requesting a renewal to the existing Part 70 permit for the Neoprene Unit. This application also includes updates to the emissions calculations.

1.1 Process Description

The Neoprene Unit belongs to the Polymer and Resins I MACT Group. Neoprene is a synthetic rubber, which is a product of the polymerization of chloroprene. Chloroprene is manufactured at the Pontchartrain Site in the Chloroprene Unit. Prior to polymerization, refined chloroprene is stored in brine cooled tanks. From the tanks, the chloroprene is pumped to a make up area where various viscosity modifiers and emulsification agents are added to create a chloroprene emulsion. The emulsion is then transferred to one of the poly kettles (PKs), where polymerization occurs in the presence of a catalyst to form neoprene. Once the emulsion reaches the desired specific gravity, stabilizers are added to stop the reaction. The emulsion is then cooled and pumped to the unstripped emulsion tanks. From the tanks the emulsion is sent to the steam strippers to recover unreacted chloroprene. The chloroprene vapor is sent to condensers for recovery and the stripped emulsion is sent to storage. From storage, the emulsion is fed to the freeze roll pan. Acetic acid is added to help isolate the neoprene in the pan. As the freeze roll rotates, a film of neoprene and ice is formed on the surface and removed in a continuous sheet. The film is sent to the wash belt where it is washed with filtered water. From the wash belt, the film goes to squeeze rolls to remove excess water. The film is then sent to the air dryers where steam heated air is forced across the film. From the dryers, the film passes over a cooling roll and is gathered into a rope. The rope is fed to a cutter where the neoprene is cut into small chips. Talc is added to prevent chips from sticking together. The chips are sent through a conveyor where they are weighed and packaged in 55 pound bags.

Emissions at the facility are from the poly kettles, tanks, dryers and fugitive emissions.

ACR (2,3-dichloro-1,3-butadiene) manufactured at the Chloroprene Unit is sent to the Neoprene Unit via pipeline to be refined and stored until needed to manufacture certain neoprene types. A Process Flow Diagram of the Neoprene Unit is included as Figure 2.

1.2 Emission Sources

The following table (Table 1.1) provides a list of all the emission sources at the Neoprene Unit.

| TABLE 1.1 EMISSION SOURCE SUMMARY DUPONT – NEOPRENE UNIT | | |
|---|------------|--|
| Number | EQT | Equipment Description |
| 1700-1 | 134 | No. 7, 8, 10, 13, 14 Emulsion Storage Tanks Manhole and Exhaust Blower |
| 1700-2 | RLP0014 | Strippers Condenser Vent |
| 1700-2A | 219 | Stripper No. 1 |
| 1700-2B | 220 | Stripper No. 2 |
| 1700-2C | 221 | Stripper No. 3 |
| 1700-3 | RLP0015 | Poly Kettles Vent Condenser |
| 1700-3A | 222 | Poly Kettle No. 1 |
| 1700-3B | 223 | Poly Kettle No. 2 |
| 1700-3C | 224 | Poly Kettle No. 3 |
| 1700-3D | 225 | Poly Kettle No. 4 |
| 1700-3E | 226 | Poly Kettle No. 5 |
| 1700-5 | GRP0008 | Unstripped Emulsion Storage Tanks Common Vent (CAP) |
| 1700-5.3 | 150 | Unstripped Emulsion Storage Tank. No. 6 |
| 1700-5.4 | 151 | Unstripped Emulsion Storage Tank. No. 7 |
| 1700-5.5 | 152 | Unstripped Emulsion Storage Tank. No. 8 |
| 1700-5.6 | 153 | Unstripped Emulsion Storage Tank. No. 10 |
| 1700-5.7 | 154 | Unstripped Emulsion Storage Tank. No. 13 |
| 1700-5.8 | 155 | Unstripped Emulsion Storage Tank. No. 14 |
| 1700-5A | 167 | No. 6 Emulsion Storage Tank Manhole |
| 1700-13 | 135 | Poly Kettles Manholes/Strainers (1 and 2) Common Vent |
| 1700-13A | 136 | Poly Kettles Manholes/Strainers (3, 4 and 5) Common Vent |
| 1700-14B.3 | RLP0013 | Stabilizer and Catalyst Tanks Manhole Vent |
| 1700-14B | GRP0006 | Solution Make up Manhole Common Vent |
| 1700-14B.1 | 137 | Acetic Acid Make-up Tank |
| 1700-14B.2 | 138 | Acetic Acid Hold-up Tank |
| 1700-20 | 139 | CD Refining Column Jet |

TABLE 1.1
EMISSION SOURCE SUMMARY
DUPONT - NEOPRENE UNIT

| Number | EQT | Equipment Description |
|---------------|------------|--|
| 1700-20A | 140 | CD Refining Column Jet (Spare) |
| 1700-21A | 141 | 2MM Pound CD Storage Tank |
| 1700-25A | GRP0007 | Product Drying CAP |
| 1700-25 | 142 | East Wash Belt Dryer |
| 1700-26 | 143 | West Wash Belt Dryer |
| 1700-27 | 144 | East Hot Dryer Exhaust |
| 1700-28 | 145 | West Hot Dryer Exhaust |
| 1700-45 | 146 | No. 1 East Dryer Cooling Compartment |
| 1700-46 | 147 | No. 1 West Dryer Cooling Compartment |
| 1700-47 | 148 | No. 2 East Dryer Cooling Compartment |
| 1700-48 | 149 | No. 2 West Dryer Cooling Compartment |
| 1700-50 | GRP0009 | Stabilizer Tanks Common Vent (CAP) |
| 1700-50.1 | 156 | Stabilizer Tank No. 1 |
| 1700-50.2 | 157 | Stabilizer Tank No. 2 |
| 1700-50.3 | 158 | Stabilizer Tank No. 3 |
| 1700-50.4 | 159 | Stabilizer Tank No. 4 |
| 1700-50.5 | 160 | Stabilizer Tank No. 5 |
| 1700-50.6 | 161 | Stabilizer Tank - LD750 |
| 1700-51 | 162 | Inhibitor Mix Tank |
| 1700-53 | 163 | Stripped Emulsion Tank No. 1 |
| 1700-54 | 164 | Stripped Emulsion Tank No. 2 |
| 1700-55 | 165 | Stripped Emulsion Tank No. 3 |
| 1700-56 | RLP0016 | No. 6, 7, 8, 10, 13 and 14 Unstripped Storage Tanks Depressure Vent |
| 1700-57 | 166 | Diisobutylene (DIB) Storage Tank |
| 1700-60 | 168 | Diisobutylene Nitrosate (DIBN) Storage Tank No. 3 |
| 1700-61 | 169 | Diisobutylene Nitrosate (DIBN) Storage Tank No. 4 |
| 1700-62 | 170 | Diisobutylene Nitrosate (DIBN) Storage Tank No. 5 |
| 1700-63 | GRP0010 | Vent Header System (CAP) |
| 1700-63.1 | 171 | No. 1 CD Solution Tank |
| 1700-63.2 | 175 | No. 2 CD Solution Tank |
| 1700-63.3 | 176 | Recovered CD Storage Tank No. 1 |
| 1700-63.4 | 177 | Recovered CD Storage Tank No. 2 |
| 1700-63.5 | 178 | CD Heels Tank |
| 1700-63.8 | 181 | Crude CD Storage Tank No. 3 |
| 1700-63.9 | 182 | Refined CD Storage Tank |
| 1700-63.10 | 172 | Inhibitor Final Make-up Tank |
| 1700-63.11 | 173 | Inhibitor Hold-up Tank |
| 1700-64 | 183 | Water Solution Exhaust Fan |

TABLE 1.1
EMISSION SOURCE SUMMARY
DUPONT - NEOPRENE UNIT

| Number | EQT | Equipment Description |
|---------------|------------|---|
| 1700-66 | 185 | Poly Building Wall Fans |
| 1700-67 | 186 | Stripped Emulsion Tank No. 4 |
| 1700-68 | 187 | Stripped Emulsion Tank No. 5 |
| 1700-69 | 188 | Stripped Emulsion Tank No. 9 |
| 1700-70 | 189 | Stripped Emulsion Tank No. 11 |
| 1700-71 | 190 | Stripped Emulsion Tank No. 12 |
| 1700-72 | 191 | Stripped Emulsion Tank No. 15 |
| 1700-73 | 192 | Stripped Emulsion Tank No. 16 |
| 1700-74 | 193 | Finishing Stabilizer Makeup Bag Filter |
| 1700-75 | 194 | Resin 90 Railcar |
| 1700-76 | 195 | Rosin S Railcar |
| 1700-77 | 196 | Octopol Storage Tank |
| 1700-79 | 198 | Emergency Stabilizer Drumming |
| 1700-80 | RLP017 | ACR Storage Common Vent Header |
| 1700-80.1 | 199 | Refined ACR Storage Tank |
| 1700-80.2 | 200 | Chlorinated ACR Storage Tank |
| 1700-81 | RLP018 | ACR Refining Vent |
| 1700-81.1 | 205 | NMP/PTZ Tote |
| 1700-81.2 | 206 | Aqueous Actrene Tote |
| 1700-81.3 | 207 | Recovery Column Heels Tote |
| 1700-81.4 | 208 | TBC Tote |
| 1700-81.5 | 209 | ACR Refining Column |
| 1700-81.6 | 210 | ACR RC Condenser |
| 1700-81.7 | 211 | ACR RC Reboiler |
| 1700-82 | 201 | ACR/Solvent Blend Tank |
| 1700-83 | RLP019 | ACR Drumming Vent |
| 1 - 93 | FUG0004 | Fugitive Emissions - Neoprene Unit |
| 3 - 95 | 202 | Diversion Tank |
| 4 - 95 | 203 | Surge Tank |
| 5 - 95 | 204 | Aeration Tank |
| 1700-84A | 212 | Advanced Fibres System (AFS) Emulsion Shipping (Emulsion Blend Tank) |
| 1700-84B | 213 | Advanced Fibres System (AFS) Emulsion Shipping (Tote Loading) |
| 1700-85 | 214 | Liquid Dispersion Loading Emissions (Truck, Tote, Railcar) |
| 1700-86 | 215 | Rosin S Storage Tank |
| 6-95 | New | Clarifier |
| 1700-87 | New | No. 10 Emulsion Storage Tank Manway |
| 1700-88 | New | No. 13 Emulsion Storage Tank Manway |
| 1700-89 | New | No. 14 Emulsion Storage Tank Manway |

1.3 Emissions Calculation Methodology

Potential emissions from poly kettles, tanks, dryers and fugitive emissions are based on material balance, stack testing, and engineering calculations. Where appropriate, the latest version of USEPA emission factors and the Tanks program are used to calculate emissions. Emission calculations are presented in Appendix A.

Calculations were updated to reflect current operations; also four new sources were added. Below is a comparison of the current permitted limits and the proposed limits.

| Pollutant | Current Permit (tpy) | Proposed Permit (tpy) | Change (tpy) |
|------------------|---------------------------------|----------------------------------|-------------------------|
| Chloroprene | 173.48 | 174.3 | +0.82 |
| Toluene | 33.81 | 33.14 | -0.67 |
| VOC | 210.68 | 206.35 | -4.33 |
| Ammonia | 10.51 | 5.27 | -5.24 |
| Particulates | 0.15 | 0.19 | +0.04 |

1.4 Consolidation of Fugitive Emissions

On November 18, 2013, DuPont submitted a site wide Fugitive Emissions Program Consolidation Notice. A copy of this document is included in Appendix C. DuPont is requesting to incorporate this program with the permit renewal.

SECTION 2.0
REGULATORY APPLICABILITY

2.0 REGULATORY APPLICABILITY

2.1 Federal and State Regulations

The Pontchartrain Site is subject to a variety of federal and state air quality regulations. State requirements are outlined in Chapters 9, 11, 13, 21, 51, 56 and 59 of the Louisiana Air Quality Regulations. In accordance with LAC 33:III.517.D.10, state and federal requirements have been identified in a matrix on Table 1 contained in Item 22 of the Application for Approval of Emissions of Air Pollutants from Part 70 Sources (Section 3.0 of this document). Table 2 of Item 22 clearly identifies potentially applicable state and federal requirements for the facility. Table 2 also contains a description and reference to compliance methods/provisions required by regulations and/or current permit. Table 3, also contained in Item 22, indicates exempt status or non-applicability for emission sources.

2.2 Prevention of Significant Deterioration (PSD) Regulations

This application does not include a significant modification; therefore, a PSD review is not required.

2.3 Nonattainment New Source Review (NNSR)

St. John the Baptist Parish, in which the DuPont, Neoprene facility is located, is designated as an attainment area for all criteria pollutants. Therefore, NNSR does not apply.

2.4 New Source Performance Standards (NSPS)

Certain units or equipment items at the Neoprene Unit are designated as affected facilities under 40 CFR 60, Subpart Kb.

2.5 National Emission Standards for Hazardous Air Pollutants (40 CFR 61 AND 63)

The Pontchartrain Site is a major source of hazardous air pollutants (HAPs). The facility is subject to certain provisions of 40 CFR 61 and 63, which are stated in the applicability matrices of the permit application form, Item 22 in Section 3.0 of this document.

2.6 Louisiana Air Toxics Program - LAC 33:III.Chapter 51 (State Only Requirements)

The Pontchartrain Site is a major source of toxic air pollutants (TAPs). The facility is subject to certain provisions of LAC 33:III.Chapter 51, which are stated in the

applicability matrices of the permit application form, Item 22 in Section 3.0 of this document.

2.7 Insignificant Activities

The Neoprene facility engages in a variety of activities which are defined as insignificant under LAC 33:III.501.B.5. Activities exempt based on size or emission rate are addressed in Item 20 of The Application for Approval of Emissions from Part 70 Sources, Section 3.0 of this document.

2.8 General Condition XVII Activities

The Neoprene facility performs various activities which are authorized under LDEQ General Permit Condition XVII which are included in the current Air Permit No. 2249-V6. These activities are listed in Item 19 of the Application for Approval of Emissions from Part 70 Sources, Section 3.0 of this document.

SECTION 3.0

APPLICATION FOR APPROVAL OF EMISSIONS OF AIR POLLUTANTS FROM PART 70 SOURCES

Department of Environmental Quality
Office of Environmental Services
Air Permits Division
P.O. Box 4313
Baton Rouge, LA 70821-4313
(225) 219-3181

LOUISIANA

Application for Approval of Emissions of Air Pollutants from Part 70 Sources



PLEASE TYPE OR PRINT

1. Facility Information [LAC 33:III.517.D.1]

| | | |
|---|---|--|
| Facility Name or Process Unit Name (if any) Pontchartrain Works, Neoprene Unit | | <input type="checkbox"/> All Process Units <input checked="" type="checkbox"/> Process Unit-specific Permit |
| Agency Interest Number (A.I. Number) 38806 | Currently Effective Permit Number(s) 2249-V6 | |
| Company - Name of Owner E.I. DuPont de Nemours and Co., Inc. (DuPont) | | |
| Company - Name of Operator (if different from Owner) | | |
| Parent Company (if Company - Name of Owner given above is a division) | | |

Ownership:

Check the appropriate box.

- ☒ corporation, partnership, or sole proprietorship ☐ regulated utility ☐ municipal government
☐ state government ☐ federal government ☐ other, specify _____

2. Physical Location and Process Description [LAC 33:III.517.D.18, unless otherwise stated]

What does this facility produce? Add more rows as necessary.

This unit manufactures, neoprene, which is a synthetic rubber made by the polymerization of chloroprene.

What modifications/changes are proposed in this application? Add more rows as necessary.

This is the five year renewal application for the Neoprene Unit.

Nearest town (in the same parish as the facility):

LaPlace

Parish(es) where facility is located:

St. John the Baptist

| | | | | |
|-------------------------------------|-----------|--------------|----------------|------------------|
| Distance To (mi): | 194 Texas | 210 Arkansas | 56 Mississippi | 131 Alabama |
| Latitude of Facility Front Gate: | 30 Deg | 03 Min | 14 Sec | _____ Hundredths |
| Longitude of Facility Front Gate: | 90 Deg | 31 Min | 29 Sec | _____ Hundredths |
| Distance from nearest Class I Area: | 113 | kilometers | | |

Add physical address and description of location of the facility below. If the facility has no address, provide driving directions. Add more rows as necessary.

The facility is located at 586 Highway 44, LaPlace, Louisiana. The facility is bordered on the south by the Mississippi River, to the North by John L. Ory School and Airline Highway. Residential properties adjoin the facility to the east and the west.

- ☒ Map attached (required per LAC 33:III.517.D.1)
☒ Description of processes and products attached (required per LAC 33:III.517.D.2)
☒ Introduction/Description of the proposed project attached (required per LAC 33:III.517.D.5)

3. Confidentiality [LAC 33.I.Chapter 5]

Are you requesting confidentiality for any information except air pollutant emission rates? ☐ Yes ☒ No

If "yes," list the sections for which confidentiality is requested below. Add rows as necessary. Confidentiality requests require a submittal that is separate from this application. Information for which confidentiality is requested should not be submitted with this application. Consult instructions.

4. Type of Application [LAC 33:III.517.D]

Complete the appropriate column (1 or 2) that corresponds to the type of permit being sought. Check all that apply within the appropriate column.

| Column 1 | Column 2 |
|--|--|
| <input type="checkbox"/> Part 70 General | <input type="checkbox"/> Part 70 Regular |
| <input type="checkbox"/> Renewal | <input checked="" type="checkbox"/> Renewal |
| Select one, if applicable: <input type="checkbox"/> Entirely new facility <input type="checkbox"/> Modification or expansion of existing facility (may also include reconciliations) <input type="checkbox"/> Reconciliation only <input type="checkbox"/> Individual emissions unit(s) addition | Select one, if applicable: <input type="checkbox"/> Entirely new facility <input type="checkbox"/> Significant modification or expansion of existing facility (may also include reconciliations) [LAC 33:III.527] <input checked="" type="checkbox"/> Minor modification or expansion of existing facility (may also include reconciliations) [LAC 33:III.525] <input type="checkbox"/> Reconciliation only NSR Analysis: PSD <input type="checkbox"/> NNSR <input type="checkbox"/> |

Does this submittal update or replace an application currently under review? ☐ Yes ☒ No

If yes, provide date that the prior application was submitted: _____

Select one if this application is for an existing facility that does not have an air quality permit:

- ☐ Previously Grandfathered (LAC 33:III.501.B.6)
☐ Previously Exempted (e.g., Small Source Exemption; LAC 33:III.501.B.2.d)
☐ Previously Unpermitted

5. Fee Information [LAC 33:III.517.D.17]

Fee Parameter: If the fee code is based on an operational parameter (such as number of employees or capital cost), enter that parameter here. _____

Industrial Category: Enter the Standard Industrial Classification (SIC) and North American Industry Classification (NAICS) Codes that apply to the facility.

Primary SICC: 2822 **NAICS Code:** 325212

Secondary SICC(s): _____

Project Fee Calculation: Enter fee code, permit type, production capacity/throughput, and fee amount pursuant to LAC 33:III.Chapter 2. Add rows to this table as needed. Include with the application the amount in the Grand Total blank as the permit application fee.

| FEE CODE | TYPE | EXISTING CAPACITY | INCREMENTAL CAPACITY INCREASE | SURCHARGES | | | | TOTAL AMOUNT |
|-------------|------|-------------------|-------------------------------|------------|--------------------------|--------------------------|--------------------------|--------------|
| | | | | MULTIPLIER | NSPS | PSD | AIR TOXICS | |
| 0580 | | | | | <input type="checkbox"/> | <input type="checkbox"/> | <input type="checkbox"/> | \$1,866.00 |
| | | | | | <input type="checkbox"/> | <input type="checkbox"/> | <input type="checkbox"/> | \$ |
| GRAND TOTAL | | | | | | | | \$ |

****Optional** Fee Explanation:** Use the space provided to give an explanation of the fee determination displayed above. Using this area will help to avoid confusion.

Electronic Fund Transfer (EFT): If paying the permit application fee using an Electronic Fund Transfer (EFT), please include the EFT Transaction Number, the Date that the EFT was made, and the total dollar amount submitted in the EFT. If not paying the permit application fee using EFT, leave blank.

EFT Transaction Number

Date of Submittal

Total Dollar Amount

\$

6. Key Dates

Estimated date construction will commence:

NA

Estimated date operation will commence:

NA

7. Pending Permit Applications – For Process Unit-Specific Permits Only

[LAC 33:III.517.D.18]

List all other process units at this facility for which Part 70 permit applications have been submitted, but have not been acted upon by LDEQ as of the date of submittal of this application. If none, state "none" in the table. ****It is not necessary to update this table during the permit review process, unless requested by LDEQ.****

| Process Unit Name | Permit Number | Date Submitted |
|-------------------|---------------|----------------|
| | | |
| | | |
| | | |
| | | |

8. LAC 33:I.1701 Requirements – Answer all below for new sources and permit renewals - ☒ Yes ☐ No

Does the company or owner have federal or state environmental permits identical to, or of a similar nature to, the permit for which you are applying in Louisiana or other states? (This requirement applies to all individuals, partnerships, corporations, or other entities who own a controlling interest of 50% or more in your company, or who participate in the environmental management of the facility for an entity applying for the permit or an ownership interest in the permit.)

☐ Yes ☒ No

If yes, list States:

Do you owe any outstanding fees or final penalties to the Department? ☐ Yes ☒ No

If yes, explain below. Add rows if necessary.

Is your company a corporation or limited liability company? ☒ Yes ☐ No

If yes, attach a copy of your company's Certificate of Registration and/or Certificate of Good Standing from the Secretary of State. The appropriate certificate(s) should be attached to the end of this application as an appendix.

9. Permit Shield Request [LAC 33:III.517.E.7] - ☐ Yes ☒ No

If yes, check the appropriate boxes to indicate the type of permit shield being sought. Include the specific regulatory citation(s) for which the shield is being requested. Give an explanation of the circumstances that will justify the permit shield request. Attach additional pages if necessary. If additional pages are used, attach them directly behind this page and enter "See Attached Pages" into the Explanation field.

Type of Permit Shield request (check all that apply):

| Non-applicability determination for: | Specific Citation(s) | Explanation |
|--|----------------------|-------------|
| <input type="checkbox"/> 40 CFR 60 | | |
| <input type="checkbox"/> 40 CFR 61 | | |
| <input type="checkbox"/> 40 CFR 63 | | |
| <input type="checkbox"/> Prevention of Significant Deterioration | | |
| <input type="checkbox"/> Nonattainment New Source Review | | |

| Interpretation of monitoring, recordkeeping, and/or reporting requirements, and/or means of compliance for: | Specific Citation(s) | Explanation |
|---|----------------------|-------------|
| <input type="checkbox"/> 40 CFR 60 | | |
| <input type="checkbox"/> 40 CFR 61 | | |
| <input type="checkbox"/> 40 CFR 63 | | |
| <input type="checkbox"/> Prevention of Significant Deterioration | | |
| <input type="checkbox"/> Nonattainment New Source Review | | |
| <input type="checkbox"/> State Implementation Plan (SIP) Regulation(s) referenced in 40 CFR 52 Subpart T | | |

10. Certification of Compliance With Applicable Requirements

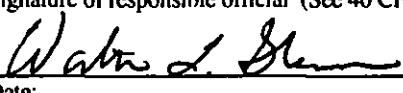
Statement for Applicable Requirements for Which the Company and Facility Referenced In This Application Is In Compliance

Based on information and belief, formed after reasonable inquiry, the company and facility referenced in this application is in compliance with and will continue to comply with all applicable requirements pertaining to the sources covered by the permit application, as outlined in Tables 1 and 2 in the permit application. For requirements promulgated as of the date of this certification with compliance dates effective during the permit term, I further certify that the company and facility referenced in this application will comply with such requirements on a timely basis and will continue to comply with such requirements.

For corporations only: By signing this form, I certify that, in accordance with the definition of Responsible Official found in LAC 33:III.502, (1) I am a president, secretary, treasurer, or vice-president in charge of a principal business function, or other person who performs similar policy or decision-making functions; or (2) I am a duly authorized representative of such person; am responsible for the overall operation of one or more manufacturing, production, or operating facilities addressed in this permit application; and either the facilities employ more than 250 persons or have gross annual sales or expenditures exceeding \$25 million (in second quarter 1980 dollars); or the delegation of authority has been approved by LDEQ prior to this certification.*

CERTIFICATION: I certify, under provisions in Louisiana and United States law which provide criminal penalties for false statements, that based on information and belief formed after reasonable inquiry, the statements and information contained in this Application for Approval of Emissions of Air Pollutants from Part 70 Sources, including all attachments thereto and the compliance statement above, are true, accurate, and complete.

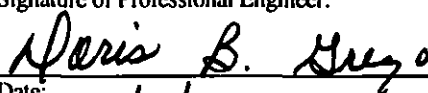
| | | |
|--|-------------|--------------|
| a. Responsible Official | | |
| Name Walter L. Glenn | | |
| Title Plant Manager | | |
| Company E.I. DuPont de Nemours and Company | | |
| Suite, mail drop, or division | | |
| Street or P.O. Box 586 Highway 44 | | |
| City LaPlace | State LA | Zip 70068 |
| Business phone 985-536-5129 | | |
| Email Address walter.l.glenn@usa.dupont.com | | |

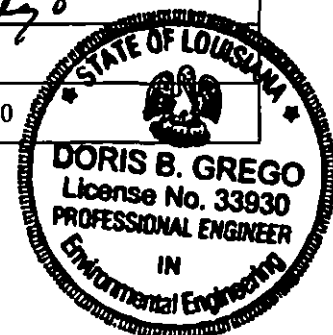
| | |
|---|--|
| Signature of responsible official (Sec 40 CFR 70.2):  | |
| Date: 12-8-13 | |

*Approval of a delegation of authority can be requested by completing a Duly Authorized Representative Designation Form (Form_7218) available on LDEQ's website at <http://www.deq.louisiana.gov/portal/tabid/2758/Default.aspx>

CERTIFICATION: I certify that the engineering calculations, drawings, and design are true and accurate to the best of my knowledge.

| | | |
|---|-------------|--------------|
| b. Professional Engineer | | |
| Name Doris B. Grego | | |
| Title Senior Environmental Consultant | | |
| Company E.I. DuPont de Nemours and Company | | |
| Suite, mail drop, or division | | |
| Street or P.O. Box 586 Highway 44 | | |
| City LaPlace | State LA | Zip 70068 |
| Business phone 985-536-5437 | | |
| Email Address doris.b.grego@usa.dupont.com | | |

| | |
|---|-------|
| Signature of Professional Engineer:  | |
| Date: 12/2/13 | |
| Louisiana Registration No. | 33930 |



11. Personnel [LAC 33:III.517.D.1]

| | | |
|--|-------------|--|
| a. Manager of Facility who is located at plant site | | |
| Name Walter L. Glenn | | <input type="checkbox"/> Primary contact |
| Title Plant Manager | | |
| Company E.I. DuPont de Nemours and Company | | |
| Suite, mail drop, or division | | |
| Street or P.O. Box 586 Highway 44 | | |
| City LaPlace | State LA | Zip 70068 |
| Business phone 985-536-5129 | | |
| Email address walter.l.glenn@usa.dupont.com | | |

| | | |
|---|-------------|---|
| b. On-site contact regarding air pollution control | | |
| Name Doris B. Grego | | <input checked="" type="checkbox"/> Primary contact |
| Title Senior Environmental Consultant | | |
| Company E.I. DuPont de Nemours and Company | | |
| Suite, mail drop, or division | | |
| Street or P.O. Box 586 Highway 44 | | |
| City LaPlace | State LA | Zip 70068 |
| Business phone 985-536-5437 | | |
| Email address doris.b.grego@usa.dupont.com | | |

| | | |
|---|-------|--|
| c. Person to contact with written correspondence | | |
| Name | | <input type="checkbox"/> Primary contact |
| Title | | |
| Company | | |
| Suite, mail drop, or division | | |
| Street or P.O. Box | | |
| City | State | Zip |
| Business phone | | |
| Email address | | |

| | | |
|---|-------|--|
| d. Person who prepared this report | | |
| Name | | <input type="checkbox"/> Primary contact |
| Title | | |
| Company | | |
| Suite, mail drop, or division | | |
| Street or P.O. Box | | |
| City | State | Zip |
| Business phone | | |
| Email address | | |

| | | | |
|---|--|---|-----------|
| e. Person to contact about Annual Maintenance Fees | | <input type="checkbox"/> a <input checked="" type="checkbox"/> b <input type="checkbox"/> c <input type="checkbox"/> d <input type="checkbox"/> other (specify below) | |
| Name | | <input type="checkbox"/> Primary contact | |
| Title | | Suite, mail drop, or division | |
| Company | | Street or P.O. Box | |
| Business Phone | | City | State Zip |
| | | Email Address | |

List the total emissions following the proposed project for this facility or process unit (for process unit-specific permits). Speciate all criteria pollutants, TAP, and HAP for the proposed project.

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09/04/13

List each of the following in chronological order:

- [illegible]

14.a. Enforcement Actions [LAC 33:III.517.D.18] - ☐ Yes ☒ No

If yes, list all federal and state air quality enforcement actions, settlement agreements, and consent decrees received for this facility and/or process unit (for process unit-specific permits) since the issuance of the currently effective Title V Operating Permit or State Operating Permit. For each action, list the type of action (or its tracking number), the regulatory authority or authorities that issued the action, and the date that the action was issued. Summarize the conditions imposed by the enforcement action, settlement agreement, and consent decree in Section 22, Table 2. It is not necessary to submit a copy of the referenced action. Add rows to table as necessary.

| Type of Action or Tracking Number | Issuing Authority | Date Action Issued | Summary of Conditions Included? |
|-----------------------------------|-------------------|--------------------|--|
| | | | <input type="checkbox"/> Yes <input type="checkbox"/> No |
| | | | <input type="checkbox"/> Yes <input type="checkbox"/> No |

14.b. Schedule for Compliance [LAC 33:III.517.E.4] ☐ Yes ☒ No

If the facility or process unit for which application is being made is not in full compliance with all applicable regulations, give a description of how compliance will be achieved, including a schedule for compliance below. Add rows as necessary. See instructions.

15. Letters of Approval for Alternate Methods of Compliance - ☒ Yes ☐ No

If yes, list all correspondence with LDEQ, EPA, or other regulatory bodies that provides for or supports a request for alternate methods of compliance with any applicable regulations for this facility or process unit (for process unit-specific permits). List the date of issuance of the letter and the regulation referenced by the letter. **Attach as an appendix a copy of all documents referenced in this table.** Letters that are not included may not be incorporated into a final permit. Add rows to table as necessary.

| Date Letter Issued | Issuing Authority | Referenced Regulation(s) | Copy of Letter Attached? |
|--------------------|-------------------|--------------------------|---|
| 1997 | LDEQ | 40 CFR 63.114(b)(2) | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| | | | <input type="checkbox"/> Yes <input type="checkbox"/> No |
| | | | <input type="checkbox"/> Yes <input type="checkbox"/> No |
| | | | <input type="checkbox"/> Yes <input type="checkbox"/> No |

16. Initial Notifications and Performance Tests [LAC 33:III.517.D.18] - ☐ Yes ☒ No

If yes, list any initial notifications that have been submitted or one-time performance tests that have been performed for this facility or process unit (for process unit-specific permits) since the issuance of the currently effective Title V Operating Permit or State Operating Permit in order to satisfy regulatory requirements. Any initial notification or one-time performance test requirements that have not been satisfied should be listed in Section 22, Table 2 of this application. Any notifications or performance tests that recur periodically should also be properly noted in Section 22, Table 2 of this application. Add rows to table as necessary.

| Initial Notification or One-time Performance Test? | Regulatory Citation Satisfied | Applicable Source(s) | Date Completed/Approved |
|--|-------------------------------|----------------------|-------------------------|
| | | | |
| | | | |
| | | | |

17. Existing Prevention of Significant Deterioration or Nonattainment New Source Review Limitations [LAC 33:III.517.D.18]

Do one or more emissions sources represented in this permit application currently operate under one or more NSR permits?

☐ Yes ☒ No

If "yes," summarize the limitations from such permit(s) in the following table. Add rows to table as necessary. Be sure to note any annual emissions limitations from such permit(s) in Sections 12 and 13 of this application.

| Permit Number | Date Issued | Emission Point ID No. | Pollutant | BACT/LAER Limit ¹ | Averaging Period | Description of Control Technology/Work Practice Standards |
|---------------|-------------|-----------------------|-----------|------------------------------|------------------|---|
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |

¹For example, lb/MM Btu, ppmvd @ 15% O₂, lb/ton, lb/hr

18. Air Quality Dispersion Modeling [LAC 33:III.517.D.15]

Was Air Quality Dispersion Modeling as required by LAC 33:III performed in support of this permit application? (Air Quality Dispersion Modeling is only required when applying for PSD permits and as requested by LDEQ.)

☐ Yes ☒ No

Has Air Quality Dispersion Modeling completed in accordance with LAC 33:III ever been performed for this facility in support of a air permit application previously submitted for this facility or process unit (for process unit-specific permits) or as required by other regulations AND approved by LDEQ?

☒ Yes ☐ No

If yes, enter the date the most recent Air Quality Dispersion Modeling results as required by LAC 33:III were submitted:

If the answer to either question above is "yes," enter a summary of the most recent results in the following table. If the answer to both questions is "no," enter "none" in the table. Add rows to table as necessary.

| Pollutant | Time Period | Calculated Maximum Ground Level Concentration | Louisiana Toxic Air Pollutant Ambient Air Standard or (National Ambient Air Quality Standard {NAAQS}) |
|-------------|-------------|---|---|
| Chloroprene | 8 hours | 250 µg/m ³ | 857 µg/m ³ |
| | | | |
| | | | |
| | | | |
| | | | |

19. General Condition XVII Activities- ☒ Yes ☐ No

Enter all activities that qualify as Louisiana Air Emissions Permit General Condition XVII Activities.

- Expand this table as necessary to include all such activities.
- See instructions to determine what qualifies as a General Condition XVII Activity.
- Do not include emissions from General Condition XVII Activities in the proposed emissions totals for the permit application.

| | | Emission Rates - TPY | | | | | |
|--|-------------|----------------------|-----------------|-----------------|----|-------|-------|
| Work Activity | Schedule | PM ₁₀ | SO ₂ | NO _x | CO | VOC | Other |
| Inhibitor Mix Tank Cleaning | 1 time/yr | | | | | 0.003 | |
| Refining Column Cleaning | 9 times/yr | | | | | 0.11 | |
| Acetic Acid Rail Car | 1 time/yr | | | | | 0.02 | |
| Routine Maintenance Activities | NA | | | | | 1.75 | |
| Railcars During Shutdown (20 Loading/Steaming) | 2 times/yr | | | | | 0.17 | |
| ACR Refining Column and Tanks Cleaning | 25 times/yr | | | | | 0.25 | |

20. Insignificant Activities [LAC 33:III.501.B.5] - ☐ Yes ☐ No

Enter all activities that qualify as Insignificant Activities.

- Expand this table as necessary to include all such activities.
- For sources claimed to be insignificant based on size or emission rate (LAC 33:III.501.B.5.A), information must be supplied to verify each claim. This may include but is not limited to operating hours, volumes, and heat input ratings.
- If aggregate emissions from all similar pieces of equipment (i.e. all LAC 33:III.501.B.5.A.1 activities) claimed to be insignificant are greater than 5 tons per year for any pollutant, then the activities can not be claimed as insignificant and must be represented as permitted emission sources. Consult instructions.

| Emission Point ID No. | Description | Physical/Operating Data | Citation |
|-----------------------|--------------------------------|-------------------------|------------------------|
| | No. 1 Blend Tank | | LAC 33:III.501.B.5.A.3 |
| | No. 2 Blend Tank | | LAC 33:III.501.B.5.A.3 |
| | Precondenser Rundown Tank | | LAC 33:III.501.B.5.A.3 |
| | EDMA Tote | | LAC 33:III.501.B.5.A.3 |
| | Calight RPO Tote | | LAC 33:III.501.B.5.A.3 |
| | DAXAD Tote | | LAC 33:III.501.B.5.A.3 |
| | Dresinate Tote | | LAC 33:III.501.B.5.A.3 |
| | Poly Witcolake Tote | | LAC 33:III.501.B.5.A.3 |
| | Finishing Witcolake Tote | | LAC 33:III.501.B.5.A.3 |
| | DEA Tote | | LAC 33:III.501.B.5.A.3 |
| | Keltrol Solution Tank | | LAC 33:III.501.B.5.A.3 |
| | Sulfur Slurry Batch Tank No. 1 | | LAC 33:III.501.B.5.A.3 |
| | Sulfur Slurry Batch Tank No. 2 | | LAC 33:III.501.B.5.A.3 |

| Emission Point ID No. | Description | Physical/Operating Data | Citation |
|-----------------------|--|-------------------------|------------------------|
| | Finishing Stabilizer M/U Tank | | LAC 33:III.501.B.5.A.3 |
| | Finishing Stabilizer Hold Tank | | LAC 33:III.501.B.5.A.3 |
| | Finishing Stabilizer Batch Scale Tank | | LAC 33:III.501.B.5.A.3 |
| | Lomar Head Tank | | LAC 33:III.501.B.5.A.3 |
| | KOH Tote | | LAC 33:III.501.B.5.A.4 |
| | KOH Storage Tank | | LAC 33:III.501.B.5.A.4 |
| | DDM Storage Tank | | LAC 33:III.501.B.5.A.3 |
| | No. 1 Vent Hood (ACR Lab) | | LAC 33:III.501.B.5.A.6 |
| | No. 2 Vent Hood (Neoprene Lab) | | LAC 33:III.501.B.5.A.6 |
| | ACR Refining Decanter, Emergency Vent | | LAC 33:III.501.B.5.A.6 |

21. Regulatory Applicability for Commonly Applicable Regulations – Answer all below [LAC 33:III.517.D.10]

Does this facility contain asbestos or asbestos containing materials? ☒ Yes ☐ No

If "yes," the facility or any portion thereof may be subject to 40 CFR 61, Subpart M, LAC 33:III.Chapter 27, and/or LAC 33:III.5151 and this application must address compliance as stated in Section 22 of this application

Is the facility or process unit represented in this permit subject to 40 CFR 68, or is any other process unit located at the same facility as the process unit represented in this application subject to 40 CFR 68? ☒ Yes ☐ No

If "yes," the entire facility is subject to 40 CFR 68 and LAC 33:III.Chapter 59 and this application must address compliance as stated in Section 22 of this application.

Is the facility listed in LAC 33:III.5611

Table 5 ☒ Yes ☐ No

Table 6 ☒ Yes ☐ No

Table 7 ☒ Yes ☐ No

Does the applicant own or operate commercial refrigeration equipment normally containing more than 50 pounds of refrigerant at this facility or process unit? ☒ Yes ☐ No

If "yes," the entire facility is subject to 40 CFR 82, Subpart F and this application must address compliance as stated in Section 22 of this application.

22. Applicable Regulations, Air Pollution Control Measures, Monitoring, and Recordkeeping

Important points for Table 1 [LAC 33:III.517.D.10]:

- List in Table 1, by Emission Point ID Number and Descriptive Name of the Equipment, state and federal pollution abatement programs and note the applicability or non-applicability of the regulations to each source.
- Adjust the headings for the columns in Table 1 as necessary to reflect all applicable regulations, in addition to any regulations that do not apply but need an applicability determination to verify this fact.
- For each piece of equipment, enter "1" for each regulation that applies. Enter "2" for each regulation that applies to this type of source, but from which this source of emissions is exempt. Enter "3" for equipment that is subject to a regulation, but does not have any applicable requirements. Also, enter "3" for each regulation that have applicable requirements that apply to the particular emission source but the regulations currently do not apply due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.
- Leave the spaces blank when the regulations clearly would not apply under any circumstances to the source. For example, LAC 33:III.2103 – Storage of Volatile Organic Compounds would never apply to a steam generating boiler, no matter the circumstances.
- Consult instructions.

Important points for Table 2 [LAC 33:III.517.D.4; LAC 33:III.517.D.7; LAC 33:III.517.D.10]:

- For each piece of equipment listed in Table 2, include all applicable limitation, recordkeeping, reporting, monitoring, and testing requirements. Also include any one-time notification or one-time tests performance test requirements that have not been fulfilled.
- Each of these regulatory aspects (limitation, recordkeeping, reporting, etc.) should be addressed for each regulation that is applicable to each emissions source or emissions point.
- For each regulation that provides a choice regarding the method of compliance, indicate the method of compliance that will be employed. It is not sufficient to state that all compliance options will be employed, though multiple compliance options may be approved as alternative operating scenarios.
- Consult instructions.

Important points for Table 3 [LAC 33:III.517.D.16]:

- Each time a 2 or a 3 is used to describe applicability of a source in Table 1, an entry should be made in Table 3 that explains the exemption or non-applicability status of the regulation to that source.
- Fill in all requested information in the table.
- The exact regulatory citation that provides for the specific exemption or non-applicability determination should be entered into the Citation Providing for Exemption or Non-applicability column.
- Consult Instructions.

Important points for Table 4 [LAC 33:III.517.D.18]

- List any single emission source that routes its emissions to another point where these emissions are commingled with the emissions of other sources before being released to the atmosphere. Do not list any single emission source in this table that does not route its emissions in this manner.
- List any and all emission sources that are routed as described above. This includes emission sources that do not otherwise appear in this permit application.
- Consult instructions.

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | LAC 33:III | | | | | | | | LAC 33:III.Chapter | | | | | | | | | | |
|----------------|---|------------|------|------|------|------|------|------|------|--------------------|---|----|----|----|----|----|----|----|----|----|
| | | 509 | 2103 | 2104 | 2107 | 2111 | 2113 | 2115 | 2121 | 5 | 9 | 11 | 13 | 15 | 22 | 29 | 51 | 53 | 56 | 59 |
| UNF001 | Plant Wide | | | | | 1 | 1 | | | 1 | 1 | 1 | 1 | 1 | | | 1 | | 1 | 1 |
| EQT134 | 1700-1 No. 7, 8, 10, 13, 14 Emulsion Storage Tanks Manhole and Exhaust Blower | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT135 | 1700-13 Poly Kettles Manholes/Strainers (1 and 2) | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT136 | 1700-13A Poly Kettles Manholes/Strainers (3, 4 and 5) | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT137 | 1700-14B.1 Acetic Acid Make-up Tank | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT138 | 1700-14B.2 Acetic Acid Hold-up Tank | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT139 | 1700-20 CD Refining Column Jet | | | | | | | 1 | | | | | | | | | 1 | | | |
| EQT140 | 1700-20A CD Refining Column Jet (Spare) | | | | | | | 1 | | | | | | | | | 1 | | | |
| EQT141 | 1700-21A 2MM Pound CD Storage Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT142 | 1700-25 East Wash Belt Dryer | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT143 | 1700-26 West Wash Belt Dryer | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT144 | 1700-27 East Hot Dryer Exhaust | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT145 | 1700-28 West Hot Dryer Exhaust | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT146 | 1700-45 No. 1 East Dryer Cooling Compt. | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT147 | 1700-46 No. 1 West Dryer Cooling Compt. | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT148 | 1700-47 No. 2 East Dryer Cooling Compt. | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT149 | 1700-48 No. 2 West Dryer Cooling Compt. | | | | | | | 2 | | | | | | | | | 1 | | | |
| EQT150 | 1700-5.3 Unstripped Emulsion Storage Tank. No. 6 | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT151 | 1700-5.4 Unstripped Emulsion Storage Tank. No. 7 | | 1 | | | | | | | | | | | | | | 1 | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | LAC 33:III | | | | | | | | LAC 33:III.Chapter | | | | | | | | | | |
|----------------|---|------------|------|------|------|------|------|------|------|--------------------|---|----|----|----|----|----|----|----|----|----|
| | | 509 | 2103 | 2104 | 2107 | 2111 | 2113 | 2115 | 2121 | 5 | 9 | 11 | 13 | 15 | 22 | 29 | 51 | 53 | 56 | 59 |
| EQT152 | 1700-5.5 Unstripped Emulsion Storage Tank. No. 8 | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT153 | 1700-5.6 Unstripped Emulsion Storage Tank. No. 10 | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT154 | 1700-5.7 Unstripped Emulsion Storage Tank. No. 13 | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT155 | 1700-5.8 Unstripped Emulsion Storage Tank. No. 14 | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT156 | 1700-50.1 Stabilizer Tank No. 1 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT157 | 1700-50.2 Stabilizer Tank No. 2 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT158 | 1700-50.3 Stabilizer Tank No. 3 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT159 | 1700-50.4 Stabilizer Tank No. 4 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT160 | 1700-50.5 Stabilizer Tank No. 5 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT161 | 1700-50.6 Stabilizer Tank – LD750 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT162 | 1700-51 Inhibitor Mix Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT163 | 1700-53 Stripped Emulsion Tank No. 1 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT164 | 1700-54 Stripped Emulsion Tank No. 2 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT165 | 1700-55 Stripped Emulsion Tank No. 3 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT166 | 1700-57 Diisobutylene (DIB) Storage Tank | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT167 | 1700-5A No. 6 Emulsion Storage Tank Manhole | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT168 | 1700-60 Diisobutylene Nitrosate (DIBN) Storage Tank No. 3 | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT169 | 1700-61 Diisobutylene Nitrosate (DIBN) Storage Tank No. 4 | | 3 | | | | | | | | | | | | | | 3 | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | LAC 33:III | | | | | | | | LAC 33:III.Chapter | | | | | | | | | | |
|----------------|---|------------|------|------|------|------|------|------|------|--------------------|---|----|----|----|----|----|----|----|----|----|
| | | 509 | 2103 | 2104 | 2107 | 2111 | 2113 | 2115 | 2121 | 5 | 9 | 11 | 13 | 15 | 22 | 29 | 51 | 53 | 56 | 59 |
| EQT170 | 1700-62 Diisobutylene Nitrosate (DIBN) Storage Tank No. 5 | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT171 | 1700-63.1 No. 1 CD Solution Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT172 | 1700-63.10 Inhibitor Final Make-up Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT173 | 1700-63.11 Inhibitor Hold-up Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT175 | 1700-63.2 No. 2 CD Solution Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT176 | 1700-63.3 Recovered CD Storage Tank No. 1 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT177 | 1700-63.4 Recovered CD Storage Tank No. 2 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT178 | 1700-63.5 CD Heels Tank | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT181 | 1700-63.8 Crude CD Storage Tank No. 3 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT182 | 1700-63.9 Refined CD Storage Tank | | 1 | | | | | | | | | | | | | | 1 | | | |
| EQT183 | 1700-64 Water Solution Exhaust Fan | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT185 | 1700-66 Poly Building Wall Fans | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT186 | 1700-67 Stripped Emulsion Tank No. 4 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT187 | 1700-68 Stripped Emulsion Tank No. 5 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT188 | 1700-69 Stripped Emulsion Tank No. 9 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT189 | 1700-70 Stripped Emulsion Tank No. 11 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT190 | 1700-71 Stripped Emulsion Tank No. 12 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT191 | 1700-72 Stripped Emulsion Tank No. 15 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT192 | 1700-73 Stripped Emulsion Tank No. 16 | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT193 | 1700-74 Finishing Stabilizer Makeup Bag Filter | | | | | | | | | | | | 1 | | | | | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | LAC 33:III | | | | | | | | LAC 33:III.Chapter | | | | | | | | | | |
|----------------|--|------------|------|------|------|------|------|------|------|--------------------|---|----|----|----|----|----|----|----|----|----|
| | | 509 | 2103 | 2104 | 2107 | 2111 | 2113 | 2115 | 2121 | 5 | 9 | 11 | 13 | 15 | 22 | 29 | 51 | 53 | 56 | 59 |
| EQT194 | 1700-75 Resin 90 Railcar | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT195 | 1700-76 Rosin S Railcar | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT196 | 1700-77 Octopol StorageTank | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT198 | 1700-79 Emergency Stablizer Drumming | | | | | | | 2 | | | | | | | | | 3 | | | |
| EQT199 | 1700-80.1 Refined ACR Storage Tank | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT200 | 1700-80.2 Chlorinated ACR Storage Tank | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT201 | 1700-82 ACR/Solvent Blend Tank | | 1 | | | | | | | | | | | | | | 2 | | | |
| EQT202 | 3-95 Diversion Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT203 | 4-95 Surge Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT204 | 5-95 Aeration Tank | | 3 | | | | | | | | | | | | | | 1 | | | |
| EQT205 | 1700-81.1 NMP/PTZ Tote | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT206 | 1700-81.2 Aqueous Actrene Tote | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT207 | 1700-81.3 Recovery Column Heels Tote | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT208 | 1700-81.4 TBC Tote | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT209 | 1700-81.5 ACR Refining Column | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT210 | 1700-81.6 ACR RC Condenser | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT211 | 1700-81.7 ACR RC Reboiler | | 3 | | | | | | | | | | | | | | 3 | | | |
| EQT212 | 1700-84A Advance Fibres System (AFS) Emulsion Shipping (Emulsion Blend Tank) | | 2 | | | | | | | | | | | | | | | | | |
| EQT213 | 1700-84B Advance Fibres System (AFS) Emulsion Shipping (Tote Loading) | | | | 2 | | | | | | | | | | | | | | | |
| EQT214 | 1700-85 Liquid Dispersion Loading Emissions | | | | 2 | | | | | | | | | | | | | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | LAC 33:III | | | | | | | | LAC 33:III.Chapter | | | | | | | | | | |
|----------------|--|------------|------|------|------|------|------|------|------|--------------------|---|----|----|----|----|----|----|----|----|----|
| | | 509 | 2103 | 2104 | 2107 | 2111 | 2113 | 2115 | 2121 | 5 | 9 | 11 | 13 | 15 | 22 | 29 | 51 | 53 | 56 | 59 |
| EQT215 | 1700-86 Rosin S Storage Tank | | 2 | | | | | | | | | | | | | | | | | |
| FUG004 | 1-93 Fugitive Emissions – Neoprene Unit | | | | | | | | 1 | | | | | | | | 1 | | | |
| RLP013 | 1700-14B.3 Stabilizer & Catalyst Yanks Manhole Vent | | 2 | | | | | | | | | 1 | | | | | 3 | | | |
| RLP014 | 1700-2 Strippers Condenser Vent | | | | | | | 1 | | | | | | | | | 1 | | | |
| RLP015 | 1700-3 Poly Kettles Vent Condenser | | | | | | | 1 | | | | | | | | | 1 | | | |
| RLP016 | 1700-56 No. 6, 7, 8, 10, 13 and 14 Unstripped Storage Tanks Depressure Vent | | | | | | | 2 | | | | | | | | | 1 | | | |
| RLP017 | 1700-80 ACR Storage Vent Header | | | | | | | | | | | | | | | | 3 | | | |
| RLP018 | 1700-81 ACR Refining Vent | | | | | | | | | | | | | | | | 3 | | | |
| RLP019 | 1700-83 ACR Drumming Vent | | | | | | | 2 | | | | | | | | | 2 | | | |
| UNF001 | Plant Wide | | | | | 1 | 1 | | | 1 | 1 | 1 | 1 | | | | 1 | | 1 | 1 |
| | 6-95 Clarifier | | 3 | | | | | | | | | | | | | | 1 | | | |
| | 1700-87, 1700-88, 1700-89 No. 10, No. 13 & No. 14 Emulsion Storage Tank Manway | | | | | | | 2 | | | | | | | | | 3 | | | |

KEY TO MATRIX

- 1 (Applicable) The regulations have applicable requirements that apply to this particular emissions source. This includes any monitoring, recordkeeping, or reporting requirements.
- 2 (Exempt) The regulations apply to this general type of emission source (i.e. vents, furnaces, towers, and fugitives) but do not apply to this particular emission source.
- 3 (Does Not Apply) The regulations do not apply to this emissions source. The regulations may have applicable requirements that could apply to this emissions source but the requirements do not currently apply to the source due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.
- Blank – The regulations clearly do not apply to this type of emission source.

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | 40 CFR 60 NSPS | | | | | | | 40 CFR 61 | | | 40 CFR 63 NESHAP | | | | | 40 CFR | | | |
|----------------|---|----------------|----|----|----|----|----|-----|-----------|---|----|------------------|---|------|---|--|--------|----|----|----|
| | | A | Ka | Kb | Db | Dc | GG | KKK | A | M | FF | A | H | FFFF | U | | 60 | 64 | 68 | 70 |
| UNF001 | Plant Wide | 1 | | | | | | | 1 | 1 | 1 | | | 1 | 1 | | | 1 | 1 | |
| EQT134 | 1700-1 No. 7, 8, 10, 13, 14 Emulsion Storage Tanks Manhole and Exhaust Blower | | | | | | | | | | | | | | 3 | | | | | |
| EQT135 | 1700-13 Poly Kettles Manholes/Strainers (1 and 2) | | | | | | | | | | | | | | 3 | | | | | |
| EQT136 | 1700-13A Poly Kettles Manholes/Strainers (3, 4 and 5) | | | | | | | | | | | | | | 3 | | | | | |
| EQT137 | 1700-14B.1 Acetic Acid Make-up Tank | | | 3 | | | | | | | | | | | 2 | | | | | |
| EQT138 | 1700-14B.2 Acetic Acid Hold-up Tank | | | 3 | | | | | | | | | | | 2 | | | | | |
| EQT139 | 1700-20 CD Refining Column Jet | | | | | | | | | | | | | | 1 | | | | | |
| EQT140 | 1700-20A CD Refining Column Jet (Spare) | | | | | | | | | | | | | | 1 | | | | | |
| EQT141 | 1700-21A 2MM Pound CD Storage Tank | | | 3 | | | | | | | | | | | 1 | | | | | |
| EQT142 | 1700-25 East Wash Belt Dryer | | | | | | | | | | | | | | 2 | | | | | |
| EQT143 | 1700-26 West Wash Belt Dryer | | | | | | | | | | | | | | 2 | | | | | |
| EQT144 | 1700-27 East Hot Dryer Exhaust | | | | | | | | | | | | | | 2 | | | | | |
| EQT145 | 1700-28 West Hot Dryer Exhaust | | | | | | | | | | | | | | 2 | | | | | |
| EQT146 | 1700-45 No. 1 East Dryer Cooling Compt. | | | | | | | | | | | | | | 2 | | | | | |
| EQT147 | 1700-46 No. 1 West Dryer Cooling Compt. | | | | | | | | | | | | | | 2 | | | | | |
| EQT148 | 1700-47 No. 2 East Dryer Cooling Compt. | | | | | | | | | | | | | | 2 | | | | | |
| EQT149 | 1700-48 No. 2 West Dryer Cooling Compt. | | | | | | | | | | | | | | 2 | | | | | |
| EQT150 | 1700-5.3 Unstripped Emulsion Storage Tank. No. 6 | | | 2 | | | | | | | | | 2 | | 1 | | | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | 40 CFR 60 NSPS | | | | | | | 40 CFR 61 | | | 40 CFR 63 NESHAP | | | | 40 CFR | | | |
|----------------|---|----------------|----|----|----|----|----|-----|-----------|---|----|------------------|---|------|---|--------|----|----|----|
| | | A | Ka | Kb | Db | Dc | GG | KKK | A | M | FF | A | H | FFFF | U | 60 | 64 | 68 | 70 |
| EQT151 | 1700-5.4 Unstripped Emulsion Storage Tank. No. 7 | | | 2 | | | | | | | | | 2 | | 1 | | | | |
| EQT152 | 1700-5.5 Unstripped Emulsion Storage Tank. No. 8 | | | 2 | | | | | | | | | 2 | | 1 | | | | |
| EQT153 | 1700-5.6 Unstripped Emulsion Storage Tank. No. 10 | | | | | | | | | | | | 2 | | 1 | | | | |
| EQT154 | 1700-5.7 Unstripped Emulsion Storage Tank. No. 13 | | | | | | | | | | | | 2 | | 1 | | | | |
| EQT155 | 1700-5.8 Unstripped Emulsion Storage Tank. No. 14 | | | | | | | | | | | | 2 | | 1 | | | | |
| EQT156 | 1700-50.1 Stabilizer Tank No. 1 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT157 | 1700-50.1 Stabilizer Tank No. 2 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT158 | 1700-50.3 Stabilizer Tank No. 3 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT159 | 1700-50.4 Stabilizer Tank No. 4 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT160 | 1700-50.5 Stabilizer Tank No. 5 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT161 | 1700-50.6 Stabilizer Tank – LD750 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT162 | 1700-51 Inhibitor Mix Tank | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT163 | 1700-53 Stripped Emulsion Tank No. 1 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT164 | 1700-54 Stripped Emulsion Tank No. 2 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT165 | 1700-55 Stripped Emulsion Tank No. 3 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT166 | 1700-57 Diisobutylene (DIB) Storage Tank | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT167 | 1700-5A No. 6 Emulsion Storage Tank Manhole | | | | | | | | | | | | | | 3 | | | | |
| EQT168 | 1700-60 Diisobutylene Nitrosate (DIBN) Storage Tank No. 3 | | | 3 | | | | | | | | | | | 3 | | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | 40 CFR 60 NSPS | | | | | | | 40 CFR 61 | | | 40 CFR 63 NESHAP | | | | 40 CFR | | | |
|----------------|---|----------------|----|----|----|----|----|-----|-----------|---|----|------------------|---|------|---|--------|----|----|----|
| | | A | Ka | Kb | Db | Dc | GG | KKK | A | M | FF | A | H | FFFF | U | 60 | 64 | 68 | 70 |
| EQT169 | 1700-61 Diisobutylene Nitrosate (DIBN) Storage Tank No. 4 | | | 3 | | | | | | | | | | | 3 | | | | |
| EQT170 | 1700-62 Diisobutylene Nitrosate (DIBN) Storage Tank No. 5 | | | 3 | | | | | | | | | | | 3 | | | | |
| EQT171 | 1700-63.1 No. 1 CD Solution Tank | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT172 | 1700-63.10 Inhibitor Final Make-up Tank | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT173 | 1700-63.11 Inhibitor Hold-up Tank | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT175 | 1700-63.2 No. 2 CD Solution Tank | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT176 | 1700-63.3 Recovered CD Storage Tank No. 1 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT177 | 1700-63.4 Recovered CD Storage Tank No. 2 | | | 3 | | | | | | | | | 2 | | 1 | | | | |
| EQT178 | 1700-63.5 CD Heels Tank | | | 2 | | | | | | | | | 2 | | 1 | | | | |
| EQT181 | 1700-63.8 Crude CD Storage Tank No. 3 | | | 3 | | | | | | | | | | | 1 | | | | |
| EQT182 | 1700-63.9 Refined CD Storage Tank | | | 3 | | | | | | | | | | | 1 | | | | |
| EQT183 | 1700-64 Water Solution Exhaust Fan | | | | | | | | | | | | | | 3 | | | | |
| EQT185 | 1700-66 Poly Building Wall Fans | | | | | | | | | | | | | | 3 | | | | |
| EQT186 | 1700-67 Stripped Emulsion Tank No. 4 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT187 | 1700-68 Stripped Emulsion Tank No. 5 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT188 | 1700-69 Stripped Emulsion Tank No. 9 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT189 | 1700-70 Stripped Emulsion Tank No. 11 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT190 | 1700-71 Stripped Emulsion Tank No. 12 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT191 | 1700-72 Stripped Emulsion Tank No. 15 | | | 3 | | | | | | | | | | | 2 | | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | 40 CFR 60 NSPS | | | | | | | 40 CFR 61 | | | 40 CFR 63 NESHAP | | | | 40 CFR | | | |
|----------------|--|----------------|----|----|----|----|----|-----|-----------|---|----|------------------|---|------|---|--------|----|----|----|
| | | A | Ka | Kb | Db | Dc | GG | KKK | A | M | FF | A | H | FFFF | U | 60 | 64 | 68 | 70 |
| EQT192 | 1700-73 Stripped Emulsion Tank No. 16 | | | 3 | | | | | | | | | | | 2 | | | | |
| EQT193 | 1700-74 Finishing Stabilizer Makeup Bag Filter | | | | | | | | | | | | | | | | | | |
| EQT194 | 1700-75 Resin 90 Railcar | | | 2 | | | | | | | | | | | 2 | | | | |
| EQT195 | 1700-76 Rosin S Railcar | | | 2 | | | | | | | | | | | 2 | | | | |
| EQT196 | 1700-77 Octopol Storage Tank | | | 2 | | | | | | | | | | | 2 | | | | |
| EQT198 | 1700-79 Emergency Stabilizer Drumming | | | | | | | | | | | | | | 3 | | | | |
| EQT199 | 1700-80.1 Refined ACR Storage Tank | | | 3 | | | | | | | | | | 3 | 3 | | | | |
| EQT200 | 1700-80.2 Chlorinated ACR Storage Tank | | | 3 | | | | | | | | | | 3 | 3 | | | | |
| EQT201 | 1700-82 ACR/Solvent Blend Tank | | | 3 | | | | | | | | | | 3 | | | | | |
| EQT202 | 3-95 Diversion Tank | | | 3 | | | | | | | | | | | 1 | | | | |
| EQT203 | 4-95 Surge Tank | | | 3 | | | | | | | | | | | 1 | | | | |
| EQT204 | 5-95 Aeration Tank | | | 3 | | | | | | | | | | | 1 | | | | |
| EQT205 | 1700-81.1 NMP/PTZ Tote | | | 3 | | | | | | | | | | 3 | | | | | |
| EQT206 | 1700-81.2 Aqueous Actrene Tote | | | 3 | | | | | | | | | | 3 | | | | | |
| EQT207 | 1700-81.3 Recovery Column Heels Tote | | | 3 | | | | | | | | | | 3 | | | | | |
| EQT208 | 1700-81.4 TBC Tote | | | 3 | | | | | | | | | | 3 | | | | | |
| EQT209 | 1700-81.5 ACR Refining Column | | | | | | | | | | | | | 3 | 3 | | | | |
| EQT210 | 1700-81.6 ACR RC Condenser | | | | | | | | | | | | | 3 | 3 | | | | |
| EQT211 | 1700-81.7 ACR RC Reboiler | | | | | | | | | | | | | 3 | 3 | | | | |
| EQT212 | 1700-84A Advance Fibers System (AFS) Emulsion Shipping (Emulsion Blend Tank) | | | 3 | | | | | | | | | | 2 | 3 | | | | |

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

| Source ID No.: | Descriptive Name of the Source | 40 CFR 60 NSPS | | | | | | | 40 CFR 61 | | | 40 CFR 63 NESHAP | | | | 40 CFR | | | |
|----------------|--|----------------|----|----|----|----|----|-----|-----------|---|----|------------------|---|------|---|--------|----|----|----|
| | | A | Ka | Kb | Db | Dc | GG | KKK | A | M | FF | A | H | FFFF | U | 60 | 64 | 68 | 70 |
| EQT213 | 1700-84B Advance Fibers System (AFS) Emulsion Shipping (Tote Loading) | | | | | | | | | | | | | 2 | 3 | | | | |
| EQT214 | 1700-85 Liquid Dispersion Loading Emissions | | | | | | | | | | | | | 2 | 3 | | | | |
| EQT215 | 1700-86 Rosin S Storage Tank | | 3 | | | | | | | | | | | 2 | 3 | | | | |
| FUG004 | 1-93 Fugitive Emissions – Neoprene Unit | | | | | | | | | | | | | | 1 | | | | |
| RLP013 | 1700-14B.3 Stabilizer & Catalyst Yanks Manhole Vent | | | | | | | | | | | | | | 3 | | | | |
| RLP014 | 1700-2 Strippers Condenser Vent | | | | | | | | | | | | | | 1 | | | | |
| RLP015 | 1700-3 Poly Kettles Vent Condenser | | | | | | | | | | | | | | 1 | | | | |
| RLP016 | 1700-56 No. 6, 7, 8, 10, 13 and 14 Unstripped Storage Tanks Depressure Vent | | | | | | | | | | | | | | 1 | | | | |
| RLP017 | 1700-80 ACR Storage Vent Header | | | | | | | | | | | | | 3 | 3 | | | | |
| RLP018 | 1700-81 ACR Refining Vent | | | | | | | | | | | | | 3 | 3 | | | | |
| RLP019 | 1700-83 ACR Drumming Vent | | | | | | | | | | | | | 2 | 3 | | | | |
| | 6-95 Clarifier | | | 3 | | | | | | | | | | | 1 | | | | |
| | 1700-87, 1700-88, 1700-89 No. 10, No. 13 & No. 14 Emulsion Storage Tank Manway | | | | | | | | | | | | | | 3 | | | | |

KEY TO MATRIX

- 1 (Applicable) The regulations have applicable requirements that apply to this particular emissions source. This includes any monitoring, recordkeeping, or reporting requirements.
- 2 (Exempt) The regulations apply to this general type of emission source (i.e. vents, furnaces, towers, and fugitives) but do not apply to this particular emission source.
- 3 (Does Not Apply) The regulations do not apply to this emissions source. The regulations may have applicable requirements that could apply to this emissions source but the requirements do not currently apply to the source due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.

Blank – The regulations clearly do not apply to this type of emission source.

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| 1700-21A 2 MM Pound CD Storage Tank EQT 0141 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group 1 Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)]. This Tank is Group 2. | 40 CFR 63.484(a) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-21A 2 MM Pound CD Storage Tank EQT 0141 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U as applicable determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|--|---------------------|--------------------------------|------------------------|
| 1700-21A 2 MM Pound CD Storage Tank EQT 0141 | Title 33 Chapter 51: (Continued) | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-25: East Wash Belt Dryer 1700-26: West Wash Belt Dryer 1700-27: East Hot Dryer Exhaust 1700-28: West Hot Dryer Exhaust 1700-45: No. 1 East Dryer Cooling Compartment 1700-46: No. 1 West Dryer Cooling Compartment 1700-47: No. 2 East Dryer Cooling Compartment 1700-48: No. 2 West Dryer Cooling Compartment EQT 0142-0149 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U as applicable determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| | | | | | |
| | | | | | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|----------------------------|-----------------------------------|-------------------------------|
| 1700-5.3: Unstripped Emulsion Storage Tank No. 6 1700-5.4: Unstripped Emulsion Storage Tank No. 7 1700-5.5: Unstripped Emulsion Storage Tank No. 8 1700-5.6: Unstripped Emulsion Storage Tank No. 10 1700-5.7: Unstripped Emulsion Storage Tank No. 13 1700-5.8: Unstripped Emulsion Storage Tank No. 14 EQT 0150 - 0155 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that limit emissions or operations - | | | |
| | | Equip with a submerged fill pipe. | LAC 33:III.2103.A | N/A | |
| | | Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e. | LAC 33:III.2103.H.3 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| 1700-5.3: Unstripped Emulsion Storage Tank No. 6 1700-5.4: Unstripped Emulsion Storage Tank No. 7 1700-5.5: Unstripped Emulsion Storage Tank No. 8 1700-5.6: Unstripped Emulsion Storage Tank No. 10 1700-5.7: Unstripped Emulsion Storage Tank No. 13 1700-5.8: Unstripped Emulsion Storage Tank No. 14 1700-5.3 to 1700-5.8 EQT 0150 - 0155 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|--|----------------------------|-----------------------------------|-------------------------------|
| 1700-5.3: Unstripped Emulsion Storage Tank No. 6 1700-5.4: Unstripped Emulsion Storage Tank No. 7 1700-5.5: Unstripped Emulsion Storage Tank No. 8 1700-5.6: Unstripped Emulsion Storage Tank No. 10 1700-5.7: Unstripped Emulsion Storage Tank No. 13 1700-5.8: Unstripped Emulsion Storage Tank No. 14 1700-5.3 to 1700-5.8 EQT 0150 - 0155 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | Comply with the requirements of 40 CFR 63 Subpart H, except as specified in 40 CFR 63.502(b) through (m). Subpart U. | 40 CFR 63.502(a) | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|---|---------------------|----------------------------|------------------------|
| 1700-50.1: Stabilizer Tank No. 1 1700-50.2: Stabilizer Tank No. 2 1700-50.3: Stabilizer Tank No. 3 1700-50.4: Stabilizer Tank No. 4 1700-50.5: Stabilizer Tank No. 5 1700-50.6: Stabilizer Tank No. 6 EQT 0156 - 0161 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] These tanks are Group 2. | 40 CFR 63.484(a) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|---------------------|----------------------------|------------------------|
| 1700-51 Inhibitor Mix Tank EQT 0162 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] This tank is Group 2. | 40 CFR 63.484(a) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-51: Inhibitor Mix Tank EQT 0162 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| 1700-51: Inhibitor Mix Tank EQT 0162 | Title 33 Chapter 51 (Continued) | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-53: Stripped Emulsion Tank No. 1 1700-54: Stripped Emulsion Tank No. 2 1700-55: Stripped Emulsion Tank No. 3 1700-67: Stripped Emulsion Tank No. 4 1700-68: Stripped Emulsion Tank No. 5 1700-69: Stripped Emulsion Tank No. 9 1700-70: Stripped Emulsion Tank No. 11 1700-71: Stripped Emulsion Tank No. 12 1700-72: Stripped Emulsion Tank No. 15 1700-73: Stripped Emulsion Tank No. 16 EQT 0163 to 0165;0186 to 0192 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. No additional controls determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|---|---------------------|----------------------------|------------------------|
| 1700-63.1: No. 1 CD Solution Tank 1700-63.2: No. 2 CD Solution Tank 1700-63.3: Recovered CD Storage Tank No. 1 1700-63.4: Recovered CD Storage Tank No. 2 1700-63.8 Crude CD Storage Tank No. 3 1700-63.10: Inhibitor Final Make-Up Tank 1700-63.11: Inhibitor Hold-up Tank EQT 0171 to 0173, 0175 to 0177 and 0181 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] These tanks are Group 2. | 40 CFR 63.484(a) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| 1700-63.1: No. 1 CD Solution Tank 1700-63.2: No. 2 CD Solution Tank 1700-63.3: Recovered CD Storage Tank No. 1 1700-63.4: Recovered CD Storage Tank No. 2 1700-63.8 Crude CD Storage Tank No. 3 1700-63.10: Inhibitor Final Make-Up Tank 1700-63.11: Inhibitor Hold-up Tank EQT 0171 to 0173, 0175 to 0177 and 0181 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|--|--|---------------------|--------------------------------|------------------------|
| 1700-63.5 CD Heels Tank 1700-63.9 Refined CD Storage Tank EQT 0178 and 0182 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that limit emissions or operations - | | | |
| | | Equip with a submerged fill pipe. | LAC 33:III.2103.A | N/A | |
| | | Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e. | LAC 33:III.2103.H.3 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-63.5 CD Heels Tank 1700-63.9 Refined CD Storage Tank EQT 0178 and 0182 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|---------------------|----------------------------|------------------------|
| 1700-63.5 CD Heels Tank 1700-63.9 Refined CD Storage Tank EQT 0178 and 0182 | Title 33 Chapter 51: (Continued) | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-63.5 CD Heels Tank 1700-63.9 Refined CD Storage Tank EQT 0178 and 0182 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] This tank is Group 2. | 40 CFR 63.484(a) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|---|---------------------|----------------------------|------------------------|
| 1700-74: Finishing Stabilizer Makeup Bag Filter EQT 0193 | Title 33 Chapter 13: Emission Standards for Particulate Matter (Including Standards for Some Specific Facilities) | Requirements that limit emissions or operations - | | | |
| | | Prevent particulate matter from becoming airborne by taking all reasonable precautions. These precautions shall include, but not be limited to, those specified in LAC 33:III.1305.A.1-7. | LAC 33:III.1305 | N/A | |
| | | Opacity ≤ 20 percent; except emissions may have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes. | LAC 33:III.1311.C | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|---------------------|----------------------------|------------------------|
| 1700-82: ACR/Solvent Blend Tank EQT 0201 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with LAC 33:III.2103 determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-82: ACR/Solvent Blend Tank EQT 0201 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that limit emissions or operations - | | | |
| | | Equip with a submerged fill pipe. | LAC 33:III.2103.A | N/A | |
| | | Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e. | LAC 33:III.2103.H.3 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|--|--|---------------------|--------------------------------|------------------------|
| 1700-82: ACR/Solvent Blend Tank EQT 0201 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 3-95 Diversion Tank 4-95 Surge Tank 5-95 Aeration Tank 6-95 Clarifier EQT 0202 to 0204 | Subpart G - National Emission Standards For Organic Hazardous Air Pollutants From The Synthetic Organic Chemical Manufacturing Industry For Process Vents, Storage Vessels, Transfer Operations, And Wastewater | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Maintain records specified in 40 CFR 63.147(a) through (f), as applicable. Subpart G. | 40 CFR 63.147 | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| 3-95 Diversion Tank 4-95 Surge Tank 5-95 Aeration Tank EQT 0202 to 0204 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | Comply with the requirements of 40 CFR 63.132 through 63.148, except as specified in 40 CFR 63.501(a)(1) through (a)(23) and (c). Subpart U [40 CFR 63.501(a)] | 40 CFR 63.501(a) | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 3-95 Diversion Tank 4-95 Surge Tank 5-95 Aeration Tank EQT 0202 to 0204 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|---|---------------------|----------------------------|------------------------|
| 3-95 Diversion Tank 4-95 Surge Tank 5-95 Aeration Tank EQT 0202 to 0204 | Title 33 Chapter 51: (Continued) | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-84A: Advance Fibers System (AFS) – Emulsion Shipping (Blend Tank) EQT 0212 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that limit emissions or operations - | | | |
| | | Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e. | LAC 33:III.2103.H.3 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-84A: Advance Fibers System (AFS) – Emulsion Shipping (Blend Tank) EQT 0212 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with LAC 33:III.2103 determined as MACT. | LAC 33:III.5109.A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|---|---------------------|--------------------------------|------------------------|
| 1700-84A: Advance Fibers System (AFS) – Emulsion Shipping (Blend Tank) EQT 0212 | Title 33 Chapter 51: (Continued) | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| 1700-84B: Advance Fibers System (AFS) – Emulsion Shipping (Tote Loading) 1700-85 Liquid Dispersion Loading EQT 0213 and 0214 | Subpart FFFF - National Emission Standards For Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy annually. Keep records of the information specified in 40 CFR 63.130(f)(1) through (f)(3) (as per Subpart FFFF). Subpart G [40 CFR 63.130(f)] | 40 CFR 63.130(f) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|----------------------------|-----------------------------------|-------------------------------|
| 1700-84B and 1700-85 EQT 0213 and 0214 | Subpart FFFF (Continued) | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-84B: Advance Fibers System (AFS) – Emulsion Shipping (Tote Loading) 1700-85 Liquid Dispersion Loading EQT 0213 and 0214 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with 40 CFR 63 Subpart FFFF determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|--|---------------------|--------------------------------|------------------------|
| 1-93: Fugitive Emissions – Neoprene Unit FUG 0004 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | Comply with the requirements of 40 CFR 63 Subpart H, except as specified in 40 CFR 63.502(b) through (m). Subpart U. | 40 CFR 63.502(a) | N/A | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1-93: Fugitive Emissions – Neoprene Unit FUG 0004 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that limit emissions or operations - | | | |
| | | Repair according to LAC 33:III.2121.B.3 any regulated component observed leaking by sight, sound, or smell, regardless of the leak's concentration. | LAC 33:III.2121.B.1 | | |
| | | Do not locate any valve, except safety pressure relief valves, valves on sample lines, valves on drain lines and valves that can be removed and replaced without a shutdown, at the end of a pipe or line containing VOC unless the end of such line is sealed with a second valve, a blind flange, a plug, or a cap. Remove such sealing devices only when the line is in use, for example, when a sample is being taken. When the line has been used and is subsequently resealed, close the upstream valve first, followed by the sealing device. | LAC 33:III.2121.B.2 | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|---|---------------------|----------------------------|------------------------|
| 1-93: Fugitive Emissions – Neoprene Unit FUG 0004 (Continued) | Title 33 Chapter 21: Control of Emission of Organic Compounds | Make every reasonable effort to repair a leaking component, as described in LAC 33:III.2121.B, within 15 days, except as provided. | LAC 33:III.2121.B.3 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due semiannually, by the 31 st of January and July, to the Office of Environmental Assessment, Air Quality Assessment Division. Include the information specified in LAC 33:III.2121.F.1 through 4 for each calendar quarter during the reporting period. | LAC 33:III.2121.F | Semiannually | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|--|---|---------------------|--------------------------------|------------------------|
| 1700-14B – Solution Make Up Manhole Common Vent GRP 0006 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | VOC, Total <= 0.72 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | VOC, Total monitored by technically sound method as needed, (when source is venting). | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | VOC. Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months. Make records available for inspection by DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|---|---------------------|----------------------------|------------------------|
| 1700-25A – Product Drying CAP GRP 0007 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | VOC, Total <= 69.17 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. The VOC emissions shall be calculated based on operation and throughput. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | VOC, Total monitored by technically sound method daily. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions calculated based on operation and throughput). Make records available for inspection by DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| 1700- 5 Unstripped Emulsion Storage Yanks Common Vent & CAP GRP 0008 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | VOC, Total <= 2.77 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. VOC emissions shall be calculated based on operation and throughput. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | VOC, Total monitored by technically sound method daily. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions calculated based on operation and throughput). Make records available for inspection by DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|--|---------------------|----------------------------|------------------------|
| 1700- 50 Stabilizer tanks Common Vent & CAP GRP 0009 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | VOC, Total <= 0.59 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. VOC emissions shall be calculated based on operation and throughput. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | VOC, Total monitored by technically sound method daily. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions based on operation and throughput). Make records available for inspection by DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|--|---------------------|----------------------------|------------------------|
| 1700- 63 Vent Header System CAP GRP 0010 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | VOC, Total <= 2.18 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. VOC emissions shall be calculated based on operation and throughput. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | VOC, Total monitored by technically sound method daily. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions based on operation and throughput). Make records available for inspection by DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| Facility Wide CAP - Neoprene Types Production CAP GRP 0011 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Neoprene Types: Production rate \leq 98 MM lbs/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if total Neoprene Types produced exceeds the maximum listed in this specific condition for any twelve consecutive month period. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | Neoprene Types: Production rate monitored by technically sound method daily. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Neoprene Types: Production rate recordkeeping by electronic or hard copy monthly. Keep records of the total Neoprene Products production each month, as well as the total Neoprene Products production for the last twelve months. Make records available for inspection by DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the Total Neoprene Types produced for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|---------------------|----------------------------|------------------------|
| 1700-20: CD Refining Column Jets Emissions CAP GRP 0012 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | Comply with the requirements of 40 CFR 63.113 through 63.118, except as provided in 40 CFR 63.485(b) through (v). Subpart U. [40 CFR 63.485(a)] | 40 CFR 63.485(a) | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent to become a Group 1 continuous front-end process vent, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the Group 1 provisions in 40 CFR 63.113 through 63.118 in accordance with 40 CFR 63.480(i)(2)(ii) or (i)(2)(iii), as applicable. Subpart U. [40 CFR 63.485(l)(1)] | 40 CFR 63.485(l)(1) | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|---|---------------------|----------------------------|------------------------|
| 1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that specify reports to be submitted | | | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a TRE greater than 4.0 to become a Group 2 continuous front-end process vent with a TRE less than 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(1)(2)] | 40 CFR 63.485(1)(2) | N/A | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a flow rate less than 0.005 standard cubic meter per minute (scmm) to become a Group 2 continuous front-end process vent with a flow rate of 0.005 scmm or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(1)(3)] | 40 CFR 63.485(1)(3) | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|--|---------------------|----------------------------|------------------------|
| 1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that specify reports to be submitted | | | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with an organic HAP concentration less than 50 parts per million by volume (ppmv) to become a Group 2 continuous frontend process vent with an organic HAP concentration of 50 ppmv or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(1)(4)] | 40 CFR 63.485(1)(4) | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | Conduct performance testing in accordance with 40 CFR 63.7(a)(1), (a)(3), (d), (e)(1), (e)(2), (e)(4), (g), and (h), with the exceptions specified in 40 CFR 63.504(a)(1) through (a)(5) and the additions specified in 40 CFR 63.504(b). Subpart U. [40 CFR 63.504(a)] | 40 CFR 63.504(a) | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|---|---------------------|----------------------------|------------------------|
| 1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012 | Title 33 Chapter 21: Control of Emission of Organic Compounds: Waste Gas Disposal | Requirements that limit emissions or operations - | | | |
| | | Halogenated hydrocarbons, total \geq 95 % removal efficiency as determined in accordance with LAC 33:III.2115.J.1, by combustion or other methods specified in LAC 33:III.2115.G. If combusted, reduce the halogenated products of combustion to an emission level acceptable to DEQ. | LAC 33:III.2115.F | N/A | |
| | | Alternative Control Requirements. Other methods of control (such as, but not limited to, carbon adsorption, refrigeration, catalytic and/or thermal reaction, secondary steam stripping, recycling, or vapor recovery system) may be substituted for burning provided the substitute is acceptable to the administrative authority* and it achieves the same removal efficiency as required by this Section and determined in accordance with Paragraph J.1 of this Section or it achieves a degree of control not practically or safely achieved by other means. Permittee is using a condenser as control device. | LAC 33:III.2115.G | | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|---|---|---------------------|--------------------------------|------------------------|
| 1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. | LAC 33:III.5109.A | N/A | |
| | | Operating time \leq 8760 hr/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if total Neoprene Types produced exceeds the maximum listed in this specific condition for any twelve consecutive month period. Only one vacuum jet shall operate at a time. | LAC 33:III.501.C.6 | N/A | State Only |
| | | VOC, Total \leq 12.40 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | Operating time monitored by technically sound method daily. Only one vacuum jet shall operate at a time. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Operating time recordkeeping by electronic or hard copy monthly. Keep records of the total operating time and total VOC emissions each month, as well as the total operating time and total VOC emissions for the last twelve months, (VOC emissions based on operation and throughput). Make records available for inspection by DEQ personnel. Only one vacuum jet shall operate at a time. | LAC 33:III.501.C.6 | N/A | State Only |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| 1700-20: CD Refining Column Jets Emission's CAP (Continued) GRP 0012 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the Total operating time and Total VOC emissions for the preceding calendar year to the Office of Env. Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-14B.3 Stabilizer & Catalyst Tanks Manhole Vent RLP 0013 | Title 33 Chapter 13: Emission Standards for Particulate Matter (Including Standards for Some Specific Facilities) | Requirements that limit emissions or operations - | | | |
| | | Prevent particulate matter from becoming airborne by taking all reasonable precautions. These precautions shall include, but not be limited to, those specified in LAC 33:III.1305.A.1-7. | LAC 33:III.1305 | N/A | |
| | | Total suspended particulate <= 11.22 lb/hr. The rate of emission shall be the total of all emission points from the source. | LAC 33:III.1311.B | N/A | |
| | | Opacity <= 20 percent; except emissions may have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive min. | LAC 33:III.1311.C | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|---|---------------------|----------------------------|------------------------|
| 1700-2: Strippers Condenser Vent RLP0014 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | Comply with the requirements of 40 CFR 63.113 through 63.118, except as provided in 40 CFR 63.485(b) through (v). Subpart U. [40 CFR 63.485(a)] | 40 CFR 63.485(a) | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | The owner or operator of a Group 2 process vent having a flow rate greater than or equal to 0.005 standard cubic meter per minute, a HAP concentration greater than or equal to 50 parts per million by volume, and a TRE index value greater than 1.0 but less than or equal to 4.0 shall maintain a TRE index value greater than 1.0 and shall comply with the monitoring of recovery device parameters in §63.114(b) or (c) of this subpart, the TRE index calculations of §63.115 of this subpart, and the applicable reporting and recordkeeping provisions of §§63.117 and 63.118 of this subpart. Such owner or operator is not subject to any other provisions of §§63.114 through 63.118 of this subpart. . [40 CFR 63.113(d)] | 40 CFR 63.113(d) | N/A | |
| | | Temperature monitored by temperature monitoring device continuously. Equip the temperature monitoring device with a continuous recorder. Monitor the exit (product side) temperature. Subpart G As allowed by 40 CFR 63.114 (c), DPP uses an alternate method due to low flow on the process side of the condenser. [40 CFR 63.114(b)(2)] | 40 CFR 63.114(b)(2) | Continuously | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|--|---------------------|--------------------------------|------------------------|
| 1700-2: Strippers Condenser Vent RLP0014 (Continued) | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | An owner or operator of a process vent may request approval to monitor parameters other than those listed in paragraph (a) or (b) of this section. The request shall be submitted according to the procedures specified in 40 CFR 63.151(f) or 40 CFR 63.152(e) of this subpart. Approval shall be requested if the owner or operator uses one of the combustion or recovery or recapture devices listed in paragraphs (a) and (b) of this section, but seeks to monitor a parameter other than those specified in paragraphs (a) and (b) of this section. DPP monitors the cooling media temperature for each condenser. The daily average cooling media should not exceed the following limits: --Cooling Water Loop on Water Condenser : 50 degrees Centigrade at Cooling Water Loop Sample Point --Cooling Brine Loop on CD Condenser : 5 degrees Centigrade at Cooling Brine Loop Sample Point --Condenser Brine Inlet on Common Condenser : (Negative) - 15 degrees Centigrade at Condenser Brine Inlet Sample Point. [40 CFR 63.114(c)(3)] | 40 CFR 63.114(c)(3) | Continuously | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|---|--|---------------------|--------------------------------|------------------------|
| 1700-2: Strippers Condenser Vent RLP0014 (Continued) | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Keep up-to-date, readily accessible records of the data specified in 40 CFR 63.118(b)(1) and (b)(2). Subpart G. [40 CFR 63.118(b)] | 40 CFR 63.118(b) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent to become a Group 1 continuous front-end process vent, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the Group 1 provisions in 40 CFR 63.113 through 63.118 in accordance with 40 CFR 63.480(i)(2)(ii) or (i)(2)(iii), as applicable. Subpart U. [40 CFR 63.485(l)(1)] | 40 CFR 63.485(1)(1) | N/A | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a TRE greater than 4.0 to become a Group 2 continuous front-end process vent with a TRE less than 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(2)] | 40 CFR 63.485(1)(2) | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|--|---------------------|----------------------------|------------------------|
| 1700-2: Strippers Condenser Vent RLP0014 (Continued) | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a flow rate less than 0.005 standard cubic meter per minute (scmm) to become a Group 2 continuous front-end process vent with a flow rate of 0.005 scmm or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(3)] | 40 CFR 63.485(1)(3) | N/A | |
| | | Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with an organic HAP concentration less than 50 parts per million by volume (ppmv) to become a Group 2 continuous frontend process vent with an organic HAP concentration of 50 ppmv or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(4)] | 40 CFR 63.485(1)(4) | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|---------------------|----------------------------|------------------------|
| 1700-2: Strippers Condenser Vent RLP0014 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with 40 CFR 63 Subpart U determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| 1700-2: Strippers Condenser Vent RLP0014 | Title 33 Chapter 21: Control of Emission of Organic Compounds: Waste Gas Disposal | Requirements that limit emissions or operations - | | | |
| | | Halogenated hydrocarbons, total \geq 95 % removal efficiency as determined in accordance with LAC 33:III.2115.J.1, by combustion or other methods specified in LAC 33:III.2115.G. If combusted, reduce the halogenated products of combustion to an emission level acceptable to DEQ. Permittee uses an alternate compliance method for control (condenser) as per LAC 33:III.2115.G. | LAC 33:III.2115.F | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|---|---|---------------------|--------------------------------|------------------------|
| 1700-2: Strippers Condenser Vent RLP0014 (Continued) | Title 33 Chapter 21: Control of Emission of Organic Compounds: Waste Gas Disposal | Alternative Control Requirements. Other methods of control (such as, but not limited to, carbon adsorption, refrigeration, catalytic and/or thermal reaction, secondary steam stripping, recycling, or vapor recovery system) may be substituted for burning provided the substitute is acceptable to the administrative authority* and it achieves the same removal efficiency as required by this Section and determined in accordance with Paragraph J.1 of this Section or it achieves a degree of control not practically or safely achieved by other means. Permittee is using a condenser as a control device. | LAC 33:III.2115.G | | |
| | | Demonstrate compliance with LAC 33:III.2115 as requested by DEQ. | LAC 33:III.2115.J.1 | | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|---------------------|----------------------------|------------------------|
| 1700-3: Poly Kettles Vent Condenser RLP 0015 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | Organic HAP >= 90 % reduction by weight using a control device. Subpart U To ensure that the Poly Kettles maintain the status of Group 2, the temperature of the condenser brine outlet is monitored to ensure it is below 5 degrees Centigrade. [40 CFR 63.487(a)(2)] | 40 CFR 63.487(a)(2) | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Keep records of the information specified in 40 CFR 63.491(a) through (g), as applicable. Subpart U. | 40 CFR 63.491 | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit Notification: Due within 180 days after a process change, as defined in 40 CFR 63.488(i)(1), is made that causes a Group 2 batch front-end process vent to become a Group 1 batch front-end process vent, or with the next Periodic Report, whichever is later. Submit a description of the process change. Comply with the Group 1 batch front-end process vent provisions in 40 CFR 63.486 through 63.492 in accordance with 40 CFR 63.480(i)(2)(ii). Subpart U. [40 CFR 63.492(b)] | 40 CFR 63.492(b) | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|--|---|---------------------|--------------------------------|------------------------|
| 1700-3: Poly Kettles Vent Condenser RLP 0015 | Title 33 Chapter 21: Control of Emission of Organic Compounds: Waste Gas Disposal | Requirements that limit emissions or operations - | | | |
| | | Halogenated hydrocarbons, total \geq 95 % removal efficiency as determined in accordance with LAC 33:III.2115.J.1, by combustion or other methods specified in LAC 33:III.2115.G. If combusted, reduce the halogenated products of combustion to an emission level acceptable to DEQ. Permittee uses an alternate compliance method for control (condenser) as per LAC 33:III.2115.G. | LAC 33:III.2115.F | N/A | |
| | | Alternative Control Requirements. Other methods of control (such as, but not limited to, carbon adsorption, refrigeration, catalytic and/or thermal reaction, secondary steam stripping, recycling, or vapor recovery system) may be substituted for burning provided the substitute is acceptable to the administrative authority* and it achieves the same removal efficiency as required by this Section and determined in accordance with Paragraph J.1 of this Section or it achieves a degree of control not practically or safely achieved by other means. | LAC 33:III.2115.G | | |
| | | Demonstrate compliance with LAC 33:III.2115 as requested by DEQ. | LAC 33:III.2115.J.1 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| 1700-3: Poly Kettles Vent Condenser RLP 0015 (Continued) | Title 33 Chapter 21: (Continued) | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| 1700-3: Poly Kettles Vent Condenser RLP 0015 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ Compliance with 40 CFR 63 Subpart U and LAC 33:III.2115 determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | Monitor the temperature of the Condenser Brine Outlet to ensure it is below 5 degrees Centigrade. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Daily records of cooling temperature and valve monitoring shall be kept on site and available for inspection DEQ personnel. | LAC 33:III.501.C.6 | N/A | State Only |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due annually, by the 31st of March. Report the cooling media temperature showing the total number of hours during which the maximum temperature was exceeded for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division. | LAC 33:III.501.C.6 | Annually | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|---------------------|----------------------------|------------------------|
| 1700-56: No. 6, 7, 8, 10, 13 & 14 Unstripped Storage Tanks Depressure Vent RLP 0016 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] This tank is Group 2. | 40 CFR 63.484(a) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|---|--|---------------------|--------------------------------|------------------------|
| 1700-56: No. 6, 7, 8, 10, 13 & 14 Unstripped Storage Tanks Depressure Vent RLP 0016 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that limit emissions or operations - | | | |
| | | Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT. | LAC 33:III.5109.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 60 – Standards of Performance for New Stationary Sources. Subpart A: General Provisions | Requirements that limit emissions or operations - | | | |
| | | All affected facilities shall comply with all applicable provisions in 40 CFR 60 Subpart A. | 40 CFR 60 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 61 – National Emission Standards for Hazardous Air Pollutants Subpart A: General Provisions | Requirements that limit emissions or operations - | | | |
| | | All affected facilities shall comply with all applicable provisions in 40 CFR 61 Subpart A. | 40 CFR 61 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|----------------------------|-----------------------------------|-------------------------------|
| Facility Wide – UNF 0001 (Continued) | Part 61 – (Continued) | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Subpart M: National Emission Standards for Asbestos | Requirements that limit emissions or operations - | | | |
| | | Do not install or reinstall on a facility component any insulating materials that contain commercial asbestos if the materials are either molded and friable or wet-applied and friable after drying. Subpart M. | 40 CFR 61.148 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Provide DEQ with written notice of intention to demolish or renovate prior to performing activities to which 40 CFR 61 Subpart M applies. Delivery of the notice by U.S. Postal Service, commercial delivery service, or hand delivery is acceptable. Subpart M. [40 CFR 61.145(b)(1)] | 40 CFR 61.145(b)(1) | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|------------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Subpart FF: National Emission Standards for Benzene Waste Operations | Requirements that limit emissions or operations - | | | |
| | | Benzene < 1 Mg/yr (1.1 ton/yr) total quantity. Subpart FF. [40 CFR 61.342(d)(2)(i)] | 40 CFR 61.342(d)(2)(i) | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | Determine compliance with 40 CFR 61 Subpart FF using the test methods and procedures specified in 40 CFR 61.355(a) through (i), as applicable. Subpart FF. | 40 CFR 61.355 | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency Maintain records as specified in 40 CFR 61.356(a) through (n), as applicable. Maintain each record in a readily accessible location at the facility site for a period not less than two years from the date the information is recorded unless otherwise specified. Subpart FF. | 40 CFR 61.356 | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit report: Due whenever there is a change in the process generating the waste stream that could cause the total annual benzene quantity from facility waste to increase to 1 Mg/yr (1.1 ton/yr) or more. Submit updates to the information listed in 40 CFR 61.357(a)(1) through (a)(3). Subpart FF. [40 CFR 61.357(b)] | 40 CFR 61.357(b) | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|---|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Keep copies of all applicable records and reports required by 40 CFR 63 Subpart U for at least 5 years, as specified in 40 CFR 63.506(a)(1), with the exception listed in 40 CFR 63.506(a)(2). Subpart U. [40 CFR 63.506(a)] | 40 CFR 63.506(a) | N/A | |
| | | Comply with the applicable recordkeeping and reporting requirements in 40 CFR 63 Subpart A, as specified in 40 CFR 63 Subpart U Table 1. Subpart U. [40 CFR 63.506(b)] | 40 CFR 63.506(b) | N/A | |
| | | Equipment/operational data recordkeeping by electronic or hard copy continuously. Keep records of the information specified in 40 CFR 63.506(d)(1) through (d)(9), unless an alternative recordkeeping system has been requested and approved as specified in 40 CFR 63.506(g), and except as provided in 40 CFR 63.506(h). Subpart U. [40 CFR 63.506(d)] | 40 CFR 63.506(d) | Continuously | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|---|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins | Requirements that specify reports to be submitted - | | | |
| | | Submit Notification of Compliance Status: Due no later than 150 days after the compliance dates specified in 40 CFR 63 Subpart U. Submit the information specified in 40 CFR 63.506(e)(5)(i) through (e)(5)(xii), as applicable. Subpart U. [40 CFR 63.506(e)(5)] | 40 CFR 63.506(e)(5) | N/A | |
| | | Submit Periodic Report: Due semiannually no later than 60 days after the end of each 6-month period. Submit the first report no later than 240 days after the date the Notification of Compliance Status is due, covering the 6-month period beginning on the date the Notification of Compliance Status is due. Submit the information specified in 40 CFR 63.506(e)(6)(i) through (e)(6)(xii). Subpart U. [40 CFR 63.506(e)(6)] | 40 CFR 63.506(e)(6) | Semiannually | |
| | | Requirements that specify performance testing - | | | |
| | | Conduct performance testing in accordance with 40 CFR 63.7(a)(1), (a)(3), (d), (e)(1), (e)(2), (e)(4), (g), and (h), with the exceptions specified in 40 CFR 63.504(a)(1) through (a)(5) and the additions specified in 40 CFR 63.504(b). Subpart U. [40 CFR 63.504(a)] | 40 CFR 63.504(a) | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 63 – National Emission Standards for Hazardous Air | Requirements that limit emissions or operations - | | | |
| | | All affected facilities shall comply with all applicable provisions in 40 CFR 63 Subpart A. | 40 CFR 63 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|---|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Part 63 – National Emission Standards for Hazardous Air | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Subpart FFFF: National Emission Standards for Hazardous Air Pollutants: Miscellaneous Organic Chemical Manufacturing | Requirements that limit emissions or operations - | | | |
| | | Shall comply with all the applicable requirements of 40 CFR 63 Subpart FFFF - Miscellaneous Organic Chemical Manufacturing. | 40 CFR 63.2430 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 68 – Chemical Accident Prevention Provisions. Subpart A: General Provisions | Requirements that limit emissions or operations - | | | |
| | | Ensure that response actions have been coordinated with local emergency planning and response agencies. [40 CFR 68.12(b)(3)] | 40 CFR 68.12(b)(3) | N/A | |
| | | Include in the RMP the certification specified in 68.12(b)(4). [40 CFR 68.12(b)(4)] | 40 CFR 68.12(b)(4) | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy continuously. Document that the nearest public receptor is beyond the distance to a toxic or flammable endpoint defined in 68.22. [40 CFR 68.12(b)(1)] | 40 CFR 68.12(b)(1) | Continuously | |
| | | Complete the five-year accident history for the process as provided in 68.42. [40 CFR 68.12(b)(2)] | 40 CFR 68.12(b)(2) | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 68 – Chemical Accident Prevention Provisions. Subpart B: Hazard Assessment | Requirements that limit emissions or operations - | | | |
| | | Use the endpoints specified in 68.22(a) through (g) for analyses of offsite consequences. | 40 CFR 68.22 | N/A | |
| | | Analyze the release scenarios in 68.25, as specified in 68.25(a) through (h). | 40 CFR 68.25 | N/A | |
| | | Identify and analyze at least one alternative release scenario for each regulated toxic substance held in a covered process(es) and at least one alternative release scenario to represent all flammable substances held in covered processes, as specified in 68.28(b) through (e). | 40 CFR 68.28 | N/A | |
| | | Estimate in the RMP the population within a circle with its center at the point of the release and a radius determined by the distance to the endpoint defined in 68.22(a). | 40 CFR 68.30 | N/A | |
| | | List in the RMP environmental receptors within a circle with its center at the point of the release and a radius determined by the distance to the endpoint defined in 68.22(a). | 40 CFR 68.33 | N/A | |
| | | Review and update the offsite consequence analyses at least once every five years. Complete a revised analysis within six months if changes in processes, quantities stored or handled, or any other aspect of the stationary source might reasonably be expected to increase or decrease the distance to the endpoint by a factor of two or more. | 40 CFR 68.36 | Every 5 Years | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|---|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Part 68 – Chemical Accident Prevention Provisions. Subpart B: Hazard Assessment (Continued) | Include in the five-year accident history all accidental releases from covered processes that resulted in deaths, injuries, or significant property damage on site, or known offsite deaths, injuries, evacuations, sheltering in place, property damage, or environmental damage. Include the information specified in 68.42(b)(1) through (10) for each accidental release. | 40 CFR 68.42 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Equipment/operational data recordkeeping by electronic or hard copy continuously. Maintain the records specified in 68.39(a) through (e) on the offsite consequence analyses. | 40 CFR 68.39 | Continuously | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit revised RMP: Due within six months after changes in processes, quantities stored or handled, or any other aspect of the stationary source increase or decrease the distance to the endpoint by a factor of two or more. [40 CFR 68.36(b)] | 40 CFR 68.36(b) | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 68 – Chemical Accident Prevention Provisions. Subpart G: Risk Management Plan | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Provide in the RMP an executive summary that includes a brief description of the elements listed in 68.155(a) through (g) | 40 CFR 68.155 | N/A | |
| | | Submit in the RMP information one worst-case release scenario for each Program 1 process. Include the data specified in 68.165(b)(1) through (13). | 40 CFR 68.165 | N/A | |
| | | Submit in the RMP the information provided in 68.42(b) on each accident covered by 68.42(a). | 40 CFR 68.168 | N/A | |
| | | Provide in the RMP the emergency response information listed in 68.180(a) through (c). | 40 CFR 68.180 | N/A | |
| | | Submit Risk Management Plan (RMP): Due no later than June 21, 1999, or three years after the date on which a regulated substance is first listed under 68.130, or the date on which a regulated substance is first present above a threshold quantity in a process. Submit in a method and format to a central point as specified by EPA prior to June 21, 1999. | 40 CFR 68.150 | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|--|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Part 68 – Chemical Accident Prevention Provisions. Subpart G: Risk Management Plan. (Continued) | Complete a single registration form and include in the RMP. Cover all regulated substances handled in covered processes. Include in the registration the information specified in 68.160(b)(1) through (13). | 40 CFR 68.160 | N/A | |
| | | Submit revised registration to EPA: Due within six months after a stationary source is no longer subject to 40 CFR 68. Indicate that the stationary source is no longer covered. [40 CFR 68.190(c)] | 40 CFR 68.190(c) | N/A | |
| | | Review and update the RMP as specified in 68.190(b) and submit it in a method and format to a central point specified by EPA prior to June 21, 1999. | 40 CFR 68.190 | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 68 – Chemical Accident Prevention Provisions. Subpart H: Other Requirements | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Maintain records supporting the implementation of 40 CFR 68 for five years unless otherwise provided. | 40 CFR 68.200 | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|--|------------------------------|--------------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Part 70 – State Operating Permit Programs | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit Title V permit application for renewal: Due 6 months before permit expiration date. [40 CFR 70.5(a)(1)(iii)] | 40 CFR 70.5(a)(1)(iii) | N/A | |
| | | Submit Title V monitoring results report: Due semiannually, by March 31st and September 30th for the preceding periods encompassing July through December and January through June, respectively. Submit reports to the Office of Environmental Compliance, Surveillance Division. Certify reports by a responsible company official. Clearly identify all instances of deviations from permitted monitoring requirements. For previously reported deviations, in lieu of attaching the individual deviation reports, clearly reference the communication(s)/ correspondence(s) constituting the prior report, including the date the prior report was submitted. [40 CFR 70.6(a)(3)(iii)(A)] | 40 CFR 70.6(a)(3)(iii)(A) | Semiannually | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|---|---------------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Part 70 – State Operating Permit Programs (Continued) | Submit Title V excess emissions report: Due quarterly, by June 30, September 30, December 31, March 31. Submit reports of all permit deviations to the Office of Environmental Compliance, Surveillance Division. Certify all reports by a responsible official in accordance with 40 CFR 70.5(d). The reports submitted on March 31 and September 30 may be consolidated with the semi-annual reports required by 40 CFR 70.6(a)(3)(iii)(A) as long as the report clearly indicates this and all required information is included and clearly delineated in the consolidated report. Unless required by an applicable reporting requirement, a written report is not required during periods in which there is no deviation. [40 CFR 70.6(a)(3)(iii)(B)] | 40 CFR 70.6(a)(3)(iii)(B) | Quarterly | |
| | | Submit Title V compliance certification: Due annually, by the 31st of March. Submit to the Office of Environmental Compliance, Surveillance Division. [40 CFR 70.6(c)(5)(iv)] | 40 CFR 70.6(c)(5)(iv) | Annually | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 11: Control of Emission of Smoke – Impairment of Visibility on Public Roads Prohibited | Requirements that limit emissions or operations - | | | |
| | | Emissions of smoke which pass onto or across a public road and create a traffic hazard by impairment of visibility as defined in LAC 33:III.111 or intensify an existing traffic hazard condition are prohibited. | LAC 33:III.1103 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|--|---|----------------------------|--|-------------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 11: Control of Emission of Smoke – Impairment of Visibility on Public Roads Prohibited | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 13: Emission Standards for Particulate Matter (Including Standards for Some Specific Facilities) – Provisions Governing Specific Activities | Requirements that limit emissions or operations - | | | |
| | | Emissions of particulate matter which pass onto or across a public road and create a traffic hazard by impairment of visibility or intensify an existing traffic hazard condition are prohibited. | LAC 33:III.1303.B | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|--|---------------------|--------------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 21: Control of Emission of Organic Compounds | Requirements that limit emissions or operations - | | | |
| | | Equip all rotary pumps and compressors handling volatile organic compounds having a true vapor pressure of 1.5 psia or greater at handling conditions with mechanical seals or other equivalent equipment. | LAC 33:III.2111 | N/A | |
| | | Maintain best practical housekeeping and maintenance practices at the highest possible standards to reduce the quantity of organic compounds emissions. Good housekeeping shall include, but not be limited to, the practices listed in LAC 33:III.2113.A.1-5. | LAC 33:III.2113.A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 2: Rules and Regulations for the Fee System of the Air Quality Control Programs | Requirements that limit emissions or operations - | | | |
| | | Failure to pay the prescribed application fee or annual fee as provided herein, within 90 days after the due date, will constitute a violation of these regulations and shall subject the person to applicable enforcement actions under the Louisiana Environmental Quality Act including, but not limited to, revocation or suspension of the applicable permit, license, registration, or variance. | LAC 33:III.219 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|--|---|----------------------------|--|-------------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 5: Permit Procedures | Requirements that limit emissions or operations - | | | |
| | | Permittee shall comply with the Part 70 General Conditions as set forth in LAC 33:III.535 and the Louisiana General Conditions as set forth in LAC 33:III.537. [LAC 33:III.535 and LAC 33:III.535 | LAC 33:III.535 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|--|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Prohibited Activities and Special Provisions | Requirements that limit emissions or operations - | | | |
| | | Do not construct or modify any stationary source subject to any standard set forth in LAC 33:III.Chapter 51.Subchapter A without first obtaining written authorization from DEQ in accordance with LAC 33:III.Chapter 51.Subchapter A, after the effective date of the standard. | LAC 33:III.5105.A.1 | | |
| | | Do not cause a violation of any ambient air standard listed in LAC 33:III.Table 51.2, unless operating in accordance with LAC 33:III.5109.B. | LAC 33:III.5105.A.2 | N/A | |
| | | Do not build, erect, install, or use any article, machine, equipment, process, or method, the use of which conceals an emission that would otherwise constitute a violation of an applicable standard. | LAC 33:III.5105.A.3 | | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | Do not fail to keep records, notify, report or revise reports as required under LAC 33:III.Chapter 51.Subchapter A. | LAC 33:III.5105.A.4 | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|---|---|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Reporting Requirements | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify reports to be submitted - | | | |
| | | Submit Annual Emissions Report (TED): Due annually, by the 31st of March unless otherwise directed by DEQ, to the Office of Environmental Assessment in a format specified by DEQ. Identify the quantity of emissions in the previous calendar year for any toxic air pollutant listed in Table 51.1 or Table 51.3. | LAC 33:III.5107.A | Annually | State Only |
| | | Include a certification statement with the annual emission report and revisions to any emission report that attests that the information contained in the emission report is true, accurate, and complete, and that is signed by a responsible official, as defined in LAC 33:III.502. Include the full name of the responsible official, title, signature, date of signature and phone number of the responsible official. | LAC 33:III.5107.A.2 | N/A | State Only |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|---|--|---------------------|--------------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Reporting Requirements | Submit notification: Due to the Department of Public Safety 24-hour Louisiana Emergency Hazardous Materials Hotline at (225) 925-6595 immediately, but in no case later than 1 hour, after any discharge of a toxic air pollutant into the atmosphere that results or threatens to result in an emergency condition (a condition which could reasonably be expected to endanger the health and safety of the public, cause significant adverse impact to the land, water or air environment, or cause severe damage to property). | LAC 33:III.5107.B.1 | N/A | State Only |
| | | Submit notification: Due to SPOC, except as provided in LAC 33:III.5107.B.6, no later than 24 hours after the beginning of any unauthorized discharge into the atmosphere of a toxic air pollutant as a result of bypassing an emission control device, when the emission control bypass was not the result of an upset, and the quantity of the unauthorized bypass is greater than or equal to the lower of the Minimum Emission Rate (MER) in LAC 33:III.5112, Table 51.1, or a reportable quantity (RQ) in LAC 33:I.3931, or the quantity of the unauthorized bypass is greater than one pound and there is no MER or RQ for the substance in question. Submit notification in the manner provided in LAC 33:I.3923. | LAC 33:III.5107.B.2 | N/A | State Only |
| | | Submit notification: Due to SPOC, except as provided in LAC 33:III.5107.B.6, immediately, but in no case later than 24 hours after any unauthorized discharge of a toxic air pollutant into the atmosphere that does not cause an emergency condition, the rate or quantity of which is in excess of that allowed by permit, compliance schedule, or variance, or for upset events that exceed the reportable quantity in LAC 33:I.3931. Submit notification in the manner provided in LAC 33:I.3923. | LAC 33:III.5107.B.3 | N/A | State Only |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|----------------------------|-----------------------------------|-------------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Reporting Requirements | Submit written report: Due by certified mail to SPOC within seven calendar days of learning of any such discharge or equipment bypass as referred to in LAC 33:III.5107.B.1 through B.3. Include the information specified in LAC 33:III.5107.B.4.a.i through B.4.a.viii. | LAC 33:III.5107.B.4 | N/A | State Only |
| | | Report all discharges to the atmosphere of a toxic air pollutant from a safety relief device, a line or vessel rupture, a sudden equipment failure, or a bypass of an emission control device, regardless of quantity, IF THEY CAN BE MEASURED AND CAN BE RELIABLY QUANTIFIED USING GOOD ENGINEERING PRACTICES, to DEQ along with the annual emissions report and where otherwise specified. Include the identity of the source, the date and time of the discharge, and the approximate total loss during the discharge. | LAC 33:III.5107.B.5 | N/A | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that limit emissions or operations - | | | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|--|--|----------------------------|--|-------------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards | Requirements that specify reports to be submitted - | | | |
| | | Develop a standard operating procedure (SOP) within 120 days after achieving or demonstrating compliance with the standards specified in LAC 33:III. Chapter 51. Detail in the SOP all operating procedures or parameters established to ensure that compliance with the applicable standards is maintained and address operating procedures for any monitoring system in place, specifying procedures to ensure compliance with LAC 33:III.5113.C.5. Make a written copy of the SOP available on site or at an alternate approved location for inspection by DEQ. Provide a copy of the SOP within 30 days upon request by DEQ. | LAC 33:III.5109.C | N/A | State Only |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Standard for Asbestos | Requirements that limit emissions or operations - | | | |
| | | An individual or company contracted to perform a demolition or renovation activity which disturbs RACM must be recognized by the Licensing Board for Contractors to perform asbestos abatement, and shall meet the requirements of LAC 33:III.5151.F.2 and F.3 for each demolition or renovation activity. | LAC 33:III.5151.F.1.f | N/A | State Only |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|--|---|---|-----------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Standard for Asbestos | Requirements that specify reports to be submitted - | | | |
| | | Submit notification in writing: Due to SPOC not more than 60 days nor less than 30 days prior to initial start-up. Submit the anticipated date of the initial start-up. | LAC 33:III.5113.A.1 | N/A | |
| | | Submit notification in writing: Due to SPOC within 10 working days after the actual date of initial start-up of the source. Submit the actual date of initial start-up of the source. | LAC 33:III.5113.A.2 | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 56: Prevention of Air Pollution Emergency Episodes: Preplanned Strategies Required | Requirements that limit emissions or operations - | | | |
| | | Activate the preplanned abatement strategy listed in LAC 33:III.5611.Table 5 when the administrative authority declares an Air Pollution Alert. | LAC 33:III.5609.A.1.b | N/A | |
| | | Activate the preplanned strategy listed in LAC 33:III.5611.Table 6 when the administrative authority declares an Air Pollution Warning. | LAC 33:III.5609.A.2.b | N/A | |
| | | Activate the preplanned abatement strategy listed in LAC 33:III.5611.Table 7 when the administrative authority declares an Air Pollution Emergency. | LAC 33:III.5609.A.3.b | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|--|---|---|---------------------|--------------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 56: Prevention of Air Pollution Emergency Episodes: Preplanned Strategies Required | Requirements that specify reports to be submitted - | | | |
| | | Prepare standby plans for the reduction of emissions during periods of Air Pollution Alert, Air Pollution Warning and Air Pollution Emergency. Design standby plans to reduce or eliminate emissions in accordance with the objectives as set forth in LAC 33:III.5611. Tables 5, 6, and 7. | LAC 33:III.5609.A | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 59: Chemical Accident Prevention and Minimization of Consequences | Requirements that limit emissions or operations - | | | |
| | | Comply with the provisions in 40 CFR 68, except as specified in LAC 33:III.5901. | LAC 33:III.5901.A | N/A | |
| | | Identify hazards that may result from accidental releases of the substances listed in 40 CFR 68.130, Table 59.0 of LAC 33:III.5907, or Table 59.1 of LAC 33:III.5913 using appropriate hazard assessment techniques, design and maintain a safe facility, and minimize the off-site consequences of accidental releases of such substances that do occur. | LAC 33:III.5907 | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/Frequency | State Only Requirement |
|---|--|---|---------------------|----------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 59: Chemical Accident Prevention and Minimization of Consequences | Requirements that specify reports to be submitted - | | | |
| | | Submit registration: Due January 31, 1998, or within 60 days after the source becomes subject to LAC 33:III.Chapter 59, whichever is later. Include the information listed in LAC 33:III.5911.B, and submit to the Department of Environmental Quality, Office of Environmental Compliance, Emergency and Radiological Services Division. | LAC 33:III.5911.A | N/A | |
| | | Submit amended registration: Due to the Department of Environmental Quality, Office of Environmental Compliance, Emergency and Radiological Services Division, within 60 days after the information in the submitted registration is no longer accurate. | LAC 33:III.5911.C | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |
| | | | | | |
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 | Title 33 Chapter 9: General Regulations on Control of Emissions and Emission Standards | Requirements that limit emissions or operations - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify monitoring - | | | |
| | | N/A | N/A | N/A | |
| | | Requirements that specify records to be kept and requirements that specify record retention time - | | | |
| | | N/A | N/A | N/A | |

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

| Emission Point ID No.: | Applicable Requirement | Compliance Method/Provision | Compliance Citation | Averaging Period/ Frequency | State Only Requirement |
|---|--|--|---------------------|--------------------------------|------------------------|
| Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued) | Title 33 Chapter 9: General Regulations on Control of Emissions and Emission Standards | Requirements that specify reports to be submitted - | | | |
| | | Submit Emission Inventory (EI)/Annual Emissions Statement: Due annually, by the 31st of March for the period January 1 to December 31 of the previous year unless otherwise directed. Submit emission inventory data in the format specified by the Office of Environmental Assessment, Air Quality Assessment Division. Include all data applicable to the emissions source(s), as specified in LAC 33:III.919.A-D. | LAC:III.919.D | N/A | |
| | | Report the unauthorized discharge of any air pollutant into the atmosphere in accordance with LAC 33:I.Chapter 39, Notification Regulations and Procedures for Unauthorized Discharges. Submit written reports to the department pursuant to LAC 33:I.3925. Submit timely and appropriate follow-up reports detailing methods and procedures to be used to prevent similar atmospheric releases. | LAC:III.927 | N/A | |
| | | Requirements that specify performance testing - | | | |
| | | N/A | N/A | N/A | |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|---|--------------------------|--------------------------|---|---|
| EQT150 thru EQT155 | 40 CFR 60.110b | Does Not Apply | Storage tanks have a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |
| 1700-5.3 thru 5.8 EQT178 1700-63.5 | 40 CFR 63.160 | Exempted | Exempt from controls as surge vessels do not meet the conditions specified in Table 2. Vessels have capacities less than 75 m ³ . | 40 CFR 63.160 |
| RLP016 1700-56 | LAC 33:III.2115 | Exempted | As per requirement of LAC 33:III.2115.H.1.c | LAC 33:III.2115.H.1.c |
| EQTs - 134, 167, 135, 136, 183, 0185, 0198 1700-1, 5A, 13, 13A, 64, 66 and 79 | LAC 33:III.2115 | Exempted | As per requirement of LAC 33:III.2115.H.2.b. | LAC 33:III.2115.H.2.b |
| | LAC 33:III.5107 and 5109 | Does Not Apply | Emissions are intermittent. Controlling these emissions is not practical or safe. | |
| | 40 CFR 63.480 | Does Not Apply | Does not meet the definition of batch or continuous front-end process vent. | |
| EQT142 thru EQT149 | LAC 33:III.2115. | Exempted | As per requirements of LAC 33:III.2115.H.2.b | LAC 33:III.2115.H.2.b |
| 1700-25 thru 28, and 45 thru 48 | 40 CFR 63 Subpart U | Exempted | As per requirements of 40 CFR 63.494(a)(4). There are no process back end requirements for the Neoprene Units. These sources are exempted from Subpart U under the back-end process provisions. | 40 CFR 63.494(a)(4) |
| EQT141 1700-21A | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 60.110b | Does Not Apply | No construction or modification after 7/23/84. | |
| EQT137 & ETQ138 1700-14B.1 and 14B.2 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | LAC 33:III.5107 and 5109 | Does Not Apply | These vessels do not store TAP compounds. | |
| | 40 CFR 60.110b | Does Not Apply | Tanks have a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |
| | 40 CFR 63.480 | Exempted | As per the requirements of 40 CFR 63.480(c)(1). These vessels do not store HAPs. | 40 CFR 63.480(c)(1) |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|---|--------------------------------------|--------------------------|--|---|
| RLP013 1700-14B.3 | LAC 33:III.2115 | Exempted | As per the requirements of LAC 33:III.2115.H.4. | LAC 33:III.2115.H.4 |
| | LAC 33:III.5107 and 5109 | Does Not Apply | Emissions are intermittent. Controlling these emissions is not practical or safe | |
| | 40 CFR 63.480 | Does Not Apply | Does not meet the definition of batch or continuous front-end process vent. | |
| ETQ166, 168, 169, 170 1700-57 1700-60 thru 62 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | LAC 33:II.5107 and 5109 | Does Not Apply | Does not store TAP compounds. | |
| | 40 CFR 60.110b | Does Not Apply | Tanks have a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |
| | 40 CFR 63.480 | Exempted | As per the requirements of 40 CFR 63.480(c)(1). These vessels do not store HAPs. | 40 CFR 63.480(c)(1) |
| EQT163 thru EQT165 1700-53 thru 55 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 60.110b | Does Not Apply | Tanks have a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |
| | 40 CFR 63 Subpart U 40 CFR 63.480 | Exempted | As per requirements of 40 CFR 63.484(b)(2) | 40 CFR 63.484(b)(2) |
| EQT156 thru EQT161, EQT171, EQT175 thru EQT177, and EQT162 1700-50.1 thru 50.6, 63.1 thru 63.4 and 1700-51 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 60.110b | Does Not Apply | Tanks have a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|--|----------------------------|---------------------------------|---|--|
| EQT172, EQT173, & EQT181 1700-63.8, 1700-63.10 and 1700-63.11 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 60.110b | Exempted | As per the requirements of 40 CFR 110b(b), vapor pressure of contents is less than 2.1 psia (15 kpa). | 40 CFR 60.110b(a) |
| EQT182 1700-63.9 | 40 CFR 60.110b | Does Not Apply | No Construction or modification after 7/23/84. | |
| EQT186 thru EQT192 1700-67 thru 73 | 40 CFR 63 Subpart U | Exempted | As per requirements of 40 CFR 63.484(b)(2) | 40 CFR 63.484(b)(2) |
| | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 60.110b | Does Not Apply | Tanks have a capacity of less than 75 cubic meters (19,813 gallons). 40 CFR 60.110b(a) | 40 CFR 60.110b(a) |
| EQT194 thru EQT196 1700-75 thru 77 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | LAC 33:III. 5107, and 5109 | Does Not Apply | Tanks do not store TAP compounds. | |
| | 40 CFR 60.110b | Exempted | As per the requirements of 40 CFR 110b(b), vapor pressure of contents is less than 2.1 psia (15 kpa). | 40 CFR 110b(b) |
| | 40 CFR 63.480 | Exempted | As per the requirements of 40 CFR 63.480(c)(1). These vessels do not store HAPs. | 40 CFR 63.480(c)(1) |
| ET202 thru EQT204 3-95, 4-95, and 5-95 | 40 CFR 60.110b | Does Not Apply | No Construction or modification after 7/23/84. | |
| | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|---|---------------------------|---------------------------------|--|--|
| EQT199 and EQT200 1700-80.1 1700-80.2 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | LAC 33:III. 5107 and 5109 | Does Not Apply | Tanks do not store TAP compounds. | |
| | 40 CFR 60.110b | Exempted | As per the requirements of 40 CFR 110b(b), vapor pressure of contents is less than 2.1 psia (15 kpa). | 40 CFR 110b(b) |
| | 40 CFR 63.480 | Does Not Apply | These tanks are associated with the ACR production Unit which is covered under Subpart FFFF | |
| | 40 CFR 63.2470 | Exempted | These vessels do not store organic HAPs. | |
| RLP 017 1700-80 | LAC 33:III. 5107 and 5109 | Does Not Apply | This header does not emit TAP compounds. | |
| | 40 CFR 63.480 | Does Not Apply | Sources venting thru this header are associated with the ACR production Unit which is covered under Subpart FFFF | |
| | 40 CFR 63.2470 | Exempted | This header does not emit organic HAPs. | |
| EQT205 thru EQT208 1700-81.1 1700-81.2 1700-81.3 1700-81.4 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | LAC 33:III. 5107 and 5109 | Does Not Apply | Tanks do not store TAP compounds. | |
| | 40 CFR 60.110b | Does Not Apply | Tanks have a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |
| | 40 CFR 63.2470 | Exempted | These vessels do not store organic HAPs. | |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|--|--------------------------|--------------------------|---|---|
| EQT209 thru EQT211 1700-81.5 1700-81.6 1700-81.7 | LAC 33:III.2115 | Exempted | The waste gas stream has a combined weight of VOC of less than 100 pounds in any continuous 24-hour period. | LAC 33:III.2115.H.1.c |
| | LAC 33:III.5107 and 5109 | Does Not Apply | Does not store TAP compounds. | |
| | 40 CFR 63.480 | Does Not Apply | These sources are associated with the ACR production Unit which is covered under Subpart FFFF. | |
| | 40 CFR 63.2470 | Does Not Apply | These sources do not emit TAP compounds. | |
| RLP018 1700-81 | LAC 33:III.2115 | Exempted | The waste gas stream has a combined weight of VOC of less than 100 pounds in any continuous 24-hour period. | LAC 33:III.2115 |
| | LAC 33:III.5107 and 5109 | Does Not Apply | Does not store TAP compounds. | LAC 33:III.5107 and 5109 |
| | 40 CFR 63.480 | Does Not Apply | This vent is associated with the ACR production Unit which is covered under Subpart FFFF. | 40 CFR 63.480 |
| | 40 CFR 63.2470 | Does Not Apply | This vent does not emit TAP compounds. | 40 CFR 63.2470 |
| EQT201 1700-82 | 40 CFR 60.110b | Does Not Apply | This tank has a capacity of less than 75 cubic meters (19,813 gallons). | 40 CFR 60.110b(a) |
| | 40 CFR 63.480 | Does Not Apply | This tank is associated with the ACR production Unit which is covered under Subpart FFFF. | |
| | 40 CFR 63.2470 | Exempted | The volume of this tank is less than 10,000 gallons. | |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|---|--------------------------|--------------------------|---|---|
| RLP019 1700-83 | LAC 33:III.2115 | Exempted | The waste gas stream has a combined weight of VOC of less than 100 pounds in any continuous 24-hour period. | LAC 33:III.2115.H.1.c |
| | LAC 33:III.5107 and 5109 | Does Not Apply | TAPs emissions from this source are emitted below their respective MER facility wide. No MACT required. | |
| | 40 CFR 63.480 | Does Not Apply | This tank is associated with the ACR production Unit which is covered under Subpart FFFF. | |
| | 40 CFR 63.2470 | Exempted | This source does not meet the definition of process vent per 40 CFR 63.2455. | 40 CFR 63.2455 |
| EQT212 1700-84A | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 60.110b | Does Not Apply | This tank has a capacity of less than 75 cubic meters (19,813 gallons). | |
| | 40 CFR 63.480 | Does Not Apply | This tank is associated with the ACR production Unit which is covered under Subpart FFFF. | |
| | 40 CFR 63.2470 | Exempted | The volume of this tank is less than 10,000 gallons.. | |
| EQT213 1700-84B EQT214 1700-85 | LAC 33:III.2107 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | 40 CFR 63.2470 | Exempted | As per 63.2550 – definition of Group 1 transfer racks, since the vapor pressure of the liquid being loaded is less than 1.5 psia this facility is a Group 2 and there are no requirements other than recordkeeping under 40 CFR 63.130(f) | 40 CFR 63.130(f) |

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

| Emission Point ID No: | Requirement | Exempt or Does Not Apply | Explanation | Citation Providing for Exemption or Non-applicability |
|---------------------------------|--------------------------|--------------------------|---|---|
| EQT215 1700-86 | LAC 33:III.2103 | Does Not Apply | VOC total vapor pressure is less than the regulated threshold of 1.5 psia. | |
| | LAC 33:III.5107 and 5109 | Does Not Apply | Does not store TAP compounds | |
| | 40 CFR 60.110b | Does Not Apply | Tank has a capacity of less than 75 cubic meters (19,813 gallons). | |
| | 40 CFR 63.480 | Exempted | As per the requirements of 40 CFR 63.480(c)(1). This vessel does not store HAHPs. | 40 CFR 63.480(c)(1). |
| 1700-87, 1700-88, 1700-89 | LAC 33:III.2115 | Exempted | As per requirement of LAC 33:III.2115.H.2.b. | LAC 33:III.2115.H.2.b |
| No. 10, No. 13 & No. 14 | LAC 33:III.5107 and 5109 | Does Not Apply | Emissions are intermittent. Controlling these emissions is not practical or safe. | |
| Emulsion Storage Tank Manway | 40 CFR 63.480 | Does Not Apply | Does not meet the definition of batch or continuous front-end process vent. | |

The above table provides explanation for either the exemption status or non-applicability of a source cited by 2 or 3 in the matrix presented in Table 1 of this application.

TABLE 4: EQUIPMENT LIST

Enter each single emission point that routes its emissions to another source (i.e., a control device) or a common stack, or is part of an Emissions Cap. List the emissions source to which each single emission point is routed or the Cap of which the source is a member, if applicable. Consult instructions.

| Emission Point ID No: | Description | Construction Date | Routes to: | Operating Rate/Volume | Applicable Requirement(s)? |
|-----------------------------|---|-------------------|---------------------|-----------------------|---|
| 1700-2 (RLP0014) | Strippers Condenser Vent | | | | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-2A (EQT219) | No. 1 Stripper | | 1700-2 (RLP0014) | 12,600 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-2B (EQT220) | No. 2 Stripper | | 1700-2 (RLP0014) | 12,600 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-2C (EQT221) | No. 3 Stripper | | 1700-2 (RLP0014) | 12,600 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-3 (RLP0015) | Poly Kettles Vent Condenser | | | | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-3A (EQT222) | Poly Kettle No. 1 | | 1700-3 (RLP0015) | 1420 charges/yr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-3B (EQT223) | Poly Kettle No. 2 | | 1700-3 (RLP0015) | 1420 charges/yr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-3C (EQT224) | Poly Kettle No. 3 | | 1700-3 (RLP0015) | 1420 charges/yr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-3D (EQT225) | Poly Kettle No. 4 | | 1700-3 (RLP0015) | 1420 charges/yr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-3E (EQT226) | Poly Kettle No. 5 | | 1700-3 (RLP0015) | 1420 charges/yr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-5 (GRP0008) | Unstripped Emulsion Storage Tanks Vent | | | | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-5.3 (EQT150) | Unstripped Emulsion Storage Tank. No. 6 | 7/1968 | 1700-5 (GRP0008) | 11,622 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-5.4 (EQT151) | Unstripped Emulsion Storage Tank. No. 7 | 8/1972 | 1700-5 (GRP0008) | 14,950 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-5.5 (EQT152) | Unstripped Emulsion Storage Tank. No. 8 | 8/1972 | 1700-5 (GRP0008) | 14,950 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |

TABLE 4: EQUIPMENT LIST

| Emission Point ID No: | Description | Construction Date | Routes to: | Operating Rate/Volume | Applicable Requirement(s)? |
|-------------------------------|--|--------------------------|-----------------------|------------------------------|---|
| 1700-5.6 (EQT153) | Unstripped Emulsion Storage Tank. No. 10 | 9/2007 | 1700-5 (GRP0008) | 16,000 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-5.7 (EQT154) | Unstripped Emulsion Storage Tank. No. 13 | 9/2007 | 1700-5 (GRP0008) | 10,000 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-5.8 (EQT155) | Unstripped Emulsion Storage Tank. No. 14 | 9/2007 | 1700-5 (GRP0008) | 10,000 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-14B (GRP0006) | Acetic Acid Tanks | | | | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-14B.1 (EQT137) | Acetic Acid Make-up Tank | 1975 | 1700-14B (GRP0006) | 1,590 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-14B.2 (EQT138) | Acetic Acid Hold-up Tank | 1975 | 1700-14B (GRP0006) | 600 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-25A (GRP0007) | Product Drying CAP | | | | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-25 (EQT142) | East Wash Belt Dryer | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-26 (EQT143) | West Wash Belt Dryer | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-27 (EQT144) | East Hot Dryer Exhaust | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-28 (EQT145) | West Hot Dryer Exhaust | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-45 (EQT146) | No. 1 East Dryer Cooling Compt. | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-46 (EQT147) | No. 1 West Dryer Cooling Compt. | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-47 (EQT148) | No. 2 East Dryer Cooling Compt. | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-48 (EQT149) | No. 2 West Dryer Cooling Compt. | 1970 | 1700-25A (GRP0007) | 30,000 lb/hr | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |

TABLE 4: EQUIPMENT LIST

| Emission Point ID No: | Description | Construction Date | Routes to: | Operating Rate/Volume | Applicable Requirement(s)? |
|------------------------------|---------------------------------|--------------------------|-------------------|------------------------------|---|
| 1700-50 (GRP0009) | Stabilizer Tanks Vent | | | | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-50.1 (EQT156) | Stabilizer Tank No. 1 | 10/1975 | 1700-50 (GRP0009) | 1,070 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-50.2 (EQT157) | Stabilizer Tank No. 2 | 10/1975 | 1700-50 (GRP0009) | 1,070 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-50.3 (EQT158) | Stabilizer Tank No. 3 | 7/1968 | 1700-50 (GRP0009) | 1,070 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-50.4 (EQT159) | Stabilizer Tank No. 4 | 7/1968 | 1700-50 (GRP0009) | 1,070 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-50.5 (EQT160) | Stabilizer Tank No. 5 | 9/2007 | 1700-50 (GRP0009) | 1,070 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-50.6 (EQT161) | Stabilizer Tank – LD750 | 9/2007 | 1700-50 (GRP0009) | 300 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63 (GRP0010) | Vent Header System | | | | |
| 1700-63.1 (EQT171) | No. 1 CD Solution Tank | 8/1968 | 1700-63 (GRP0010) | 3,690 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.2 (EQT175) | No. 2 CD Solution Tank | 7/1972 | 1700-63 (GRP0010) | 3,690 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.3 (EQT176) | Recovered CD Storage Tank No. 1 | 6/1968 | 1700-63 (GRP0010) | 8,156 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.4 (EQT177) | Recovered CD Storage Tank No. 2 | 6/1968 | 1700-63 (GRP0010) | 8,156 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.5 (EQT178) | CD Heels Tank | 9/1990 | 1700-63 (GRP0010) | 8,315 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.8 (EQT181) | Crude CD Storage Tank No. 3 | 3/1971 | 1700-63 (GRP0010) | 25,750 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |

TABLE 4: EQUIPMENT LIST

| Emission Point ID No: | Description | Construction Date | Routes to: | Operating Rate/Volume | Applicable Requirement(s)? |
|------------------------------|--------------------------------|--------------------------|----------------------|------------------------------|---|
| 1700-63.9 V182) | Refined CD Storage Tank | 3/1971 | 1700-63 (GRP0010) | 50,000 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.10 (EQT172) | Inhibitor Final Make-up Tank | 6/1968 | 1700-63 (GRP0010) | 22,164 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-63.11 (EQT173) | Inhibitor Hold-up Tank | 6/1968 | 1700-63 (GRP0010) | 22,164 gal | <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No |
| 1700-80 (RLP017) | ACR Storage Vent Header | | | | |
| 1700-80.1 (EQT199) | Refined ACR Storage Tank | 3/1971 | 1700-8 (RLP017) | 55,000 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-80.2 (EQT200) | Chlorinated ACR Storage Tank | 6/1968 | 1700-8 (RLP017) | 22,164 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81 (RLP018) | ACR Refining Vent | | | | |
| 1700-81.1 (EQT205) | NMP/PTZ Tote | 1/2008 | 1700-81 (RLP018) | 400 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81.2 (EQT 206) | Aqueous Actrene Tote | 1/2008 | 1700-81 (RLP018) | 400 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81.3 (EQT207) | Recovery Column Heels Tote | 1/2008 | (1700-81 (RLP018) | 400 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81.4 (EQT208) | TBC Tote | 1/2008 | 1700-81 (RLP018) | 400 gal | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81.5 (EQT209) | ACR Refining Column | 9/2007 | 1700-81 (RLP018) | 3 MMlb/yr | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81.6 (EQT210) | ACR RC Condenser | 9/2007 | 1700-81 (RLP018) | 3 MMlb/yr | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |
| 1700-81.7 (EQT211) | ACR RC Reboiler | 9/2007 | 1700-81 (RLP018) | 3 MMlb/yr | <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No |

23. Emissions Inventory Questionnaire (EIQ) Forms [LAC 33:III.517.D.3; 517.D.6]

Complete one (1) EIQ for:

- Each emission source. If two emission sources have a common stack, the applicant may submit one EIQ sheet for the common emissions point. Note any emissions sources that route to this common point in Table 4 of the application.
- Each emissions CAP that is proposed. In general, this applies to each source that is part of the CAP.
- Each alternate operating scenario that a source may operate under. Some common scenarios are:
 1. Sources that combust multiple fuels
 2. Sources that have Startup/Shutdown max lb/hr emission rates higher than the max lb/hr for normal operating conditions would need an EIQ for the Startup/Shutdown emission rates for those sources
- Fugitive emissions releases. One (1) EIQ should be completed for each of the following types of fugitive emissions sources or emissions points:
 1. Equipment leaks.
 2. Non-equipment leaks (i.e. road dust, settling ponds, etc).

For each EIQ:

- Fill in all requested information.
- Speciate all Toxic Air Pollutants and Hazardous Air Pollutants emitted by the source.
- Use appropriate significant figures.
- Consult instructions.

The EIQ is in Microsoft Word Excel. Visit the following website to get to the EIQ form.

<http://www.deq.louisiana.gov/portal/DIVISIONS/AirPermits/AirPermitApplications.aspx>

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|--|--|--|--|--|---|
| Emission Point ID No. (Designation) 1700-1 | Descriptive Name of the Emissions Source (Alt. Name) No. 7, 8, 10, 13, and 14 Emulsion Storage Tank Manhole and Exhaust Blower | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical 3327400 mN 15 " 15 " |
| Tempo Subject Item ID No. EQT0134 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 1.25 ft ft ² | 53.8 ft | 34.00 ft/sec | 2,500 ft ³ /min | 77 °F | 8,760 hr/yr | Aug 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 42,000 lb/charge | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-1 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.81 | 2.57 | 3.56 | 3.56 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.55 | 1.75 | 2.42 | 2.42 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.09 | 0.27 | 0.38 | 0.38 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|---|--|--|---|
| Emission Point ID No. (Designation) 1700-2 | Descriptive Name of the Emissions Source (Alt. Name) Strippers Condenser Vent | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. RLP0014 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 15 " | | Datum NAD83 3327400 mN hundredths hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.33 ft ft ² | 62.4 ft | 1.36 ft/sec | 7.1 ft ³ /min | 0 °F | 8,760 hr/yr | 2006 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|---|--|------------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 12,600 lbs/hr/stripper | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes VOC emission rate includes 0.01 lbs/yr of 1,2-dichlorobenzene | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-2 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 047 | >95 | | 3.02 | 4.43 | 13.22 | 17.36 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 047 | >95 | 00126-99-8 | 3 | 4.4 | 13.14 | 17.30 | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.018 | 0.03 | 0.077 | 0.03 | C | | ppm by vol |
| Ammonia | 000 | 0% | 07664-41-7 | 1.2 | 1.8 | 5.26 | 10.51 | C | | ppm by vol |

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|--|--|---|--|---|--|---|--|--|------------------------------|---|
| Emission Point ID No. (Designation) 1700-3 | | Descriptive Name of the Emissions Source (Alt. Name) Poly Kettles Vent Condenser | | | Approximate Location of Stack or Vent (see instructions) | | | | | |
| Tempo Subject Item ID No. RLP0015 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30</u> ° <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90</u> ° <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | |
| | | | | | | | | | | |
| | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) 0.33 ft ft ² | Height of Stack Above Grade (ft) 62.4 ft | Stack Gas Exit Velocity 4.20 ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) 22 ft ³ /min | Stack Gas Exit Temperature (°F) 34 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification 2006 | Percent of Annual Throughput Through This Emission Point | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | 25% | 25% | 25% | 25% |
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | | Operating Parameters (include units) | | | | | | |
| | a | Type of Fuel | Heat Input (MMBTU/hr) | | | | Parameter | Description | | |
| | b | NA | NA | Normal Operating Rate/Throughput | | | 7,060 charges/yr | | | |
| | c | | | Maximum Operating Rate/Throughput | | | NA | | | |
| Notes VOC emission rate includes 10 lbs/yr of 1,2-dichlorobenzene | | | | Design Capacity/Volume/Cylinder Displacement | | | NA | | | |
| | | | | Shell Height (ft) | | | NA | | | |
| | | | | Tank Diameter (ft) | | | NA | | | |
| | | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered <input type="checkbox"/> Engine Model Year <input type="checkbox"/> Date Engine Was Built by Manufacturer <input type="checkbox"/> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | |
| Emission Point ID No. (Designation) 1700-3 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 047 | >95 | | 7.84 | 35.54 | 34.35 | 34.92 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 047 | >95 | 00126-99-8 | 7.72 | 35.2 | 33.82 | 34.39 | C | | ppm by vol |
| Toluene | 047 | >95 | 00108-88-3 | 0.12 | 0.34 | 0.53 | 0.53 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-5 | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tanks Vent | Approximate Location of Stack or Vent (see instructions) | |
| Tempo Subject Item ID No. GRP0008 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN Datum NAD83 3 hundredths 15 hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 0.167 ft ft ² | 55.3 ft | 74.72 ft/sec | 10.1 ft ³ /min | 77 °F | 8,760 hr/yr | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | |
|--|---|-----------------------|---|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description |
| a | NA | NA | Normal Operating Rate/Throughput | 35.0 MMgal/yr |
| b | | | Maximum Operating Rate/Throughput | NA |
| c | | | Design Capacity/Volume/Cylinder Displacement | NA |
| Notes *CAP for EIQ nos. 1700-5.3, 5.4, 5.5, 5.6, 5.7, and 5.8. VOC emissions rate includes 10 lbs/yr of 1,2-dichlorobenzene | | | Shell Height (ft) | NA |
| | | | Tank Diameter (ft) | NA |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | |
| | | | Date Engine Ordered | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |

| Emission Point ID No. (Designation) 1700-5 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.67 | * | 2.94 | 2.77 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.67 | * | 2.91 | 2.73 | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | <0.01 | * | 0.03 | 0.03 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|--|--|---|--|---|--|--|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-5.3 | | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tank No. 6 | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT0150 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jul 1968 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | |
| | | | | | | | 25% | 25% | 25% | 25% | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | | | | | | | |
| a | NA | | NA | | | | | | | | |
| b | | | | | | | | | | | |
| c | | | | | | | | | | | |
| Notes *Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent | | | | Normal Operating Rate/Throughput 35 MMgal/yr Maximum Operating Rate/Throughput 35 MMgal/yr Design Capacity/Volume/Cylinder Displacement 11,622 gal Shell Height (ft) 16.83 Tank Diameter (ft) 11.5 Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered _____ Engine Model Year _____ Date Engine Was Built by Manufacturer _____ SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-5.3 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | 000 | 0% | | * | 5.29 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| Chloroprene | | 000 | 0% | 00126-99-8 | * | 5.23 | * | * | U | | ppm by vol |
| Toluene | | 000 | 0% | 00108-88-3 | * | 0.05 | * | * | U | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-5.4 | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tank No. 7 | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0151 | | Method UTM Zone 15 Latitude 30° Longitude -90° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN Datum NAD83 | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|---|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft² | NA ft | NA ft/sec | NA | 77 °F | 8,760 hr/yr | Aug 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|--|--|--------------------|-------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a | NA | NA | Normal Operating Rate/Throughput | 35 MMgal/yr | |
| | b | | | Maximum Operating Rate/Throughput | 35 MMgal/yr | |
| c | | | | Design Capacity/Volume/Cylinder Displacement | 14,950 gal | |
| Notes | | | | | Shell Height (ft) | 20.75 |
| *Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent | | | | | Tank Diameter (ft) | 12 |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-5.4 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 5.40 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 5.34 | * | * | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 0.05 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-5.5 | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tank No. 8 | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 Horizontal 739000 mE 30° 3' 15" N -90° 31' 15" W | | Datum NAD83 3327400 mN hundredths hundredths |
| Tempo Subject Item ID No. EQT0152 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|---|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft² | NA ft | NA ft/sec | NA | 77 °F | 8,760 hr/yr | Aug 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 35 MMgal/yr | |
| b | | | Maximum Operating Rate/Throughput | | 35 MMgal/yr | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 14,950 gal | |
| Notes *Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent | | | Shell Height (ft) | | 20.75 | |
| | | | Tank Diameter (ft) | | 12 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-5.5 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 5.40 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 5.34 | * | * | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 0.05 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|---|--|--|--|--|
| Emission Point ID No. (Designation) 1700-5.6 | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tank No. 10 | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0153 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum NAD83 Horizontal 739000 31 Vertical mE 15 " 15 " |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA | 77 °F | 8,760 hr/yr | Sept 2007 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|--|---|-----------------------|--|----------------|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description |
| a | NA | NA | Normal Operating Rate/Throughput | 17.5 MM gal/yr | |
| b | | | Maximum Operating Rate/Throughput | 17.5 MM gal/yr | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 16,000 gal | |
| Notes *Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent | | | Shell Height (ft) | 22 | |
| | | | Tank Diameter (ft) | 12.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) 1700-5.6 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 5.40 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 5.34 | * | * | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 0.05 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|---|---|--|---|---|---|--|--|------------------------------------|--|
| Emission Point ID No. (Designation) 1700-5.7 | | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tank No. 13 | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT0154 | | | | | Method 06, "Address Matching-Primary Name" Datum NAD83 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN Latitude 30 ° 3 ' 15 " hundredths Longitude -90 ° 31 ' 15 " hundredths | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Sept 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | | | | | | | |
| | a | NA | NA | | | | | | | | |
| | b | | | | | | | | | | |
| | c | | | | | | | | | | |
| Notes | | | | | | | | | | | |
| *Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent | | | | Normal Operating Rate/Throughput 17.5 MM gal/yr Maximum Operating Rate/Throughput 17.5 MM gal/yr Design Capacity/Volume/Cylinder Displacement 10,000 gal Shell Height (ft) 17 Tank Diameter (ft) 11.5 Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered _____ Engine Model Year _____ Date Engine Was Built by Manufacturer _____ SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | |
| Emission Point ID No. (Designation) 1700-5.7 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) Annual (tons/yr) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | 000 | 0% | | * | 2.33 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| Chloroprene | | 000 | 0% | 00126-99-8 | * | 2.31 | * | * | U | | ppm by vol |
| Toluene | | 000 | 0% | 00108-88-3 | * | 0.02 | * | * | U | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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|--|---|--|--|--|---|
| Emission Point ID No. (Designation) 1700-5.8 | Descriptive Name of the Emissions Source (Alt. Name) Unstripped Emulsion Storage Tank No. 14 | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0155 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical 3327400 mN 15 " 15 " |

| | | | | | | | | | | | |
|--|---|---|--|---|--|---|---|--|----------------|----------------|----------------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Sept 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| | | | | | | |
|--|---|-----------------------|--|--|-------------------|--|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a | NA | Normal Operating Rate/Throughput | | 17.5 MM gal/yr | |
| | b | | Maximum Operating Rate/Throughput | | 17.5 MM gal/yr | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 10,000 gal | |
| Notes | | | Shell Height (ft) | | 17 | |
| *Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent | | | Tank Diameter (ft) | | 11.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-5.8 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 2.33 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 2.31 | * | * | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 0.02 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|---|---|--|---|
| Emission Point ID No. (Designation) 1700-5A | Descriptive Name of the Emissions Source (Alt. Name) No. 6 Emulsion Storage Tank Manhole | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0167 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN 15" hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 1.33 ft ft ² | 53.8 ft | 88.30 ft/sec | 7,400 ft ³ /min | 77 °F | 8,760 hr/yr | Jul 1968 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 42,000 lb/charges | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *Blower operating time. Emission rates vary depending upon manhole opening, sampling, and other activities. | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-5A | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.50 | 0.76 | 2.19 | 2.19 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.34 | 0.52 | 1.49 | 1.49 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.05 | 0.08 | 0.23 | 0.23 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|---|--|---|
| Emission Point ID No. (Designation) 1700-13 | Descriptive Name of the Emissions Source (Alt. Name) Pol Kettles Manholes/Strainers (1 and 2) | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN hundredths |
| Tempo Subject Item ID No. EQT0135 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 1.33 ft ft ² | 58.2 ft | 82.40 ft/sec | 6,900 ft ³ /min | 77 °F | 8,760 hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|---|--------------|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description | | |
| a | NA | NA | Normal Operating Rate/Throughput | 82,000 lb/hr | | |
| b | | | Maximum Operating Rate/Throughput | NA | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | NA | | |
| Notes *Blower operating time. Emission rates vary depending upon manhole opening, sampling, and other activities. | | | Shell Height (ft) | NA | | |
| | | | Tank Diameter (ft) | NA | | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-13 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 1.86 | 2.18 | 8.15 | 8.15 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 1.33 | 1.56 | 5.82 | 5.82 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.18 | 0.21 | 0.79 | 0.79 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|---|---|---|--|---|
| Emission Point ID No. (Designation) 1700-13A | Descriptive Name of the Emissions Source (Alt. Name) Pol Kettles Manholes/Strainers (3, 4 and 5) | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0136 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN 3 " 15 " 31 ' 15 " | | Datum NAD83 3327400 mN hundredths hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 2 ft ft ² | 59 ft | 45.10 ft/sec | 8,500 ft ³ /min | 77 °F | 8,760 hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 82,000 lb/hr | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *Blower operating time. Emission rates vary depending upon manhole opening, sampling, and other activities. | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-13A | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) Annual (tons/yr) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|---|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 2.29 | 2.68 | 10.04 | 10.04 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 1.64 | 1.92 | 7.17 | 7.17 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.22 | 0.26 | 0.98 | 0.98 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|---|--|--|---|
| Emission Point ID No. (Designation) 1700-14B.3 | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer and Catalyst Tanks Manhole Vent | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. RLP0013 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN | | Datum NAD83 hundredths hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | NA °F | 8,760 hr/yr | Oct 1975 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 3,000 lb/batch | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *Common vent for EIQ Nos. 1700-14B.1, 1700-14B.3. ** 89 hr/yr. | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-14B.3 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | 1.5** | 9.10 | 0.067** | 0.10** | C | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.11 | 0.60 | 0.50 | 0.72 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.08 | 0.09 | 0.37 | 0.37 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.03 | 0.49 | 0.12 | 0.12 | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|--|---|--|-------------|
| Emission Point ID No. (Designation) 1700-14B | Descriptive Name of the Emissions Source (Alt. Name) Solution Make up Manhole Common Vent | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone 15 Latitude 30° Longitude -90° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN 3' 15" hundredths 31' 15" hundredths | | Datum NAD83 |
| Tempo Subject Item ID No. GRP0006 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 1.5 ft ft ² | 57 ft | 104.70 ft/sec | 11,100 ft ³ /min | 77 °F | 8,760 hr/yr | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 3,000 lb/batch | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-14B | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | 000 | 0% | | 1.47 | 9.10 | 0.07 | 0.00 | A | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.13 | 0.60 | 0.56 | 0.09 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | | 0.084 | 0.09 | 0.37 | 0 | A | | ppm by vol |
| Toluene | 000 | 0% | | 0.03 | 0.5 | 0.12 | 0 | A | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|---|--|--|--|---|---|--|---|-----------------------------------|-----------------------------------|---|
| Emission Point ID No. (Designation) 1700-14B.1 | | Descriptive Name of the Emissions Source (Alt. Name) Acetic Acid Make Up Tank | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT0137 | | | | | Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA ft ³ /min | Stack Gas Exit Temperature (°F) NA °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | |
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | | Operating Parameters (include units) | | | | | | | |
| | Type of Fuel | | Heat Input (MMBTU/hr) | | | | Parameter | Description | | | |
| | a NA | | NA | | | | Normal Operating Rate/Throughput | 3,000 lb/batch | | | |
| | b | | | | | | Maximum Operating Rate/Throughput | 134,173 gal | | | |
| | c | | | | | | Design Capacity/Volume/Cylinder Displacement | 1,590 gal | | | |
| Notes *This tank is vented to a common vent, EQI No. 1700-14B, Acetic Acid Tanks. | | | | Shell Height (ft) | | | 10.83 | | | | |
| | | | | Tank Diameter (ft) | | | NA | | | | |
| | | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof | | <input type="checkbox"/> Floating Roof | | <input type="checkbox"/> External | | <input type="checkbox"/> Internal | |
| | | | | Date Engine Ordered | | | | Engine Model Year | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn | | <input type="checkbox"/> Lean Burn | | <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |
| Emission Point ID No. (Designation) 1700-14B.1 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | 000 | 0% | | * | 2.79 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| Chloroprene | | 000 | 0% | | * | 0.09 | * | | A | | ppm by vol |
| Toluene | | 000 | 0% | | * | 0.50 | * | | A | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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|--|--|--|-------------------|-------------|------------------|------------|
| Emission Point ID No. (Designation) 1700-14B.2 | Descriptive Name of the Emissions Source (Alt. Name) Acetic Acid Hold Up Tank | Approximate Location of Stack or Vent (see instructions) | | | | |
| | | Method 06, "Address Matching-Primary Name" | | Datum NAD83 | | |
| Tempo Subject Item ID No. EQT0138 | | UTM Zone 15 | Horizontal 739000 | mE | Vertical 3327400 | mN |
| | | Latitude 30 ° | 3' | 15" | | hundredths |
| | | Longitude -90 ° | 31' | 15" | | hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | NA °F | 8,760 hr/yr | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|---|---|-----------------------|---|--|----------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | | Parameter | Description |
| a | NA | NA | | Normal Operating Rate/Throughput | 3,000 lb/batch |
| b | | | | Maximum Operating Rate/Throughput | 481,601 gal |
| c | | | | Design Capacity/Volume/Cylinder Displacement | 600 gal |
| Notes *This tank is vented to a common vent, EQI No. 1700-14B, Acetic Acid Tanks. | | | | Shell Height (ft) | 5.83 |
| | | | | Tank Diameter (ft) | 4.25 |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) 1700-14B.2 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 0.46 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | | * | 0.09 | * | | A | | ppm by vol |
| Toluene | 000 | 0% | | * | 0.50 | * | | A | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|---|--|---|
| Emission Point ID No. (Designation) 1700-20 | Descriptive Name of the Emissions Source (Alt. Name) CD Refining Column Jet | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0139 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3 15 " | | Datum NAD83 3327400 mN hundredths hundredths |

| | | | | | | | | | | | |
|--|--|---|--|--|--|---|--|--|----------------|----------------|----------------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.167 ft ft² | Height of Stack Above Grade (ft) 63.5 ft | Stack Gas Exit Velocity 3.50 ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) 5 ft³/min | Stack Gas Exit Temperature (°F) 65 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification 1970 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| | | | | | | |
|-------|---|-----------------------|---|--|-------------------|--|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a NA | NA | Normal Operating Rate/Throughput | | 17,000 lb/hr | |
| | b | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-20 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | 000 | 0% | | 0.75 | 0.83 | 3.30 | 3.30 | U | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 2.83 | 3.11 | 12.40 | 12.40 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 045 | 95% | 00126-99-8 | 2.83 | 3.11 | 12.4 | 12.4 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Ammonia | 000 | 0% | 07664-41-7 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |

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|--|--|---|--|--|---------------------------|
| Emission Point ID No. (Designation) 1700-20A | Descriptive Name of the Emissions Source (Alt. Name) CD Refining Column Jet (Spare) | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0140 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN | | Datum NAD83 3327400 mN |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 63.4 ft | 3.50 ft/sec | 5 ft ³ /min | 65 °F | Spare hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|-------|---|-----------------------|---|--|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description |
| a | NA | NA | Normal Operating Rate/Throughput | | 17,000 lb/hr |
| b | | | Maximum Operating Rate/Throughput | | NA |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA |
| Notes | | | Shell Height (ft) | | NA |
| | | | Tank Diameter (ft) | | NA |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) 1700-20A | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | | | | | | | | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | | | | | | | | | | ppm by vol |
| Toluene | | | | | | | | | | ppm by vol |
| Ammonia | | | | | | | | | | ppm by vol |

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|--|---|---|--|--|---|
| Emission Point ID No. (Designation) 1700-21A | Descriptive Name of the Emissions Source (Alt. Name) 2MM Pound CD Storage Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE 3' 15" 31' 15" | | Datum NAD83 3327400 mN hundredths hundredths |
| Tempo Subject Item ID No. EQT0141 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.25 ft ft ² | 48.2 ft | 0.38 ft/sec | 1 ft ³ /min | 23 °F | 8,760 hr/yr | Jan 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 93.6 MMlb/yr | |
| b | | | Maximum Operating Rate/Throughput | | 19,753,377 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 279,700 gal | |
| Notes | | | Shell Height (ft) | | 48 | |
| | | | Tank Diameter (ft) | | 31.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-21A | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 1.32 | 1.69 | 5.77 | 5.77 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 1.32 | 1.69 | 5.77 | 5.77 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-25A | Descriptive Name of the Emissions Source (Alt. Name) Product Drying CAP | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " _____ hundredths Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " _____ hundredths |
| Tempo Subject Item ID No. GRP0007 | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|---------|
| no | NA ft _____ ft ² | NA ft | NA ft/sec | NA ft ³ /min | NA °F | 8,760 hr/yr | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|--|--------------|-------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | | | Parameter | Description |
| a | NA | NA | Normal Operating Rate/Throughput | | 30,000 lb/hr | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered _____ Engine Model Year _____ | | | |
| | | | Date Engine Was Built by Manufacturer _____ | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-25A | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 15.6 | * | 68.20 | 69.17 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 13.0 | * | 56.8 | 57.55 | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 5.3 | * | 23.1 | 24.16 | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|---|---|--|---|
| Emission Point ID No. (Designation) 1700-25 | Descriptive Name of the Emissions Source (Alt. Name) East Wash Belt Dryer | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0142 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 14.1 ft ft ² | 31 ft | 18.20 ft/sec | 15,400 ft ³ /min | 104 °F | 8,760 hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 30,000 lb/hr | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes * Covered under EIQ NO. 1700-25A, Product Drying CAP | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-25 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 2.55 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 2.12 | * | * | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 0.86 | * | * | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|--|---|--|--|
| Emission Point ID No. (Designation) 1700-26 | Descriptive Name of the Emissions Source (Alt. Name) West Wash Belt Dryer | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0143 | | Method UTM Zone 15 Latitude 30° Longitude -90° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN 15 hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|---|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 14.1 ft ft² | 31 ft | 18.20 ft/sec | 15,400 ft³/min | 104 °F | 8,760 hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|---|-------------------|-------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a | NA | Normal Operating Rate/Throughput | 30,000 lb/hr | | |
| | b | | Maximum Operating Rate/Throughput | NA | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | NA | | |
| Notes | | | Shell Height (ft) | NA | | |
| *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | Tank Diameter (ft) | NA | | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | Engine Model Year | | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-26 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 2.55 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 2.12 | * | * | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 0.86 | * | * | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|---|--|-------------|
| Emission Point ID No. (Designation) 1700-27 | Descriptive Name of the Emissions Source (Alt. Name) East Hot Dryer Exhaust | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0144 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN 3 " hundredths 31 " hundredths | | Datum NAD83 |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 3 ft | 65.5 ft | 67.40 ft/sec | 28,600 ft ³ /min | 250 °F | 8,760 hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | |
|---|---|-----------------------|--|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description |
| a | NA | NA | Normal Operating Rate/Throughput | 30,000 lb/hr |
| b | | | Maximum Operating Rate/Throughput | NA |
| c | | | Design Capacity/Volume/Cylinder Displacement | NA |
| Notes *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | Shell Height (ft) | NA |
| | | | Tank Diameter (ft) | NA |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | |
| | | | Date Engine Ordered | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-27 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 13.03 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 10.86 | * | * | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 4.41 | * | * | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|--|--|---|
| Emission Point ID No. (Designation) 1700-28 | Descriptive Name of the Emissions Source (Alt. Name) West Hot Dryer Exhaust | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06,"Address Matching-Primary Name" Horizontal 739000 mE 3' 15" 31' 15" | | Datum NAD83 3327400 mN hundredths hundredths |
| Tempo Subject Item ID No. EQT0145 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 3 ft | 65.5 ft | 67.40 ft/sec | 28,600 ft ³ /min | 250 °F | 8,760 hr/yr | 1970 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | ft ² | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 30,000 lb/hr | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-28 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 13.03 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | 10.86 | * | * | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | 4.41 | * | * | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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Emission Point ID No.
 (Designation)
 1700-45

Descriptive Name of the Emissions Source (Alt. Name)

No. 1 East Dryer Cooling Compartment

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30° 3 ' 15 " hundredths
 Longitude -90° 31 ' 15 " hundredths

Tempo Subject Item ID No.
 EQT0146

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 2.67 ft ft ² | 49.6 ft | 61.60 ft/sec | 20,650 ft ³ /min | 122 °F | 8,760 hr/yr | 1970 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|--|--|--|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a | NA | Normal Operating Rate/Throughput | | 30,000 lb/hr | |
| | b | | Maximum Operating Rate/Throughput | | NA | |
| | c | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: | | <input type="checkbox"/> Fixed Roof | <input type="checkbox"/> Floating Roof |
| | | | | | <input type="checkbox"/> External | <input type="checkbox"/> Internal |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: | | <input type="checkbox"/> Rich Burn | <input type="checkbox"/> Lean Burn |
| | | | | | <input checked="" type="checkbox"/> 2 Stroke | <input type="checkbox"/> 4 Stroke |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-45 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | <0.01 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | <0.01 | * | * | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | <0.01 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|---|---|---|--|---|--|--|------------------------------|---|----|--|--|--|
| Emission Point ID No. (Designation) 1700-46 | Descriptive Name of the Emissions Source (Alt. Name) No. 1 West Dryer Cooling Compartment | | | | Approximate Location of Stack or Vent (see instructions) | | | | | | | | | |
| Tempo Subject Item ID No. EQT0147 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3</u> <u>15</u> " <u>hundredths</u> Longitude <u>-90°</u> <u>31</u> <u>15</u> " <u>hundredths</u> | | | | | | | | | |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 2.67 ft ft² | Height of Stack Above Grade (ft) 49.6 ft | Stack Gas Exit Velocity 61.60 ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) 20,650 ft³/min | Stack Gas Exit Temperature (°F) 122 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification 1970 | Percent of Annual Throughput Through This Emission Point | | | | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | | | | |
| | | | | | | | 25% | 25% | 25% | 25% | | | | |
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | | | |
| | Type of Fuel | | Heat Input (MMBTU/hr) | | Parameter | | | Description | | | | | | |
| | a NA | | NA | | Normal Operating Rate/Throughput | | | 30,000 lb/hr | | | | | | |
| | b | | | | Maximum Operating Rate/Throughput | | | NA | | | | | | |
| c | | | | | Design Capacity/Volume/Cylinder Displacement | | | NA | | | | | | |
| Notes | | | | | Shell Height (ft) | | | | | | NA | | | |
| *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | | | Tank Diameter (ft) | | | | | | NA | | | |
| | | | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | |
| | | | | | Date Engine Ordered | | | Engine Model Year | | | | | | |
| | | | | | Date Engine Was Built by Manufacturer | | | | | | | | | |
| | | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input checked="" type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-46 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ | | | | |
| Sulfur dioxide | | | | | | | | | | ppm by vol | | | | |
| Nitrogen oxides | | | | | | | | | | ppm by vol | | | | |
| Carbon monoxide | | | | | | | | | | ppm by vol | | | | |
| Total VOC (including those listed below) | 000 | 0% | | * | <0.01 | * | * | U | | ppm by vol | | | | |
| Lead | | | | | | | | | | ppm by vol | | | | |
| Chloroprene | 000 | 0% | 00126-99-8 | * | <0.01 | * | * | U | | ppm by vol | | | | |
| Toluene | 000 | 0% | 00108-88-3 | * | <0.01 | * | * | U | | ppm by vol | | | | |
| | | | | | | | | | | ppm by vol | | | | |

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| Emission Point ID No. (Designation) 1700-47 | | Descriptive Name of the Emissions Source (Alt. Name) No. 2 East Dryer Cooling Compartment | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> hundredths Longitude <u>-90°</u> <u>31'</u> <u>15"</u> hundredths | | | | |
| Tempo Subject Item ID No. EQT0148 | | | | | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 2.67 ft ft ² | 49.6 ft | 61.60 ft/sec | 20,650 ft ³ /min | 122 °F | 8,760 hr/yr | 1970 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Type of Fuel Used and Heat Input (see instructions) | | | Operating Parameters (include units) | | | |
|--|--------------|-----------------------|--|--|-------------------|--|
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 30,000 lb/hr | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input checked="" type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-47 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | <0.01 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | * | <0.01 | * | * | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | * | <0.01 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-48 | | Descriptive Name of the Emissions Source (Alt. Name) No. 2 West Dryer Cooling Compartment | | | Approximate Location of Stack or Vent (see instructions) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|---|---|--|---|--|--|---|--|--|------------------------------|---|---|--|--|---|--|--|--|--|--|--|--|-----------|-------------|----------------------------------|--------------|-----------------------------------|----|--|----|-------------------|----|--------------------|----|---|--|---------------------|-------------------|---------------------------------------|--|--|--|
| Tempo Subject Item ID No. EQT0149 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3</u> ' <u>15</u> " <u></u> hundredths Longitude <u>-90°</u> <u>31</u> ' <u>15</u> " <u></u> hundredths | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 2.67 ft ft² | Height of Stack Above Grade (ft) 49.6 ft | Stack Gas Exit Velocity 61.60 ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) 20,650 ft³/min | Stack Gas Exit Temperature (°F) 122 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification 1970 | Percent of Annual Throughput Through This Emission Point | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | 25% | 25% | 25% | 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:5%;">Fuel</th> <th style="width:35%;">Type of Fuel</th> <th style="width:60%;">Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:65%;">Parameter</th> <th style="width:35%;">Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>30,000 lb/hr</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>NA</td> </tr> <tr> <td>Shell Height (ft)</td> <td>NA</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>NA</td> </tr> <tr> <td colspan="2"> Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal </td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2"> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input checked="" type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke </td> </tr> </table> | | | | | Parameter | Description | Normal Operating Rate/Throughput | 30,000 lb/hr | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | NA | Shell Height (ft) | NA | Tank Diameter (ft) | NA | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input checked="" type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 30,000 lb/hr | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input checked="" type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes *Covered under EIQ NO. 1700-25A, Product Drying CAP | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-48 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Sulfur dioxide | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Nitrogen oxides | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Carbon monoxide | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Total VOC (including those listed below) | 000 | 0% | | * | <0.01 | * | * | U | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Lead | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Chloroprene | 000 | 0% | 00126-99-8 | * | <0.01 | * | * | U | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Toluene | 000 | 0% | 00108-88-3 | * | <0.01 | * | * | U | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

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| | | | | | |
|---|--|---|----------------------|---------------------|------------|
| Emission Point ID No. (Designation) 1700-50 | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tanks Vent | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. GRP0009 | | Method 06, "Address Matching-Primary Name" | Datum NAD83 | | |
| | | UTM Zone 15 | Horizontal 739000 mE | Vertical 3327400 mN | |
| | | Latitude 30 ° | 3 " | 15 " | hundredths |
| | | Longitude -90 ° | 31 ' | 15 " | hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 0.25 ft | 54 ft | 5.43 ft/sec | 16 ft ³ /min | 77 °F | * hr/yr | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | ft ² | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *61.12 hr/yr venting; Common vent for EIQ Nos. 1700-50.1, 50.2, 50.3, 50.4, 50.5, 50.6. | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-50 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 19.3 | * | 0.57 | 0.59 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 19.3 | * | 0.57 | 0.59 | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-50.1 | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tank No. 1 | Approximate Location of Stack or Vent (see instructions) | |
| Tempo Subject Item ID No. EQT0156 | | Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 65 °F | * hr/yr | Oct 1975 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 12,200 lb/batch | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 1,050 gal | |
| Notes *Covered under EIQ No. 1700-50, Stabilizer Tanks Vent. Maximum emission rate occurs only when tanks are filling. | | | Shell Height (ft) | | 5 | |
| | | | Tank Diameter (ft) | | 4 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-50.1 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 595.89 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 595.89 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-50.2 | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tank No. 2 | Approximate Location of Stack or Vent (see instructions) Method 06, "Address Matching-Primary Name" Datum NAD83 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN Latitude 30 ° 3 ' 15 " hundredths Longitude -90 ° 31 ' 15 " hundredths |
| Tempo Subject Item ID No. EQT0157 | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 65 °F | * hr/yr | Oct 1975 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | | |
|--|---|-----------------------|---|-----------------|-------------------|--|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | | |
| a | NA | NA | Normal Operating Rate/Throughput | 12,200 lb/batch | | | |
| b | | | Maximum Operating Rate/Throughput | NA | | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 1,050 gal | | | |
| | | | Shell Height (ft) | 5 | | | |
| | | | Tank Diameter (ft) | 4 | | | |
| Notes *Covered under EIQ No. 1700-50, Stabilizer Tanks Vent. Maximum emission rate occurs only when tanks are filling. | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | |
| | | | Date Engine Ordered | | Engine Model Year | | |
| | | | Date Engine Was Built by Manufacturer | | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | |
| | | | | | | | |

| Emission Point ID No. (Designation) 1700-50.2 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 595.89 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 595.89 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|---|--|--|---|---|--|--|-----------------------------------|------------------------------|---|--|--|--|
| Emission Point ID No. (Designation) 1700-50.3 | | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tank No. 3 | | | Approximate Location of Stack or Vent (see instructions) Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> hundredths Longitude <u>-90°</u> <u>31'</u> <u>15"</u> hundredths | | | | | | | | | |
| Tempo Subject Item ID No. EQT0158 | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 65 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Jul 1968 | Percent of Annual Throughput Through This Emission Point | | | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | Normal Operating Rate/Throughput | | | Parameter | | Description | | | | |
| | a NA | | NA | | Maximum Operating Rate/Throughput | | | 12,200 lb/batch | | | | | | |
| | b | | | | Design Capacity/Volume/Cylinder Displacement | | | NA | | | | | | |
| | c | | | | Shell Height (ft) | | | 1,050 gal | | | | | | |
| Notes *Covered under EIQ No. 1700-50, Stabilizer Tanks Vent. Maximum emission rate occurs only when tanks are filling. | | | | Tank Diameter (ft) | | | 5 | | | | | | | |
| | | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | |
| | | | | Date Engine Ordered | | | Engine Model Year | | | | | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-50.3 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | |
| Pollutant | Average (lb/hr) | | | | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ | | | |
| Sulfur dioxide | | | | | | | | | | | ppm by vol | | | |
| Nitrogen oxides | | | | | | | | | | | ppm by vol | | | |
| Carbon monoxide | | | | | | | | | | | ppm by vol | | | |
| Total VOC (including those listed below) | | 088 | 0% | | * | 595.89 | * | * | U | | ppm by vol | | | |
| Lead | | | | | | | | | | | ppm by vol | | | |
| Toluene | | 088 | 0% | 00108-88-3 | * | 595.89 | * | * | U | | ppm by vol | | | |
| | | | | | | | | | | | ppm by vol | | | |
| | | | | | | | | | | | ppm by vol | | | |

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| Emission Point ID No. (Designation) 1700-50.4 | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tank No. 4 | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0159 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical 3327400 mE 15 " 15 " |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft | NA ft | NA ft/sec | NA ft ³ /min | 65 °F | * hr/yr | Jul 1968 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | |
|---|---|-----------------------|--|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description |
| a | NA | NA | Normal Operating Rate/Throughput | 12,200 lb/batch |
| b | | | Maximum Operating Rate/Throughput | NA |
| c | | | Design Capacity/Volume/Cylinder Displacement | 2,330 gal |
| Notes *Covered under EIQ No. 1700-50, Stabilizer Tanks Vent. Maximum emission rate occurs only when tanks are filling. | | | Shell Height (ft) | 9.5 |
| | | | Tank Diameter (ft) | 4.5 |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | |
| | | | Date Engine Ordered | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-50.4 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 595.89 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 595.89 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|--|-------------------------------------|------------|-----------|----------|------------|
| Emission Point ID No. (Designation) 1700-50.5 | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tank No. 5 | Approximate Location of Stack or Vent (see instructions) | | | | | |
| | | Method | 06, "Address Matching-Primary Name" | | Datum | NAD83 | |
| Tempo Subject Item ID No. EQT0160 | | UTM Zone | 15 | Horizontal | 739000 mE | Vertical | 3327400 mN |
| | | Latitude | 30 ° | | 3' 15" | | hundredths |
| | | Longitude | -90 ° | | 31' 15" | | hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 65 °F | * hr/yr | Jul 2007 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|--|----------------|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | | Parameter | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | 5,000 lb/batch | | |
| b | | | Maximum Operating Rate/Throughput | NA | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 1,050 gal | | |
| Notes *Covered under EIQ No. 1700-50, Stabilizer Tanks Vent. Maximum emission rate occurs only when tanks are filling. | | | Shell Height (ft) | 5 | | |
| | | | Tank Diameter (ft) | 4 | | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-50.5 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 595.89 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 595.89 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-50.6 | | Descriptive Name of the Emissions Source (Alt. Name) Stabilizer Tank - LD750 | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|---|---|---|--|--|--|---|--|--|----------------|----------------|----------------|--|---|--|--|---|--|--|--|--|-----------|-------------|----------------------------------|----------------|-----------------------------------|----|--|---------|-------------------|---|--------------------|---|--|--|---------------------|-------------------|---------------------------------------|--|---|--|
| Tempo Subject Item ID No. EQT0161 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 65 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Jul 2007 | Percent of Annual Throughput Through This Emission Point | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:5%;">Fuel</th> <th style="width:25%;">Type of Fuel</th> <th style="width:25%;">Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:65%;">Parameter</th> <th style="width:35%;">Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>1,800 lb/batch</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>300 gal</td> </tr> <tr> <td>Shell Height (ft)</td> <td>5</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>3</td> </tr> <tr> <td colspan="2"> Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal </td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2"> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke </td> </tr> </table> | | | | | Parameter | Description | Normal Operating Rate/Throughput | 1,800 lb/batch | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | 300 gal | Shell Height (ft) | 5 | Tank Diameter (ft) | 3 | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 1,800 lb/batch | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | 300 gal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | 5 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes * Covered under EIQ No. 1700-50, Stabilizer Tanks Vent. Maximum emission rate occurs only when tanks are filling. | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

| | | | | | | | | | | |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-50.6 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 595.89 | * | * | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 595.89 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|---|--|--|
| Emission Point ID No. (Designation) 1700-51 | Descriptive Name of the Emissions Source (Alt. Name) Inhibitor Mix Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0162 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN Datum NAD83 | | |

| | | | | | | | | | | | |
|--|--|---|--|--|--|---|--|--|---------|---------|---------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.167 ft ft² | Height of Stack Above Grade (ft) 59 ft | Stack Gas Exit Velocity 1.06 ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) 1 ft³/min | Stack Gas Exit Temperature (°F) 37 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Jun 1968 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| | | | | | | |
|-----------------------|---|-----------------------|--|--|-------------------|-------------|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | Normal Operating Rate/Throughput | | Parameter | Description |
| | a NA | NA | 3,500 lbs/batch | | | |
| | b | | Maximum Operating Rate/Throughput | | NA | |
| | | | Design Capacity/Volume/Cylinder Displacement | | 660 gals | |
| | | | Shell Height (ft) | | 7 | |
| | | | Tank Diameter (ft) | | 4 | |
| Notes *1060 hrs/yr | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-51 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 2.0 | 2.0 | 1.06 | 1.17 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 2.0 | 2.0 | 1.06 | 1.17 | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | |
|---|---|---|
| Emission Point ID No. (Designation) 1700-53 | Descriptive Name of the Emissions Source (Alt. Name) Stripped Emulsion Tank No. 1 | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> hundredths Longitude <u>-90°</u> <u>31'</u> <u>15"</u> hundredths |
| Tempo Subject Item ID No. EQT0163 | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 38 ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Jun 1968 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 60,000 lbs/batch | |
| b | | | Maximum Operating Rate/Throughput | | 25,141,309 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 11,622 gal | |
| Notes | | | Shell Height (ft) | | 16.83 | |
| | | | Tank Diameter (ft) | | 11.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-53 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | | | | |
|---|--|--|--|--|--|
| Emission Point ID No. (Designation) 1700-54 | Descriptive Name of the Emissions Source (Alt. Name) Stripped Emulsion Tank No. 2 | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0164 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30° -90° | | Datum Horizontal Vertical 3327400 mE 15" 15" |

| | | | | | | | | | | | |
|--|--|---|--|--|--|---|--|--|---------|---------|---------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.167 ft ft² | Height of Stack Above Grade (ft) 38 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jun 1968 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| | | | | | |
|-------|---|-----------------------|---|--|--|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | | | |
| | a | NA | | | |
| | b | | | | |
| | c | | | | |
| Notes | | | Normal Operating Rate/Throughput Maximum Operating Rate/Throughput Design Capacity/Volume/Cylinder Displacement Shell Height (ft) Tank Diameter (ft) Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered Date Engine Was Built by Manufacturer SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| | | | | | | | | | | |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-54 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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Emission Point ID No.
 (Designation)
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Descriptive Name of the Emissions Source (Alt. Name)

Stripped Emulsion Tank No. 3

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30 ° 3 ' 15 " hundredths
 Longitude -90 ° 31 ' 15 " hundredths

Tempo Subject Item ID No.

EQT0165

Stack and Discharge
 Physical Characteristics
 Change? (yes or no)

no

Diameter (ft) or Stack
 Discharge Area (ft²)

0.167 ft
 ft²

Height of Stack
 Above Grade (ft)

38 ft

Stack Gas Exit
 Velocity

NA ft/sec

Stack Gas Flow at
 Conditions, not at
 Standard (ft³/min)

NA ft³/min

Stack Gas Exit
 Temperature
 (°F)

77 °F

Normal Operating
 Time
 (hours per year)

8,760 hr/yr

Date of
 Construction or
 Modification

Jun | 1968

Percent of Annual
 Throughput Through This
 Emission Point

| | | | |
|---------|---------|---------|---------|
| Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| 25% | 25% | 25% | 25% |

Fuel Type of Fuel Used and Heat Input (see instructions)

| | Type of Fuel | Heat Input (MMBTU/hr) |
|---|--------------|-----------------------|
| a | NA | NA |
| b | | |
| c | | |

Notes

Operating Parameters (include units)

| Parameter | Description |
|--|-------------------|
| Normal Operating Rate/Throughput | 60,000 lbs/batch |
| Maximum Operating Rate/Throughput | 25,141,309 gal |
| Design Capacity/Volume/Cylinder Displacement | 11,622 gal |
| Shell Height (ft) | 16.83 |
| Tank Diameter (ft) | 11.5 |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | |
| Date Engine Ordered | Engine Model Year |
| Date Engine Was Built by Manufacturer | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |

Emission Point ID No. (Designation)

1700-55

Control
 Equipment
 Code

Control
 Equipment
 Efficiency

HAP / TAP
 CAS Number

Proposed Emission Rates

Permitted
 Emission Rate
 (Current)

Add,
 Change,
 Delete, or
 Unchanged

Continuous
 Compliance
 Method

Concentration in Gases
 Exiting at Stack

| Pollutant | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
|--|--------------------|---------------------|---------------------|---------------------|-------|---|------------------------|
| Particulate matter (PM ₁₀) | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | <0.01 | <0.01 | <0.01 | U | ppm by vol |
| Lead | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | U | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | U | ppm by vol |
| | | | | | | | ppm by vol |

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| | | | | | |
|---|---|--|--|--|--|
| Emission Point ID No. (Designation) 1700-56 | Descriptive Name of the Emissions Source (Alt. Name) No. 6, 7, 8, 10, 13, and 14 Unstripped Storage Tanks Depressure Vent | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. RLP0016 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical 3327400 mE 15 " 15 " |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 55 ft | 719.00 ft/sec | 945 ft ³ /min | 77 °F | 2.92* hr/yr | Aug 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 42,000 lb/charge | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *2.92 hr/yr combined venting time | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-56 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 2178 | 2178 | 3.18 | 4.41 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 1484.7 | 1484.7 | 2.17 | 3.00 | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 232.2 | 232.2 | 0.34 | 0.47 | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|--|--|--|--|
| Emission Point ID No. (Designation) 1700-57 | Descriptive Name of the Emissions Source (Alt. Name) Diisobutylene (DIB) Storage Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0166 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum NAD83 3327400 mN Horizontal 739000 mE Vertical 15 " 31 " 15 " |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 10 ft | 0.09 ft/sec | 0 ft ³ /min | 82 °F | 8,760 hr/yr | Jun 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 144,180 lb/yr | |
| b | | | Maximum Operating Rate/Throughput | | 25,000 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 2,700 gal | |
| Notes | | | Shell Height (ft) | | 12 | |
| | | | Tank Diameter (ft) | | 8 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-57 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.02 | 0.02 | 0.11 | 0.11 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|---|--|--|--|---|---|--|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-60 | | Descriptive Name of the Emissions Source (Alt. Name) Diisobutylene Nitrosate (DIBN) Storage Tank No. 3 | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT0168 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> hundredths Longitude <u>-90°</u> <u>31'</u> <u>15"</u> hundredths | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.083 ft ft² | Height of Stack Above Grade (ft) 6 ft | Stack Gas Exit Velocity 0.34 ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) 0 ft³/min | Stack Gas Exit Temperature (°F) 82 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Sept 1977 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | |
| | | | | | | | 25% | 25% | 25% | 25% | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | Parameter | | | Description | | | |
| a | NA | | NA | | Normal Operating Rate/Throughput | | | 4,600 lb/batch | | | |
| b | | | | | Maximum Operating Rate/Throughput | | | 32,900 gal | | | |
| c | | | | | Design Capacity/Volume/Cylinder Displacement | | | 700 gal | | | |
| Notes | | | | Shell Height (ft) | | | 6 | | | | |
| | | | | Tank Diameter (ft) | | | 4.5 | | | | |
| | | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | |
| | | | | Date Engine Ordered | | | Engine Model Year | | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | |
| Emission Point ID No. (Designation) 1700-60 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | Average (lb/hr) | | | | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.01 | 0.01 | 0.06 | 0.06 | U | | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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Emission Point ID No.
 (Designation)
 1700-61

Descriptive Name of the Emissions Source (Alt. Name)

Diisobutylene Nitrosate (DIBN) Storage Tank No. 4

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30° 3' 15" hundredths
 Longitude -90° 31' 15" hundredths

Tempo Subject Item ID No.
 EQT0169

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 0.083 ft ft ² | 6 ft | 0.34 ft/sec | 0 ft ³ /min | 82 °F | 8,760 hr/yr | Sept 1977 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 4,600 lb/batch | |
| b | | | Maximum Operating Rate/Throughput | | 32,900 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 700 gal | |
| Notes | | | Shell Height (ft) | | 6 | |
| | | | Tank Diameter (ft) | | 4.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-61 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.01 | 0.01 | 0.06 | 0.06 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|--|---|--|-------------|
| Emission Point ID No. (Designation) 1700-62 | Descriptive Name of the Emissions Source (Alt. Name) Diisobutylene Nitrosate (DIBN) Storage Tank No. 5 | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0170 | | Method UTM Zone 15 Latitude 30° Longitude -90° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN 3' 15" hundredths 31' 15" hundredths | | Datum NAD83 |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft³/min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|---|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.083 ft ft² | 6 ft | 0.34 ft/sec | 0 ft³/min | 82 °F | 8,760 hr/yr | Sept 1977 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|----------------|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a | NA | Normal Operating Rate/Throughput | 4,600 lb/batch | | |
| | b | | Maximum Operating Rate/Throughput | 32,900 gal | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 700 gal | | |
| Notes | | | Shell Height (ft) | 6 | | |
| | | | Tank Diameter (ft) | 4.5 | | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-62 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.01 | 0.01 | 0.06 | 0.06 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|--|--|------------------------------------|
| Emission Point ID No. (Designation) 1700-63 | Descriptive Name of the Emissions Source (Alt. Name) Vent Header System | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. GRP0010 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE 3' 15" hundredths 31' 15" hundredths | | Datum NAD83 Vertical 3327400 mN |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.125 ft ft ² | 33.1 ft | 6.52 ft/sec | 5 ft ³ /min | 41 °F | 1,004* hr/yr | Sept 2001 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | NA | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-63 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 5.41 | * | 2.72 | 2.18 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 5.4 | * | 2.7 | 2.17 | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.01 | * | 0.01 | 0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-63.1 | Descriptive Name of the Emissions Source (Alt. Name) No. 1 CD Solution Tank | | | | Approximate Location of Stack or Vent (see instructions) Method 06, "Address Matching-Primary Name" Datum NAD83 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN Latitude 30 ° 3 ' 15 " hundredths Longitude -90 ° 31 ' 15 " hundredths | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|--|---|--|---|--|--|--|---|---|------------------|----|-------|---------|---|---|-------------------------------------|--|---|-----|-----|--|--|-----------|-------------|----------------------------------|------------------|-----------------------------------|----|--|-----------|-------------------|----|--------------------|-----|---|--|---------------------|-------------------|---------------------------------------|--|--|--|
| Tempo Subject Item ID No. EQT0171 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft _____ ft ² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 32 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Aug 1968 | Percent of Annual Throughput Through This Emission Point <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <td>Jan-Mar</td> <td>Apr-Jun</td> <td>Jul-Sep</td> <td>Oct-Dec</td> </tr> <tr> <td>25%</td> <td>25%</td> <td>25%</td> <td>25%</td> </tr> </table> | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | 25% | 25% | 25% | 25% | | | | | | | | | | | | | | | | | | | | | | |
| Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 25% | 25% | 25% | 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th>Fuel</th> <th>Type of Fuel</th> <th>Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th>Parameter</th> <th>Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>20,750 lb/charge</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>3,690 gal</td> </tr> <tr> <td>Shell Height (ft)</td> <td>13</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>7.5</td> </tr> <tr> <td colspan="2"> Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal </td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2"> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke </td> </tr> </table> | | | | | Parameter | Description | Normal Operating Rate/Throughput | 20,750 lb/charge | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | 3,690 gal | Shell Height (ft) | 13 | Tank Diameter (ft) | 7.5 | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 20,750 lb/charge | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | 3,690 gal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | 13 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | 7.5 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-63.1 | Control Equipment Code 088 | Control Equipment Efficiency 0% | HAP / TAP CAS Number 00126-99-8 00108-88-3 | Proposed Emission Rates <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th>Average (lb/hr)</th> <th>Maximum (lbs/hr)</th> <th>Annual (tons/yr)</th> </tr> <tr> <td>*</td> <td>98.30</td> <td>*</td> </tr> </table> | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | * | 98.30 | * | Permitted Emission Rate (Current) Annual (tons/yr) * | Add, Change, Delete, or Unchanged C | Continuous Compliance Method | Concentration in Gases Exiting at Stack gr/std ft ³ ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | |
| Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| * | 98.30 | * | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Pollutant Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) Lead Chloroprene Toluene | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

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Emission Point ID No.
 (Designation)
 1700-63.2

Descriptive Name of the Emissions Source (Alt. Name)

No. 2 CD Solution Tank

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30 ° 3 ' 15 " hundredths
 Longitude -90 ° 31 ' 15 " hundredths

Tempo Subject Item ID No.

EQT0175

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 32 °F | * hr/yr | Jul 1972 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|--|---|-----------------------|--|------------------|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | 20,750 lb/charge | |
| b | | | Maximum Operating Rate/Throughput | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 3,690 gal | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | Shell Height (ft) | 13 | |
| | | | Tank Diameter (ft) | 7.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-63.2 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | | | | |
|---|---|---|--|--|---|
| Emission Point ID No. (Designation) 1700-63.3 | Descriptive Name of the Emissions Source (Alt. Name) Recovered CD Storage Tank No. 1 | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical mE 739000 31' 15" |
| Tempo Subject Item ID No. EQT0176 | | Datum NAD83 3327400 mN hundredths hundredths | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 65 °F | * hr/yr | Jun 1968 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|--|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 40,000 lb/day | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 8,156 gal | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | Shell Height (ft) | | 15 | |
| | | | Tank Diameter (ft) | | 10 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-63.3 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|---|---|----------------------------|--|--|--|--|--|------------------------------------|--|-------------|
| Emission Point ID No. (Designation) 1700-63.4 | | Descriptive Name of the Emissions Source (Alt. Name) Recovered CD Storage Tank No. 2 | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT0177 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30</u> ° <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90</u> ° <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 65 °F | * hr/yr | Jun 1968 | Jan- Mar | Apr- Jun | Jul-Sep | Oct- Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | Normal Operating Rate/Throughput | | Parameter | | Description | | | |
| a | NA | NA | | 40,000 lb/day | | NA | | | | | |
| b | | | | Maximum Operating Rate/Throughput | | 8,156 gal | | | | | |
| c | | | | Design Capacity/Volume/Cylinder Displacement | | 15 | | | | | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | | Shell Height (ft) | | 10 | | | | | |
| | | | | Tank Diameter (ft) | | 15 | | | | | |
| | | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | |
| | | | | Date Engine Ordered | | Engine Model Year | | | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | |
| Emission Point ID No. (Designation) 1700-63.4 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ | |
| Sulfur dioxide | | | | | | | | | | ppm by vol | |
| Nitrogen oxides | | | | | | | | | | ppm by vol | |
| Carbon monoxide | | | | | | | | | | ppm by vol | |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol | |
| Lead | | | | | | | | | | ppm by vol | |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol | |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol | |
| | | | | | | | | | | ppm by vol | |

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| Emission Point ID No. (Designation) 1700-63.5 | | Descriptive Name of the Emissions Source (Alt. Name) CD Heels Tank | | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> " <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> " <u>15</u> " <u>hundredths</u> | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|---|--|---|--|---|--|--|---|--|-----------------------------------|------------------------------|---|--|---|--|--|--|--|--|--|-----------|-------------|----------------------------------|-----------|-----------------------------------|----|--|-----------|-------------------|----|--------------------|----|--|--|---------------------|-------------------|---------------------------------------|--|---|--|
| Tempo Subject Item ID No. EQT0178 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft ft ² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 75 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Sept 1990 | Percent of Annual Throughput Through This Emission Point | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:5%;">Fuel</th> <th style="width:20%;">Type of Fuel</th> <th style="width:20%;">Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:60%;">Parameter</th> <th style="width:40%;">Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>650 lb/hr</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>8,315 gal</td> </tr> <tr> <td>Shell Height (ft)</td> <td>14</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>10</td> </tr> <tr> <td colspan="2">Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal</td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2">SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke</td> </tr> </table> | | | | Parameter | Description | Normal Operating Rate/Throughput | 650 lb/hr | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | 8,315 gal | Shell Height (ft) | 14 | Tank Diameter (ft) | 10 | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 650 lb/hr | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | 8,315 gal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | 14 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | 10 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-63.5 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Pollutant | Average (lb/hr) | | | | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft ³ | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Sulfur dioxide | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Nitrogen oxides | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Carbon monoxide | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Lead | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

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|---|---|---|---|--|---|---|--|---|------------------------------------|--|---|----------------|---|----------------|----------------|--|--|--|--|--|-----------|-------------|----------------------------------|-------------|-----------------------------------|----|--|------------|-------------------|----|--------------------|----|--|--|---------------------|-------------------|---------------------------------------|--|---|--|
| Emission Point ID No. (Designation) 1700-63.8 | | Descriptive Name of the Emissions Source (Alt. Name) Crude CD Storage Tank No. 3 | | | Approximate Location of Stack or Vent (see instructions) Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tempo Subject Item ID No. EQT0181 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft ft ² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 59 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Mar 1971 | Percent of Annual Throughput Through This Emission Point <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <td>Jan-Mar 25%</td> <td>Apr-Jun 25%</td> <td>Jul-Sep 25%</td> <td>Oct-Dec 25%</td> </tr> </table> | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | | | | | | | | | | | | | | | | | | | | | | |
| Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Fuel <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th colspan="2">Type of Fuel Used and Heat Input (see instructions)</th> </tr> <tr> <th>Type of Fuel</th> <th>Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> </tr> <tr> <td>c</td> <td></td> </tr> </table> | | | Type of Fuel Used and Heat Input (see instructions) | | Type of Fuel | Heat Input (MMBTU/hr) | a NA | NA | b | | c | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th>Parameter</th> <th>Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>36 MM lb/yr</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>25,750 gal</td> </tr> <tr> <td>Shell Height (ft)</td> <td>27</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>13</td> </tr> <tr> <td colspan="2">Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal</td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2">SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke</td> </tr> </table> | | | | | | | | Parameter | Description | Normal Operating Rate/Throughput | 36 MM lb/yr | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | 25,750 gal | Shell Height (ft) | 27 | Tank Diameter (ft) | 13 | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Type of Fuel Used and Heat Input (see instructions) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 36 MM lb/yr | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | 25,750 gal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | 27 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | 13 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-63.8 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Sulfur dioxide | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Nitrogen oxides | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Carbon monoxide | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Lead | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

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| | | | | | |
|---|---|--|--|--|--|
| Emission Point ID No. (Designation) 1700-63.9 | Descriptive Name of the Emissions Source (Alt. Name) Refined CD Storage Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | |
| Tempo Subject Item ID No. EQT0182 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | NA °F | * hr/yr | Mar 1971 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|--|---|-----------------------|--|-------------|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | | | |
| a | NA | NA | Normal Operating Rate/Throughput | 77 MM lb/yr | |
| b | | | Maximum Operating Rate/Throughput | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 50,000 gal | |
| Notes *Consolidated under EIQ No. 1700-63, Vent Header System | | | Shell Height (ft) | 24 | |
| | | | Tank Diameter (ft) | 16 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) 1700-63.9 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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Emission Point ID No.
 (Designation)
 1700-63.10

Descriptive Name of the Emissions Source (Alt. Name)

Inhibitor Final Make-up Tank

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30 ° 3 ' 15 " hundredths
 Longitude -90 ° 31 ' 15 " hundredths

Tempo Subject Item ID No.

EQT0172

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 34 °F | * hr/yr | Jun 1968 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 12,000 lb/batch | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 22,164 gal | |
| Notes | | | Shell Height (ft) | | 27 | |
| *Consolidated under EIQ No. 1700-63, Vent Header System | | | Tank Diameter (ft) | | 12 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-63.10 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|--|---|--|--|--|
| Emission Point ID No. (Designation) 1700-63.11 | Descriptive Name of the Emissions Source (Alt. Name) Inhibitor Hold-up Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE 3 15 " hundredths 31 15 " hundredths | | Datum NAD83 Vertical 3327400 mN hundredths |
| Tempo Subject Item ID No. EQT0173 | | | | | |

| | | | | | | | | | | | |
|--|---|---|--|---|--|---|--|--|---------|---------|---------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 34 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Jun 1968 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| | | | | | | |
|---|---|-----------------------|--|--|-------------------|--|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a NA | NA | Normal Operating Rate/Throughput | | 12,000 lb/batch | |
| | b | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 22,164 gal | |
| Notes | | | Shell Height (ft) | | 27 | |
| *Consolidated under EIQ No. 1700-63, Vent Header System | | | Tank Diameter (ft) | | 12 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-63.11 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | * | 98.30 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | * | 98.47 | * | * | C | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | * | 0.19 | * | * | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|---|--|---|
| Emission Point ID No. (Designation) 1700-64 | Descriptive Name of the Emissions Source (Alt. Name) Water Solution Exhaust Fan | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0183 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN hundredths hundredths |

| | | | | | | | | | | | |
|--|---|---|---|--|--|---|--|--|----------------|----------------|----------------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 1.33 ft ft² | Height of Stack Above Grade (ft) 53.6 ft | Stack Gas Exit Velocity 29.80 ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) 2,500 ft³/min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8760* hr/yr | Date of Construction or Modification 1972 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| | | | | | | |
|----------------------------------|---|-----------------------|---|-----------|-----------|-------------|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | Normal Operating Rate/Throughput | | Parameter | Description |
| | a | NA | NA | 2,500 cfm | | |
| | b | | | NA | | |
| | c | | | NA | | |
| Notes *Blower operating time. | | | Design Capacity/Volume/Cylinder Displacement Shell Height (ft) Tank Diameter (ft) Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered Date Engine Was Built by Manufacturer SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-64 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | 0.01 | 1.56 | 0.05 | 0.04 | C | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.025 | 0.13 | 0.11 | 0.11 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.02 | 0.02 | 0.08 | 0.08 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | <0.01 | 0.11 | 0.03 | 0.03 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|--|--|--|--|--|--|--|
| Emission Point ID No. (Designation) 1700-66 | | Descriptive Name of the Emissions Source (Alt. Name) Poly Building Wall Fans | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30</u> ° <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90</u> ° <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | |
| Tempo Subject Item ID No. EQT0185 | | | | | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | 476,365 ft ³ /min | 77 °F | 8,760 hr/yr | 1968 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | | |
|-------|---|-----------------------|---|--|-------------|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | | |
| a | NA | NA | Normal Operating Rate/Throughput | | 476,365 CFM | | |
| b | | | Maximum Operating Rate/Throughput | | NA | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | | |
| Notes | | | Shell Height (ft) | | NA | | |
| | | | Tank Diameter (ft) | | NA | | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | |
| | | | Date Engine Ordered | | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | |

| Emission Point ID No. (Designation) 1700-66 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 6.38 | 53.74 | 27.94 | 27.94 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 3.61 | 4.34 | 15.83 | 15.83 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 1.19 | 21.19 | 5.19 | 5.19 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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Emission Point ID No.
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 1700-67

Descriptive Name of the Emissions Source (Alt. Name)

Stripped Emulsion Tank No. 4

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30° 3' 15" hundredths
 Longitude -90° 31' 15" hundredths

Tempo Subject Item ID No.
 EQT0186

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 0.167 ft ft ² | 38 ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Jun 1968 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|--------------|--|--|-------|-------------------|
| | | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description |
| | a | NA | NA | Normal Operating Rate/Throughput | | 60,000 lbs/batch |
| | b | f | | Maximum Operating Rate/Throughput | | 25,141,309 gal |
| | c | | | Design Capacity/Volume/Cylinder Displacement | | 11,622 gal |
| Notes | | | Shell Height (ft) | | 16.83 | |
| | | | Tank Diameter (ft) | | 11.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-67 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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Emission Point ID No.
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 1700-68

Descriptive Name of the Emissions Source (Alt. Name)

Stripped Emulsion Tank No. 5

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30° 3' 15" hundredths
 Longitude -90° 31' 15" hundredths

Tempo Subject Item ID No.

EQT0187

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 0.167 ft ft ² | 38 ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Jul 1968 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|-------|---|-----------------------|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | 60,000 lbs/batch | |
| b | | | Maximum Operating Rate/Throughput | 25,141,309 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 11,622 gal | |
| Notes | | | Shell Height (ft) | 16.83 | |
| | | | Tank Diameter (ft) | 11.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-68 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | | | | | | | | |
|---|--|--|--|--|--|--|--|--|--|
| Emission Point ID No. (Designation) 1700-69 | | Descriptive Name of the Emissions Source (Alt. Name) Stripped Emulsion Tank No. 9 | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | |
| Tempo Subject Item ID No. EQT0188 | | | | | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 38 ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Jul 2007 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 60,000 lbs/batch | |
| b | | | Maximum Operating Rate/Throughput | | 25,141,309 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 16,000 gal | |
| Notes | | | Shell Height (ft) | | 20.75 | |
| | | | Tank Diameter (ft) | | 12 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-69 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | | | | | | | | | | | |
|--|--|---|--|--|---|---|--|--|-----------------------------------|------------------------------|---|--|
| Emission Point ID No. (Designation) 1700-70 | | Descriptive Name of the Emissions Source (Alt. Name) Stripped Emulsion Tank No. 11 | | | Approximate Location of Stack or Vent (see instructions) Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> <u>hundredths</u> Longitude <u>-90°</u> <u>31'</u> <u>15"</u> <u>hundredths</u> | | | | | | | |
| Tempo Subject Item ID No. EQT0189 | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.167 ft ft² | Height of Stack Above Grade (ft) 38 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jul 2007 | Percent of Annual Throughput Through This Emission Point | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | | | | | | | | |
| | a NA | | NA | | Normal Operating Rate/Throughput 60,000 lbs/batch | | | | | | | |
| | b | | | | Maximum Operating Rate/Throughput 25,141,309 gal | | | | | | | |
| | c | | | | Design Capacity/Volume/Cylinder Displacement 16,000 gal | | | | | | | |
| Notes | | | | Shell Height (ft) 20.75 | | | | | | | | |
| | | | | Tank Diameter (ft) 12 | | | | | | | | |
| | | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | |
| | | | | Date Engine Ordered | | | | Engine Model Year | | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | |
| Emission Point ID No. (Designation) 1700-70 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | |
| Pollutant | Average (lb/hr) | | | | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ | |
| Sulfur dioxide | | | | | | | | | | | ppm by vol | |
| Nitrogen oxides | | | | | | | | | | | ppm by vol | |
| Carbon monoxide | | | | | | | | | | | ppm by vol | |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | | ppm by vol | |
| Lead | | | | | | | | | | | ppm by vol | |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | | ppm by vol | |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | | ppm by vol | |
| | | | | | | | | | | | ppm by vol | |

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| Emission Point ID No. (Designation) 1700-71 | Descriptive Name of the Emissions Source (Alt. Name) Stripped Emulsion Tank No. 12 | Approximate Location of Stack or Vent (see instructions) Method 06, "Address Matching-Primary Name" Datum NAD83 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN Latitude 30° 3' 15" hundredths Longitude -90° 31' 15" hundredths |
| Tempo Subject Item ID No. EQT0190 | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 38 ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Jul 2007 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|-------|---|-----------------------|--|--|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description |
| a | NA | NA | Normal Operating Rate/Throughput | | 60,000 lbs/batch |
| b | | | Maximum Operating Rate/Throughput | | 17,287,069 gal |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 16,000 gal |
| Notes | | | Shell Height (ft) | | 20.75 |
| | | | Tank Diameter (ft) | | 12 |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) 1700-71 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|-------------|
| Emission Point ID No. (Designation) 1700-72 | Descriptive Name of the Emissions Source (Alt. Name) Stripped Emulsion Tank No. 15 | Approximate Location of Stack or Vent (see instructions) | |
| Tempo Subject Item ID No. EQT0191 | | Method 06, "Address Matching-Primary Name" | Datum NAD83 |
| | | UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN | |
| | | Latitude 30 ° 3 ' 15 " | hundredths |
| | | Longitude -90 ° 31 ' 15 " | hundredths |

| | | | | | | | | | | | |
|---|--|--|---|--|---|--|---|---|---------|---------|---------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.167 ft ft ² | Height of Stack Above Grade (ft) 38 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jul 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| | | | | | | |
|--------------|--|------------------------------|---|--|------------------|--------------------|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | | | Parameter | Description |
| | a NA | NA | Normal Operating Rate/Throughput | | 60,000 lbs/batch | |
| | b | | Maximum Operating Rate/Throughput | | 17,287,069 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 10,000 gal | |
| Notes | | | Shell Height (ft) | | 20.75 | |
| | | | Tank Diameter (ft) | | 12 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered _____ Engine Model Year _____ Date Engine Was Built by Manufacturer _____ SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|---|-------------------------------|-------------------------------------|-----------------------------|--------------------------------|-------------------------|-------------------------|--|--|-------------------------------------|--|
| Emission Point ID No. (Designation) 1700-72 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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Emission Point ID No.
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 1700-73

Descriptive Name of the Emissions Source (Alt. Name)

Stripped Emulsion Tank No. 16

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30° 3' 15" hundredths
 Longitude -90° 31' 15" hundredths

Tempo Subject Item ID No.
 EQT0192

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | 0.167 ft ft ² | 38 ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Jul 2007 | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 60,000 lbs/batch | |
| b | | | Maximum Operating Rate/Throughput | | 17,287,069 gal | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 10,000 gal | |
| Notes | | | Shell Height (ft) | | 20.75 | |
| | | | Tank Diameter (ft) | | 12 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-73 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 088 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 088 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 088 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|--|--|--|---|
| Emission Point ID No. (Designation) 1700-74 | Descriptive Name of the Emissions Source (Alt. Name) Finishing Stabilizer Make-up Bag Filter | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical 739000 mE 31 15 " |
| Tempo Subject Item ID No. EQT0193 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.67 ft ft ² | 25 ft | 30.00 ft/sec | 1,200 ft ³ /min | 77 °F | * hr/yr | Jul 2007 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|---------------------|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 3,000 cfm | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes *214 hr/yr | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-74 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | 018 | 99% | | 0.023 | 0.023 | 0.001 | 0.01 | C | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | | | | | | | | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | | | | | | | | | | ppm by vol |
| Toluene | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|---|--|---|
| Emission Point ID No. (Designation) 1700-75 | Descriptive Name of the Emissions Source (Alt. Name) Resin 90 Railcar | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0194 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN 15" hundredths |

| | | | | | | | | | | | |
|--|---|--|--|--|---|---|--|--|----------------|----------------|----------------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.25 ft ft² | Height of Stack Above Grade (ft) 4 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 356 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jul 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| | | | | | | |
|------|---|-----------------------|---|--|-------------|--|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| | a | NA | NA | | | |
| | b | | | | | |
| | Notes | | Normal Operating Rate/Throughput 260,000 gal/yr Maximum Operating Rate/Throughput NA Design Capacity/Volume/Cylinder Displacement 20,000 gal Railcar Shell Height (ft) NA Tank Diameter (ft) NA Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered _____ Engine Model Year _____ Date Engine Was Built by Manufacturer _____ SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-75 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | <0.01 | 0.23 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|--|---|--|---|
| Emission Point ID No. (Designation) 1700-76 | Descriptive Name of the Emissions Source (Alt. Name) Rosin S Railcar | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone 15 Latitude 30° Longitude -90° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN hundredths |
| Tempo Subject Item ID No. EQT0195 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.25 ft ft ² | 4 ft | NA ft/sec | NA ft ³ /min | 356 °F | 8,760 hr/yr | Jul 2007 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|----------------|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description | | |
| a | NA | NA | Normal Operating Rate/Throughput | 260,000 gal/yr | | |
| b | | | Maximum Operating Rate/Throughput | NA | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 20,000 gal | Railcar | |
| Notes | | | Shell Height (ft) | NA | | |
| | | | Tank Diameter (ft) | NA | | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-76 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | <0.01 | 0.23 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|--|--|--|--|
| Emission Point ID No. (Designation) 1700-77 | Descriptive Name of the Emissions Source (Alt. Name) Octopol Storage Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30° -90° | | Datum Horizontal Vertical 739000 mE 3 15" 31" 15" |
| Tempo Subject Item ID No. EQT0196 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|---|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.25 ft ft² | 4 ft | NA ft/sec | NA ft³/min | 77 °F | 8,760 hr/yr | Jul 2007 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|--|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 80,000 gal/yr | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | 12,500 gal | |
| Notes | | | Shell Height (ft) | | 17 | |
| | | | Tank Diameter (ft) | | 11.5 | |
| | | | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-77 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | <0.01 | 0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|---|---|---|---|---|---|--|--|--|------------------------------------|--|
| Emission Point ID No. (Designation) 1700-79 | | Descriptive Name of the Emissions Source (Alt. Name) Emergency Stabilizer Drumming | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT0198 | | | | | Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> <u>hundredths</u> Longitude <u>-90°</u> <u>31'</u> <u>15"</u> <u>hundredths</u> | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft ft ² | Height of Stack Above Grade (ft) 4 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Jul 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | |
| | | | | | | | 25% | 25% | 25% | 25% | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | |
| a | NA | NA | | | | | | | | | |
| b | | | | | | | | | | | |
| c | | | | | | | | | | | |
| Notes * 20 DRUMS (1,000 gallons) per year | | | | Normal Operating Rate/Throughput 1,000 gal/yr Maximum Operating Rate/Throughput NA Design Capacity/Volume/Cylinder Displacement NA Shell Height (ft) NA Tank Diameter (ft) NA Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered Date Engine Was Built by Manufacturer SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | |
| Emission Point ID No. (Designation) 1700-79 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | 000 | 0% | | 0.35 | 0.35 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| Toluene | | 000 | 0% | 00108-88-3 | 0.35 | 0.35 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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|--|---|---|--|---|--|---|--|--|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-80 | | Descriptive Name of the Emissions Source (Alt. Name) ACR Storage Vent Header | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. RLP0017 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> " <u>15</u> " Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.17 ft² | Height of Stack Above Grade (ft) 50 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 23 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jul 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | |
| | | | | | | | 25% | 25% | 25% | 25% | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | | | | | | | |
| a | NA | | NA | | Normal Operating Rate/Throughput | | | | | | |
| b | | | | | Maximum Operating Rate/Throughput | | | | | | |
| c | | | | | Design Capacity/Volume/Cylinder Displacement | | | | | | |
| Notes VOC emission rate includes 2.4 lbs/yr of 1,2 dichlorobenzene | | | | Shell Height (ft) | | | | | | | |
| | | | | Tank Diameter (ft) | | | | | | | |
| | | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | |
| | | | | Date Engine Ordered | | | | | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | |
| Emission Point ID No. (Designation) 1700-80 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | 000 | 0% | | 0.02 | 0.09 | 0.09 | 0.07 | C | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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|--|---|--|--|---|--|---|--|--|-----------------------------------|------------------------------|---|--|
| Emission Point ID No. (Designation) 1700-80.1 | | Descriptive Name of the Emissions Source (Alt. Name) Refined ACR Storage Tank | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u> </u> hundredths Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u> </u> hundredths | | | | | | | |
| Tempo Subject Item ID No. EQT0199 | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NS ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 23 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Mar 1971 | Percent of Annual Throughput Through This Emission Point | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | Normal Operating Rate/Throughput | | | Parameter | | Description | | |
| | a | NA | NA | | Maximum Operating Rate/Throughput | | | NA | | | | |
| | b | | | | Design Capacity/Volume/Cylinder Displacement | | | 50,000 gal | | | | |
| | c | | | | Shell Height (ft) | | | 34 | | | | |
| Notes Emissions from this source are routed to emission point 1700-80 | | | | Tank Diameter (ft) 16 Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered <input type="checkbox"/> Engine Model Year <input type="checkbox"/> Date Engine Was Built by Manufacturer <input type="checkbox"/> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | |
| Emission Point ID No. (Designation) 1700-80.1 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | |
| Pollutant | Average (lb/hr) | | | | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ | |
| Sulfur dioxide | | | | | | | | | | | ppm by vol | |
| Nitrogen oxides | | | | | | | | | | | ppm by vol | |
| Carbon monoxide | | | | | | | | | | | ppm by vol | |
| Total VOC (including those listed below) | 000 | 0% | | * | 0.03 | * | * | C | | | ppm by vol | |
| Lead | | | | | | | | | | | ppm by vol | |
| | | | | | | | | | | | ppm by vol | |
| | | | | | | | | | | | ppm by vol | |
| | | | | | | | | | | | ppm by vol | |

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| Emission Point ID No. (Designation) 1700-80.2 | Descriptive Name of the Emissions Source (Alt. Name) Chlorinated ACR Storage Tank | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> hundredths Longitude <u>-90°</u> <u>31'</u> <u>15"</u> hundredths | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|--|---|---|---|--|---|--|---|---|---|--|--|---------|---------|---------|---|-----|-----|-----|-----|--|-----------|-------------|----------------------------------|------------|-----------------------------------|----|--|------------|-------------------|----|--------------------|----|---|--|---------------------|-------------------|---------------------------------------|--|--|--|
| Tempo Subject Item ID No. EQT0200 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft ² | Height of Stack Above Grade (ft) NS ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 23 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Jun 1968 | Percent of Annual Throughput Through This Emission Point <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <td>Jan-Mar</td> <td>Apr-Jun</td> <td>Jul-Sep</td> <td>Oct-Dec</td> </tr> <tr> <td>25%</td> <td>25%</td> <td>25%</td> <td>25%</td> </tr> </table> | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | 25% | 25% | 25% | 25% | | | | | | | | | | | | | | | | | | | | | |
| Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 25% | 25% | 25% | 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:5%;">Fuel</th> <th style="width:20%;">Type of Fuel</th> <th style="width:20%;">Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:65%;">Parameter</th> <th style="width:35%;">Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>3 MM lb/yr</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>22,164 gal</td> </tr> <tr> <td>Shell Height (ft)</td> <td>27</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>12</td> </tr> <tr> <td colspan="2"> Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal </td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2"> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke </td> </tr> </table> | | | | | | Parameter | Description | Normal Operating Rate/Throughput | 3 MM lb/yr | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | 22,164 gal | Shell Height (ft) | 27 | Tank Diameter (ft) | 12 | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 3 MM lb/yr | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | 22,164 gal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | 27 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | 12 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes Emissions from this source are routed to emission point 1700-80 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1700-80.2 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | * | 0.04 | * | * | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-81 | | Descriptive Name of the Emissions Source (Alt. Name) ACR Refining Vent | | | Approximate Location of Stack or Vent (see instructions) | | | | | | | | | | | | | | | | | | | | | | | | | | |
|---|---|---|--|--|--|---|--|-----------------------------------|--|------------------------------|---|-----------|-------------|----------------------------------|-------------|-----------------------------------|----|--|----|-------------------|----|--------------------|----|---|--|---------------------|-------------------|---------------------------------------|--|---|--|
| Tempo Subject Item ID No. RLP0018 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u></u> hundredths Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u></u> hundredths | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.33 ft ft² | Height of Stack Above Grade (ft) 70.2 ft | Stack Gas Exit Velocity 0.13 ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) 1 ft³/min | Stack Gas Exit Temperature (°F) 82 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Jul 2007 | | Percent of Annual Throughput Through This Emission Point | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Fuel | Type of Fuel | | | Heat Input (MMBTU/hr) | | | <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th style="width:65%;">Parameter</th> <th style="width:35%;">Description</th> </tr> </thead> <tbody> <tr><td>Normal Operating Rate/Throughput</td><td>1,123 lb/hr</td></tr> <tr><td>Maximum Operating Rate/Throughput</td><td>NA</td></tr> <tr><td>Design Capacity/Volume/Cylinder Displacement</td><td>NA</td></tr> <tr><td>Shell Height (ft)</td><td>NA</td></tr> <tr><td>Tank Diameter (ft)</td><td>NA</td></tr> <tr><td colspan="2">Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal</td></tr> <tr><td>Date Engine Ordered</td><td>Engine Model Year</td></tr> <tr><td colspan="2">Date Engine Was Built by Manufacturer</td></tr> <tr><td colspan="2">SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke</td></tr> </tbody> </table> | | | | | Parameter | Description | Normal Operating Rate/Throughput | 1,123 lb/hr | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | NA | Shell Height (ft) | NA | Tank Diameter (ft) | NA | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 1,123 lb/hr | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | | | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-81 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | | | | | | | | | | | | | | | | | |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | | | | | | | | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ | | | | | | | | | | | | | | | | | | | | |
| Sulfur dioxide | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| Nitrogen oxides | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| Carbon monoxide | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| Total VOC (including those listed below) | | 000 | 0% | | 1.00 | 10.00 | 2.20 | 2.20 | U | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| Lead | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| Hydrochloric acid | | 000 | 0% | | 0.3 | 4.5 | 0.7 | 0.7 | U | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | |

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| Emission Point ID No. (Designation) 1700-82 | | Descriptive Name of the Emissions Source (Alt. Name) ACR Solvent Blend Tank | | | Approximate Location of Stack or Vent (see instructions) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|---|---|--|--|--|--|---|---|--|------------------------------|---|--|--|---|--|--|--|--|--|--|--|--|-----------|-------------|----------------------------------|----------------|-----------------------------------|----|--|----------|-------------------|---|--------------------|---|--|--|---------------------|-------------------|---------------------------------------|--|---|--|
| Tempo Subject Item ID No. EQT0201 | | | | | Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u></u> hundredths Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u></u> hundredths | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) 0.167 ft ft ² | Height of Stack Above Grade (ft) 30 ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 25 °F | Normal Operating Time (hours per year) * hr/yr | Date of Construction or Modification Sept 2007 | Percent of Annual Throughput Through This Emission Point | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | 25% | 25% | 25% | 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:5%;">Fuel</th> <th style="width:25%;">Type of Fuel</th> <th style="width:25%;">Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:65%;">Parameter</th> <th style="width:35%;">Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>2,000 drums/yr</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>960 gals</td> </tr> <tr> <td>Shell Height (ft)</td> <td>9</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>4</td> </tr> <tr> <td colspan="2"> Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal </td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2"> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke </td> </tr> </table> | | | | | | Parameter | Description | Normal Operating Rate/Throughput | 2,000 drums/yr | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | 960 gals | Shell Height (ft) | 9 | Tank Diameter (ft) | 4 | Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 2,000 drums/yr | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | 960 gals | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | 9 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | 4 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input checked="" type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes *Hours of venting vary per solvent used. | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-82 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Sulfur dioxide | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Nitrogen oxides | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Carbon monoxide | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Total VOC (including those listed below) | 000 | 0% | | 0.13 | 0.14 | 0.01 | 0.037 | C | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Lead | | | | | | | | | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tetrachloroethylene | 000 | 0% | 00127-18-4 | 0.40 | 0.56 | 0.01 | 0.01 | C | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Xylene (mixed isomers) | 000 | 0% | 01330-20-7 | 0.10 | 0.14 | 0.001 | 0.001 | C | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Dichloromethane | 000 | 0% | 00075-09-2 | 7.05 | 9.90 | 0.02 | 0.02 | C | | ppm by vol | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

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| | | | | | |
|--|--|--|--|--|---|
| Emission Point ID No. (Designation) 3-95 | Descriptive Name of the Emissions Source (Alt. Name) Diversion Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical NAD83 739000 mE 3327400 mN 15 " 15 " |
| Tempo Subject Item ID No. EQT0202 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Sept 1995 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|---------------|-------------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description | | |
| a | NA | NA | Normal Operating Rate/Throughput | 27,000 gal/hr | | |
| b | | | Maximum Operating Rate/Throughput | NA | | |
| c | | | Design Capacity/Volume/Cylinder Displacement | 660,222 gal | Open tank WWT treatment | |
| Notes | | | Shell Height (ft) | NA | | |
| | | | Tank Diameter (ft) | NA | | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 3-95 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | <0.01 | <0.01 | <0.01 | 0.21 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | 0.19 | C | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | 0.01 | C | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | | | | |
|--|--|--|---|--|---|
| Emission Point ID No. (Designation) 4-95 | Descriptive Name of the Emissions Source (Alt. Name) Surge Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0203 | | Method UTM Zone 15 Latitude 30° Longitude -90° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31' 15" | | Datum NAD83 3327400 mN hundredths hundredths |

| | | | | | | | | | | | |
|--|---|---|--|---|--|---|---|--|----------------|----------------|----------------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Sept 1995 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| | | | | | |
|-------|---|-----------------------|--|--|--|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | | | |
| | a NA | NA | | | |
| | b | | | | |
| c | | | | | |
| Notes | | | Normal Operating Rate/Throughput 27,000 gal/hr Maximum Operating Rate/Throughput NA Design Capacity/Volume/Cylinder Displacement 660,000 gal Open tank WWT treatment Shell Height (ft) NA Tank Diameter (ft) NA Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered <input type="checkbox"/> Engine Model Year <input type="checkbox"/> Date Engine Was Built by Manufacturer <input type="checkbox"/> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| | | | | | | | | | | |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 4-95 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.52 | 2.36 | 2.29 | 2.11 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.5 | 2.14 | 2.17 | 1.99 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.01 | 0.1 | 0.06 | 0.06 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|--|---|--|--|--|---|
| Emission Point ID No. (Designation) 5-95 | Descriptive Name of the Emissions Source (Alt. Name) Aeration Tank | Approximate Location of Stack or Vent (see instructions) | | | |
| | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30 ° -90 ° | | Datum Horizontal Vertical NAD83 739000 mE 3327400 mN 31' 15" hundredths 15" hundredths |
| Tempo Subject Item ID No. EQT0204 | | | | | |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | NA ft ft ² | NA ft | NA ft/sec | NA ft ³ /min | 77 °F | 8,760 hr/yr | Sept 1995 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | |
|-------|---|-----------------------|---|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | Description |
| a | NA | NA | Normal Operating Rate/Throughput | 27,000 gal/hr |
| b | | | Maximum Operating Rate/Throughput | NA |
| c | | | Design Capacity/Volume/Cylinder Displacement | 660,000 gal |
| Notes | | | Shell Height (ft) | NA |
| | | | Tank Diameter (ft) | NA |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | |
| | | | Date Engine Ordered | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |

| Emission Point ID No. (Designation) 5-95 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | <0.01 | 0.03 | 0.02 | 0.02 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | <0.01 | 0.02 | 0.02 | 0.02 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|--|---|-------------------------------------|------------|-----------|----------|------------|
| Emission Point ID No. (Designation) 1700-83 | Descriptive Name of the Emissions Source (Alt. Name) ACR Drumming Vent | Approximate Location of Stack or Vent (see instructions) | | | | | |
| Tempo Subject Item ID No. RLP0019 | | Method | 06, "Address Matching-Primary Name" | | Datum | NAD83 | |
| | | UTM Zone | 15 | Horizontal | 739000 mE | Vertical | 3327400 mN |
| | | Latitude | 30 ° | | 3 " 15 " | | hundredths |
| | | Longitude | -90 ° | | 31 ' 15 " | | hundredths |

| | | | | | | | | | | | |
|---|---|--|---|--|---|--|--|---|---------|---------|---------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) NA °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Sept 2007 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |

| | | | | | | |
|---|--|------------------------------|--|-----------------------------------|-------------------|--------------------|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | | | Parameter | Description |
| | a | NA | NA | Normal Operating Rate/Throughput | | 2,000 drums/yr |
| | b | | | Maximum Operating Rate/Throughput | | NA |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| These emissions are from an open shed which is equipped with a ventilation fan to minimize employee exposure. | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|---|-------------------------------|-------------------------------------|-----------------------------|--------------------------------|-------------------------|-------------------------|--|--|-------------------------------------|--|
| Emission Point ID No. (Designation) 1700-83 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.20 | 0.35 | 0.020 | 0.340 | C | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Tetrachloroethylene | 000 | 0% | 00127-18-4 | 0.04 | 0.08 | 0.01 | 0.01 | U | | ppm by vol |
| Xylene (mixed isomers) | 000 | 0% | 01330-20-7 | 0.003 | 0.02 | 0.001 | 0.001 | U | | ppm by vol |
| Dichloromethane | 000 | 0% | 00075-09-2 | 0.10 | 1.44 | 0.02 | 0.02 | U | | ppm by vol |

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|--|---|--|--|---|---|---|--|--|-----------------------------------|------------------------------|---|--|--|--|--|
| Emission Point ID No. (Designation) 1700-84A | | Descriptive Name of the Emissions Source (Alt. Name) Advance Fibres System (AFS) Emulsion Shipping (Emulsion Blend Tank) | | | Approximate Location of Stack or Vent (see instructions) Method <u>06,"Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30°</u> <u>3'</u> <u>15"</u> hundredths Longitude <u>-90°</u> <u>31'</u> <u>15"</u> hundredths | | | | | | | | | | |
| Tempo Subject Item ID No. EQT0212 | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) NA °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification 2008 | Percent of Annual Throughput Through This Emission Point | | | | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | |
| Type of Fuel Used and Heat Input (see instructions) | | | | Operating Parameters (include units) | | | | | | | | | | | |
| Fuel | Type of Fuel | | Heat Input (MMBTU/hr) | | Normal Operating Rate/Throughput | | | Parameter | | Description | | | | | |
| | NA | | NA | | Maximum Operating Rate/Throughput | | | NA | | | | | | | |
| | | | | | Design Capacity/Volume/Cylinder Displacement | | | NA | | | | | | | |
| | | | | | Shell Height (ft) | | | NA | | | | | | | |
| Notes | | | | Tank Diameter (ft) | | | NA | | | | | | | | |
| | | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | |
| | | | | Date Engine Ordered | | | Engine Model Year | | | | | | | | |
| | | | | Date Engine Was Built by Manufacturer | | | | | | | | | | | |
| | | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | |
| Emission Point ID No. (Designation) 1700-84A | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack | | | | |
| Pollutant | Average (lb/hr) | | | | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft³ | | | | |
| Sulfur dioxide | | | | | | | | | | | ppm by vol | | | | |
| Nitrogen oxides | | | | | | | | | | | ppm by vol | | | | |
| Carbon monoxide | | | | | | | | | | | ppm by vol | | | | |
| Total VOC (including those listed below) | | 000 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol | | | | |
| Lead | | | | | | | | | | | ppm by vol | | | | |
| Chloroprene | | 000 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol | | | | |
| Toluene | | 000 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol | | | | |
| | | | | | | | | | | | ppm by vol | | | | |

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|--|---|---|---|--|---|
| Emission Point ID No. (Designation) 1700-84B | Descriptive Name of the Emissions Source (Alt. Name) Advance Fibres System (AFS) Emulsion Shipping (Tote Loading) | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0213 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 31 ' 15 " | | Datum NAD83 3327400 mN hundredths |

| | | | | | | | | | | | |
|--|---|---|--|---|--|---|--|--|----------------|----------------|----------------|
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) NA ft ft² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) NA ft³/min | Stack Gas Exit Temperature (°F) NA °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification 2008 | Percent of Annual Throughput Through This Emission Point | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| | | | | | | |
|-------|---|-----------------------|---|--|-------------------|-------------|
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
| | Type of Fuel | Heat Input (MMBTU/hr) | | | Parameter | Description |
| | a NA | NA | Normal Operating Rate/Throughput | | | |
| | b | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| | | | | | | | | | | |
|---|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Emission Point ID No. (Designation) 1700-84B | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | <0.01 | U | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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 (Designation)
 1700-85

Descriptive Name of the Emissions Source (Alt. Name)

Liquid Dispersion Loading
 (Truck, Tote, Railcar Loading)

Approximate Location of Stack or Vent (see instructions)

Method 06, "Address Matching-Primary Name" Datum NAD83
 UTM Zone 15 Horizontal 739000 mE Vertical 3327400 mN
 Latitude 30° 3' 15" hundredths
 Longitude -90° 31' 15" hundredths

Tempo Subject Item ID No.
 EQT0214

Stack and Discharge
 Physical Characteristics
 Change? (yes or no)

no

Diameter (ft) or Stack
 Discharge Area (ft²)

NA ft
 ft²

Height of Stack
 Above Grade (ft)

NA ft

Stack Gas Exit
 Velocity

NA ft/sec

Stack Gas Flow at
 Conditions, not at
 Standard (ft³/min)

NA ft³/min

Stack Gas Exit
 Temperature
 (°F)

NA °F

Normal Operating
 Time
 (hours per year)

8,760 hr/yr

Date of
 Construction or
 Modification

2008

Percent of Annual
 Throughput Through This
 Emission Point

| | | | |
|---------|---------|---------|---------|
| Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| 25% | 25% | 25% | 25% |

Fuel Type of Fuel Used and Heat Input (see instructions)

| | Type of Fuel | Heat Input (MMBTU/hr) |
|---|--------------|-----------------------|
| a | NA | NA |
| b | | |
| c | | |

Notes

Operating Parameters (include units)

| Parameter | Description |
|---|-------------------|
| Normal Operating Rate/Throughput | NA |
| Maximum Operating Rate/Throughput | NA |
| Design Capacity/Volume/Cylinder Displacement | NA |
| Shell Height (ft) | NA |
| Tank Diameter (ft) | NA |
| Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | |
| Date Engine Ordered | Engine Model Year |
| Date Engine Was Built by Manufacturer | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |

Emission Point ID No. (Designation)
 1700-85

Control
 Equipment
 Code

Control
 Equipment
 Efficiency

HAP / TAP
 CAS Number

Proposed Emission Rates

Permitted
 Emission Rate
 (Current)

Add,
 Change,
 Delete, or
 Unchanged

Continuous
 Compliance
 Method

Concentration in Gases
 Exiting at Stack

| Pollutant | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
|--|--------------------|---------------------|---------------------|---------------------|---|--|------------------------|
| Particulate matter (PM ₁₀) | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 0.003 | 0.003 | 0.01 | 0.01 | U | | ppm by vol |
| Lead | | | | | | | ppm by vol |
| Chloroprene | 0.003 | 0.003 | 0.01 | 0.01 | U | | ppm by vol |
| Toluene | <0.001 | <0.001 | <0.001 | <0.001 | U | | ppm by vol |
| | | | | | | | ppm by vol |

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|--|--|--|--|--|---|
| Emission Point ID No. (Designation) 1-93 | Descriptive Name of the Emissions Source (Alt. Name) Fugitive Emissions - Neoprene Unit | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. FUG0004 | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 30° -90° | | Datum Horizontal Vertical 3327400 mE 15" 31' 15" |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|---------|---------|---------|
| no | NA ft | NA ft | NA ft/sec | NA ft ³ /min | NA °F | 8,760 hr/yr | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | ft ² | | | | | | | 25% | 25% | 25% | 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | |
|-------|---|-----------------------|---|-----------|-------------------|
| | Type of Fuel | Heat Input (MMBTU/hr) | | Parameter | Description |
| a | NA | NA | Normal Operating Rate/Throughput | NA | |
| b | | | Maximum Operating Rate/Throughput | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | NA | |
| Notes | | | Shell Height (ft) | NA | |
| | | | Tank Diameter (ft) | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | |
| | | | Date Engine Ordered | | Engine Model Year |
| | | | Date Engine Was Built by Manufacturer | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | |

| Emission Point ID No. (Designation) | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| 1-93 | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Pollutant | | | | | | | | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 0.57 | 0.57 | 2.23 | 2.23 | U | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 0.37 | 0.37 | 1.60 | 1.60 | U | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 0.05 | 0.05 | 0.22 | 0.22 | U | | ppm by vol |
| Xylene (mixed isomers) | 000 | 0% | 01330-20-7 | <0.01 | <0.01 | 0.02 | 0.02 | U | | ppm by vol |

| Emission Point ID No. (Designation) 1-93 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|---|------------------------------|------------------------------------|-------------------------|-------------------------|---------------------|---------------------|---|--|------------------------------------|--|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Dichloromethane | | | 00075-09-2 | <0.01 | <0.01 | 0.02 | 0.02 | U | | ppm by vol |
| Tetrachloroethylene | | | 00127-18-4 | <0.01 | <0.01 | 0.02 | 0.02 | U | | ppm by vol |

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| | | | | | | | | | | | |
|--|--|---|--|--|---|---|---|-----------------------------------|--|------------------------------|---|
| Emission Point ID No. (Designation) 6-95 | | Descriptive Name of the Emissions Source (Alt. Name) Clarifier | | | Approximate Location of Stack or Vent (see instructions) | | | | | | |
| Tempo Subject Item ID No. EQT | | | | | Method _____ 06, "Address Matching-Primary Name" _____ Datum NAD83 UTM Zone _____ 15 Horizontal _____ 739000 mE Vertical _____ 3327400 mN Latitude _____ 30 ° _____ 3 ' _____ 15 " _____ hundredths Longitude _____ -90 ° _____ 31 ' _____ 15 " _____ hundredths | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft ²) NA ft ft ² | Height of Stack Above Grade (ft) NA ft | Stack Gas Exit Velocity NA ft/sec | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) NA ft ³ /min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 8,760 hr/yr | Date of Construction or Modification Sept 1995 | | Percent of Annual Throughput Through This Emission Point | | |
| | | | | | | | | Jan-Mar | Apr-Jun | Jul-Sep | Oct-Dec |
| | | | | | | | | 25% | 25% | 25% | 25% |
| Fuel | Type of Fuel Used and Heat Input (see instructions) | | | Operating Parameters (include units) | | | | | | | |
| | Type of Fuel | | | Parameter | | | | | | | |
| | Heat Input (MMBTU/hr) | | | Description | | | | | | | |
| | a | NA | NA | Normal Operating Rate/Throughput | | | | 27,000 gal/hr | | | |
| | b | | | Maximum Operating Rate/Throughput | | | | NA | | | |
| | c | | | Design Capacity/Volume/Cylinder Displacement | | | | 125,000 gal | | Open tank WWT treatment | |
| | | | | Shell Height (ft) | | | | NA | | | |
| | | | | Tank Diameter (ft) | | | | NA | | | |
| Notes | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered _____ Engine Model Year _____ Date Engine Was Built by Manufacturer _____ SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| | | | | | | | | | | | |
| Emission Point ID No. (Designation) 6-95 | | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
| Pollutant | | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | | 000 | 0% | | <0.01 | <0.01 | <0.01 | | A | | ppm by vol |
| Lead | | | | | | | | | | | ppm by vol |
| Chloroprene | | 000 | 0% | 00126-99-8 | <0.01 | <0.01 | <0.01 | | A | | ppm by vol |
| Toluene | | 000 | 0% | 00108-88-3 | <0.01 | <0.01 | <0.01 | | A | | ppm by vol |
| | | | | | | | | | | | ppm by vol |

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| Emission Point ID No. (Designation) 1700-87 | | Descriptive Name of the Emissions Source (Alt. Name) No. 10 Emulsion Storage Tank Manway | | | Approximate Location of Stack or Vent (see instructions) Method <u>06, "Address Matching-Primary Name"</u> Datum <u>NAD83</u> UTM Zone <u>15</u> Horizontal <u>739000</u> mE Vertical <u>3327400</u> mN Latitude <u>30 °</u> <u>3</u> ' <u>15</u> " <u>hundredths</u> Longitude <u>-90 °</u> <u>31</u> ' <u>15</u> " <u>hundredths</u> | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
|--|--|---|---|--|--|--|--|--|----------------|----------------|----------------|--|---|--|--|--|--|--|--|--|--|--|-----------|-------------|----------------------------------|------------------|-----------------------------------|----|--|----|-------------------|----|--------------------|----|---|--|---------------------|-------------------|---------------------------------------|--|---|--|
| Tempo Subject Item ID No. EQT0 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Stack and Discharge Physical Characteristics Change? (yes or no) no | Diameter (ft) or Stack Discharge Area (ft²) 0.167 ft ft² | Height of Stack Above Grade (ft) 55 ft | Stack Gas Exit Velocity 60.00 ft/sec | Stack Gas Flow at Conditions, not at Standard (ft³/min) 750 ft³/min | Stack Gas Exit Temperature (°F) 77 °F | Normal Operating Time (hours per year) 81 hr/yr | Date of Construction or Modification 2013 | Percent of Annual Throughput Through This Emission Point | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Type of Fuel Used and Heat Input (see instructions) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:5%;">Fuel</th> <th style="width:25%;">Type of Fuel</th> <th style="width:25%;">Heat Input (MMBTU/hr)</th> </tr> <tr> <td>a</td> <td>NA</td> <td>NA</td> </tr> <tr> <td>b</td> <td></td> <td></td> </tr> <tr> <td>c</td> <td></td> <td></td> </tr> </table> | | | | Fuel | Type of Fuel | Heat Input (MMBTU/hr) | a | NA | NA | b | | | c | | | Operating Parameters (include units) <table border="1" style="width:100%; border-collapse: collapse;"> <tr> <th style="width:65%;">Parameter</th> <th style="width:35%;">Description</th> </tr> <tr> <td>Normal Operating Rate/Throughput</td> <td>42,000 lb/charge</td> </tr> <tr> <td>Maximum Operating Rate/Throughput</td> <td>NA</td> </tr> <tr> <td>Design Capacity/Volume/Cylinder Displacement</td> <td>NA</td> </tr> <tr> <td>Shell Height (ft)</td> <td>NA</td> </tr> <tr> <td>Tank Diameter (ft)</td> <td>NA</td> </tr> <tr> <td colspan="2"> Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal </td> </tr> <tr> <td>Date Engine Ordered</td> <td>Engine Model Year</td> </tr> <tr> <td colspan="2">Date Engine Was Built by Manufacturer</td> </tr> <tr> <td colspan="2"> SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke </td> </tr> </table> | | | | | | | Parameter | Description | Normal Operating Rate/Throughput | 42,000 lb/charge | Maximum Operating Rate/Throughput | NA | Design Capacity/Volume/Cylinder Displacement | NA | Shell Height (ft) | NA | Tank Diameter (ft) | NA | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | Date Engine Ordered | Engine Model Year | Date Engine Was Built by Manufacturer | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | |
| Fuel | Type of Fuel | Heat Input (MMBTU/hr) | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| a | NA | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| b | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| c | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Parameter | Description | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Normal Operating Rate/Throughput | 42,000 lb/charge | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Maximum Operating Rate/Throughput | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Design Capacity/Volume/Cylinder Displacement | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Shell Height (ft) | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tank Diameter (ft) | NA | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Ordered | Engine Model Year | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Date Engine Was Built by Manufacturer | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Notes | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

| Emission Point ID No. (Designation) 1700-87 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 30.25 | 4097 | 1.23 | | A | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 20.57 | 2527 | 0.83 | | A | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 3.22 | 785 | 0.13 | | A | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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| | | | | | |
|---|---|---|---|--|-------------|
| Emission Point ID No. (Designation) 1700-88 | Descriptive Name of the Emissions Source (Alt. Name) No. 13 Emulsion Storage Tank Manway | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQT0 | | Method UTM Zone 15 Latitude 30 ° Longitude -90 ° | 06, "Address Matching-Primary Name" Horizontal 739000 mE Vertical 3327400 mN 3' 15" hundredths 31' 15" hundredths | | Datum NAD83 |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, not at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|--|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 55 ft | 60.00 ft/sec | 750 ft ³ /min | 77 °F | 26 hr/yr | 2013 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 42,000 lb/charge | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-88 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 46.41 | 4097 | 0.60 | | A | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 40 | 2527 | 0.52 | | A | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 2.14 | 785 | 0.028 | | A | | ppm by vol |
| | | | | | | | | | | ppm by vol |

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|---|---|--|---|--|--|
| Emission Point ID No. (Designation) 1700-89 | Descriptive Name of the Emissions Source (Alt. Name) No. 14 Emulsion Storage Tank Manway | Approximate Location of Stack or Vent (see instructions) | | | |
| Tempo Subject Item ID No. EQTO | | Method UTM Zone Latitude Longitude | 06, "Address Matching-Primary Name" 15 Horizontal 739000 mE 30° 3' 15" Vertical -90° 31' 15" | | Datum NAD83 3327400 mN hundredths hundredths |

| Stack and Discharge Physical Characteristics Change? (yes or no) | Diameter (ft) or Stack Discharge Area (ft ²) | Height of Stack Above Grade (ft) | Stack Gas Exit Velocity | Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) | Stack Gas Exit Temperature (°F) | Normal Operating Time (hours per year) | Date of Construction or Modification | Percent of Annual Throughput Through This Emission Point | | | |
|--|--|----------------------------------|-------------------------|---|---------------------------------|--|--------------------------------------|--|----------------|----------------|----------------|
| no | 0.167 ft ft ² | 55 ft | 60.00 ft/sec | 750 ft ³ /min | 77 °F | 26 hr/yr | 2013 | Jan-Mar 25% | Apr-Jun 25% | Jul-Sep 25% | Oct-Dec 25% |

| Fuel | Type of Fuel Used and Heat Input (see instructions) | | Operating Parameters (include units) | | | |
|-------|---|-----------------------|---|--|-------------------|--|
| | Type of Fuel | Heat Input (MMBTU/hr) | Parameter | | Description | |
| a | NA | NA | Normal Operating Rate/Throughput | | 42,000 lb/charge | |
| b | | | Maximum Operating Rate/Throughput | | NA | |
| c | | | Design Capacity/Volume/Cylinder Displacement | | NA | |
| Notes | | | Shell Height (ft) | | NA | |
| | | | Tank Diameter (ft) | | NA | |
| | | | Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal | | | |
| | | | Date Engine Ordered | | Engine Model Year | |
| | | | Date Engine Was Built by Manufacturer | | | |
| | | | SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke | | | |

| Emission Point ID No. (Designation) 1700-89 | Control Equipment Code | Control Equipment Efficiency | HAP / TAP CAS Number | Proposed Emission Rates | | | Permitted Emission Rate (Current) | Add, Change, Delete, or Unchanged | Continuous Compliance Method | Concentration in Gases Exiting at Stack |
|--|------------------------|------------------------------|----------------------|-------------------------|------------------|------------------|-----------------------------------|-----------------------------------|------------------------------|---|
| Pollutant | | | | Average (lb/hr) | Maximum (lbs/hr) | Annual (tons/yr) | Annual (tons/yr) | | | |
| Particulate matter (PM ₁₀) | | | | | | | | | | gr/std ft ³ |
| Sulfur dioxide | | | | | | | | | | ppm by vol |
| Nitrogen oxides | | | | | | | | | | ppm by vol |
| Carbon monoxide | | | | | | | | | | ppm by vol |
| Total VOC (including those listed below) | 000 | 0% | | 46.41 | 4097 | 0.60 | | A | | ppm by vol |
| Lead | | | | | | | | | | ppm by vol |
| Chloroprene | 000 | 0% | 00126-99-8 | 40 | 2527 | 0.52 | | A | | ppm by vol |
| Toluene | 000 | 0% | 00108-88-3 | 2.14 | 785 | 0.028 | | A | | ppm by vol |
| | | | | | | | | | | ppm by vol |

24. NSR Applicability Summary [LAC 33:III.504 and LAC 33:III.509] ☒ N/A

This section consists of five tables, A-E, and is applicable only to new and existing major stationary sources (as defined in LAC 33:III.504 or in LAC 33:III.509) proposing to permit a physical change or change in the method of operation. It would also apply to existing minor stationary sources proposing a physical change or change in the method of operation where the change would be a major source in and of itself. Add rows to each table as necessary. Provide a written explanation of the information summarized in these tables. Consult instructions.

24.A. Project Summary

| Emission Point ID | Description | A New, Modified, Affected, or Unaffected* | B Pre-Project Allowables (TPY) | C Baseline Actual Emissions (over 24-month period) | D Projected Actual Emissions (TPY) | E Post-Project Potential to Emit (TPY) | F Change |
|-------------------|--|--|-----------------------------------|---|---------------------------------------|---|-------------|
| PM _{2.5} | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | PM _{2.5} Change: | |
| PM ₁₀ | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | PM ₁₀ Change: | |
| SO ₂ | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | SO ₂ Change: | |
| NO _x | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | NO _x Change: | |
| CO | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |

| | | | | | | | |
|-----|--|--|--|--|--|-------------|--|
| | | | | | | CO Change: | |
| VOC | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | VOC Change: | |

| | | | | | | | |
|-------------------|--|--|--|--|--|---------------------------|--|
| CO ₂ e | 24-Month Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | CO ₂ e Change: | |

* Unaffected emissions units are not required to be listed individually. By choosing not to list unaffected emissions units, the applicant asserts that all emissions units not listed in Table 24.A will not be modified or experience an increase in actual annual emissions as part of the proposed project.

24.B. Creditable Contemporaneous Changes

| Contemporaneous Period: MM/DD/YYYY – MM/DD/YYYY | | | | | | | |
|---|-------------|----------------------|------------------------------|--|-----------------|--------------------------------------|--------|
| | | A | B | C | D | E | F |
| Emission Point ID | Description | Date of Modification | Pre-Project Allowables (TPY) | Baseline Actual Emissions (over 24-month period) | 24-Month Period | Post-Project Potential to Emit (TPY) | Change |
| PM _{2.5} | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | PM _{2.5} Change: | |
| PM ₁₀ | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | PM ₁₀ Change: | |
| SO ₂ | | | | | | | |
| | | | | | | | |

24.B. Creditable Contemporaneous Changes

| | | | | | | | |
|------------------------|--|--|--|--|--|--------------------------------|--|
| | | | | | | | |
| | | | | | | SO₂ Change: | |
| NO_x | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | NO_x Change: | |
| CO | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | CO Change: | |
| VOC | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | VOC Change: | |
| CO₂e | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | CO₂e Change: | |

For each source identified as "New" or "Modified" in Section 24.A, complete the following table for each pollutant that will trigger NSR. If LAER is not required per LAC 33:III.504.D.3, indicate such.

24.C. BACT/LAER Summary

| Emission Point ID | Pollutant | BACT/LAER | Limitation | Averaging Period | Description of Control Technology/Work Practice Standard(s) |
|-------------------|-----------|-----------|------------|------------------|---|
| | | | | | |
| | | | | | |
| | | | | | |

24.D. PSD Air Quality Analyses Summary

| | | A | B | C | D | E | F | G | H | I |
|-------------------|------------------|--|--|---|---|--|---|------------------------------------|--|---|
| Pollutant | Averaging Period | Preliminary Screening Concentration ($\mu\text{g}/\text{m}^3$) | Level of Significant Impact ($\mu\text{g}/\text{m}^3$) | Significant Monitoring Concentration ($\mu\text{g}/\text{m}^3$) | Background ($\mu\text{g}/\text{m}^3$) | Maximum Modeled Concentration ($\mu\text{g}/\text{m}^3$) | Modeled + Background Concentration ($\mu\text{g}/\text{m}^3$) | NAAQS ($\mu\text{g}/\text{m}^3$) | Modeled PSD Increment Consumption ($\mu\text{g}/\text{m}^3$) | Allowable Class II PSD Increment ($\mu\text{g}/\text{m}^3$) |
| PM _{2.5} | 24-hour | | 1.2 | 4 | | | | 35 | | - |
| | Annual | | 0.3 | - | | | | 15 | | - |
| PM ₁₀ | 24-hour | | 5 | 10 | | | | 150 | | 30 |
| | Annual | | 1 | - | | | | 50 | | 17 |
| SO ₂ | 1-hour | | 7.8 | - | | | | 195 | | - |
| | 3-hour | | 25 | - | | | | 1300 | | 512 |
| | 24-hour | | 5 | 13 | | | | 365 | | 91 |
| | Annual | | 1 | - | | | | 80 | | 20 |
| NO _x | 1-hour | | 7.5 | - | | | | 188 | | - |
| | Annual | | 1 | 14 | | | | 100 | | 25 |
| CO | 1-hour | | 2000 | - | | | | 40,000 | - | - |
| | 8-hour | | 500 | 575 | | | | 10,000 | - | - |
| Lead | 3-month | | - | 0.1 | | | | 1.5 | - | - |

24.E Nonattainment New Source Review Offsets [LAC 33:III.517.D.16, LAC 33:III.504.D.4 & 5] ☒ N/A

Complete this section only if the proposed project triggers Nonattainment New Source Review (NNSR).

This project triggers NNSR review for: ☐ NO_x ☐ VOC

NO_x:

Is the applicant proposing to use internal offsets? ☐ Yes ☐ No

If not, identify the source of the offsets. **Company:** _____

Facility/Unit: _____

Permit No.: _____

Is an ERC Bank Application included with this application, or has an application already been submitted to LDEQ?

☐ Yes ☐ No

If the ERC application has already been submitted, give the date: _____

Identify the emissions units from which the offsets will be obtained (reference specific Emission Point ID numbers).

VOC:

Is the applicant proposing to use internal offsets? ☐ Yes ☐ No

If not, identify the source of the offsets. **Company:** _____

Facility/Unit: _____

Permit No.: _____

Is an ERC Bank Application included with this application, or has an application already been submitted to LDEQ?

☐ Yes ☐ No

If the ERC application has already been submitted, give the date: _____

Identify the emissions units from which the offsets will be obtained (reference specific Emission Point ID numbers).

In order to expedite processing, please be sure the ERC Bank Application is completed properly. In the case of NO_x, the document should clearly differentiate between ozone season and non-ozone season actual emissions during the baseline period. Regarding NO_x and VOC, be sure to indicate if a portion of the reductions are no longer surplus (e.g., due to new or revised federal or state regulations, use in a netting analysis, etc.).

24.F. Economic Impact

Answer the following questions.

How many temporary jobs will be added as a result of this project? _____

How many permanent jobs will be added as a result of this project? _____

24.G Notification of Federal Land Manager [LAC 33:III.504.E.1, LAC 33:III.509.P.1]

Complete this section only if the proposed project triggers NNSR or PSD.

- a. Is the proposed facility or modification located within 100 kilometers of a Class I Area? ☐ Yes ☒ No
If Yes, determination of Q/d is not required; skip to the next question. If No, complete the Q/d equation below:

$$Q/d = \frac{PM_{10(NEI)} + SO_{2(NEI)} + NO_{X(NEI)} + H_2SO_{4(NEI)}}{\text{Class I km}}$$

where:

| | |
|------------------|--|
| $PM_{10(NEI)}$ | = net emissions increase of PM_{10} ^{1,2} |
| $SO_{2(NEI)}$ | = net emissions increase of SO_2 ^{1,2} |
| $NO_{X(NEI)}$ | = net emissions increase of NO_X ^{1,2} |
| $H_2SO_{4(NEI)}$ | = net emissions increase of H_2SO_4 ^{1,2} |
| Class I km | = distance to nearest Class I Area ³ |

$$Q/d = \frac{\quad + \quad + \quad + \quad}{\quad} = \quad$$

If Q/d < 10, proceed to Section 25. If Q/d ≥ 10, complete the remainder of this Section.

- b. Has the applicant provided a copy of the application to the Federal Land Manager? ☐ Yes ☐ No
- c. Does the application contain modeling that demonstrates no adverse impact on Air Quality Related Values (AQRVs) in the Class I Area? ☐ Yes ☐ No
- d. If Yes, indicate the model used: ☐ VISCREEN ☐ PLUVUE II ☐ CALPUFF ☐ Other:⁴ _____
- e. Has the Federal Land Manager concurred that the proposed project will not adversely impact any AQRVs?
☐ Yes ☐ No If Yes, please attach correspondence.

¹If the net emissions increase of any pollutant is negative, enter "0."²If the project did not trigger a netting analysis, use the project increase. In this case, the value will be less than the pollutant's significance level.³In kilometers.⁴Model must be approved by LDEQ and the Federal Land Manager.

25. Environmental Assessment Statement (EAS or "IT" Question Responses)

[La. R.S. 30:2018] ☐ Yes ☒ No

**** This section is required when applying for new Part 70 operating permits and/or major modifications. Any applications for these permit types that do not include answers to these questions will not be considered to be administratively complete. ****

For new Part 70 operating permits and/or major modifications, answers to these questions must be provided by the applicant to the local governmental authority and the designated public library at no additional costs to these entities. Consult instructions to determine what is considered to be a "local governmental authority" and a "designated public library". Indicate the name and address of the local governmental authority and the designated public library to which the answers to these questions were sent:

| Name of Local Governing Authority | | | Name of Designated Public Library | | |
|-----------------------------------|-------|-----|-----------------------------------|-------|-----|
| Street or P.O. Box | | | Street or P.O. Box | | |
| City | State | ZIP | City | State | ZIP |

Answer the following five questions on separate pages using full and complete answers. Include as many pages as necessary in order to provide full and complete answers. This information is required per Louisiana Revised Statutes 30:2018 (La. R.S. 30:2018).

Question 1: Have the potential and real adverse environmental effects of the proposed facility been avoided to the maximum extent possible? (This question requires the permittee to identify adverse environmental effects, both potential and real.)

Question 2: Does a cost benefit analysis of the environmental impact costs balanced against the social and economic benefits of the proposed facility demonstrate that the latter outweighs the former? (This question requires the permittee to perform a cost-benefit analysis, or at least a quantitative indication of the economic benefits and a qualitative description of the negative impacts expected from the permittee's operation. The latter should come from the answer to Question 1.)

Question 3: Are there alternative projects which would offer more protection to the environment than the proposed facility without unduly curtailing non-environmental benefits? (This question requires the permittee to demonstrate having considered alternate technologies.)

Question 4: Are there alternative sites which would offer more protection to the environment than the proposed facility site without unduly curtailing non-environmental benefits? (This is the question that deals directly with siting criteria.)

Question 5: Are there mitigating measures which would offer more protection to the environment than the facility as proposed without unduly curtailing non-environmental benefits? (This question requires the permittee to demonstrate having considered the most stringent techniques for reducing or more efficiently handling waste.)

PART 70 OPERATING PERMIT APPLICATION COMPLETENESS CHECKLIST

Instructions: Complete this checklist and submit with the completed air permit application.

| LAC 33:III. | Completeness Questions Relative to the Part 70 Permit Application | Yes | No | NA | Location Within the Permit Application |
|--|---|-----|----|----|--|
| 517.A Timely Submittal | Was a Copy of the Application Also Submitted to EPA? | X | | | Under Separate Cover |
| 517.B.1.2 Certification | Does the Application include a Certification by a Responsible Official? | X | | | Item 10 Section 3 |
| 517.B.3 Certification | Does the Application Include Certification by a Professional Engineer or their Designee: | X | | | Item 10 Section 3 |
| 517.D.1 Identifying Information | Does the Application Include: | | | | |
| | 1. Company Name, Physical and Mailing Address of Facility? | X | | | Items 1 & 2 Section 3 |
| | 2. Map showing Location of the Facility? | X | | | Figure 1 |
| | 3. Owner and Operator Names and Agent? | X | | | Item 1 Section 3 |
| | 4. Name and Telephone Number of Plant Manager or Contact? | X | | | Item 11 Section 3 |
| 517.D.2 SIC Codes, Source Categories | Does the Application Include a Description of the Source's Processes and Products? | X | | | Item 2 Section 3 |
| | Does the Application Include the Source's SIC Code? | X | | | Item 5 Section 3 |
| | Does the Application Include EPA Source Category of HAPs if applicable? | X | | | Section 3 |
| 517.D.3.6 EIQ Sheets | Has an EIQ Sheet been Completed for each Emission Point whether an Area or Point Source? | X | | | Item 23 Section 3 |
| 517.D.4 Monitoring Devices | Does the Application Include Identification and Description of Compliance Monitoring Devices or Activities? | X | | | Item 22 Section 3 |
| 517.D.5 Revisions and Modifications Only | For Revisions or Modifications, Does the Application include a Description of the Proposed Change and any Resulting Change in Emissions? | X | | | Section 1 & Item 1, Section 3 |
| 517.D.7 General Information | Does the Application Include Information Regarding Fuels, Fuel Use, Raw Materials, Production Rates, and Operating Schedules as necessary to substantiate emission rates? | X | | | Item 23 Section 3 |
| 517.D.8 Operating Limitations | Has Information Regarding any Limitations on Source Operation or any Applicable Work Practice Standards been Identified? | X | | | Item 22 Section 3 |
| 517.D.9 Calculations | Are Emission Calculations Provided? | X | | | Appendix A |

| LAC 33:III. | Completeness Questions Relative to the Part 70 Permit Application | Yes | No | NA | Location Within the Permit Application |
|---|--|-----|----|----|--|
| 517.D.10 Regulatory Review | Does the Application Include a Citation and Description of Applicable Louisiana and Federal Air Quality Requirements and Standards? | X | | | Item 22 Section 3 |
| 517.D.11 Test Methods | Has a Description of or a Reference to Applicable Test Methods Used to Determine Compliance with Standards been Provided? | X | | | Item 22 Section 3 |
| 517.D.12 Major Sources of TAPs | Does the Application include Information Regarding the Compliance History of Sources Owned or Operated by the Applicant (per LAC 33.III.5111)? | X | | | Item 14a Section 3 |
| 517.D.13 Major Sources of TAPs | Does the Application include a Demonstration to show that the Source Meets all Applicable MACT and Ambient Air Standard Requirements? | X | | | Section 2 |
| 517.D.14 PSD Sources Only | If Required by DEQ, Does the Application Include Information Regarding the Ambient Air Impact for Criteria Pollutants as Required for the Source Impact Analysis per LAC 33:III.509.K, L, and M? | | | X | |
| 517.D.15 PSD Sources Only | If Required by DEQ, Does the Application Include a Detailed Ambient Air Analysis? | | | X | |
| 517.D.16, 18 | Has any Additional Information been Provided? | | X | | |
| 517.D.17 Fees | Has the Fee Code been Identified? | X | | | Item 5 Section 2 |
| | Is the Applicable Fee Included with the Application? | | | X | |
| 517.E.1 Additional Part 70 Requirements | Does the Certification Statement Include a Description of the Compliance Status of Each Emission Point in the Source with All Applicable Requirements? | X | | | Item 10 Section 3 |
| 517.E.2 Additional Part 70 Requirements | Does the Certification Statement Include a Statement that the Source will continue to Comply with All Applicable Requirements with which the Source is in Compliance? | X | | | Item 10 Section 3 |
| 517.E.3 Additional Part 70 Requirements | Does the Certification Statement Include a Statement that the Source will, on a timely basis, meet All Applicable Requirements that will Become Effective During the Permit Term? | X | | | Item 10 Section 3 |
| 517.E.4 Additional Part 70 Requirements | Are there Applicable Requirements for which the Source is not in Compliance at the Time of Submittal? | | X | | |
| | Does the Application include a Compliance Plan Schedule? | | | X | |
| | Does the Schedule Include Milestone Dates for which Significant Actions will occur? | | | X | |
| | Does the Schedule Include Submittal Dates for Certified Progress Reports? | | | X | |

| LAC 33:III. | Completeness Questions Relative to the Part 70 Permit Application | Yes | No | NA | Location Within the Permit Application |
|---|---|-----|----|----|--|
| 517.E.5 Additional Part 70 Requirements Acid Rain | Is this Source Covered by the Federal Acid Rain Program? | | X | | |
| | Are the Requirements of LAC 33:III.517.E 1-4 included in the Acid Rain Portion of the Compliance Plan? | | | X | |
| 517.E.6 Additional Part 70 Requirements | Have any Exemptions from any Applicable Requirements been Requested? | | X | | |
| | Is the List and explanations Provided? | | | X | |
| 517.E.7 Additional Part 70 Requirements | Does the Application Include a Request for a Permit Shield? | | X | | |
| | Does the Request List those Federally Applicable Requirements for which the Shield is Requested along with the Corresponding Draft Permit Terms and conditions which are Proposed to Maintain Compliance? | | | X | |
| 517.E.8 Additional Part 70 Requirements | Does the Application Identify and Reasonably Anticipated Alternative Operating Scenarios? | | X | | |
| | Does the Application include Sufficient Information to Develop permit Terms and Conditions for Each Scenario, Including Source Process and Emissions Data? | | | X | |
| 517.F Confidentiality | Does the Application Include a Request for Non-Disclosure (Confidentiality)? | | X | | |
| 525.B. Minor Permit Modifications | Does the Application Include a Listing of New Requirements Resulting for the Change? | | X | | |
| | Does the Application Include Certification by the Responsible Official that the Proposed Action Fits the Definition of a Minor Modification as per LAC 33:III.525.A. | | X | | |
| | Does the Certification also Request that Minor Modification Procedures be Used? | | X | | |
| | Does the Application, for Part 70 Sources, Include the Owner's Suggested Draft Permit and Completed Forms for the Permitting Authority to Use to Notify Affected States? | | X | | |
| La. R.S. 30:2018 – PSD/NNSR only | Has a copy of the answers to the questions posed in the Environmental Assessment Statement (Section 25) been sent to the local governing authority at no cost to the local governing authority? | | | X | |
| | Has a copy of the answers to the questions posed in the Environmental Assessment Statement (Section 25) been sent to the designated public library at no cost to the designated public library? | | | X | |

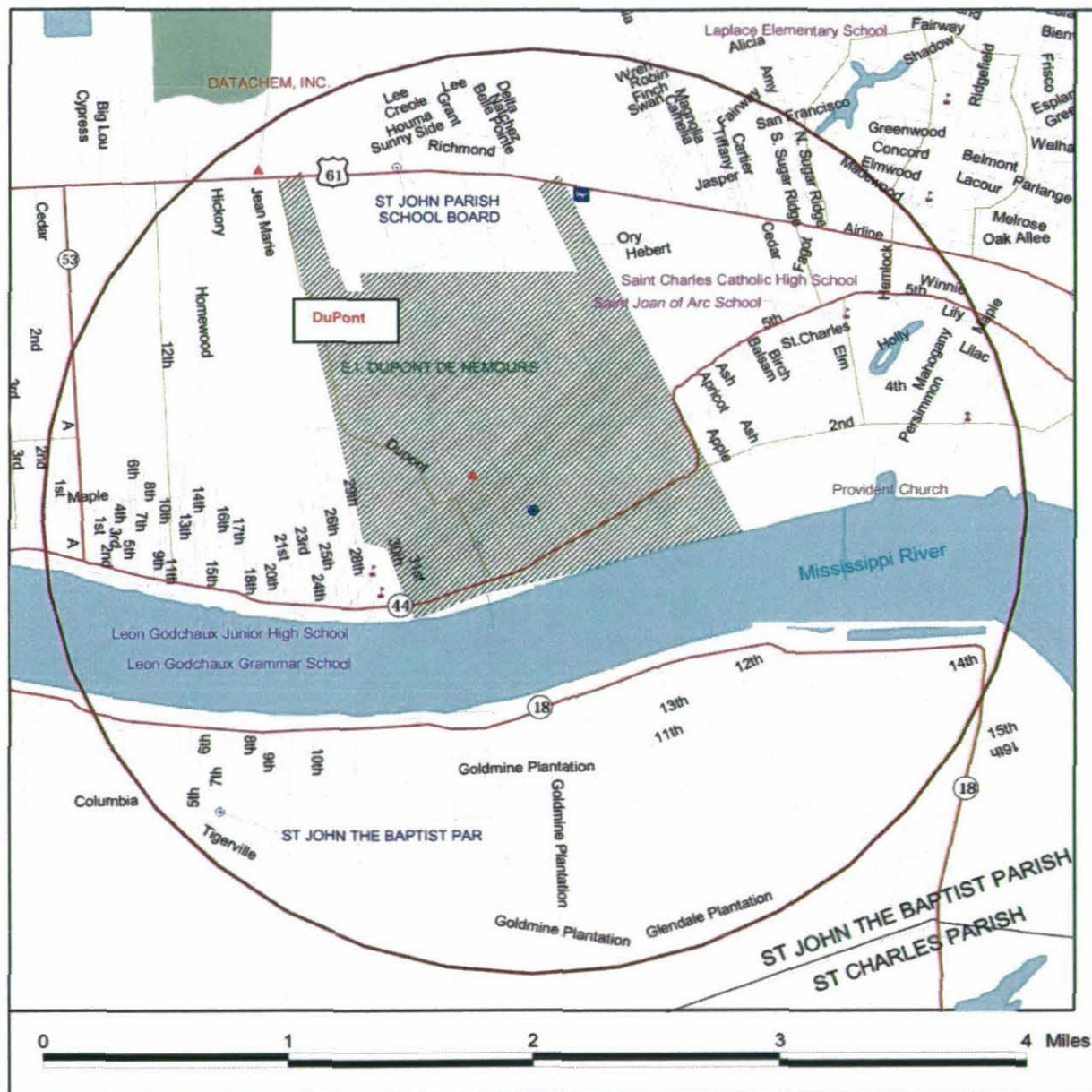
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FIGURES

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FIGURE 1
SITE LOCATION MAP

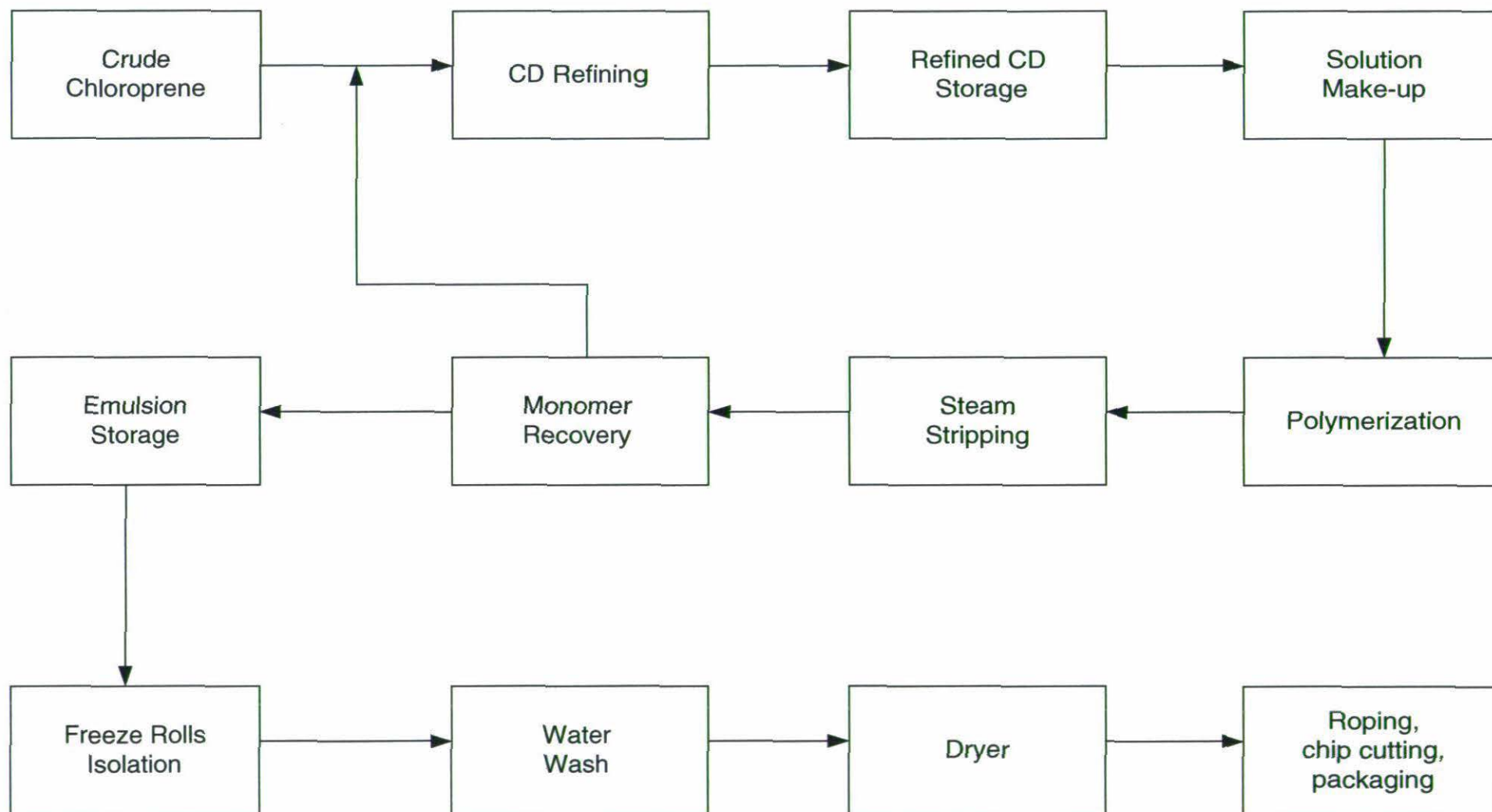


DuPont
Neoprene Unit
Figure 1
Site Location Map



FIGURE 2
NEOPRENE UNIT PROCESS FLOW DIAGRAM

FIGURE 2
NEOPRENE UNIT PROCESS FLOW DIAGRAM



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APPENDICES

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APPENDIX A

AIR EMISSION CALCULATIONS



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT- PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page 1 of 4

Basis:

The unstripped emulsion tank is vented down to atmospheric pressure and the nitrogen blanket which enters the top of the tank is turned off before opening the manway.

Emissions from the open manway and the agitator shaft seals are captured by the shaft seal ventilation system.

Emissions are based on spot sampling data conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 16.3 ppm with a maximum concentration of 47 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD.

Conservatively assume ACR is still present in the material.

Based on field observation and engineering judgement, emissions from EST 13 & 14 drop strainer are insignificant.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------|-----------------------|
| Rated Capacity of Blower = | 2500 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Average CD in Air Exhausted = | 16.3 ppm CD by volume |
| Maximum CD in Air Exhausted = | 51.7 ppm CD by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 25 °C |
| Pressure = | 14.696 psia |

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.0408 cfm CD



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Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT- PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page 2 of 4

Using the Ideal Gas Law,

| | |
|------------------------|--------------------------|
| Average CD Emissions = | 0.000104 moles CD/minute |
| Average CD Emissions = | 0.009221 lbs CD/minute |
| Average CD Emissions = | 0.553 lbs CD/hour |
| Average CD Emissions = | 4847 lbs/yr |
| Average CD Emissions = | 2.42 tons/yr |

Toluene

Using the Ideal Gas Law,

| | |
|---------------------------------|-----------------------------------|
| V.P. of CD at Saturation = | 189.00 mm Hg |
| Total Vapor = | 0.002550 moles/ft ³ |
| Mole Fraction CD = | 0.001633333 % |
| CD Vapor = | 0.00000004 moles/ft ³ |
| CD Partial Pressure = | 0.012 mm Hg |
| Ratio = | 0.000066 |
| V.P. of Toluene at Saturation = | 28.40 mm Hg |
| Toluene Partial Pressure = | 0.0019 mm Hg |
| Toluene Vapor = | 0.000000006 moles/ft ³ |
| Toluene Vapor = | 0.00002 moles/min |
| Toluene Vapor = | 0.001 lb/min |
| Toluene Vapor = | 0.09 lb/hr |
| Toluene Vapor = | 0.38 tpy |

ACR

| | |
|-----------------------------|----------------------------------|
| Ratio = | 0.000066 |
| V.P. of ACR at Saturation = | 42.28 mm Hg |
| ACR Partial Pressure = | 0.0028 mm Hg |
| ACR Vapor = | 0.00000001 moles/ft ³ |
| ACR Vapor = | 0.00002 moles/min |
| ACR Vapor = | 0.0029 lb/min |
| ACR Vapor = | 0.17 lb/hr |
| ACR Vapor = | 0.75 tpy |



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Air Emissions Calculation Sheet

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Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page 3 of 4

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.1293 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000330 moles CD/minute

Maximum CD Emissions = 0.029187 lbs CD/minute

Maximum CD Emissions = 1.751 lbs CD/hour

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 189.00 mm Hg

Total Vapor = 0.002550 moles/ft³

Mole Fraction CD = 0.00517 %

CD Vapor = 0.00000013 moles/ft³

CD Partial Pressure = 0.039 mm Hg

Ratio = 0.000208

V.P. of Toluene at Saturation = 28.40 mm Hg

Toluene Partial Pressure = 0.0059 mm Hg

Toluene Vapor = 0.00000002 moles/ft³

Toluene Vapor = 0.00005 moles/min

Toluene Vapor = 0.0046 lb/min

Toluene Vapor = 0.27 lb/hr



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page 4 of 4

ACR

Ratio = 0.000208
V.P. of ACR at Saturation = 42.28 mm Hg
ACR Partial Pressure = 0.0088 mm Hg
ACR Vapor = 0.00000003 moles/ft³
ACR Vapor = 0.00007 moles/min
ACR Vapor = 0.0091 lb/min
ACR Vapor = 0.54 lb/hr

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 7110 | 0.812 | 2.569 | 3.555 |
| Chloroprene | 4847 | 0.553 | 1.751 | 2.423 |
| Toluene | 758 | 0.087 | 0.274 | 0.379 |
| Total HAPs | 5605 | 0.640 | 2.025 | 2.802 |
| Total TAPs | 5605 | 0.640 | 2.025 | 2.802 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2

Page 1 of 4

Basis:

Vapors from all three strippers pass through a vacuum pump to a single vent condenser cooled with -20 deg C brine.

Nitrogen flow is based on sampling data conducted by METCO on March 13, 2002 and March 19, 2002.

Toluene emissions are estimated using the partial pressure of toluene produced in the unstripped emulsion.

Ammonia is added to the inlet of the condenser as an antifreeze and is emitted.

Calculation basis provided by Mr. P. Offut, DuPont

1,2-Dichlorobenzene emissions are based on a mass balance.

| | |
|-------------------------------|--|
| Condenser Feed Temperature = | 2 C |
| Condenser Exit Temperature = | -14 C |
| Vapor Pressure of CD = | 27.094 mm Hg @ -14 C |
| Vapor Pressure of Toluene = | 2.566 mm Hg @ -14 C |
| Vapor Pressure of Toluene = | 42.427 mm Hg @ 30 C |
| Vapor Pressure of ACR = | 5.203 mm Hg @ -14 C |
| Vapor Pressure of ACR = | 60.824 mm Hg @ 30 C |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Max. Mole Fraction Toluene = | 0.00398 |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Max. Mole Fraction ACR = | 0.000970 |
| Operating Hours = | 8760 hr |
| N2 flow = | 0.41250 lb/min N2 @ 760 mm Hg and 20 C |

Average Emission Rates

Chloroprene

| | | |
|-----------------|---------------------------------|----------------------|
| Total vapor = | 0.002934 moles/ft3 | |
| CD vapor = | 0.000105 moles/ft3 | 3.57 mole % CD |
| CD vapor = | 0.009261 lbs CD/ft3 total vapor | |
| Density of N2 = | 0.08270 lb/ft3 | 760 mmHg & -14 deg C |
| N2 flow = | 4.99 ft3/min for 3 strippers | |
| Total flow = | 5.20 ft3/min for 3 strippers | |
| CD Vapor flow = | 0.19 ft3/min | |



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Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2

Page 2 of 4

CD Vapor flow = 0.0482 lbs/min
CD Vapor flow = 2.89 lbs/hr
CD Vapor flow = 25309 lbs/yr

Toluene

Determine toluene content of feed to stripper condenser

| | | |
|--------------------------------|---------------------------------|-----------------------|
| Total vapor = | 0.002764 moles/ft ³ | |
| Liquid Mole Fraction Toluene = | 0.003977 | 0.40 mole % toluene |
| Partial Pressure Toluene = | 0.169 mm Hg | |
| Toluene Vapor = | 0.0000061 moles/ft ³ | 0.0222 mole % toluene |
| Toluene Vapor flow = | 0.0012 ft ³ /min | |
| Total flow = | 5.20 ft ³ /min | |
| Toluene Vapor = | 0.000003 moles/min | |
| Toluene Vapor = | 0.000294 lb/min | |

Determine toluene saturation at condenser exit conditions

Toluene Vapor = 0.000010 moles/ft³
Toluene Vapor = 0.000052 moles/min
Toluene Vapor = 0.004746 lb/min

Toluene enters the stripper below saturation conditions at the exit of the stripper. Assume that no toluene is removed.

Toluene Vapor = 0.000294 lb/min
Toluene Vapor = 0.02 lb/hr
Toluene Vapor = 154 lb/yr
Toluene Vapor = 0.08 tpy



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2

Page 3 of 4

ACR

Determine ACR content of feed to stripper condenser

| | | |
|----------------------------|----------------------------------|-------------------|
| Total vapor = | 0.002764 moles/ft ³ | |
| Liquid Mole Fraction ACR = | 0.000970 | 0.10 mole % ACR |
| Partial Pressure ACR = | 0.0590 mm Hg | |
| ACR Vapor = | 0.00000021 moles/ft ³ | 0.0078 mole % ACR |
| ACR Vapor flow = | 0.00040 ft ³ /min | |
| Total flow = | 5.20 ft ³ /min | |
| ACR Vapor = | 0.000001 moles/min | |
| ACR Vapor = | 0.000137 lb/min | |

Determine ACR saturation at condenser exit conditions

| | |
|-------------|--------------------------------|
| ACR Vapor = | 0.000020 moles/ft ³ |
| ACR Vapor = | 0.000104 moles/min |
| ACR Vapor = | 0.012845 lb/min |

ACR enters the stripper below saturation conditions at the exit of the stripper. Assume that no ACR is removed.

| | |
|-------------|-----------------|
| ACR Vapor = | 0.000137 lb/min |
| ACR Vapor = | 0.01 lb/hr |
| ACR Vapor = | 72 lb/yr |
| ACR Vapor = | 0.04 tpy |



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2

Page 4 of 4

Ammonia

Based on Standard Operating Conditions,

Min NH₃ addition per Stripper = 0 lb/hr

Max NH₃ addition per Stripper = 1.5 lb/hr

Typically ammonia runs at 0.2 lb/hr

Ammonia has single addition point on vacuum pump discharge

NH₃ Addition to vacuum pump = 5256 lb/yr

Max NH₃ Addition = 39420 lb/yr at top of SOC

Mean NH₃ emissions assumed 2 x of typical addition 10512 lb/yr

NH₃ Emissions = 10512 lbs/yr

NH₃ Emissions = 1.20 lbs/hr

NH₃ Emissions = 5.256 tpy

Maximum Emission Rates

Maximum emission rates are conservatively assumed to be 1.5 times the average emission rates.

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|---------------------|-----------------------------------|-----------------------------------|-------------------------|
| Total VOC | 25535 | 2.915 | 4.372 | 12.768 |
| Chloroprene | 25309 | 2.889 | 4.334 | 12.654 |
| 1,2-Dichlorobenzene | 0.01 | 0.000001 | 0.000002 | 0.000005 |
| Toluene | 154 | 0.018 | 0.026 | 0.077 |
| Ammonia | 10512 | 1.200 | 1.800 | 5.256 |
| Total HAPs | 25463 | 2.907 | 4.360 | 12.732 |
| Total TAPs | 35975 | 4.107 | 6.160 | 17.988 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

Page 1 of 11

Basis:

Vapors from all 5 PK pass to a single vent condenser cooled by 2 deg C brine.

Assume all of the nitrogen flowing through the vent condenser will saturate with CD.

Assume vapors inlet and exit vent condenser are saturated with water

CD condensation in the condenser starts at about 6% CD in the inlet stream

Toluene emissions are based on sampling data on March 14, 2002 and March 18, 2002 by METCO Environmental.

On March 14, 2002 type AD was being produced, which includes toluene.

On March 18, 2002 type WHV was being produced which does not include toluene.

The average toluene emission rate measured was 0.2033 lb/hr for a product using a toluene-based stabilizer.

The highest toluene emission rate measured was 0.34 lb/hr for a product using a toluene-based stabilizer.

The average toluene emission rate measured was 0.0033 lb/hr for a product not using a toluene-based stabilizer.

The highest toluene emission rate measured was 0.0054 lb/hr for a product not using a toluene-based stabilizer.

Stabilizer, defoamer, Octopool and Dresinate are added with the vent closed - insignificant emissions
1,2-Dichlorobenzene emissions are based on a mass balance.

| | |
|------------------------------|-----------------|
| Emulsification Temperature = | 35 C |
| Condenser Exit Temperature = | 6 C |
| Worst case charge size = | 41708 lb/charge |

| | |
|------------------------------------|-----------------|
| Worst Case Product Total Charges = | 6743 charges/yr |
| ACR Type Charges = | 6743 charges/yr |
| Toluene Stabilizer Charges = | 6557 charges/yr |
| Maximum Other Type Charges = | 6381 charges/yr |
| Spec. Grav. Unstripped Emulsion = | 1.060 |
| Venting Time for Emulsification = | 31.6 min/charge |

| | |
|-----------------------------|---|
| Average Toluene Emissions = | 0.2033 lb/hr with toluene-based stabilizer |
| Maximum Toluene Emissions = | 0.3400 lb/hr with toluene-based stabilizer |
| Average Toluene Emissions = | 0.0033 lb/hr without toluene-based stabilizer |
| Maximum Toluene Emissions = | 0.0054 lb/hr without toluene-based stabilizer |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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Emission Rates

Emulsification

Determine the VOC's inlet the vent condenser to be piped to the new condensing system

CD exit LPK =

- 1.5 % at start of emulsification
- 4.8 % 10 min after start of emulsification
- 6.8 % 15 min after start of emulsification
- 15.4 % 20 min after start of emulsification
- 26 % 31.6 min after start of emulsification

| | |
|-----------------------------------|---|
| Charge Volume = | 631 ft ³ /charge |
| Nitrogen Purge Rate = | 158 ft ³ /charge |
| Avg. Displacement Charging Rate = | 19.95 ft ³ /min |
| CD Displacement Rate = | 0.30 ft ³ /min @ start of emulsification |
| CD Displacement Rate = | 0.96 ft ³ /min @ 8.54 min after start of emulsification |
| CD Displacement Rate = | 1.36 ft ³ /min @ 12.82 min after start of emulsification |
| CD Displacement Rate = | 3.07 ft ³ /min @ 17.09 min after start of emulsification |
| CD Displacement Rate = | 5.19 ft ³ /min @ 27 min after start of emulsification |

nitrogen purge is off during emulsification

| | |
|-----------------------------|---|
| Average Displacement Rate = | 19.95 ft ³ /min |
| % CD = | 1.50 % @ start of emulsification |
| % CD = | 4.80 % @ start of emulsification + 8.54 min |
| % CD = | 6.80 % @ start of emulsification + 12.82 min |
| % CD = | 15.40 % @ start of emulsification + 17.09 min |
| % CD = | 26.00 % @ start of emulsification + 27 min |

Worst case of nitrogen saturated with CD and H₂O at 35 C inlet condenser

| | | |
|--------------------------------------|---|------------------------------|
| Vapor Pressure of CD = | 334.34 mm Hg | |
| Vapor Pressure of H ₂ O = | 43.57 mm Hg | |
| Total Vapor = | 0.002468 moles/ft ³ | |
| CD Vapor = | 0.001086 moles/ft ³ | 43.99 mole % CD |
| CD Vapor = | 0.096122 lbs CD/ft ³ total vapor | |
| H ₂ O Vapor = | 0.000141 moles/ft ³ | 5.73 mole % H ₂ O |
| H ₂ O Vapor = | 0.002547 lbs H ₂ O/ft ³ total vapor | |
| N ₂ Vapor = | 0.001241 moles/ft ³ | 50.28 mole % N ₂ |
| N ₂ Vapor = | 0.034739 lbs N ₂ /ft ³ total vapor | |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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At saturation exit condenser

Temperature = 6 C
Total Vapor = 0.002724 moles/ft³
CD Vapor Pressure = 104.34 mm Hg
CD Vapor = 0.00037399 moles/ft³ 13.73 mole % CD
CD Vapor = 0.03311293 lbs CD/ft³ total vapor
H₂O Vapor Pressure = 7.36 mm Hg
H₂O Vapor = 0.00002637 moles/ft³ 0.97 mole % H₂O
H₂O Vapor = 0.00047470 lbs H₂O/ft³ total vapor
N₂ Vapor = 0.00232362 moles/ft³ 85.30 mole % N₂
N₂ Vapor = 0.06506138 lbs N₂/ft³ total vapor

N₂ Flow = 16.77 ft³/min @ start of emulsification
N₂ Flow = 16.17 ft³/min @ 8.54 min after start of emulsification
N₂ Flow = 15.81 ft³/min @ 12.82 min after start of emulsification
N₂ Flow = 14.26 ft³/min @ 17.09 min after start of emulsification
N₂ Flow = 12.34 ft³/min @ 27 min after start of emulsification
Total Flow = 18.08 ft³/min @ start of emulsification
Total Flow = 17.16 ft³/min @ 8.54 min after start of emulsification
Total Flow = 18.08 ft³/min @ 12.82 min after start of emulsification
Total Flow = 17.70 ft³/min @ 17.09 min after start of emulsification
Total Flow = 15.32 ft³/min @ 27 min after start of emulsification
CD Flow = 0.0654 lb/min @ start of emulsification
CD Flow = 0.1987 lb/min @ 8.54 min after start of emulsification
CD Flow = 0.2965 lb/min @ 12.82 min after start of emulsification
CD Flow = 0.5862 lb/min @ 17.09 min after start of emulsification
CD Flow = 0.5074 lb/min @ 27 min after start of emulsification

Straight line fit points and obtain area under curve

For first 8.54 min CD = 1.1283 lbs
For 8.54 to 12.82 min CD = 1.0577 lbs
For 12.82 to 17.09 min CD = 1.8855 lbs
For 17.09 to 27 min CD = 5.4195 lbs
Total CD per Charge = 9.4910 lbs
Total CD per Year = 64002 lbs/yr
Total CD per Year = 32.00 tons/yr



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Air Emissions Calculation Sheet

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Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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During emulsification, toluene emissions are quite low, per sampling much less than saturation at 2 C.

Conservatively assume toluene emissions are the same as measured by METCO even with the the larger, more efficient 2 C condenser.

Assume that toluene-based stabilizer types emit the same toluene as A-types (even though A-type stabilizer toluene is 2 times G-types).

| | |
|--------------------------------|---------------|
| A and G-type Maximum Toluene = | 0.3400 lbs/hr |
| Other Type Maximum Toluene = | 0.0054 lbs/hr |
| Average A and G-type Toluene = | 0.2033 lbs/hr |
| Average Other Type Toluene = | 0.0033 lbs/hr |
| Average A and G-type Toluene = | 600 lbs/yr |
| Average Other Type Toluene = | 9 lbs/yr |
| Total Toluene = | 609 lbs/yr |
| Total Average Toluene = | 0.2065 lbs/hr |

A similar DuPont facility in Louisville reported 0.054 lb/charge of ACR emissions for the types Pontchartrain will be making.

Conservatively assume ACR emissions are the same as the Louisville facility even with a larger, more efficient 2 C condenser.

| | |
|-------------------------|------------------|
| ACR per Charge = | 0.054 lbs/charge |
| Maximum ACR Emissions = | 0.120 lbs/hr |
| Annual ACR Emissions = | 364 lbs/yr |
| Average ACR Emissions = | 0.120 lbs/hr |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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Decompress Sampling

After stabilization, W types are cooled to 25 C, G-Types cooled to 33 C (GW to 30 C) and A-types are about 20 C.

After stabilization, the PK is vented for sampling through the sample port.

Once in a while, floating coag will be seen at this time and the manhole must be opened for skimming after stabilization.

Venting down occurs when the vast majority of the CD is converted to polymer and entrapped in the polymer, and after cool down of W types, so CD concentration in the vapor will be much less than during charging.

Although it is almost completely reacted in the process, assume ACR is still present.

Assume worst case of nitrogen saturated with CD, toluene, ACR and H₂O and the Slocum vapor pressure for CD used in EST calculations.

| | | |
|--------------------------------------|---|-------------------------------|
| Temperature = | 25 C | |
| Vapor Pressure of CD = | 189 mm Hg | |
| Vapor Pressure of Toluene = | 28.40 mm Hg | |
| Vapor Pressure of ACR = | 42.28 mm Hg | |
| Vapor Pressure of H ₂ O = | 23.6 mm Hg | |
| Total Vapor = | 0.002550 moles/ft ³ | |
| CD Vapor = | 0.000634 moles/ft ³ | 24.87 mole % CD |
| CD Vapor = | 0.056158 lbs CD/ft ³ total vapor at saturation | |
| Toluene Vapor = | 0.000095 moles/ft ³ | 3.74 mole % toluene |
| Toluene Vapor = | 0.008782 lbs toluene/ft ³ total vapor at saturation | |
| ACR Vapor = | 0.000142 moles/ft ³ | 5.56 mole % ACR |
| ACR Vapor = | 0.017450 lbs ACR/ft ³ total vapor at saturation | |
| H ₂ O Vapor = | 0.000079 moles/ft ³ | 3.11 mole % H ₂ O |
| H ₂ O Vapor = | 0.001426 lbs H ₂ O/ft ³ total vapor at saturation | |
| Nitrogen Vapor = | 0.001600 moles/ft ³ | 62.73 mole % H ₂ O |
| Nitrogen Vapor = | 0.053274 lbs N ₂ /ft ³ total vapor at saturation | |

Assume after the vent down occurs, 5 cfm nitrogen purge channels to vent and carries very little CD with it.



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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| | | |
|-----------------------------------|----------------------------|---------------|
| Total Volume of LPK = | 825 ft3 | |
| Vapor Volume of LPK = | 194 ft3 when fully charged | |
| Amount of Vapor Decompression = | 13.23 ft3 | exit the vent |
| CD in Vapor Decompressed = | 3.29 ft3 | exit the vent |
| CD in Vapor Decompressed = | 0.18 lbs/charge | exit the vent |
| CD in Vapor Decompressed = | 1246 lbs/yr | exit the vent |
| Toluene in Vapor Decompressed = | 0.49 ft3 | exit the vent |
| Toluene in Vapor Decompressed = | 0.0043 lbs/charge | exit the vent |
| Toluene in Vapor Decompressed = | 29.28 lbs/yr | exit the vent |
| ACR in Vapor Decompressed = | 0.74 ft3 | exit the vent |
| ACR in Vapor Decompressed = | 0.01 lbs/charge | exit the vent |
| ACR in Vapor Decompressed = | 86.60 lbs/yr | exit the vent |
| N2 in Vapor Decompressed = | 8.30 ft3 | exit the vent |
| H2O in Vapor Decompressed = | 0.41 ft3 | exit the vent |
| 0.5 N2 Purge = | 0.00 ft3/min | exit the vent |
| Venting Time = | 1 min | |
| Total N2 Flow = | 8.30 ft3/min | exit the vent |
| Total Venting Rate = | 13.23 ft3/min | exit the vent |
| % CD of Total Venting Rate = | 24.87 % CD | exit the vent |
| % Toluene of Total Venting Rate = | 3.74 % toluene | exit the vent |
| % ACR of Total Venting Rate = | 5.56 % ACR | exit the vent |
| Venting Temperature = | 25 C | exit the vent |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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The PK emissions are directed to the vent condenser.

Using the same assumptions as for final emulsification venting calculations for initial vent down after stabilization,

| | |
|--------------------------|--|
| Temperature = | 6 C |
| Total Vapor = | 0.002724 moles/ft3 |
| CD Vapor Pressure = | 104.34 mm Hg |
| CD Vapor = | 0.00037399 moles/ft3 13.73 mole % CD |
| CD Vapor = | 0.03311293 lbs CD/ft3 total vapor |
| Toluene Vapor Pressure = | 9.77 mm Hg |
| Toluene Vapor = | 0.000035 moles/ft3 1.29 mole % toluene |
| Toluene Vapor = | 0.003226 lbs toluene/ft3 total vapor |
| ACR Vapor Pressure = | 16.39 mm Hg |
| ACR Vapor = | 0.000059 moles/ft3 2.16 mole % ACR |
| ACR Vapor = | 0.007226 lbs ACR/ft3 total vapor |
| H2O Vapor Pressure = | 7.36 mm Hg |
| H2O Vapor = | 0.00002637 moles/ft3 0.97 mole % H2O |
| H2O Vapor = | 0.00233502 lbs H2O/ft3 total vapor |
| N2 Flow = | 8.30 ft3/min |
| % N2 of Total Flow = | 85.30 % |
| Total Venting Rate = | 9.73 ft3/min |
| CD Venting Rate = | 1.3357 ft3/min |
| CD Venting Rate = | 0.3222 lb/min |
| CD Venting Rate = | 0.3222 lbs/charge |
| CD Venting Rate = | 2172 lbs/yr |
| Toluene Venting Rate = | 0.1251 ft3/min |
| Toluene Venting Rate = | 0.0314 lb/min |
| Toluene Venting Rate = | 0.0314 lbs/charge |
| Toluene Venting Rate = | 212 lbs/yr |
| ACR Venting Rate = | 0.2098 ft3/min |
| ACR Venting Rate = | 0.0703 lb/min |
| ACR Venting Rate = | 0.0703 lbs/charge |
| ACR Venting Rate = | 474 lbs/yr |
| H2O Flow = | 0.0942 ft3/min |
| H2O Flow = | 0.1992 lb/min |
| H2O Flow = | 0.1992 lbs/charge |
| H2O Flow = | 1343 lbs/yr |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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Vent Open Sampling

In sample mode, the vent valve is opened, and the nitrogen purge closed off
This period is for 1 minute; there will be some low concentration CD flows to the vent condenser for 1 minute.
This essentially repeats the emission for Decompress Sampling

Decompress for Wash

After dropping the charge and displacing with 0.5 psig N₂, the PK is vented down for water washing through the manway.
Normally, the manway with sight glass does not need to be opened to inspect the LPK is empty after dropping. However, once in a while the manhole must be opened to clean out popcorn or coag.
For these cases use data from decompress sampling for initial CD concentration early in the charging sequence (2% by volume) and assume that the venting occurs quickly
It is assumed that toluene and ACR concentrations are proportional to the CD concentration.
Assume after the vent down occurs, nitrogen purge channels to vent and carries very little CD with it.

| | | |
|--|--|---------------------|
| Venting Temperature = | 25 C | |
| Total Volume of LPK = | 825 ft ³ | |
| Amount of Vapor Decompression = | 28 ft ³ | exit the vent |
| Total Vapor = | 0.002550 moles/ft ³ | |
| CD Vapor = | 0.000051 moles/ft ³ | 2.00 mole % CD |
| CD Vapor = | 0.004516 lbs CD/ft ³ total vapor | |
| Toluene Vapor = | 0.000008 moles/ft ³ | 0.30 mole % toluene |
| Toluene Vapor = | 0.000706 lbs toluene/ft ³ total vapor | |
| ACR Vapor = | 0.000011 moles/ft ³ | 0.45 mole % ACR |
| ACR Vapor = | 0.001403 lbs ACR/ft ³ total vapor | |
| CD in Vapor Decompressed = | 0.561 ft ³ | exit the vent |
| CD in Vapor Decompressed = | 0.127 lbs/charge | exit the vent |
| CD in Vapor Decompressed = | 855 lbs/yr | exit the vent |
| Toluene in Vapor Decompressed = | 0.084 ft ³ | exit the vent |
| Toluene in Vapor Decompressed = | 0.020 lbs/charge | exit the vent |
| Toluene in Vapor Decompressed = | 134 lbs/yr | exit the vent |
| ACR in Vapor Decompressed = | 0.126 ft ³ | exit the vent |
| ACR in Vapor Decompressed = | 0.039 lbs/charge | exit the vent |
| ACR in Vapor Decompressed = | 266 lbs/yr | exit the vent |
| N ₂ in Vapor Decompressed = | 27.51 ft ³ | exit the vent |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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| | | |
|-----------------------------------|----------------|---------------|
| 0.5 psig N2 Purge = | 5.00 ft3/min | exit the vent |
| Venting Time = | 1 min | |
| Total N2 Flow = | 32.51 ft3/min | exit the vent |
| Total Venting Rate = | 33.07 ft3/min | exit the vent |
| % CD of Total Venting Rate = | 1.70 % CD | exit the vent |
| % Toluene of Total Venting Rate = | 0.26 % toluene | exit the vent |
| % ACR of Total Venting Rate = | 0.38 % ACR | exit the vent |
| Venting Temperature = | 25 C | exit the vent |

The PK emissions are directed to the vent condenser.

Make the same assumptions as for final emulsification venting calculations.

Since nitrogen is much less than saturation at exit condenser conditions, condenser inlet and exit CD, toluene and ACR concentrations are essentially the same.

| | |
|------------------------|------------------|
| Total Venting Rate = | 33.07 ft3/min |
| CD Venting Rate = | 0.561377 ft3/min |
| CD Venting Rate = | 0.135394 lbs/min |
| CD Venting Rate = | 0.14 lbs/charge |
| CD Venting Rate = | 913 lbs/yr |
| Toluene Venting Rate = | 0.084360 ft3/min |
| Toluene Venting Rate = | 0.021173 lbs/min |
| Toluene Venting Rate = | 0.02 lbs/charge |
| Toluene Venting Rate = | 143 lbs/yr |
| ACR Venting Rate = | 0.125573 ft3/min |
| ACR Venting Rate = | 0.042070 lbs/min |
| ACR Venting Rate = | 0.04 lbs/charge |
| ACR Venting Rate = | 284 lbs/yr |

Vent Open for Wash

For PK wash, PK is empty and filled with nitrogen; vent valve is open, but nitrogen purge is off. There is a very low flow of vapor with some low CD concentration to condenser for 10 minutes. chimney effect will draw air in through manway and out the vent, located nearby. There is no depressurization, so flow is de minimus and can be neglected.



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Air Emissions Calculation Sheet

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Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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Decompress to Emulsify

Before allowing emulsification to begin (vent valve to open), 0.3 psig must be detected in the LPK.

A vent down from 0.3 to 0 psig occurs at the start of emulsification.

For this case use data from decompress sampling for initial CD concentration early in the charging sequence inlet the vent condenser (2% by volume) since the venting occurs quickly.

It is assumed that toluene and ACR concentrations are proportional to the CD concentration.

| | | |
|-----------------------------------|--------------------------------------|---------------------|
| Venting Temperature = | 25 C | |
| Total Volume of LPK = | 825 ft3 | |
| Amount of Vapor Decompression = | 16.84 ft3 | exit the vent |
| Total vapor = | 0.002550 moles/ft3 | |
| CD Vapor = | 0.000051 moles/ft3 | 2.00 mole % CD |
| CD Vapor = | 0.004516 lbs CD/ft3 total vapor | |
| Toluene Vapor = | 0.000008 moles/ft3 | 0.30 mole % toluene |
| Toluene Vapor = | 0.000706 lbs toluene/ft3 total vapor | |
| ACR Vapor = | 0.000011 moles/ft3 | 0.45 mole % ACR |
| ACR Vapor = | 0.001403 lbs ACR/ft3 total vapor | |
| CD in Vapor Decompressed = | 0.337 ft3 | exit the vent |
| CD in Vapor Decompressed = | 0.076 lbs/charge | exit the vent |
| CD in Vapor Decompressed = | 513 lbs/yr | exit the vent |
| Toluene in Vapor Decompressed = | 0.050616 ft3 | exit the vent |
| Toluene in Vapor Decompressed = | 0.011895 lbs/charge | exit the vent |
| Toluene in Vapor Decompressed = | 80 lbs/yr | exit the vent |
| ACR in Vapor Decompressed = | 0.075344 ft3 | exit the vent |
| ACR in Vapor Decompressed = | 0.023634 lbs/charge | exit the vent |
| ACR in Vapor Decompressed = | 159 lbs/yr | exit the vent |
| N2 in Vapor Decompressed = | 16.50 ft3 | exit the vent |
| 0.5 N2 Purge = | 5.00 ft3/min | exit the vent |
| Venting Time = | 1 min | |
| Total N2 Flow = | 21.50 ft3/min | exit the vent |
| Total Venting Rate = | 21.84 ft3/min | exit the vent |
| % CD of Total Venting Rate = | 1.54 % CD | exit the vent |
| % Toluene of Total Venting Rate = | 0.23 % toluene | exit the vent |
| % ACR of Total Venting Rate = | 0.34 % ACR | exit the vent |
| Venting Temperature = | 25 C | exit the vent |

**RTP**

Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

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The PK emissions are directed to the vent condenser.

Make the same assumptions as for final emulsification venting calculations.

Since nitrogen is much less than saturation at exit condenser conditions, condenser inlet and exit CD concentration are essentially the same.

For vent down prior to emulsification

Since nitrogen is much less than saturation at exit condenser conditions -

| | |
|------------------------|-------------------------------|
| Total Venting Rate = | 21.84 ft ³ /min |
| CD Venting rate = | 0.336826 ft ³ /min |
| CD Venting rate = | 0.081236 lbs/min |
| CD Venting rate = | 0.08 lbs/charge |
| CD Venting rate = | 548 lbs/yr |
| Toluene Venting Rate = | 0.050616 ft ³ /min |
| Toluene Venting Rate = | 0.012704 lbs/min |
| Toluene Venting Rate = | 0.01 lbs/charge |
| Toluene Venting Rate = | 86 lbs/yr |
| ACR Venting Rate = | 0.075344 ft ³ /min |
| ACR Venting Rate = | 0.025242 lbs/min |
| ACR Venting Rate = | 0.03 lbs/charge |
| ACR Venting Rate = | 170 lbs/yr |

Summary

ACR is potentially emitted at a level of 0.54 tpy, although it is not present in the worst case product. Therefore, ACR totals are not part of the annual VOC emission totals and are calculated only for reference.

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 68685 | 7.841 | 35.631 | 34.342 |
| Chloroprene | 67635 | 7.721 | 35.171 | 33.818 |
| 1,2-Dichlorobenze | 10 | 0.001 | 0.001 | 0.005 |
| Toluene | 1050 | 0.120 | 0.340 | 0.525 |
| Total HAPs | 68695 | 7.842 | 35.513 | 34.347 |
| Total TAPs | 68695 | 7.842 | 35.513 | 34.347 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Emulsion Storage Tanks Common Vent & Cap

TEMPO ID: GRP0008

Point Source ID No.: 1700-5

Page 1 of 1

Basis:

Common vent for Unstripped Emulsion Storage Tank No. 6 (1700-5.3/EQT0150), Unstripped Emulsion Storage Tank No. 7 (1700-5.4/EQT0151), Unstripped Emulsion Storage Tank No. 8 (1700-5.5/EQT0152), Unstripped Emulsion Storage Tank No. 10 (1700-5.6/EQT0153), Unstripped Emulsion Storage Tank No. 11 (1700-5.7/EQT0154), and Unstripped Emulsion Storage Tank No. 14 (1700-5.8/EQT0155).

Emissions:

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 5898 | 0.673 | - | 2.949 |
| Chloroprene | 5826 | 0.665 | - | 2.913 |
| 1,2-Dichlorobenzene | 0.004 | 0.000 | - | 0.000 |
| Toluene | 51 | 0.006 | - | 0.025 |
| Total HAPs | 5877 | 0.671 | - | 2.938 |
| Total TAPs | 5877 | 0.671 | - | 2.938 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A

Page 1 of 4

Basis:

No. 6 EST is used solely for storage of unstripped WBG-2 emulsion or stripped emulsion of other types. WBG-2 is fully converted, so CD emissions are de minimus even from unstripped WBG-2 emulsion.

The unstripped emulsion (USE) tank is vented down to atmospheric pressure and the nitrogen blanket which enters the top of the tank is turned off before opening the manway.

Ventilation around the two stripper feed strainers and ventilation on the popcorn drum and emulsion drum are connected to this blower. This is the source of CD to this emission point. Based on operator estimates, volume calculations and field observations, 5 to 6 gallons of emulsion drains from the strainer each cleaning.

When the emulsion drum is full, it is pumped back into the USE tank. When the popcorn drum is full it is moved to the drum pad and steamed before landfill disposal.

A strainer is to be cleaned each shift (12 hrs) minimum.

Strainer cleaning frequency does not correlate with stripper feed rate or strippers on line but does correlate with type and type changes (A's to W's in particular)

Per actual practice, while on A-types the frequency is about once/8 hr and once/12 hr while on W-types.

Emissions are based on spot sampling data conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 3.4 ppm with a maximum concentration of 4.7 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD.

Conservatively assume ACR is still present in the material.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------|-----------------------|
| Rated Capacity of Blower = | 7400 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Average CD in Air Exhausted = | 3.4 ppm CD by volume |
| Maximum CD in Air Exhausted = | 5.17 ppm CD by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 25 °C |
| Pressure = | 14.696 psia |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A

Page 2 of 4

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.0252 cfm CD

Using the Ideal Gas Law,

Average CD Emissions = 0.000064 moles CD/minute

Average CD Emissions = 0.005682 lbs CD/minute

Average CD Emissions = 0.341 lbs CD/hour

Average CD Emissions = 2986 lbs/yr

Average CD Emissions = 1.49 tons/yr

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 189.00 mm Hg

Total Vapor = 0.002550 moles/ft³

Mole Fraction CD = 0.00034 %

CD Vapor = 0.00000001 moles/ft³

CD Partial Pressure = 0.003 mm Hg

Ratio = 0.000014

V.P. of Toluene at Saturation = 28.40 mm Hg

Toluene Partial Pressure = 0.0004 mm Hg

Toluene Vapor = 0.000000001 moles/ft³

Toluene Vapor = 0.00001 moles/min

Toluene Vapor = 0.001 lb/min

Toluene Vapor = 0.05 lb/hr

Toluene Vapor = 0.23 tpy



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Air Emissions Calculation Sheet

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Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A

Page 3 of 4

ACR

| | |
|-----------------------------|-----------------------------------|
| Ratio = | 0.000014 |
| V.P. of ACR at Saturation = | 42.28 mm Hg |
| ACR Partial Pressure = | 0.0006 mm Hg |
| ACR Vapor = | 0.000000002 moles/ft ³ |
| ACR Vapor = | 0.00001 moles/min |
| ACR Vapor = | 0.0018 lb/min |
| ACR Vapor = | 0.11 lb/hr |
| ACR Vapor = | 0.46 tpy |

Maximum Emission Rates

Using given information,

Maximum CD Emissions = 0.0383 cfm CD

Using the Ideal Gas Law,

| | |
|------------------------|--------------------------|
| Maximum CD Emissions = | 0.000098 moles CD/minute |
| Maximum CD Emissions = | 0.008639 lbs CD/minute |
| Maximum CD Emissions = | 0.518 lbs CD/hour |



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Air Emissions Calculation Sheet

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Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A

Page 4 of 4

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 189.00 mm Hg
Total Vapor = 0.002550 moles/ft³
Mole Fraction CD = 0.000517 %
CD Vapor = 0.00000001 moles/ft³
CD Partial Pressure = 0.004 mm Hg
Ratio = 0.000021
V.P. of Toluene at Saturation = 28.40 mm Hg
Toluene Partial Pressure = 0.0006 mm Hg
Toluene Vapor = 0.000000002 moles/ft³
Toluene Vapor = 0.00001 moles/min
Toluene Vapor = 0.0014 lb/min
Toluene Vapor = 0.08 lb/hr

ACR

Ratio = 0.000021
V.P. of ACR at Saturation = 42.28 mm Hg
ACR Partial Pressure = 0.0009 mm Hg
ACR Vapor = 0.000000003 moles/ft³
ACR Vapor = 0.00002 moles/min
ACR Vapor = 0.0027 lb/min
ACR Vapor = 0.16 lb/hr

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 4381 | 0.500 | 0.761 | 2.191 |
| Chloroprene | 2986 | 0.341 | 0.518 | 1.493 |
| Toluene | 467 | 0.053 | 0.081 | 0.234 |
| Total HAPs | 3453 | 0.394 | 0.599 | 1.727 |
| Total TAPs | 3453 | 0.394 | 0.599 | 1.727 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page 1 of 4

Basis:

The manways and drop strainers on each PK are equipped with ventilation systems.

The strainer cleanings solids drums and emulsion drums are equipped with lids and protective ventilation.

Since the manway is seldom opened when the PK is charged, emissions should be small.

The manway on each PK is opened once per day for inhibitor spraying of the dome. Since this is done after the charge is completed and cooled, CD concentrations are low and emissions should be low.

Opening and cleaning the strainer after dropping the charge and water flushing results in emissions.

Emissions are based on spot sampling data for the exhaust blower for PK 3, 4 & 5 conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 14.45 ppm with a maximum concentration of 15.37 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD.

Conservatively assume ACR is still present in the material.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------|------------------------|
| Rated Capacity of Blower = | 6900 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Average CD in Air Exhausted = | 14.45 ppm CD by volume |
| Maximum CD in Air Exhausted = | 16.91 ppm CD by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 30 °C |
| Pressure = | 14.696 psia |

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.0997 cfm CD

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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page 2 of 4

Using the Ideal Gas Law,

| | |
|------------------------|--------------------------|
| Average CD Emissions = | 0.000250 moles CD/minute |
| Average CD Emissions = | 0.022144 lbs CD/minute |
| Average CD Emissions = | 1.329 lbs CD/hour |
| Average CD Emissions = | 11639 lbs/yr |
| Average CD Emissions = | 5.82 tons/yr |

Toluene

Using the Ideal Gas Law,

| | |
|---------------------------------|-----------------------------------|
| V.P. of CD at Saturation = | 280.10 mm Hg |
| Total Vapor = | 0.002508 moles/ft ³ |
| Mole Fraction CD = | 0.001445 % |
| CD Vapor = | 0.00000004 moles/ft ³ |
| CD Partial Pressure = | 0.011 mm Hg |
| Ratio = | 0.000039 |
| V.P. of Toluene at Saturation = | 36.61 mm Hg |
| Toluene Partial Pressure = | 0.0014 mm Hg |
| Toluene Vapor = | 0.000000005 moles/ft ³ |
| Toluene Vapor = | 0.00003 moles/min |
| Toluene Vapor = | 0.003 lb/min |
| Toluene Vapor = | 0.18 lb/hr |
| Toluene Vapor = | 0.79 tpy |

ACR

| | |
|-----------------------------|----------------------------------|
| Ratio = | 0.000039 |
| V.P. of ACR at Saturation = | 53.19 mm Hg |
| ACR Partial Pressure = | 0.0021 mm Hg |
| ACR Vapor = | 0.00000001 moles/ft ³ |
| ACR Vapor = | 0.00005 moles/min |
| ACR Vapor = | 0.0058 lb/min |
| ACR Vapor = | 0.35 lb/hr |
| ACR Vapor = | 1.54 tpy |



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Air Emissions Calculation Sheet

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Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page 3 of 4

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.1167 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000293 moles CD/minute

Maximum CD Emissions = 0.025910 lbs CD/minute

Maximum CD Emissions = 1.555 lbs CD/hour

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 280.10 mm Hg

Total Vapor = 0.002508 moles/ft³

Mole Fraction CD = 0.0016907 %

CD Vapor = 0.00000004 moles/ft³

CD Partial Pressure = 0.013 mm Hg

Ratio = 0.000046

V.P. of Toluene at Saturation = 36.61 mm Hg

Toluene Partial Pressure = 0.0017 mm Hg

Toluene Vapor = 0.00000001 moles/ft³

Toluene Vapor = 0.00004 moles/min

Toluene Vapor = 0.0035 lb/min

Toluene Vapor = 0.21 lb/hr



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page 4 of 4

ACR

Ratio = 0.000046
V.P. of ACR at Saturation = 53.19 mm Hg
ACR Partial Pressure = 0.0024 mm Hg
ACR Vapor = 0.00000001 moles/ft³
ACR Vapor = 0.00006 moles/min
ACR Vapor = 0.0068 lb/min
ACR Vapor = 0.41 lb/hr

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--|--|--------------------------------|
| Total VOC | 16292 | 1.860 | 2.176 | 8.146 |
| Chloroprene | 11639 | 1.329 | 1.555 | 5.820 |
| Toluene | 1583 | 0.181 | 0.211 | 0.792 |
| Total HAPs | 13222 | 1.509 | 1.766 | 6.611 |
| Total TAPs | 13222 | 1.509 | 1.766 | 6.611 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page 1 of 4

Basis:

The manways, sample ports and drop strainers on each PK are equipped with ventilation systems. The strainer cleanings solids drums and emulsion drums are equipped with lids and protective ventilation.

With the changes in PK nitrogen blanketing and CD concentrations being low at the end of the charge, the emissions from the sample port should be very small

Since the manhole is seldom opened when the PK is charged, emissions should be small

The manway on each PK is to be opened once per day for inhibitor spraying of the dome. Since this is done after the charge is completed and cooled, CD concentrations are low and emissions should be low.

Opening and cleaning the strainer after dropping the charge and water flushing results in emissions. Emissions are based on spot sampling data conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 14.45 ppm with a maximum concentration of 15.37 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD.

Conservatively assume ACR is still present in the material.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------|------------------------|
| Rated Capacity of Blower = | 8500 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Average CD in Air Exhausted = | 14.45 ppm CD by volume |
| Maximum CD in Air Exhausted = | 16.91 ppm CD by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 30 °C |
| Pressure = | 14.696 psia |

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.1228 cfm CD



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page 2 of 4

Using the Ideal Gas Law,

| | |
|------------------------|--------------------------|
| Average CD Emissions = | 0.000308 moles CD/minute |
| Average CD Emissions = | 0.027279 lbs CD/minute |
| Average CD Emissions = | 1.637 lbs CD/hour |
| Average CD Emissions = | 14338 lbs/yr |
| Average CD Emissions = | 7.17 tons/yr |

Toluene

Using the Ideal Gas Law,

| | |
|---------------------------------|-----------------------------------|
| V.P. of CD at Saturation = | 280.10 mm Hg |
| Total Vapor = | 0.002508 moles/ft ³ |
| Mole Fraction CD = | 0.001445 % |
| CD Vapor = | 0.00000004 moles/ft ³ |
| CD Partial Pressure = | 0.011 mm Hg |
| Ratio = | 0.000039 |
| V.P. of Toluene at Saturation = | 36.61 mm Hg |
| Toluene Partial Pressure = | 0.0014 mm Hg |
| Toluene Vapor = | 0.000000005 moles/ft ³ |
| Toluene Vapor = | 0.00004 moles/min |
| Toluene Vapor = | 0.004 lb/min |
| Toluene Vapor = | 0.22 lb/hr |
| Toluene Vapor = | 0.98 tpy |

ACR

| | |
|-----------------------------|----------------------------------|
| Ratio = | 0.000039 |
| V.P. of ACR at Saturation = | 53.19 mm Hg |
| ACR Partial Pressure = | 0.0021 mm Hg |
| ACR Vapor = | 0.00000001 moles/ft ³ |
| ACR Vapor = | 0.00006 moles/min |
| ACR Vapor = | 0.0072 lb/min |
| ACR Vapor = | 0.43 lb/hr |
| ACR Vapor = | 1.89 tpy |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page 3 of 4

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.1437 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000360 moles CD/minute

Maximum CD Emissions = 0.031918 lbs CD/minute

Maximum CD Emissions = 1.915 lbs CD/hour

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 280.10 mm Hg

Total Vapor = 0.002508 moles/ft³

Mole Fraction CD = 0.0016907 %

CD Vapor = 0.00000004 moles/ft³

CD Partial Pressure = 0.013 mm Hg

Ratio = 0.000046

V.P. of Toluene at Saturation = 36.61 mm Hg

Toluene Partial Pressure = 0.0017 mm Hg

Toluene Vapor = 0.00000001 moles/ft³

Toluene Vapor = 0.00005 moles/min

Toluene Vapor = 0.0043 lb/min

Toluene Vapor = 0.26 lb/hr



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page 4 of 4

ACR

Ratio = 0.000046
V.P. of ACR at Saturation = 53.19 mm Hg
ACR Partial Pressure = 0.0024 mm Hg
ACR Vapor = 0.00000001 moles/ft³
ACR Vapor = 0.00007 moles/min
ACR Vapor = 0.0084 lb/min
ACR Vapor = 0.51 lb/hr

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 20070 | 2.291 | 2.681 | 10.035 |
| Chloroprene | 14338 | 1.637 | 1.915 | 7.169 |
| Toluene | 1950 | 0.223 | 0.260 | 0.975 |
| Total HAPs | 16288 | 1.859 | 2.176 | 8.144 |
| Total TAPs | 16288 | 1.859 | 2.176 | 8.144 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Solution Makeup Manhole Common Vent

TEMPO ID: GRP0006

Point Source ID No.: 1700-14B

Page 1 of 4

Basis:

Common vent for Acetic Acid Make-Up Tank (1700-14B.1/EQT0137), Acetic Acid Hold-Up Tank (1700-14B.2/EQT00138), and Stabilizer & Catalyst Tanks Manholes Vent (1700-14B.3/RLP0013).

Emissions:

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| PM-10 | 131 | 1.473 | 9.092 | 0.066 |
| Total VOC | 1119 | 0.128 | 0.602 | 0.559 |
| Chloroprene | 738 | 0.084 | 0.093 | 0.369 |
| Toluene | 242 | 0.028 | 0.494 | 0.121 |
| Total HAPs | 980 | 0.112 | 0.586 | 0.490 |
| Total TAPs | 980 | 0.112 | 0.586 | 0.490 |



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Air Emissions Calculation Sheet

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Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Solution Makeup Manhole Common Vent

TEMPO ID: GRP0006

Point Source ID No.: 1700-14B

Page 2 *of* 4



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
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Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page 1 of 4

Basis:

Based on 10 hr TWA area data developed between 1999 and 2001, the average concentration of CD in the building air is 0.56 ppmv.

Monitoring data for toluene between February 2001 and September 2002 indicate an average concentration of 0.176 ppm. Toluene is emitted during makeup of toluene based stabilizer when the manhole is open.

There is no ACR present in toluene based stabilizer, and no realistic opportunity for ACR to be present in the ambient air around the Stabilizer tanks.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration for CD and toluene.

PTZ, TETD, Lowinox, and Neozone A are added to the makeup tanks through the manholes resulting in particulate emissions.

Estimated that 0.1% of the TETD, Lowinox, PTZ and Neozone A transferred becomes airborne.

Estimated that 50% of the airborne dust is captured by exhaust system. Remainder is captured in building.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|---------------------------------|---|
| Rated Capacity of Blower = | 11100 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Amount of Time Discharging = | 8760 hours/yr while on toluene stabilizer types |
| Average CD in Air Exhausted = | 0.56 ppm CD by volume |
| Maximum CD in Air Exhausted = | 0.62 ppm CD by volume |
| Avg. Toluene in Air Exhausted = | 0.176 ppm toluene by volume |
| Max. Toluene in Air Exhausted = | 3.1464 ppm toluene by volume |
| Avg. ACR in Air Exhausted = | 0 ppm ACR by volume |
| Max. ACR in Air Exhausted = | 0 ppm ACR by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.4 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 25 °C |
| Pressure = | 14.696 psia |
| PTZ Used = | 2650 lb/yr |
| Fraction Airborne = | 0.1 % |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page 2 of 4

| | |
|--------------------------------|--------------|
| TETD Used = | 191015 lb/yr |
| Lowinox Used = | 21660 lb/yr |
| Neozone A Used = | 47184 lb/yr |
| Fraction Airborne = | 0.1 % |
| Average Solids Addition Time = | 89 hours |
| Minimum Solids Addition Time = | 14.44 hours |

Average VOC Emission Rates

Chloroprene

Using given information,

| | |
|------------------------|---------------|
| Average CD Emissions = | 0.0062 cfm CD |
|------------------------|---------------|

Using the Ideal Gas Law,

| | |
|------------------------|-----------------------|
| Average CD Emissions = | 0.000016 moles/minute |
| Average CD Emissions = | 0.001404 lbs/minute |
| Average CD Emissions = | 0.084 lbs/hour |
| Average CD Emissions = | 738 lbs/yr |
| Average CD Emissions = | 0.37 tons/yr |

Toluene

Using given information,

| | |
|-----------------------------|--------------------|
| Average Toluene Emissions = | 0.0020 cfm toluene |
|-----------------------------|--------------------|

Using the Ideal Gas Law,

| | |
|-----------------------------|-----------------------|
| Average Toluene Emissions = | 0.000005 moles/minute |
| Average Toluene Emissions = | 0.000460 lbs/minute |
| Average Toluene Emissions = | 0.028 lbs/hour |
| Average Toluene Emissions = | 242 lbs/yr |
| Average Toluene Emissions = | 0.12 tons/yr |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page 3 of 4

Maximum VOC Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.0068 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000017 moles CD/minute

Maximum CD Emissions = 0.001544 lbs CD/minute

Maximum CD Emissions = 0.093 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions = 0.0349 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = 0.000089 moles/minute

Maximum Toluene Emissions = 0.008231 lbs/minute

Maximum Toluene Emissions = 0.494 lbs/hour



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page 4 of 4

PM/PM-10 Emissions

Capture Efficiency = 50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Efficiency / 104 hr/yr

$$\begin{aligned} &= (2650 \text{ lb/yr} \times 0.1\% + 259859 \text{ lb/yr} \times 0.1\%) \times 50\% / 89 \text{ hr/yr} \\ &= 1.473 \text{ lb/hr} \\ &= 0.0656 \text{ tpy} \end{aligned}$$

Maximum PM/PM-10 Emission Rates

Capture Efficiency = 50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fract. Airborne x Capture Efficiency / 16.88 hr/yr

$$\begin{aligned} &= (2650 \text{ lb/yr} \times 0.1\% + 259859 \text{ lb/yr} \times 0.1\%) \times 50\% / 14.44 \text{ hr/yr} \\ &= 9.092 \text{ lb/hr} \end{aligned}$$

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| PM-10 | 131 | 1.473 | 9.092 | 0.066 |
| Total VOC | 980 | 0.112 | 0.586 | 0.490 |
| Chloroprene | 738 | 0.084 | 0.093 | 0.369 |
| Toluene | 242 | 0.028 | 0.494 | 0.121 |
| Total HAPs | 980 | 0.112 | 0.586 | 0.490 |
| Total TAPs | 980 | 0.112 | 0.586 | 0.490 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jets Emissions Cap

TEMPO ID: GRP0012

Point Source ID No.: 1700-20 CAP

Page 1 of 1

Basis:

Emissions cap for CD Refining Column Jet (1700-20/EQT0139) and CD Refining Column Jet (Spare) (1700-20A/EQT00140).

Emissions:

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| NOx | 6597 | 0.753 | 0.828 | 3.298 |
| Total VOC | 24801 | 2.831 | 3.114 | 12.401 |
| Chloroprene | 24794 | 2.830 | 3.113 | 12.397 |
| Toluene | 7 | 0.001 | 0.001 | 0.003 |
| Ammonia | 0.07 | 0.000008 | 0.000009 | 0.00004 |
| Total HAPs | 24801 | 2.831 | 3.114 | 12.401 |
| Total TAPs | 24801 | 2.831 | 3.114 | 12.401 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20

Page 1 of 5

Basis:

Emissions are based on sampling data on March 12, 2002 and March 21, 2002 by METCO Environmental.

On March 12, 2002 type AD was being produced, which includes toluene.

On March 21, 2002 type WHV was being produced which does not include toluene.

The highest vent rate measured is 4.584 dscfm.

The highest NOx concentration measured is 22945.5 ppmv.

The highest chloroprene (CD) concentration measured is 44807 ppmv.

The highest toluene concentration measured is 12 ppmv.

Ammonia was measured at less than 0.68 ppmv. Conservatively assume a concentration of 0.68 ppmv.

The maximum concentrations are estimated to be 10% greater than the maximum measured concentration.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------|----------------------------|
| Vent Rate = | 4.584 cfm |
| Amount of Time Venting = | 8760 hours/yr |
| Average NOx in Air Vented = | 22945.5 ppm NOx by volume |
| Maximum NOx in Air Vented = | 25240 ppm NOx by volume |
| Average CD in Air Vented = | 44807 ppm CD by volume |
| Maximum CD in Air Vented = | 49288 ppm CD by volume |
| Avg. Toluene in Air Vented = | 12 ppm toluene by volume |
| Max. Toluene in Air Vented = | 13.2 ppm toluene by volume |
| Avg. Ammonia in Air Vented = | 0.68 ppm ammonia by volume |
| Max. Ammonia in Air Vented = | 0.75 ppm ammonia by volume |
| Molecular Weight of NOx = | 46 lb/lb-mole |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.4 lb/lb-mole |
| Molecular Weight of Ammonia = | 17 lb/lb-mole |
| Temperature = | 20 °C |
| Pressure = | 14.696 psia |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20

Page 2 of 5

Average Emission Rates

Nitrogen Dioxide

Using given information,

Average NOx Emissions = 0.11 cfm NOx

Using the Ideal Gas Law,

Average NOx Emissions = 0.000273 moles/minute

Average NOx Emissions = 0.012551 lbs/minute

Average NOx Emissions = 0.753 lbs/hour

Average NOx Emissions = 6597 lbs/yr

Average NOx Emissions = 3.30 tons/yr

Chloroprene

Using given information,

Average CD Emissions = 0.2054 cfm CD

Using the Ideal Gas Law,

Average CD Emissions = 0.000533 moles/minute

Average CD Emissions = 0.047173 lbs/minute

Average CD Emissions = 2.830 lbs/hour

Average CD Emissions = 24794 lbs/yr

Average CD Emissions = 12.40 tons/yr



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20

Page 3 of 5

Toluene

Using given information,

Average Toluene Emissions = 0.0001 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions = 0.0000001 moles/minute

Average Toluene Emissions = 0.000013 lbs/minute

Average Toluene Emissions = 0.0008 lbs/hour

Average Toluene Emissions = 7 lbs/yr

Average Toluene Emissions = 0.003 tons/yr

Ammonia

Using given information,

Average Ammonia Emissions = 0.000003 cfm ammonia

Using the Ideal Gas Law,

Average Ammonia Emissions = 0.00000001 moles/minute

Average Ammonia Emissions = 0.0000001 lbs/minute

Average Ammonia Emissions = 0.000008 lbs/hour

Average Ammonia Emissions = 0.07 lbs/yr

Average Ammonia Emissions = 0.00004 tons/yr



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20

Page 4 of 5

Maximum Emission Rates

NO_x

Using given information,

Maximum NO_x Emissions = 0.1157 cfm CD

Using the Ideal Gas Law,

Maximum NO_x Emissions = 0.000300 moles/minute

Maximum NO_x Emissions = 0.013806 lbs/minute

Maximum NO_x Emissions = 0.828 lbs/hour

Chloroprene

Using given information,

Maximum CD Emissions = 0.2259 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000586 moles CD/minute

Maximum CD Emissions = 0.051891 lbs CD/minute

Maximum CD Emissions = 3.113 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions = 0.0001 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = 0.0000002 moles/minute

Maximum Toluene Emissions = 0.00001 lbs/minute

Maximum Toluene Emissions = 0.0009 lbs/hour

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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20

Page 5 of 5

Ammonia

Using given information,

Maximum Ammonia Emissions = 0.000003 cfm ammonia

Using the Ideal Gas Law,

Maximum Ammonia Emissions = 0.00000001 moles/minute

Maximum Ammonia Emissions = 0.0000002 lbs/minute

Maximum Ammonia Emissions = 0.000009 lbs/hour

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| NOx | 6597 | 0.753 | 0.828 | 3.298 |
| Total VOC | 24801 | 2.831 | 3.114 | 12.401 |
| Chloroprene | 24794 | 2.830 | 3.113 | 12.397 |
| Toluene | 7 | 0.001 | 0.001 | 0.003 |
| Ammonia | 0.07 | 0.000008 | 0.000009 | 0.00004 |
| Total HAPs | 24801 | 2.831 | 3.114 | 12.401 |
| Total TAPs | 24801 | 2.831 | 3.114 | 12.401 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page 1 of 5

Basis:

Emissions are based on sampling data on March 12, 2002 and March 21, 2002 by METCO Environmental.

On March 12, 2002 type AD was being produced, which includes toluene.

On March 21, 2002 type WHV was being produced which does not include toluene.

The highest vent rate measured is 4.584 dscfm.

The highest NOx concentration measured is 22945.5 ppmv.

The highest chloroprene (CD) concentration measured is 44807 ppmv.

The highest toluene concentration measured is 12 ppmv.

Ammonia was measured at less than 0.68 ppmv. Conservatively assume a concentration of 0.68 ppmv.

The maximum concentrations are estimated to be 10% greater than the maximum measured concentration.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------|----------------------------|
| Vent Rate = | 4.584 cfm |
| Amount of Time Venting = | 8760 hours/yr |
| Average NOx in Air Vented = | 22945.5 ppm NOx by volume |
| Maximum NOx in Air Vented = | 25240 ppm NOx by volume |
| Average CD in Air Vented = | 44807 ppm CD by volume |
| Maximum CD in Air Vented = | 49288 ppm CD by volume |
| Avg. Toluene in Air Vented = | 12 ppm toluene by volume |
| Max. Toluene in Air Vented = | 13.2 ppm toluene by volume |
| Avg. Ammonia in Air Vented = | 0.68 ppm ammonia by volume |
| Max. Ammonia in Air Vented = | 0.75 ppm ammonia by volume |
| Molecular Weight of NOx = | 46 lb/lb-mole |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.4 lb/lb-mole |
| Molecular Weight of Ammonia = | 17 lb/lb-mole |
| Temperature = | 20 °C |
| Pressure = | 14.696 psia |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page 2 of 5

Average Emission Rates

NO_x

Using given information,

Average NO_x Emissions = 0.11 cfm NO_x

Using the Ideal Gas Law,

Average NO_x Emissions = 0.000273 moles/minute

Average NO_x Emissions = 0.012551 lbs/minute

Average NO_x Emissions = 0.753 lbs/hour

Average NO_x Emissions = 6597 lbs/yr

Average NO_x Emissions = 3.30 tons/yr

Chloroprene

Using given information,

Average CD Emissions = 0.2054 cfm CD

Using the Ideal Gas Law,

Average CD Emissions = 0.000533 moles/minute

Average CD Emissions = 0.047173 lbs/minute

Average CD Emissions = 2.830 lbs/hour

Average CD Emissions = 24794 lbs/yr

Average CD Emissions = 12.40 tons/yr



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page 3 of 5

Toluene

Using given information,

Average Toluene Emissions = 0.0001 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions = 0.0000001 moles/minute

Average Toluene Emissions = 0.000013 lbs/minute

Average Toluene Emissions = 0.0008 lbs/hour

Average Toluene Emissions = 7 lbs/yr

Average Toluene Emissions = 0.003 tons/yr

Ammonia

Using given information,

Average Ammonia Emissions = 0.000003 cfm ammonia

Using the Ideal Gas Law,

Average Ammonia Emissions = 0.00000001 moles/minute

Average Ammonia Emissions = 0.0000001 lbs/minute

Average Ammonia Emissions = 0.000008 lbs/hour

Average Ammonia Emissions = 0.07 lbs/yr

Average Ammonia Emissions = 0.00004 tons/yr



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page 4 of 5

Maximum Emission Rates

NOx

Using given information,

Maximum NOx Emissions = 0.1157 cfm CD

Using the Ideal Gas Law,

Maximum NOx Emissions = 0.000300 moles/minute

Maximum NOx Emissions = 0.013806 lbs/minute

Maximum NOx Emissions = 0.828 lbs/hour

Chloroprene

Using given information,

Maximum CD Emissions = 0.2259 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000586 moles CD/minute

Maximum CD Emissions = 0.051891 lbs CD/minute

Maximum CD Emissions = 3.113 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions = 0.0001 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = 0.0000002 moles/minute

Maximum Toluene Emissions = 0.00001 lbs/minute

Maximum Toluene Emissions = 0.0009 lbs/hour



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page 5 of 5

Ammonia

Using given information,

Maximum Ammonia Emissions = 0.000003 cfm ammonia

Using the Ideal Gas Law,

Maximum Ammonia Emissions = 0.00000001 moles/minute

Maximum Ammonia Emissions = 0.0000002 lbs/minute

Maximum Ammonia Emissions = 0.000009 lbs/hour

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| NOx | 6597 | 0.753 | 0.828 | 3.298 |
| Total VOC | 24801 | 2.831 | 3.114 | 12.401 |
| Chloroprene | 24794 | 2.830 | 3.113 | 12.397 |
| Toluene | 7 | 0.001 | 0.001 | 0.003 |
| Ammonia | 0.07 | 0.000008 | 0.000009 | 0.00004 |
| Total HAPs | 24801 | 2.831 | 3.114 | 12.401 |
| Total TAPs | 24801 | 2.831 | 3.114 | 12.401 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Product Drying Cap

TEMPO ID: GRP0007

Point Source ID No.: 1700-25A

Page 1 of 3

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Cap covers 1700-25, East Wash Belt Dryer, 1700-26, West Wash Belt Dryer, 1700-27, East Dryer Hot Exhaust, 1700-28, West Dryer Hot Exhaust, 1700-45, No. 1 East Dryer Cooling Compartment, 1700-46, No. 1 West Dryer Cooling Compartment, 1700-47, No. 2 East Dryer Cooling Compartment, and 1700-48, No. 2 West Dryer Cooling Compartment.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------------|---|
| % VOC Emissions from Washbelt = | 16.35 % |
| % VOC Emissions from Dryer = | 83.65 % |
| Total VOC in Stripped Emulsion = | 136416 lbs/yr |
| CD in Stripped Emulsion = | 113680 lbs/yr in worst emitting product |
| ACR in Stripped Emulsion = | 22736 lbs/yr in worst emitting product |
| Max. Toluene in Stripped Emulsion = | 46130 lbs/yr |
| Operating Hours = | 8760 hours/yr |

Wash Belt Calculations

Emission Rates

$$\text{Emissions} = \text{Total in Stripped Emulsion} / \text{Operating Hours}$$

Calculate total emissions from the washbelts and dryers

| | |
|---------------------|--------------|
| CD Emissions = | 12.98 lbs/hr |
| ACR Emissions = | 2.60 lbs/hr |
| Toluene Emissions = | 5.27 lbs/hr |

Calculate total emissions from the washbelts

| | |
|----------------|-------------|
| CD Emissions = | 2.12 lbs/hr |
| CD Emissions = | 18586 lb/yr |
| CD Emissions = | 9.29 tpy |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Product Drying Cap

TEMPO ID: GRP0007

Point Source ID No.: 1700-25A

Page 2 of 3

ACR Emissions = 0.42 lbs/hr
ACR Emissions = 3717 lb/yr
ACR Emissions = 1.86 tpy

Toluene Emissions = 0.86 lbs/hr
Toluene Emissions = 7542 lb/yr
Toluene Emissions = 3.77 tpy

Dryer Calculations

Emission Rates

Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

CD Emissions = 12.98 lbs/hr
ACR Emissions = 2.60 lbs/hr
Toluene Emissions = 5.27 lbs/hr

Calculate total emissions from the dryer vents

CD Emissions = 10.86 lbs/hr
CD Emissions = 95093 lb/yr
CD Emissions = 47.55 tpy

ACR Emissions = 2.17 lbs/hr
ACR Emissions = 19019 lb/yr
ACR Emissions = 9.51 tpy

Toluene Emissions = 4.41 lbs/hr
Toluene Emissions = 38588 lb/yr
Toluene Emissions = 19.29 tpy

1,2-Dichlorobenzene Emissions = 0.01 lbs/hr
1,2-Dichlorobenzene Emissions = 60 lb/yr
1,2-Dichlorobenzene Emissions = 0.03 tpy



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Product Drying Cap

TEMPO ID: GRP0007

Point Source ID No.: 1700-25A

Page 3 of 3

Cooling Compartment Calculations

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Summary

Toluene is potentially emitted at a level of 23.36 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 136416 | 15.573 | 15.573 | 68.208 |
| Chloroprene | 113680 | 12.977 | 12.977 | 56.840 |
| 1,2-Dichlorobenzene | 60 | 0.007 | 0.007 | 0.030 |
| Toluene | 46130 | 5.266 | 5.266 | 23.065 |
| Total HAPs | 159870 | 18.250 | 18.250 | 79.935 |
| Total TAPs | 159870 | 18.250 | 18.250 | 79.935 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Wash Belt Dryer

TEMPO ID: EQT0142

Point Source ID No.: 1700-25

Page 1 of 2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Total emissions for the wash belts are covered under 1700-25A, Product Drying Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------------|---|
| % VOC Emissions from Washbelt = | 16.35 % |
| % VOC Emissions from Dryer = | 83.65 % |
| Total VOC in Stripped Emulsion = | 136416 lbs/yr |
| CD in Stripped Emulsion = | 113680 lbs/yr in worst emitting product |
| ACR in Stripped Emulsion = | 22736 lbs/yr in worst emitting product |
| Max. Toluene in Stripped Emulsion = | 46130 lbs/yr |
| Operating Hours = | 8760 hours/yr |

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

| | |
|-----------------------------|--------------|
| Average CD Emissions = | 12.98 lbs/hr |
| Average ACR Emissions = | 2.60 lbs/hr |
| Average Toluene Emissions = | 5.27 lbs/hr |

Calculate total emissions from the washbelts

| | |
|-------------------------|-------------|
| Average CD Emissions = | 2.12 lbs/hr |
| Average CD Emissions = | 18586 lb/yr |
| Average CD Emissions = | 9.29 tpy |
| Average ACR Emissions = | 0.42 lbs/hr |
| Average ACR Emissions = | 3717 lb/yr |
| Average ACR Emissions = | 1.86 tpy |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Wash Belt Dryer

TEMPO ID: EQT0142

Point Source ID No.: 1700-25

Page 2 of 2

Average Toluene Emissions = 0.86 lbs/hr
Average Toluene Emissions = 7542 lb/yr
Average Toluene Emissions = 3.77 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 3.82 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--|--|--------------------------------|
| Total VOC | 22304 | 2.546 | 2.546 | 11.152 |
| Chloroprene | 18586 | 2.122 | 2.122 | 9.293 |
| Toluene | 7542 | 0.861 | 0.861 | 3.771 |
| Total HAPs | 26129 | 2.983 | 2.983 | 13.064 |
| Total TAPs | 26129 | 2.983 | 2.983 | 13.064 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Wash Belt Dryer

TEMPO ID: EQT0143

Point Source ID No.: 1700-26

Page 1 of 2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions. Total emissions for the wash belts are covered under 1700-25A, Product Drying Cap. Assumes full throughput for each drying line. Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-------------------------------------|---|
| % VOC Emissions from Washbelt = | 16.35 % |
| % VOC Emissions from Dryer = | 83.65 % |
| Total VOC in Stripped Emulsion = | 136416 lbs/yr |
| CD in Stripped Emulsion = | 113680 lbs/yr in worst emitting product |
| ACR in Stripped Emulsion = | 22736 lbs/yr in worst emitting product |
| Max. Toluene in Stripped Emulsion = | 46130 lbs/yr |
| Operating Hours = | 8760 hours/yr |

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

| | |
|-----------------------------|--------------|
| Average CD Emissions = | 12.98 lbs/hr |
| Average ACR Emissions = | 2.60 lbs/hr |
| Average Toluene Emissions = | 5.27 lbs/hr |

Calculate total emissions from the washbelts

| | |
|-------------------------|-------------|
| Average CD Emissions = | 2.12 lbs/hr |
| Average CD Emissions = | 18586 lb/yr |
| Average CD Emissions = | 9.29 tpy |
| Average ACR Emissions = | 0.42 lbs/hr |
| Average ACR Emissions = | 3717 lb/yr |
| Average ACR Emissions = | 1.86 tpy |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Wash Belt Dryer

TEMPO ID: EQT0143

Point Source ID No.: 1700-26

Page 2 of 2

Average Toluene Emissions = 0.86 lbs/hr
Average Toluene Emissions = 7542 lb/yr
Average Toluene Emissions = 3.77 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 3.82 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 22304 | 2.546 | 2.546 | 11.152 |
| Chloroprene | 18586 | 2.122 | 2.122 | 9.293 |
| Toluene | 7542 | 0.861 | 0.861 | 3.771 |
| Total HAPs | 26129 | 2.983 | 2.983 | 13.064 |
| Total TAPs | 26129 | 2.983 | 2.983 | 13.064 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Hot Dryer Exhaust

TEMPO ID: EQT0144

Point Source ID No.: 1700-27

Page 1 of 2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Total emissions for the dryer exhausts are covered under 1700-27A, Dryer Exhaust Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

Based on mass balances, approximately 60 lb/yr of 1,2-dichlorobenzene is emitted from the driers.

| | |
|-------------------------------------|---|
| % VOC Emissions from Washbelt = | 16.35 % |
| % VOC Emissions from Dryer = | 83.65 % |
| Total VOC in Stripped Emulsion = | 136416 lbs/yr |
| CD in Stripped Emulsion = | 113680 lbs/yr in worst emitting product |
| ACR in Stripped Emulsion = | 22736 lbs/yr in worst emitting product |
| Max. Toluene in Stripped Emulsion = | 46130 lbs/yr |
| Operating Hours = | 8760 hours/yr |

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

| | |
|-----------------------------|--------------|
| Average CD Emissions = | 12.98 lbs/hr |
| Average ACR Emissions = | 2.60 lbs/hr |
| Average Toluene Emissions = | 5.27 lbs/hr |

Calculate total emissions from the dryer vents

| | |
|-------------------------|--------------|
| Average CD Emissions = | 10.86 lbs/hr |
| Average CD Emissions = | 95093 lb/yr |
| Average CD Emissions = | 47.55 tpy |
| Average ACR Emissions = | 2.17 lbs/hr |
| Average ACR Emissions = | 19019 lb/yr |
| Average ACR Emissions = | 9.51 tpy |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Hot Dryer Exhaust

TEMPO ID: EQT0144

Point Source ID No.: 1700-27

Page 2 of 2

Average Toluene Emissions = 4.41 lbs/hr
Average Toluene Emissions = 38588 lb/yr
Average Toluene Emissions = 19.29 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 19.54 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 114172 | 13.033 | 13.033 | 57.086 |
| Chloroprene | 95093 | 10.855 | 10.855 | 47.547 |
| 1,2-Dichlorobenze | 60 | 0.007 | 0.007 | 0.030 |
| Toluene | 38588 | 4.405 | 4.405 | 19.294 |
| Total HAPs | 133741 | 15.267 | 15.267 | 66.871 |
| Total TAPs | 133741 | 15.267 | 15.267 | 66.871 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Hot Dryer Exhaust

TEMPO ID: EQT0145

Point Source ID No.: 1700-28

Page 1 of 2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Total emissions for the dryer exhausts are covered under 1700-27A, Dryer Exhaust Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

Based on mass balances, approximately 60 lb/yr of 1,2-dichlorobenzene is emitted from the driers.

| | |
|-------------------------------------|---|
| % VOC Emissions from Washbelt = | 16.35 % |
| % VOC Emissions from Dryer = | 83.65 % |
| Total VOC in Stripped Emulsion = | 136416 lbs/yr |
| CD in Stripped Emulsion = | 113680 lbs/yr in worst emitting product |
| ACR in Stripped Emulsion = | 22736 lbs/yr in worst emitting product |
| Max. Toluene in Stripped Emulsion = | 46130 lbs/yr |
| Operating Hours = | 8760 hours/yr |

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

| | |
|-----------------------------|--------------|
| Average CD Emissions = | 12.98 lbs/hr |
| Average ACR Emissions = | 2.60 lbs/hr |
| Average Toluene Emissions = | 5.27 lbs/hr |

Calculate total emissions from the dryer vents

| | |
|-------------------------|--------------|
| Average CD Emissions = | 10.86 lbs/hr |
| Average CD Emissions = | 95093 lb/yr |
| Average CD Emissions = | 47.55 tpy |
| Average ACR Emissions = | 2.17 lbs/hr |
| Average ACR Emissions = | 19019 lb/yr |
| Average ACR Emissions = | 9.51 tpy |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Hot Dryer Exhaust

TEMPO ID: EQT0145

Point Source ID No.: 1700-28

Page 2 of 2

Average Toluene Emissions = 4.41 lbs/hr
Average Toluene Emissions = 38588 lb/yr
Average Toluene Emissions = 19.29 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 20.21 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 114172 | 13.033 | 13.033 | 57.086 |
| Chloroprene | 95093 | 10.855 | 10.855 | 47.547 |
| 1,2-Dichlorobenzene | 60 | 0.007 | 0.007 | 0.030 |
| Toluene | 38588 | 4.405 | 4.405 | 19.294 |
| Total HAPs | 133741 | 15.267 | 15.267 | 66.871 |
| Total TAPs | 133741 | 15.267 | 15.267 | 66.871 |

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Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE*Source Description:* No. 1 East Dryer Cooling Compartment*TEMPO ID:* EQT0146*Point Source ID No.:* 1700-45*Page* 1 *of* 1**Basis:**

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Summary

| Compound | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|--------------------------------------|--------------------------------------|----------------------------|
| Total VOC | <0.01 | <0.01 | <0.01 |
| Chloroprene | <0.01 | <0.01 | <0.01 |
| Toluene | <0.01 | <0.01 | <0.01 |
| Total HAPs | <0.01 | <0.01 | <0.01 |
| Total TAPs | <0.01 | <0.01 | <0.01 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 West Dryer Cooling Compartment

TEMPO ID: EQT0147

Point Source ID No.: 1700-46

Page 1 of 1

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Summary

| Compound | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|--------------------------------------|--------------------------------------|----------------------------|
| Total VOC | <0.01 | <0.01 | <0.01 |
| Chloroprene | <0.01 | <0.01 | <0.01 |
| Toluene | <0.01 | <0.01 | <0.01 |
| Total HAPs | <0.01 | <0.01 | <0.01 |
| Total TAPs | <0.01 | <0.01 | <0.01 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 East Dryer Cooling Compartment

TEMPO ID: EQT0148

Point Source ID No.: 1700-47

Page 1 of 1

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Summary

| Compound | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|--------------------------------------|--------------------------------------|----------------------------|
| Total VOC | <0.01 | <0.01 | <0.01 |
| Chloroprene | <0.01 | <0.01 | <0.01 |
| Toluene | <0.01 | <0.01 | <0.01 |
| Total HAPs | <0.01 | <0.01 | <0.01 |
| Total TAPs | <0.01 | <0.01 | <0.01 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 West Dryer Cooling Compartment

TEMPO ID: EQT0149

Point Source ID No.: 1700-48

Page 1 of 1

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Summary

| Compound | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|--------------------------------------|--------------------------------------|----------------------------|
| Total VOC | <0.01 | <0.01 | <0.01 |
| Chloroprene | <0.01 | <0.01 | <0.01 |
| Toluene | <0.01 | <0.01 | <0.01 |
| Total HAPs | <0.01 | <0.01 | <0.01 |
| Total TAPs | <0.01 | <0.01 | <0.01 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Vent

TEMPO ID: GRP0009

Point Source ID No.: 1700-50

Page 1 of 3

Basis:

No. 1 Stabilizer Makeup tank is 1070 gallon capacity and used to makeup aqueous dispersion stabilizer which has no VOC emissions.

No. 2 Stabilizer Makeup tank is 1070 gallon capacity and used to makeup any type of stabilizer.

No. 3 and 4 Stabilizer Tanks are 2330 gallon capacity and used to makeup toluene base stabilizer for AD and G types.

No. 3 and 4 Stabilizer Tanks are also used to makeup Emergency Stabilizer for the PK's (about once per quarter).

No. 5 Stabilizer Makeup tank is 1070 gallon capacity and used to makeup dispersion stabilizer which has no VOC emissions but will result in particulate emissions from the manhole vent..

Toluene is used for stabilizers for A-types, G-types, and emergency stabilizer.

Each of the 5 tanks is equipped with a nitrogen blanket regulator set at 1 psig.

All 5 tanks are piped to two common vent systems.

One vent system is equipped with a flame arrestor and vents to atmosphere during preparation of the stabilizers.

The second vent system is equipped with a backpressure regulator set at 2 psig and operates after stabilizer preparation.

The five PK stabilizer tanks are vented back to the second vent system to minimize emissions.

Since during operation, the PK stabilizer tanks vent back to the stabilizer makeup tanks there are no emissions when transferring from the makeup tanks to the PK stabilizer tanks.

Solid additives are added to the toluene based and aqueous dispersion stabilizers, resulting in particulate matter emissions.

When the manhole is open for solids addition, toluene vapors and particulates are captured by the manhole exhaust system (EID No.1700-14B).

Calculation basis provided by Mr. P. Offut, DuPont Performance Polymers.

| | |
|-----------------------------------|----------------------------|
| Maximum Makeup Toluene = | 502 lb/batch |
| Temperature = | 35 C |
| Toluene Vapor Pressure = | 46.77 mm Hg |
| Toluene Liquid Density = | 53.21 lbs/ft ³ |
| H ₂ O Vapor Pressure = | 42.00 mm Hg |
| Toluene Flow Rate = | 832 lbs/min |
| Toluene Flow Rate = | 15.64 ft ³ /min |
| Vapor Displacement = | 15.64 ft ³ /min |
| Maximum Toluene Required = | 2915575 lb |
| Maximum Toluene Required = | 54792 ft ³ /yr |
| Venting Time = | 3504 min/yr |
| Venting Time = | 58.40 hr/yr |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Vent

TEMPO ID: GRP0009

Point Source ID No.: 1700-50

Page 2 of 3

VOC Emissions

Displacement Losses

Assuming worst case - vapor is saturated with toluene and H₂O - and using the ideal gas law

| | |
|--------------------------|---|
| Total Vapor = | 0.002468 moles/ft ³ |
| Toluene Vapor = | 0.000152 moles/ft ³ |
| Toluene Vapor = | 0.014033 lbs toluene/ft ³ total vapor |
| Toluene Vapor = | 0.219419 lbs toluene/min |
| H ₂ O Vapor = | 0.000136 moles/ft ³ |
| H ₂ O Vapor = | 0.002455 lbs H ₂ O/ft ³ total vapor |
| H ₂ O Vapor = | 0.038382 lbs H ₂ O/min |
| N ₂ Vapor = | 0.002180 moles/ft ³ |
| N ₂ Vapor = | 0.061027 lbs N ₂ /ft ³ total vapor |

Venting from Stabilizer Tanks

| | |
|--------------------------|-------------|
| Toluene Vapor = | 0.22 lb/min |
| Toluene Vapor = | 769 lbs/yr |
| Toluene Vapor = | 13.17 lb/hr |
| H ₂ O Vapor = | 135 lbs/yr |
| N ₂ Vapor = | 3344 lbs/yr |

Type Change Emissions

When a G or AD campaign is complete, the toluene based stabilizer tank is depressured, the heel is drained to drums, and the tank is cleaned.

For the worst case, assume each type change of G type requires tank cleaning, the tank is at 2 psig, and the nitrogen is saturated with toluene and water, and the entire volume of the tank is discharged to atmosphere.

Assume depressuring occurs within 1 minute.



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

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Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Vent

TEMPO ID: GRP0009

Point Source ID No.: 1700-50

Page 3 of 3

G or AD -type changes/yr = 37
Venting Time = 1 min/type change
Volume of No. 3 or 4 Tank = 311 ft³
Total Volume Vented = 623 ft³ @ 2psig
Total Volume Vented = 708 ft³ @ 0 psig
Toluene Vented = 367 lbs/yr
Toluene Vented = 9.93 lb/min
Toluene Vented = 595.89 lb/hr

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 1136 | 19.253 | 595.885 | 0.568 |
| Toluene | 1136 | 19.253 | 595.885 | 0.568 |
| Total HAPs | 1136 | 19.253 | 595.885 | 0.568 |
| Total TAPs | 1136 | 19.253 | 595.885 | 0.568 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Inhibitor Mix Tank

TEMPO ID: EQT0162

Point Source ID No.: 1700-51

Page 1 of 2

Basis:

Inhibitor is made by dissolving PTZ and NDPA in Crude CD

The aim limits are 0.75% PTZ and 0.25% NDPA

Inhibitor is produced in the Inhibitor Makeup Tank (IMUT) located in Poly Building

The batches are pumped to the Final Makeup Tank (FMUT), which is covered under EID No. 1700-63, Vent Header System.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|---------------------------------|----------------------------|
| CD Supply Rate = | 75 lbs/min |
| Amount of Inhibitor Produced = | 4828384 lbs/yr |
| Temperature = | 1.0 C |
| Specific Gravity of Inhibitor = | 61.655 lbs/ft ³ |
| Vapor Pressure of CD = | 84.06 mm Hg |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Max. Mole Fraction CD = | 1.0 mole/mole |

Emission Rates

IMUT Tank data

| | |
|------------------------------------|--|
| Total Volume of Tank = | 88 ft ³ |
| Crude CD in tank at 85% level = | 3384 lbs |
| Crude CD in tank at 85% level = | 55 ft ³ |
| Vapor space in tank at 85% level = | 33 ft ³ |
| Tank Charging Time = | 63565 min/yr |
| Tank Charging Rate = | 1.22 ft ³ /min |
| Number of Sub Batches = | 1427 sub batches/yr |
| Amount of CD per Sub Batch = | 3384 lbs CD/sub batch pumped |
| Amount of CD per Sub Batch = | 55 ft ³ CD/sub batch pumped |

Nitrogen supply pressure is controlled at 8 inwg and vent backpressure at 14 inwg.

| | |
|-----------------------------------|-------------|
| N ₂ Supply to Vent = | 0.2890 psig |
| Backpressure Vent Valve Setting = | 0.5058 psig |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Inhibitor Mix Tank

TEMPO ID: EQT0162

Point Source ID No.: 1700-51

Page 2 of 2

For CD saturated nitrogen at 1 C and using the ideal gas law,

Total Vapor = 0.00286909 moles/ft³
CD Vapor = 0.00030676 moles/ft³
CD Vapor = 0.02716085 lbs CD/ft³ total vapor

Total Amount Vented = 55 ft³/sub batch pumped
Venting Rate = 1.22 ft³/min
CD Venting Rate = 0.03 lb/min
CD Venting Rate = 1.99 lb/hr
CD vented = 1.49 lbs CD/sub batch
CD vented = 2127 lbs CD/yr
CD vented = 1.06 tons CD/yr

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 2127 | 1.988 | 1.988 | 1.064 |
| Chloroprene | 2127 | 1.988 | 1.988 | 1.064 |
| Total HAPs | 2127 | 1.988 | 1.988 | 1.064 |
| Total TAPs | 2127 | 1.988 | 1.988 | 1.064 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Storage Tanks Manual Vent

TEMPO ID: RLP0016

Point Source ID No.: 1700-56

Page 1 of 3

Basis:

Unstripped emulsion tanks 6, 7, 8, 10, 13, and 14 are normally vented to the pressure balancing common vent header / tank system.

To prevent backflow to other tanks resulting from venting down during product changes, the tanks are isolated from the common vent system and directed to a bypass vent to atmosphere.

Tanks 6, 7, 8, and 10 store dry type emulsions.

Tanks 13 and 14 store liquid type products.

Venting time is approximately 1 minute.

Vapor pressure of chloroprene (CD) is based on worst case product.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|---------------------------------|-------------------------------------|
| Number of Vent Downs = | 25 vent downs/yr/tank for dry types |
| Number of Vent Downs = | 50 vent downs/yr/tank for LD types |
| EST 10 Total Volume = | 2400 ft ³ |
| EST 7 or 8 Total Volume = | 2025 ft ³ |
| EST 6, 13, or 14 Total Volume = | 1545 ft ³ |
| Maximum Pressure = | 5 psig |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 25 °C |
| Atmospheric Pressure = | 14.696 psia |

Average Emission Rates

Calculate vented volume

| | |
|---------------------------------|--|
| No. 10 Vented Volume = | 817 ft ³ /vent down from 5 psig to 0 psig |
| No. 7 or 8 Vented Volume = | 689 ft ³ /vent down from 5 psig to 0 psig |
| No. 6, 13 or 14 Vented Volume = | 526 ft ³ /vent down from 5 psig to 0 psig |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Storage Tanks Manual Vent

TEMPO ID: RLP0016

Point Source ID No.: 1700-56

Page 2 of 3

Using worst case of nitrogen saturated with H₂O, toluene, ACR and Slocum CD data

| | |
|----------------------------------|---|
| Vapor Pressure of Water = | 23.6 mm Hg |
| Total Vapor = | 0.002550 moles/ft ³ |
| Vapor Pressure of CD = | 189 mm Hg |
| CD Vapor = | 0.000473 moles/ft ³ |
| CD Vapor = | 0.041902 lbs CD/ft ³ total vapor |
| Vapor Pressure of Toluene = | 28.40 mm Hg |
| Toluene Vapor = | 0.000071 moles/ft ³ |
| Toluene Vapor = | 0.006553 lbs toluene/ft ³ total vapor |
| Vapor Pressure of ACR = | 42.28 mm Hg |
| ACR Vapor = | 0.000106 moles/ft ³ |
| ACR Vapor = | 0.013020 lbs ACR/ft ³ total vapor |
| H ₂ O Vapor = | 0.000079 moles/ft ³ |
| H ₂ O Vapor = | 0.001426 lbs H ₂ O/ft ³ total vapor |
| Nitrogen Vapor = | 0.001998 moles/ft ³ |
| Nitrogen Vapor = | 0.057943 lbs N ₂ /ft ³ total vapor |
| No. 10 EST Vapor Vented = | 20414 ft ³ /yr |
| No. 10 EST CD Vented = | 855 lb/yr |
| No. 10 EST Toluene Vented = | 134 lb/yr |
| No. 10 EST ACR Vented = | 266 lb/yr |
| No. 7 or 8 EST Vapor Vented = | 17224 ft ³ /yr |
| No. 7 or 8 EST CD Vented = | 722 lb/yr |
| No. 7 or 8 EST Toluene Vented = | 113 lb/yr |
| No. 7 or 8 EST ACR Vented = | 224 lb/yr |
| No 6 EST Vapor Vented = | 13141 ft ³ /yr |
| No 6 EST CD Vented = | 551 lb/yr |
| No 6 EST Toluene Vented = | 86 lb/yr |
| No 6 EST ACR Vented = | 171 lb/yr |
| No. 13 & 14 EST Vapor Vented = | 52565 ft ³ CD/yr |
| No. 13 & 14 EST CD Vented = | 2203 lb/yr |
| No. 13 & 14 EST Toluene Vented = | 344 lb/yr |
| No. 13 & 14 EST ACR Vented = | 684 lb/yr |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Storage Tanks Manual Vent

TEMPO ID: RLP0016

Point Source ID No.: 1700-56

Page 3 of 3

Total CD Emitted = 4330 lb/yr
Total Toluene Emitted = 677 lb/yr
Total ACR Emitted = 1346 lb/yr

Venting Time Per Event = 1 min
Average CD Emission Rate = 1484.69 lb/hr
Average Toluene Emission Rate = 232.18 lb/hr
Average ACR Emission Rate = 461.32 lb/hr

Maximum Emission Rates

Maximum emission rates are equal to the average rates.

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 6353 | 2178.189 | 2178.189 | 3.177 |
| Chloroprene | 4330 | 1484.685 | 1484.685 | 2.165 |
| Toluene | 677 | 232.181 | 232.181 | 0.339 |
| Total HAPs | 5008 | 1716.866 | 1716.866 | 2.504 |
| Total TAPs | 5008 | 1716.866 | 1716.866 | 2.504 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63

Page 1 of 4

Basis:

The Refined CD Storage Tank, No. 3 Crude CD Storage Tank, CD Inhibitor FMUT, CD Inhibitor HUT, No 1 and No. 2 RCD tanks, CD Refining Column Heels tank, and No. 1 and No. 2 Monomer Solution Tanks all vent into a common vent header, which minimizes emissions as one tank or another fills, venting into the other tanks.

Actual operating data of the common vent system for the past two years show that under normal operating conditions, the system vents very little to none.

Emissions are calculated by estimating and summing up the time for abnormal operations where tank levels will vary significantly and Poly can keep running.

It is conservatively estimated that operating conditions will result in emissions for 10% of the year in addition to maintenance requirements.

Calculation basis provided by Mr. P. Offut, DuPont

Based on mass balances, approximately 2 lb/yr of 1,2-dichlorobenzene is emitted from the Column Heels Tank.

| | |
|---------------------------------|--|
| Crude CD Specific Gravity = | 60.924 lbs/ft ³ |
| Refined CD Pumped = | 139871804 lb/yr considering worst case product |
| Recovered CD Pumped = | 50529656 lb/yr considering worst case product |
| Vapor Temperature = | 5 C |
| Vapor Temperature = | 501 R |
| Header Inlet Pressure = | 4.5 psig |
| Header Inlet Pressure = | 19.196 psia |
| Header Outlet Pressure = | 0 psig |
| Header Outlet Pressure = | 14.696 psia |
| Gas Cv for Valve (100% open) = | 816 |
| Cg/Cv Gas/Liquid Cv for Valve = | 36.1 |
| Vapor Pressure of CD = | 100.671 mm Hg |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Max. Mole Fraction CD = | 1 mole/mole |
| Vapor Pressure of Toluene = | 9.189 mm Hg |
| Molecular Weight of Toluene = | 92.14 lb/lb-mole |
| Max. Mole Fraction Toluene = | 0.036 mole/mole |
| Vapor Pressure of ACR = | 15.538 mm Hg |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Max. Mole Fraction ACR = | 0.009 mole/mole |
| Operating Time = | 6679 hr considering worst case product |
| Unschd Column Maint Down Days = | 5 /yr |
| Column Water Washes = | 9 /yr |
| Other Venting = | 668 hrs/yr |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63

Page 2 of 4

Emission Rates

Estimate transfer rates

Total Crude CD Pumped = 95296213 lbs/yr
Hours Flow = 6679 hr

Based on the common vent header design, maximum flow occurs with the backpressure valve fully open and a differential pressure of 4.5 psig and temperature of 5 C

Conservatively, assuming nitrogen saturated with CD at 1 C liquid temperature and using the ideal gas law,

| | |
|-----------------|---|
| Total vapor = | 0.001284 moles/ft ³ |
| CD vapor = | 0.000130 moles/ft ³ |
| CD vapor = | 0.011525 lbs CD/ft ³ total vapor @ 5 psig |
| CD vapor = | 0.008823 lbs CD/ft ³ total vapor @ 0 psig |
| Toluene vapor = | 0.000000 moles/ft ³ |
| Toluene vapor = | 0.000022 lbs toluene/ft ³ total vapor @ 5 psig |
| Toluene vapor = | 0.000017 lbs toluene/ft ³ total vapor @ 0 psig |
| ACR vapor = | 0.000000 moles/ft ³ |
| ACR vapor = | 0.000021 lbs ACR/ft ³ total vapor @ 5 psig |
| ACR vapor = | 0.000016 lbs ACR/ft ³ total vapor @ 0 psig |

$$Q = ((520 / (1.18 \times \text{Temp}))^{0.5}) \times (\text{Gas Cv} \times \text{Inlet Pressure}) \times \text{SIN}((\pi/180)) \times (3417/\text{Gas/Liquid Cv}) \times (((\text{Inlet Pressure}-\text{Outlet Pressure})/\text{Inlet Pressure})^{0.5})/60$$

Gas Flow = 176 scfm with 100% valve open



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63

Page 3 of 4

Equal percentage valve flow characteristics

| % open | % full flow | scfm | lbs/hr CD | lbs/hr tol | lbs/hr ACR | lbs/hr VOC |
|--------|-------------|------|-----------|------------|------------|------------|
| 100 | 100 | 186 | 98.46 | 0.19 | 0.18 | 98.83 |
| 90 | 86 | 160 | 84.59 | 0.16 | 0.15 | 84.91 |
| 80 | 65 | 121 | 63.95 | 0.12 | 0.12 | 64.19 |
| 70 | 43 | 81 | 42.80 | 0.08 | 0.08 | 42.96 |
| 60 | 29 | 54 | 28.59 | 0.06 | 0.05 | 28.70 |
| 50 | 19 | 36 | 19.12 | 0.04 | 0.03 | 19.19 |
| 40 | 13 | 25 | 13.20 | 0.03 | 0.02 | 13.25 |
| 30 | 9 | 17 | 8.80 | 0.02 | 0.02 | 8.83 |
| 20 | 6 | 11 | 5.92 | 0.01 | 0.01 | 5.94 |
| 10 | 4 | 8 | 4.06 | 0.01 | 0.01 | 4.08 |

5 Unschd Column Maint Down Days per Year = 120 hrs/yr
 9 Column Water Washes per Year = 216 hrs/yr
 Other Venting = 668 hrs/yr
 Total = 1004 hrs/yr

For column down time, assume that Poly continues to run at average rates from the refined CD tank and that refill of the refined tank results in the venting. To be conservative, do not back out amount that would be compressed.

Also assume that during these outages the strippers continue to run at average rate and RCD results in venting. To be conservative, do not back out amount that would be compressed.

Amount Refined CD to Refill = 21024018 lbs/yr
 Amount RCD Displacing Vapor = 7595072 lbs/yr
 Total Displacement = 28619090 lbs/yr
 Total Displacement = 469751 ft³/yr vapor
 Total Displacement = 7.80 ft³/min vapor
 Total CD = 5414 lbs/yr CD
 Total CD = 5.39 lbs/hr CD
 Total Toluene = 10 lbs/yr toluene
 Total Toluene = 0.01 lbs/hr toluene
 Total ACR = 10 lbs/yr ACR
 Total ACR = 0.01 lbs/hr ACR



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63

Page 4 of 4

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 5434 | 5.413 | 98.834 | 2.717 |
| Chloroprene | 5414 | 5.393 | 98.465 | 2.707 |
| 1,2-Dichlorobenzene | 2 | 0.003 | 0.055 | 0.001 |
| Toluene | 10 | 0.010 | 0.190 | 0.005 |
| Total HAPs | 5426 | 5.406 | 98.709 | 2.713 |
| Total TAPs | 5426 | 5.406 | 98.709 | 2.713 |



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page 1 of 4

Basis:

Based on 10 hr TWA area data developed between 1999 and 2001, the average concentration of CD in the building air is 0.56 ppmv.

Monitoring data for toluene between February 2001 and September 2002 indicate an average concentration of 0.176 ppm.

3500 lb/yr of dextrose, 203 M lb/yr of sodium sulfite, 4665 lb sodium chloride are added manually from cartons and bags to water solution makeup tank.

Estimated that 0.1% of the material transferred becomes airborne.

Estimated that 50% of the airborne dust is captured by exhaust system. Remainder is captured in building.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|---------------------------------|------------------------------|
| Rated Capacity of Blower = | 2500 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Average CD in Air Exhausted = | 0.56 ppm CD by volume |
| Maximum CD in Air Exhausted = | 0.67 ppm CD by volume |
| Avg. Toluene in Air Exhausted = | 0.176 ppm toluene by volume |
| Max. Toluene in Air Exhausted = | 3.1464 ppm toluene by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.4 lb/lb-mole |
| Temperature = | 25 °C |
| Pressure = | 14.696 psia |
| Dextrose used = | 3500 lb/yr |
| Sodium Sulfite used = | 203,000 lb/yr |
| Sodium Chloride used = | 4665 lb/yr |
| Total Addition Time = | 66 hours |

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.0014 cfm CD



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page 2 of 4

Using the Ideal Gas Law,

| | |
|------------------------|-----------------------|
| Average CD Emissions = | 0.000004 moles/minute |
| Average CD Emissions = | 0.000316 lbs/minute |
| Average CD Emissions = | 0.019 lbs/hour |
| Average CD Emissions = | 166 lbs/yr |
| Average CD Emissions = | 0.08 tons/yr |

Toluene

Using given information,

Average Toluene Emissions = 0.0004 cfm toluene

Using the Ideal Gas Law,

| | |
|-----------------------------|-----------------------|
| Average Toluene Emissions = | 0.000001 moles/minute |
| Average Toluene Emissions = | 0.000104 lbs/minute |
| Average Toluene Emissions = | 0.006 lbs/hour |
| Average Toluene Emissions = | 55 lbs/yr |
| Average Toluene Emissions = | 0.03 tons/yr |

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.0017 cfm CD

Using the Ideal Gas Law,

| | |
|------------------------|--------------------------|
| Maximum CD Emissions = | 0.000004 moles CD/minute |
| Maximum CD Emissions = | 0.000379 lbs CD/minute |
| Maximum CD Emissions = | 0.023 lbs CD/hour |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page 3 of 4

Toluene

Using given information,

Maximum Toluene Emissions = 0.0079 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = 0.000020 moles/minute

Maximum Toluene Emissions = 0.001854 lbs/minute

Maximum Toluene Emissions = 0.111 lbs/hour

PM/PM-10 Emissions

Fraction Airborne = 0.1 %

Capture Efficiency = 50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Efficiency / 8760 hr/yr

= 211165 lb/yr x 0.1% x 50% / 8760 hr/yr

= 0.0121 lb/hr

0.05 tpy

Maximum Emission Rates

Fraction Airborne = 0.1 %

Capture Efficiency = 50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Efficiency / 40 hr/yr

= 211165 lb/yr x 0.1% x 50% / 66 hr/yr

= 1.564 lb/hr



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page 4 of 4

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| PM/PM-10 | 106 | 0.0121 | 1.564 | 0.053 |
| Total VOC | 221 | 0.025 | 0.134 | 0.110 |
| Chloroprene | 166 | 0.019 | 0.023 | 0.083 |
| Toluene | 55 | 0.006 | 0.111 | 0.027 |
| Total HAPs | 221 | 0.025 | 0.134 | 0.110 |
| Total TAPs | 221 | 0.025 | 0.134 | 0.110 |



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 10 Emulsion Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65

Page 1 of 3

Basis:

EST 10 is located outside of the main Poly building. The manway is not ventilated, so any emissions exit to atmosphere from the manway.

Emissions occur when the tank is opened for cleaning or maintenance.

EST 10 is a dry type unstripped emulsion storage tank, which is opened for inspection at every product type change, assume 4 non-compatible type changes / month. This tank requires cleaning once monthly, generally after G campaigns. Inspections last 15 minutes.

When manways opened for inspection, tanks are already vented down via point source

1700-56. Manway will be open for perhaps 15 minutes while tank wall condition is observed for fouling

Assume 1% of tank vapor content is emitted through convection to atmosphere during

inspection, since there is no motive force to displace vapor from inside the tank

When vessel entry is required to these tanks for cleaning, an air mover is used to evacuate the vapor contents of the tank, replacing it with an air atmosphere. This can take up to 6 hours.

Calculation basis provided by Mr. D. McCrea DuPont

Formerly under EID No. 1700-1 (EQT0134).

| | | |
|-----------------------|--------|--------|
| Volume EST 10 = | 2400 | cub ft |
| Ambient temperature = | 25 | deg C |
| Pressure = | 14.696 | psia |

For worst case scenarios, assuming equilibrium in tank before emptying.

ACR and toluene not present in > 80% time, but counted as if they were.

Using the Ideal Gas Law,

Loss during inspections of EST 10

| | | | |
|-----------------------------------|---------|-------------------|----------------|
| Vapor content of EST 10 = | 6.121 | lb moles | |
| EST 10 vapor density = | 0.0026 | lb moles / cub ft | |
| Inspection of EST 10 = | 36 | per year | |
| Loss to atmosphere = | 0.061 | lb moles | |
| CD in vapor lost = | 0.01522 | lb moles | per inspection |
| CD in vapor lost = | 1.3478 | lb | per inspection |
| CD lost during inspections = | 48.521 | lb / year | |
| Toluene in vapor lost = | 0.00229 | lb moles | per inspection |
| Toluene in vapor lost = | 0.2114 | lb | per inspection |
| Toluene lost during inspections = | 7.609 | lb / year | |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 10 Emulsion Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65

Page 2 of 3

| | | | |
|-------------------------------|---------|-----------|----------------|
| ACR in vapor lost = | 0.00341 | lb moles | per inspection |
| ACR in vapor lost = | 0.4188 | lb | per inspection |
| ACR lost during inspections = | 20.320 | lb / year | |

Loss during vessel entry to EST 10

| | | | |
|---------------------------------|---------|-----------|------------------|
| CD in vapor lost = | 1.522 | lb moles | per vessel entry |
| CD in vapor lost = | 134.780 | lb | per vessel entry |
| CD lost during vessel entries = | 1617 | lb / year | |

| | | | |
|-----------------------------------|---------|-----------|------------------|
| Toluene in vapor lost = | 0.22875 | lb moles | per vessel entry |
| Toluene in vapor lost = | 21.137 | lb | per vessel entry |
| Toluene lost during inspections = | 254 | lb / year | |

| | | | |
|-------------------------------|---------|-----------|------------------|
| ACR in vapor lost = | 0.34051 | lb moles | per vessel entry |
| ACR in vapor lost = | 41.8789 | lb | per vessel entry |
| ACR lost during inspections = | 503 | lb / year | |

Maximum Emission Rates

Maximum emission rate occurs at the start of tank evacuation using the air mover.
Emissions will be at the concentration within the tanks.

| | | |
|---|--------|--------|
| Coppus blower capacity | 750 | cfm |
| CD emission in first minute | 42.119 | lb/min |
| assuming no air leakage in occurs in that first minute. | | |
| Toluene emission in first minute | 6.605 | lb/min |
| ACR emission in first minute | 13.087 | lb/min |

| | | |
|-----------------------------|--------|--------|
| Maximum CD Emissions = | 42.119 | lb/min |
| Maximum toluene Emissions = | 6.605 | lb/min |
| Maximum ACR Emissions = | 13.087 | lb/min |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 10 Emulsion Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--|--|--------------------------------|
| Total VOC | 2450 | 30.247 | 4097.575 | 1.225 |
| Chloroprene | 1666 | 20.566 | 2527.117 | 0.833 |
| Toluene | 261 | 3.225 | 785.229 | 0.131 |
| Total HAPs | 1927 | 23.792 | 3312.346 | 0.964 |
| Total TAPs | 1927 | 23.792 | 3312.346 | 0.964 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 13 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65A

Page 1 of 3

Basis:

EST 13 is located outside of the main Poly building. The manway is not ventilated, so any emissions exit to atmosphere from the manway.

Emissions occur when the tanks are opened for cleaning or maintenance.

EST 13 and 14 are Liquid Dispersion unstripped emulsion storage tanks. These tanks are opened for inspection occasionally, assume once every two months. These tanks require occasional cleaning, assume once every 3 months.

When manways opened for inspection, tanks are already vented down via point source 1700-56. Manway will be open for perhaps 10 minutes while tank wall condition is observed for fouling.

Assume 1% of tank vapor content is emitted through convection to atmosphere during inspection, since there is no motive force to displace vapor from inside the tank.

When vessel entry is required to these tanks for cleaning, an air mover is used to evacuate the vapor contents of the tank, replacing it with an air atmosphere. This can take up to 6 hours.

Calculation basis provided by Mr. D. McCrea DuPont

Formerly under EID No. 1700-1 (EQT0134).

| | | |
|------------------------|--------|--------|
| Volume EST 13 and 14 = | 1545 | cub ft |
| Ambient temperature = | 25 | deg C |
| Pressure = | 14.696 | psia |

For worst case scenarios, assuming equilibrium in tank before emptying.
ACR and toluene not present in > 80% time, but counted as if they were.

Loss during inspections of EST 13

| | | |
|-----------------------------------|---------|-------------------|
| Vapor content of EST 13 or 14 = | 3.941 | lb moles |
| EST 13 or 14 vapor density = | 0.0026 | lb moles / cub ft |
| Inspection of EST 13 & 14 = | 8 | per year |
| Loss to atmosphere = | 0.039 | lb moles |
| CD in vapor lost = | 0.97995 | lb moles |
| CD in vapor lost = | 86.7644 | lb |
| CD lost during inspections = | 694.115 | lb / year |
| Toluene in vapor lost = | 0.00147 | lb moles |
| Toluene in vapor lost = | 0.1361 | lb |
| Toluene lost during inspections = | 1.089 | lb / year |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 13 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65A

Page 2 of 3

| | | | |
|-------------------------------|---------|-----------|----------------|
| ACR in vapor lost = | 0.00219 | lb moles | per inspection |
| ACR in vapor lost = | 0.2696 | lb | per inspection |
| ACR lost during inspections = | 2.157 | lb / year | |

Loss during vessel entry to EST 13

| | | | |
|---------------------------------|---------|-----------|------------------|
| CD in vapor lost = | 0.980 | lb moles | per vessel entry |
| CD in vapor lost = | 86.764 | lb | per vessel entry |
| CD lost during vessel entries = | .347.06 | lb / year | |

| | | | |
|-----------------------------------|---------|-----------|------------------|
| Toluene in vapor lost = | 0.14726 | lb moles | per vessel entry |
| Toluene in vapor lost = | 13.607 | lb | per vessel entry |
| Toluene lost during inspections = | 54.43 | lb / year | |

| | | | |
|-------------------------------|---------|-----------|------------------|
| ACR in vapor lost = | 0.21920 | lb moles | per vessel entry |
| ACR in vapor lost = | 26.9595 | lb | per vessel entry |
| ACR lost during inspections = | 107.84 | lb / year | |

Maximum Emission Rates

Maximum emission rate occurs at the start of tank evacuation using the air mover.
Emissions will be at the concentration within the tanks.

| | | |
|---|--------|--------|
| Coppus blower capacity | 750 | cfm |
| CD emission in first minute | 42.119 | lb/min |
| assuming no air leakage in occurs in that first minute. | | |
| Toluene emission in first minute | 6.605 | lb/min |
| ACR emission in first minute | 13.087 | lb/min |

| | | |
|-----------------------------|--------|--------|
| Maximum CD Emissions = | 42.119 | lb/min |
| Maximum toluene Emissions = | 6.605 | lb/min |
| Maximum ACR Emissions = | 13.087 | lb/min |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 13 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65A

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 1207 | 46.411 | 4097.575 | 0.603 |
| Chloroprene | 1041 | 40.045 | 2527.117 | 0.521 |
| Toluene | 56 | 2.135 | 785.229 | 0.028 |
| Total HAPs | 1097 | 42.180 | 3312.346 | 0.548 |
| Total TAPs | 1097 | 42.180 | 3312.346 | 0.548 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 14 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65B

Page 1 of 3

Basis:

EST 14 is located outside of the main Poly building. The manway is not ventilated, so any emissions exit to atmosphere from the manway.

Emissions occur when the tanks are opened for cleaning or maintenance.

EST 13 and 14 are Liquid Dispersion unstripped emulsion storage tanks. These tanks are opened for inspection occasionally, assume once every two months. These tanks require occasional cleaning, assume once every 3 months.

When manways opened for inspection, tanks are already vented down via point source 1700-56. Manway will be open for perhaps 10 minutes while tank wall condition is observed for fouling. Assume 1% of tank vapor content is emitted through convection to atmosphere during inspection, since there is no motive force to displace vapor from inside the tank.

When vessel entry is required to these tanks for cleaning, an air mover is used to evacuate the vapor contents of the tank, replacing it with an air atmosphere. This can take up to 6 hours.

Calculation basis provided by Mr. D. McCrea DuPont
Formerly under EID No. 1700-1 (EQT0134).

| | | |
|------------------------|--------|--------|
| Volume EST 13 and 14 = | 1545 | cub ft |
| Ambient temperature = | 25 | deg C |
| Pressure = | 14.696 | psia |

For worst case scenarios, assuming equilibrium in tank before emptying.
ACR and toluene not present in > 80% time, but counted as if they were.

Loss during inspections of EST 14

| | | |
|-----------------------------------|---------|-------------------|
| Vapor content of EST 13 or 14 = | 3.941 | lb moles |
| EST 13 or 14 vapor density = | 0.0026 | lb moles / cub ft |
| Inspection of EST 13 & 14 = | 8 | per year |
| Loss to atmosphere = | 0.039 | lb moles |
| CD in vapor lost = | 0.97995 | lb moles |
| CD in vapor lost = | 86.7644 | lb |
| CD lost during inspections = | 694.115 | lb / year |
| Toluene in vapor lost = | 0.00147 | lb moles |
| Toluene in vapor lost = | 0.1361 | lb |
| Toluene lost during inspections = | 1.089 | lb / year |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 14 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65B

Page 2 of 3

| | | | |
|-------------------------------|---------|-----------|----------------|
| ACR in vapor lost = | 0.00219 | lb moles | per inspection |
| ACR in vapor lost = | 0.2696 | lb | per inspection |
| ACR lost during inspections = | 2.157 | lb / year | |

Loss during vessel entry to EST 14

| | | | |
|---------------------------------|--------|-----------|------------------|
| CD in vapor lost = | 0.980 | lb moles | per vessel entry |
| CD in vapor lost = | 86.764 | lb | per vessel entry |
| CD lost during vessel entries = | 347.06 | lb / year | |

| | | | |
|-----------------------------------|---------|-----------|------------------|
| Toluene in vapor lost = | 0.14726 | lb moles | per vessel entry |
| Toluene in vapor lost = | 13.607 | lb | per vessel entry |
| Toluene lost during inspections = | 54.43 | lb / year | |

| | | | |
|-------------------------------|---------|-----------|------------------|
| ACR in vapor lost = | 0.21920 | lb moles | per vessel entry |
| ACR in vapor lost = | 26.9595 | lb | per vessel entry |
| ACR lost during inspections = | 107.84 | lb / year | |

Maximum Emission Rates

Maximum emission rate occurs at the start of tank evacuation using the air mover.
Emissions will be at the concentration within the tanks.

| | | |
|---|--------|--------|
| Coppus blower capacity | 750 | cfm |
| CD emission in first minute | 42.119 | lb/min |
| assuming no air leakage in occurs in that first minute. | | |
| Toluene emission in first minute | 6.605 | lb/min |
| ACR emission in first minute | 13.087 | lb/min |

| | | |
|-----------------------------|--------|--------|
| Maximum CD Emissions = | 42.119 | lb/min |
| Maximum toluene Emissions = | 6.605 | lb/min |
| Maximum ACR Emissions = | 13.087 | lb/min |



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 14 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65B

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|----------------------------|
| Total VOC | 1207 | 46.411 | 4097.575 | 0.603 |
| Chloroprene | 1041 | 40.045 | 2527.117 | 0.521 |
| Toluene | 56 | 2.135 | 785.229 | 0.028 |
| Total HAPs | 1097 | 42.180 | 3312.346 | 0.548 |
| Total TAPs | 1097 | 42.180 | 3312.346 | 0.548 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page 1 of 4

Basis:

Based on 10 hr TWA area data developed between 1999 and 2001, the average concentration of CD in the building air is 0.56 ppmv.

Monitoring data for toluene between February 2001 and September 2002 indicate an average concentration of 0.176 ppm.

ACR has a vapor pressure similar to that of toluene. Conservatively assume the same concentration in the air.

ACR is present in only 4 out of the 20 Neoprene types manufactured in Poly.

Similarly toluene is present in only 6 types Neoprene out of 20

Fans vent fugitive emissions from equipment components located in the building.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|---------------------------------|------------------------------|
| Rated Capacity of Fans = | 476365 cfm |
| Amount of Time Discharging = | 8760 hours/yr |
| Average CD in Air Exhausted = | 0.56 ppm CD by volume |
| Maximum CD in Air Exhausted = | 0.67 ppm CD by volume |
| Avg. Toluene in Air Exhausted = | 0.176 ppm toluene by volume |
| Max. Toluene in Air Exhausted = | 3.1464 ppm toluene by volume |
| Avg. ACR in Air Exhausted = | 0.176 ppm ACR by volume |
| Max. ACR in Air Exhausted = | 3.1464 ppm ACR by volume |
| Molecular Weight of CD = | 88.54 lb/lb-mole |
| Molecular Weight of Toluene = | 92.4 lb/lb-mole |
| Molecular Weight of ACR = | 122.99 lb/lb-mole |
| Temperature = | 25 °C |
| Pressure = | 14.696 psia |

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.2668 cfm CD



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page 2 of 4

Using the Ideal Gas Law,

| | |
|------------------------|-----------------------|
| Average CD Emissions = | 0.000680 moles/minute |
| Average CD Emissions = | 0.060241 lbs/minute |
| Average CD Emissions = | 3.614 lbs/hour |
| Average CD Emissions = | 31663 lbs/yr |
| Average CD Emissions = | 15.83 tons/yr |

Toluene

Using given information,

Average Toluene Emissions = 0.0838 cfm toluene

Using the Ideal Gas Law,

| | |
|-----------------------------|-----------------------|
| Average Toluene Emissions = | 0.000214 moles/minute |
| Average Toluene Emissions = | 0.019758 lbs/minute |
| Average Toluene Emissions = | 1.185 lbs/hour |
| Average Toluene Emissions = | 10385 lbs/yr |
| Average Toluene Emissions = | 5.19 tons/yr |

ACR

Using given information,

Average ACR Emissions = 0.0838 cfm ACR

Using the Ideal Gas Law,

| | |
|-------------------------|-----------------------|
| Average ACR Emissions = | 0.000214 moles/minute |
| Average ACR Emissions = | 0.026299 lbs/minute |
| Average ACR Emissions = | 1.578 lbs/hour |
| Average ACR Emissions = | 13823 lbs/yr |
| Average ACR Emissions = | 6.91 tons/yr |



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page 3 of 4

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.3201 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000816 moles CD/minute

Maximum CD Emissions = 0.072289 lbs CD/minute

Maximum CD Emissions = 4.337 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions = 1.4988 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = 0.003823 moles/minute

Maximum Toluene Emissions = 0.353225 lbs/minute

Maximum Toluene Emissions = 21.193 lbs/hour

ACR

Using given information,

Maximum ACR Emissions = 1.4988 cfm ACR

Using the Ideal Gas Law,

Maximum ACR Emissions = 0.003823 moles/minute

Maximum ACR Emissions = 0.470163 lbs/minute

Maximum ACR Emissions = 28.210 lbs/hour



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page 4 of 4

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 55871 | 6.378 | 53.741 | 27.935 |
| Chloroprene | 31663 | 3.614 | 4.337 | 15.831 |
| Toluene | 10385 | 1.185 | 21.193 | 5.192 |
| Total HAPs | 42048 | 4.800 | 25.531 | 21.024 |
| Total TAPs | 42048 | 4.800 | 25.531 | 21.024 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Finishing Stabilizer Makeup Bag Filter

TEMPO ID: EQT0193

Point Source ID No.: 1700-74

Page 1 of 1

Basis:

Keltrol Used = 2521 lb/yr
TETD Used = 150219 lb/yr
Lomar PW = 10212 lb/yr
Total Addition Time = 88 hours

Keltrol, TETD, and Lomar are added manually from bags to finishing stabilizer makeup tanks into an aqueous suspension.

Estimated that 0.25% of the material transferred becomes airborne. This is based on experience with the bag filter, which is almost clean when inspected annually.

Estimated that 50% of the airborne dust is captured by exhaust system. Remainder is captured in building.

Emissions are controlled by a bag filter with 99% control efficiency.

Calculation basis provided by Mr. D.McCrea, DuPont

PM/PM-10 Emissions

Fraction Airborne = 0.25 %
Capture Efficiency = 50 %
Control Efficiency = 99 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Efficiency
x (1 - Control Efficiency) / 214 hr/yr

= 162952 lb/yr x 0.25% x 50% x (1 - 0.99) / 88 hr/yr
= 0.0231 lb/hr
= 0.00 tpy

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|----------|---------------------|--------------------------------|--------------------------------|-------------------------|
| PM/PM-10 | 2.04 | 0.023 | 0.023 | 0.001 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Emergency Stabilizer Drumming

TEMPO ID: EQT0198

Point Source ID No.: 1700-79

Page 1 of 2

Basis:

Emergency stabilizer is produced 4 times per year.

Emergency stabilizer is drummed out from the stabilizer makeup tank.

Emissions are not controlled.

Assume that vapor displaced is saturated with VOC.

Emergency stabilizer is composed of toluene, water and dissolved inhibitors.

Calculation basis provided by Mr. P. Offut, DuPont

| | |
|-----------------------------------|-----------------|
| Drumming Rate = | 5 gal/min |
| Drumming Rate = | 0.6685 cfm |
| Stabilizer Drummed = | 20400 lb |
| Density of Emergency Stabilizer = | 7.64 lb/gal |
| Volume of Drum = | 55 gal |
| Temperature = | 25 C |
| Vapor Pressure of Toluene = | 28.40 mm Hg |
| Molecular Weight of Toluene = | 92.4 lb/lb-mole |

Emission Rates

Drumming Time = 534.03 min

Using the Ideal Gas Law,

| | |
|-----------------|--|
| Total Vapor = | 0.002550 moles/ft ³ |
| Toluene Vapor = | 0.000095 moles/ft ³ |
| Toluene Vapor = | 0.008807 lbs toluene/ft ³ total vapor |
| Toluene Vapor = | 0.005887 lbs toluene/min |
| Toluene Vapor = | 0.353250 lb/hr |
| Toluene Vapor = | 3.14 lb/yr |
| Toluene Vapor = | 0.002 tpy |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Emergency Stabilizer Drumming

TEMPO ID: EQT0198

Point Source ID No.: 1700-79

Page 2 of 2

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 3.1 | 0.353 | 0.353 | 0.002 |
| Toluene | 3.1 | 0.353 | 0.353 | 0.002 |
| Total HAPs | 3.1 | 0.353 | 0.353 | 0.002 |
| Total TAPs | 3.1 | 0.353 | 0.353 | 0.002 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Storage Common Vent Header

TEMPO ID: RLP0017

Point Source ID No.: 1700-80

Page 1 of 4

Basis:

Emissions are the total from the Refined ACR Storage Tank (1700-80.1/EQT0199) and Chlorinated ACR Storage Tank (1700-80.2/EQT0200).

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 198 | 0.023 | - | 0.099 |
| 1,2-Dichlorobenzene | 0.11 | 0.00001 | - | 0.00005 |
| Total HAPs | 0.11 | 0.00001 | - | 0.00005 |
| Total TAPs | 0.11 | 0.00001 | - | 0.00005 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1

Page 1 of 4

Basis:

Refined ACR from the ACR Refining Column is pumped into the Refined ACR storage tank. The Refined ACR Storage Tank has an external -18 C brine cooled heat exchanger. The circulating flow from the tank goes to the SMU are to feed the MST and returns to the tank via the cooler.

The ACR storage tank is 45,000 gal in size, but the capacity is limited to 172,600 lb by Neovent considerations.

The tank is nitrogen blanketed.

Refined ACR is withdrawn from the ACR supply loop in Poly batchwise at the MST.

The Refined and Chlorinated ACR Storage tanks share a common ven header, but the ACR-solvent blend tank has a separate vent to avoid possible solvent contamination of the Refined ACR Storage Tank.

All inlet streams of ACR tanks enter through droplegs.

The vent stack for the ACR Storage Tank is to be 2" in diameter and approximately 50 ft above grade.

| | |
|---|---------------|
| ACR Produced = | 2959863 lb/yr |
| Max Fill Tank = | 667 lb/hr |
| Tank Volume = | 45000 gal |
| Max. Liquid Level in Refined ACR Tank = | 17370 gal |
| Tank Temperature = | -10.00 C |
| = | 263.15 K |
| Tank Pressure = | 6 psig |
| = | 20.7 psia |
| = | 1070.20 mm Hg |
| s.g. of ACR at Specified Temp = | 1.2 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1

Page 2 of 4

Emission Rates

Use the working loss equation from Section 7.1.3.1.2 of AP-42, 5th Edition.

$$L_w, \text{ Working Loss, lb/yr} = 0.001 * M_v * P_{VA} * (Q / 42) * K_N * K_P$$

M_v = vapor molecular weight, lb/lb-mol

= 123.02 lb/lb-mole

P_{VA} = vapor pressure at daily average liquid surface temperature, psia

= 0.1250 psia

Q = throughput, gal/yr

= 295785 gal/yr

Max Level = 173818 lb

N = number of turnovers

= 295785 gal/yr / 17370 gal

= 17.03

K_N = turnover factor

= 1 for $N \leq 36$

= $(180+N) / 6N$ for $N > 36$

= 1

K_P = working loss product factor

= 1 for all liquids except crude oil



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1

Page 3 of 4

| Component | Wt % in liquid | Mol Wt | Wt%/MW | Mole Fraction in Liquid | Vapor Pressure (mm Hg) | Partial Pressure (mm Hg) |
|-----------|-------------------|--------|--------|-------------------------------|------------------------------|--------------------------------|
| ACR | 0.935 | 122.99 | 0.760 | 0.9397 | 6.66 | 6.2553 |
| ACR-1 | 0.046 | 122.99 | 0.037 | 0.0462 | 4.27 | 0.1976 |
| ACR-2 | 0.002 | 122.99 | 0.002 | 0.0020 | 2.84 | 0.0057 |
| ACR-3 | 0.002 | 122.99 | 0.002 | 0.0020 | 1.89 | 0.0038 |
| T-1,4 DCB | 0 | 125 | 0 | 0.0000 | 0.01 | 0 |
| TCB-1 | 0 | 159.5 | 0 | 0.0000 | 0.30 | 0 |
| TCB-2 | 0 | 159.5 | 0.000 | 0.0000 | 0.05 | 0.0000 |
| Meso | 0 | 196 | 0.000 | 0.0000 | 0.03 | 0.0000 |
| C4Cl4 | 0.01 | 196 | 0.005 | 0.0063 | 0.03 | 0.0002 |
| C4Cl5 | 0 | 230.5 | 0 | 0.0000 | 0.03 | 0 |
| C4Cl6 | 0 | 265 | 0 | 0.0000 | 0.03 | 0 |
| 1,2-DCB | 0.005 | 166.00 | 0.003 | 0.0037 | 1.11 | 0.0041 |
| NMP | 0 | 85.1 | 0 | 0.0000 | 0.00 | 0 |
| | 1.000 | | 0.809 | 1 | | 6.4667 |

| Component | Partial Pressure (psia) | Mole Fraction in Vapor | Mol Weight of Vapor lb/lb-mol | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------|-------------------------------|------------------------------|-------------------------------------|-----------------------------------|-----------------------------------|------------------------------|
| ACR | 0.12096 | 0.005845 | 118.97 | 0.012 | 0.026 | 104.793 |
| ACR-1 | 0.00382 | 0.000185 | 3.76 | 0.0004 | 0.001 | 3.310 |
| ACR-2 | 0.00011 | 0.000005 | 0.11 | 0.0000 | 0.000 | 0.096 |
| ACR-3 | 0.00007 | 0.000004 | 0.07 | 0.0000 | 0.000 | 0.064 |
| T-1,4 DCB | 0 | 0 | 0 | 0 | 0 | 0 |
| TCB-1 | 0 | 0 | 0 | 0 | 0 | 0 |
| TCB-2 | 0 | 0 | 0 | 0.000000 | 0.00000 | 0 |
| Meso | 0 | 0 | 0 | 0.0000000 | 0.000000 | 0 |
| C4Cl4 | 3.782E-06 | 1.82757E-07 | 0.005928087 | 3.74E-07 | 1.3E-06 | 0.003 |
| C4Cl5 | 0 | 0 | 0 | 0 | 0 | 0 |
| C4Cl6 | 0 | 0 | 0 | 0 | 0 | 0 |
| 1,2-DCB | 0.00008 | 0.000004 | 0.11 | 0.000008 | 0.00002 | 0.069 |
| NMP | 0 | 0 | 0 | 0 | 0 | 0 |
| | 0.1250 | 0.0060 | 123.02 | 0.012 | 0.027 | 108.335 |

**RTP**

Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1

Page 4 of 4

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 108 | 0.012 | - | 0.054 |
| 1,2-Dichlorobenze | 0.07 | 0.000008 | - | 0.00003 |
| Total HAPs | 0.07 | 0.000008 | - | 0.00003 |
| Total TAPs | 0.07 | 0.000008 | - | 0.00003 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2

Page 1 of 4

Basis:

Chlorinated ACR from the Transfer Tank in Monomer is pumped through the 1.5" transfer header to the Chlorinated ACR storage tank in Polly Area. The Chlorinated ACR Storage tank is jacketed with -18 deg C C brine and is nitrogen blanketed. There will be flow in and out of the tank simultaneously. The Chlorinated ACR Storage Tank is the former # 2 Crude CD Storage Tank. Tank is limited to 76.5% inventory by Neovent requirements.

The operating mode of this tank will be to run the level at a constant 50%, by matching the ACR production rate with the ACR refining rate.

Therefore working losses from this tank will be minimal.

However ACR Refining is designed to run at 50% uptime and ACR Synthesis at 80% uptime

Therefore for 30% of time chlorinated ACR will run into the tank increasing the level, since ACR Refining is down.

Therefore ACR venting will occur during this period

Assume the tank is refilled for turnarounds twice per year.

| | |
|---|---------------|
| ACR Produced = | 2921460 lb/yr |
| Max ACR produced = | 13000 lb/day |
| Chlorinated ACR per Refined ACR Produced = | 1.591 lb/lb |
| Max Chlorinated ACR Produced = | 862 lb/hr |
| Chlorinated ACR Tank Volume = | 17600 gal |
| Max. Liquid Level in Chlorinated ACR Tank = | 128040 lb |
| Tank Temperature = | 0.00 C |
| = | 273.15 K |
| Tank Pressure = | 6 psig |
| = | 20.7 psia |
| = | 1070.20 mm Hg |
| s.g. of Chlorinated ACR at 0 C = | 1.22 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2

Page 2 of 4

Emission Rates

Use the working loss equation from Section 7.1.3.1.2 of AP-42, 5th Edition.

$$L_w, \text{ Working Loss, lb/yr} = 0.001 * M_v * P_{VA} * (Q / 42) * K_N * K_P$$

M_v = vapor molecular weight, lb/lb-mol

= 123.04 lb/lb-mole

P_{VA} = vapor pressure at daily average liquid surface temperature, psia

= 0.1870 psia

Q = throughput, bbl/yr

Since tank is operated as a constant level tank for 70% of the time, the throughput is calculated for the remaining time plus 2 turnarounds

= $[2921460 \text{ lb ACR/yr} \times 1.591 \text{ lb CACR/lb ACR} \times 0.3 / (1.22 \times 8.34 \text{ lb/gal}) + 17600 \text{ gal} \times 0.765 \times 2] / 42 \text{ gal/bbl}$

= 3904 bbl/yr

N = number of turnovers

= $3904 \text{ bbl/yr} / (17600 \text{ gal} \times 0.765 / 42 \text{ bbl/gal})$

= 12.18

K_N = turnover factor

= 1 for $N \leq 36$

= $(180+N) / 6N$ for $N > 36$

= 1

K_P = working loss product factor

= 1 for all liquids except crude oil



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2

Page 3 of 4

| Component | Wt % in liquid | Mol Wt | Wt%/MW | Mole Fraction in Liquid | Vapor Pressure (mm Hg) | Partial Pressure (mm Hg) |
|-----------|-------------------|--------|--------|-------------------------------|------------------------------|--------------------------------|
| ACR | 0.720 | 122.99 | 0.585 | 0.7399 | 11.86 | 8.7716 |
| ACR-1 | 0.039 | 122.99 | 0.032 | 0.0399 | 7.96 | 0.3174 |
| ACR-2 | 0.038 | 122.99 | 0.031 | 0.0388 | 5.37 | 0.2085 |
| ACR-3 | 0.099 | 122.99 | 0.080 | 0.1013 | 3.58 | 0.3629 |
| T-1,4 DCB | 0 | 125 | 0 | 0.0000 | 0.01 | 0 |
| TCB-1 | 0 | 159.5 | 0 | 0.0000 | 0.64 | 0 |
| TCB-2 | 0.082 | 159.5 | 0.051 | 0.0647 | 0.12 | 0.0076 |
| Meso | 0.018 | 196 | 0.009 | 0.0116 | 0.07 | 0.0008 |
| C4Cl4 | 0 | 196 | 0 | 0.0000 | 0.07 | 0 |
| C4Cl5 | 0 | 230.5 | 0 | 0.0000 | 0.07 | 0 |
| C4Cl6 | 0 | 265 | 0 | 0.0000 | 0.07 | 0 |
| 1,2-DCB | 0.005 | 166.00 | 0.003 | 0.0038 | 1.11 | 0.0042 |
| NMP | 0 | 85.1 | 0 | 0.0000 | 0.00 | 0 |
| | 1.000 | | 0.791 | 1 | | 9.6730 |

| Component | Partial Pressure (psia) | Mole Fraction in Vapor | Mol Weight of Vapor lb/lb-mol | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------|-------------------------------|------------------------------|-------------------------------------|-----------------------------------|-----------------------------------|------------------------------|
| ACR | 0.16961 | 0.008196 | 111.53 | 0.009 | 0.045 | 81.479 |
| ACR-1 | 0.00614 | 0.000297 | 4.04 | 0.0003 | 0.002 | 2.949 |
| ACR-2 | 0.00403 | 0.000195 | 2.65 | 0.0002 | 0.001 | 1.937 |
| ACR-3 | 0.00702 | 0.000339 | 4.61 | 0.0004 | 0.002 | 3.371 |
| T-1,4 DCB | 0 | 0 | 0 | 0 | 0 | 0 |
| TCB-1 | 0 | 0 | 0 | 0 | 0 | 0 |
| TCB-2 | 0.00015 | 0.000007 | 0.13 | 0.000008 | 0.00005 | 0.070 |
| Meso | 0.00002 | 0.000001 | 0.02 | 0.0000008 | 0.000006 | 0.007 |
| C4Cl4 | 0 | 0 | 0 | 0 | 0 | 0 |
| C4Cl5 | 0 | 0 | 0 | 0 | 0 | 0 |
| C4Cl6 | 0 | 0 | 0 | 0 | 0 | 0 |
| 1,2-DCB | 0.00008 | 0.000004 | 0.07 | 0.000004 | 0.00003 | 0.039 |
| NMP | 0 | 0 | 0 | 0 | 0 | 0 |
| | 0.1870 | 0.0090 | 123.04 | 0.010 | 0.049 | 89.852 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2

Page 4 of 4

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 90 | 0.010 | - | 0.045 |
| 1,2-Dichlorobenzene | 0.04 | 0.000004 | - | 0.00002 |
| Total HAPs | 0.04 | 0.000004 | - | 0.00002 |
| Total TAPs | 0.04 | 0.000004 | - | 0.00002 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Refining Vent

TEMPO ID: RLP0018

Point Source ID No.: 1700-81

Page 1 of 1

Basis:

Emissions calculated using an ASPEN simulation.

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|----------------------------|--|--|--------------------------------|
| Total VOC | 4400 | 1.00 | 10.00 | 2.20 |
| 1,2-Dichlorobenze | <20 | <0.001 | <0.001 | <0.01 |
| HCl | 1400 | 0.30 | 4.50 | 0.70 |
| Total HAPs | 1420 | 0.30 | 4.50 | 0.70 |
| Total TAPs | 1420 | 0.30 | 4.50 | 0.70 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page 1 of 4

Basis:

ACR is sold to customers in drum quantities. To prevent polymerization of the ACR, the ACR is diluted with a solvent and extra polymerization inhibitors are added. The material to be drummed is made up in an ACR-solvent blend tank. Refined ACR from the ACR is added to the blend tank at -5 deg C. Solvent in Blend Tank will be at -10 deg C prior to ACR addition. Mixture temperature and composition when 50% of the ACR has been added represents average conditions during vapor displacement and was used to Initial solvent added at ambient warehouse temperature (65F). External cooler will cool solvent down as it is added. Assume at mean temperature of -1 deg C. Assume max rates are 120% of average rates.

| | Units | ACR Perclene | ACR DCM | ACR Xylene |
|---|-------------------------|-----------------|------------|---------------|
| Annual Drums Made-up | Drums/yr | 2,000 | 200 | 500 |
| Drums per Blend Tank Fill | Drums | 18 | 18 | 18 |
| Refined ACR in ACR / Perclene Drum | lbs Ref. ACR | 250 | 300 | 200 |
| Amount Solvent per Drum | lbs Solvent | 250 | 200 | 200 |
| Solvent Containers per Batch | Containers | 1 | 6 | 9 |
| Solvent Container Mass | lbs | 4,700 | 603 | 400 |
| Solvent Unloading Time | minutes | 17.12 | 15.87 | 24.57 |
| Spec. Gravity of Solvent at -1 C | g/cc | 1.65 | 1.37 | 0.88 |
| Annual Blend Tank Fills | Blends/yr | 111 | 11 | 27 |
| Volume of Blend Tank | gallons | 960 | | |
| Solvent Fill Rate | gpm | 20 | | |
| Annual ACR Used in Drum Shipments | ppy | 660,000 | | |
| Tank Pressure at Venting | psig | 2.5 | | |
| | mm Hg | 889 | | |
| Avg Tank Temp During Solvent Addition | C | -1 | | |
| | K | 272 | | |
| Adj. Gas Specific Vol. for Solvent Addition | ft ³ /lb mol | 306 | | |



RTP
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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page 2 of 4

Emission Rates

Estimation of Losses Due To Solvent Addition to Blend Tank

| Component | Mol Wt lb/lb-mol | Vapor Pressure mm Hg | Solvent Mole Fraction in Vapor | Displaced Volume in Blend Tank ft ³ | Displaced Total Moles from Tank lb-mol | Displaced Moles of Solvent from Tank lb-mol |
|-----------------|---------------------|----------------------------|--------------------------------------|---|---|---|
| Perclene | 165.83 | 4.02 | 0.005 | 45.534 | 0.149 | 0.0007 |
| Dichloromethane | 84.93 | 137.18 | 0.154 | 42.409 | 0.139 | 0.0214 |
| Xylene | 106.17 | 1.58 | 0.002 | 65.424 | 0.214 | 0.0004 |

| Component | Working Loss lb | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------------|-----------------------|-----------------------------------|-----------------------------------|------------------------------|
| Perclene | 0.112 | 0.391 | 0.470 | 12.393 |
| Dichloromethane | 1.817 | 6.871 | 8.246 | 19.992 |
| Xylene | 0.040 | 0.099 | 0.118 | 1.090 |

Estimation of Losses Due To ACR Addition to Perclene in the Blend Tank

Assume conditions at the 50% ACR addition point, i.e., -10 C.

Average Hourly ACR Fill Rate = 667 pph
Tank Temperature during ACR Addition = -10 C
Tank Temperature during ACR Addition = 263 K
Adjusted Gas Specific Volume for ACR Addition = 296 ft³/lb-mol
Density of ACR at Specific Temperature = 1.20 g/cc
Mass of ACR Added = 4700 lbs
Volume Displaced by ACR = 62.74 ft³
Moles Displaced by ACR = 0.2123 lb-mol
ACR Fill Time = 7.05 hr



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page 3 of 4

| Component | Wt % in Liquid | Mol Wt lb/lb-mol | Mole Fraction in Liquid | Vapor Pressure mm Hg | Partial Pressure mm Hg | Mole Fraction in Vapor |
|-----------|----------------|---------------------|-------------------------|-------------------------|---------------------------|------------------------|
| ACR | 0.3167 | 122.99 | 0.257 | 6.657 | 1.711 | 0.0019 |
| ACR-1 | 0.0167 | 122.99 | 0.014 | 4.274 | 0.058 | 0.0001 |
| Perclene | 0.6667 | 165.83 | 0.729 | 3.875 | 2.827 | 0.0032 |

| Component | Displaced Moles from Tank lb-mol | Working Loss lb | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------|-------------------------------------|--------------------|--------------------------------|--------------------------------|---------------------------|
| ACR | 0.00041 | 0.050 | 0.007 | 0.009 | 5.574 |
| ACR-1 | 0.00001 | 0.002 | 0.0002 | 0.000 | 0.188 |
| Perclene | 0.00067 | 0.112 | 0.016 | 0.019 | 12.419 |

Estimation of Losses Due To ACR Addition to Dichloromethane in the Blend Tank

Mass of ACR Added = 5427 lbs
Volume Displaced by ACR = 72.45 ft³
Moles Displaced by ACR = 0.2451 lb-mol
ACR Fill Time = 8.14 hr

| Component | Wt % in Liquid | Mol Wt lb/lb-mol | Mole Fraction in Liquid | Vapor Pressure mm Hg | Partial Pressure mm Hg | Mole Fraction in Vapor |
|-----------------|----------------|---------------------|-------------------------|-------------------------|---------------------------|------------------------|
| ACR | 0.4071 | 122.99 | 0.495 | 6.657 | 3.292 | 0.0037 |
| ACR-1 | 0.0214 | 122.99 | 0.026 | 4.274 | 0.111 | 0.0001 |
| Dichloromethane | 0.5714 | 84.93 | 0.479 | 132.230 | 63.387 | 0.0713 |

| Component | Displaced Moles from Tank lb-mol | Working Loss lb | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------------|-------------------------------------|--------------------|--------------------------------|--------------------------------|---------------------------|
| ACR | 0.00091 | 0.112 | 0.014 | 0.016 | 1.228 |
| ACR-1 | 0.00003 | 0.004 | 0.0005 | 0.001 | 0.041 |
| Dichloromethane | 0.01747 | 1.484 | 0.182 | 0.219 | 16.321 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page 4 of 4

Estimation of Losses Due To ACR Addition to Xylene in the Blend Tank

Mass of ACR Added = 3600 lbs
Volume Displaced by ACR = 48.06 ft³
Moles Displaced by ACR = 0.1626 lb-mol
ACR Fill Time = 5.40 hr

| Component | Wt % in Liquid | Mol Wt lb/lb-mol | Mole Fraction in Liquid | Vapor Pressure mm Hg | Partial Pressure mm Hg | Mole Fraction in Vapor |
|-----------|----------------|---------------------|-------------------------|-------------------------|---------------------------|------------------------|
| ACR | 0.3167 | 122.99 | 0.348 | 6.657 | 2.319 | 0.0026 |
| ACR-1 | 0.0167 | 122.99 | 0.018 | 4.274 | 0.078 | 0.0001 |
| Xylene | 0.6667 | 106.17 | 0.633 | 1.523 | 0.964 | 0.0011 |

| Component | Displaced Moles from Tank lb-mol | Working Loss lb | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------|-------------------------------------|--------------------|--------------------------------|--------------------------------|---------------------------|
| ACR | 0.00042 | 0.052 | 0.010 | 0.012 | 1.408 |
| ACR-1 | 0.00001 | 0.002 | 0.0003 | 0.000 | 0.048 |
| Xylene | 0.00018 | 0.019 | 0.003 | 0.004 | 0.505 |

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|--------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 10 | 0.134 | 0.142 | 0.005 |
| Dichloromethane | 36 | 7.054 | 9.895 | 0.018 |
| Tetrachlorethylene | 25 | 0.407 | 0.563 | 0.012 |
| Xylene | 2 | 0.102 | 0.142 | 0.001 |
| Total HAPs | 63 | 7.563 | 9.895 | 0.031 |
| Total TAPs | 63 | 7.563 | 9.895 | 0.031 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83

Page 1 of 4

Basis:

ACR- solvent mixtures from the ACR blend tank are added to 55-gallon drums to supply material to customers. Vapors are not recovered from the drumming operation. There is an area ventilation fan in the open drumming shed to minimize operator exposure to vapors during the filling operation. Maximum hourly emissions assume that only 4 pallets (16 drums) of material can be loaded out in one hour, based upon past experience. The max. for ACR/MeCl is 13 drums as this is the largest order experienced. Average hourly emissions was calculated by prorating the hourly emission by type by the annual order quantity by type.

| | Units | ACR Perclene | ACR DCM | ACR Xylene |
|-------------------------------|-------------------------|-----------------|------------|---------------|
| Vap Press of Solvent @ -5 C | mm Hg | 3.1 | 111.9 | 1.0 |
| Spec. Grav. Of Solvent @ -5 C | | 1.66 | 1.37 | 0.89 |
| Spec. Gravity of ACR @ -5 C | | 1.19 | 1.19 | 1.19 |
| Wt % ACR in Drum | wt % | 50% | 60% | 50% |
| s.g of ACR Solvent Blend | | 1.39 | 1.26 | 1.02 |
| Annual No. of Drums Made up | # | 2000 | 200 | 500 |
| Max No. of Drums Filled | #/hr | 16 | 13 | 16 |
| Avg No. of Drums Filled | #/hr | 12 | 12 | 12 |
| ACR Solvent Mixture per Drum | lbs | 500 | 500 | 400 |
| Drum Temperature | C | -5 | | |
| Drum Temperature | K | 268 | | |
| Drum Pressure | mm Hg | 760 | | |
| Gas Specific Volume | ft ³ /lb-mol | 352 | | |

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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83

Page 2 of 4

Emission Rates

ACR/Perclene Drum Filling

| Component | Wt % in Liquid | Mol Wt lb/lb-mol | Wt%/MW | Mole Fraction in Liquid | Vapor Pressure mm Hg | Partial Pressure mm Hg |
|-----------|----------------|---------------------|--------|-------------------------|-------------------------|---------------------------|
| ACR | 0.4750 | 122.99 | 0.386 | 0.546 | 8.932 | 4.8789 |
| ACR-1 | 0.0180 | 122.99 | 0.015 | 0.021 | 5.867 | 0.1215 |
| Others | 0.0070 | 150 | 0.005 | 0.007 | 3.930 | 0.0259 |
| Perclene | 0.5000 | 165.83 | 0.302 | 0.426 | 3.082 | 1.3144 |
| | 1 | | 0.707 | 1 | | |

| Component | Mole Fraction in Vapor | Working Loss lb/drum | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------|------------------------|-------------------------|--------------------------------|--------------------------------|---------------------------|
| ACR | 0.0064 | 0.013 | 0.155 | 0.207 | 25.850 |
| ACR-1 | 0.0002 | 0.0003 | 0.004 | 0.005 | 0.644 |
| Others | 0.00003 | 0.00008 | 0.001 | 0.001 | 0.168 |
| Perclene | 0.0017 | 0.005 | 0.056 | 0.075 | 9.390 |

ACR/Dichloromethane Drum Filling

| Component | Wt % in Liquid | Mol Wt lb/lb-mol | Wt%/MW | Mole Fraction in Liquid | Vapor Pressure mm Hg | Partial Pressure mm Hg |
|-----------------|----------------|---------------------|--------|-------------------------|-------------------------|---------------------------|
| ACR | 0.5700 | 122.99 | 0.463 | 0.484 | 8.932 | 4.3227 |
| ACR-1 | 0.0216 | 122.99 | 0.018 | 0.018 | 5.867 | 0.1076 |
| Others | 0.0084 | 150 | 0.006 | 0.006 | 3.930 | 0.0230 |
| Dichloromethane | 0.4000 | 84.93 | 0.471 | 0.492 | 111.883 | 55.0273 |
| | 1 | | 0.958 | 1 | | |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83

Page 3 of 4

| Component | Mole Fraction in Vapor | Working Loss lb/drum | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------------|------------------------|-------------------------|--------------------------------|--------------------------------|---------------------------|
| ACR | 0.0057 | 0.013 | 0.151 | 0.164 | 2.525 |
| ACR-1 | 0.0001 | 0.0003 | 0.004 | 0.004 | 0.063 |
| Others | 0.00003 | 0.00008 | 0.001 | 0.001 | 0.016 |
| Dichloromethane | 0.0724 | 0.111 | 1.332 | 1.443 | 22.194 |

ACR/Xylene Drum Filling

| Component | Wt % in Liquid | Mol Wt lb/lb-mol | Wt%/MW | Mole Fraction in Liquid | Vapor Pressure mm Hg | Partial Pressure mm Hg |
|-----------|----------------|---------------------|--------|-------------------------|-------------------------|---------------------------|
| ACR | 0.4750 | 122.99 | 0.386 | 0.441 | 8.932 | 3.9356 |
| ACR-1 | 0.0180 | 122.99 | 0.015 | 0.017 | 5.867 | 0.0980 |
| Others | 0.0070 | 150 | 0.005 | 0.005 | 3.930 | 0.0209 |
| Xylene | 0.5000 | 106.17 | 0.471 | 0.537 | 1.032 | 0.5544 |
| | 1 | | 0.876 | 1 | | |

| Component | Mole Fraction in Vapor | Working Loss lb/drum | Avg. Hourly Emissions lb/hr | Max. Hourly Emissions lb/hr | Annual Emissions lb/yr |
|-----------|------------------------|-------------------------|--------------------------------|--------------------------------|---------------------------|
| ACR | 0.0052 | 0.011 | 0.136 | 0.181 | 5.671 |
| ACR-1 | 0.0001 | 0.0003 | 0.003 | 0.005 | 0.141 |
| Others | 0.00003 | 0.00007 | 0.001 | 0.001 | 0.037 |
| Xylene | 0.00073 | 0.001 | 0.017 | 0.022 | 0.690 |

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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83

Page 4 of 4

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 45 | 0.201 | 0.346 | 0.023 |
| Dichloromethane | 22 | 0.099 | 1.443 | 0.011 |
| Tetrachloroethylene | 9 | 0.042 | 0.075 | 0.005 |
| Xylene | 1 | 0.003 | 0.022 | 0.0003 |
| Total HAPs | 32 | 0.143 | 1.443 | 0.016 |
| Total TAPs | 32 | 0.143 | 1.443 | 0.016 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Emulsion Blend Tank

TEMPO ID: EQT0212

Point Source ID No.: 1700-84A

Page 1 of 3

Basis:

AFS will purchase up to 32 totes of WRT, GRT, GW emulsion monthly

Use 48 totes for calculation

Vented annual volume of ACS tank is that of 48 totes per month

Toluene is emitted from GRT and GW emulsions.

90% of emulsion shipped will contain toluene

AFS Tank Volume = 5772 gal

= 771.72 ft³

Tank filling at ambient temperature = 35 °C

Vapor pressure CD at 35 °C is 334.3 mm Hg

Vapor pressure toluene at 35 °C is 52 mm Hg

MW of CD = 88.54 lb/lb-mol

MW of Toluene = 92.14 lb/lb-mol

CD component of emulsion = 0.099 wt % max

Toluene component of emulsion = 0.0165 wt % max

Solids component of emulsion = 45 wt %

Tote Contains = 2200 lb emulsion

Emulsion Density = 67.28 lb/ft³

No. of Totes = 48 per month

Specific Volume = 359.7 ft³/mol

Operating Time = 8760 hr

Emission Rates

Convert CD concentration to exclude the solids component

CD component of emulsion = $0.099 / (1 - 0.45)$

= 0.180 %

Mole Fraction CD = $0.18 / 88.54 / [0.18 / 88.54 + (100 - 0.18) / 18]$

= 0.00037

Partial Pressure CD in Tank = 334.3×0.00037

0.123 mm Hg

Mole Fraction CD in Vapor = $0.123 \text{ mm Hg} / 760$

= 0.000161



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Emulsion Blend Tank

TEMPO ID: EQT0212

Point Source ID No.: 170084A

Page 2 of 3

$$\begin{aligned}\text{Vapor Vented per Tote} &= 2200 \text{ lb/tote} / 67.284 \text{ lb/cu ft} \\ &= 32.70 \text{ ft}^3/\text{tote}\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 48 \text{ totes/month} \times 12 \text{ months/yr} \times 32.7 \text{ cu ft/tote} \times 0.000161 \\ &= 3.04 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 3.04 \text{ cu ft} \times 88.54 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.84 \text{ lb} \\ &= 0.0004 \text{ tpy} \\ &= 0.0001 \text{ lb/hr}\end{aligned}$$

Convert toluene concentration to exclude the solids component

$$\begin{aligned}\text{Toluene component of emulsion} &= 0.0165 / (1 - 0.45) \\ &= 0.030 \%\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction Toluene} &= 0.03 / 92.14 / [0.03 / 92.14 + (100 - 0.03) / 18] \\ &= 0.00006\end{aligned}$$

$$\begin{aligned}\text{Partial Pressure Toluene in Tank} &= 52 \times 0.00006 \\ &= 0.003 \text{ mm Hg}\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction Toluene in Vapor} &= 0.003 \text{ mm Hg} / 760 \\ &= 0.000004\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 48 \text{ totes/month} \times 12 \text{ months/yr} \times 32.7 \text{ cu ft/tote} \times 0.000004 \times 0.9 \\ &= 0.07 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 0.07 \text{ cu ft} \times 92.14 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.02 \text{ lb} \\ &= 0.00001 \text{ tpy} \\ &= 0.000002 \text{ lb/hr}\end{aligned}$$



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Emulsion Blend Tank

TEMPO ID: EQT0212

Point Source ID No.: 1700-84A

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 0.86 | 0.0001 | 0.0001 | 0.0004 |
| Chloroprene | 0.84 | 0.0001 | 0.0001 | 0.0004 |
| Toluene | 0.02 | 0.000002 | 0.000002 | 0.00001 |
| Total HAPs | 0.86 | 0.0001 | 0.0001 | 0.0004 |
| Total TAPs | 0.86 | 0.0001 | 0.0001 | 0.0004 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Totes

TEMPO ID: EQT0213

Point Source ID No.: 1700-84B

Page 1 of 3

Basis:

AFS will purchase up to 32 totes of WRT, GRT, GW emulsion monthly
Use 48 totes for calculation
Vented annual volume of ACS tank is that of 48 totes per month
Toluene is emitted from GRT and GW emulsions.
90% of emulsion shipped will contain toluene

| | |
|---------------------------------------|----------------------------|
| Tote filling at ambient temperature = | 35 C |
| Vapor pressure CD at 35 °C is | 334.3 mm Hg |
| Vapor pressure toluene at 35 °C is | 52 mm Hg |
| MW of CD = | 88.54 lb/lb-mol |
| MW of Toluene = | 92.14 lb/lb-mol |
| CD component of emulsion = | 0.099 wt % max |
| Toluene component of emulsion = | 0.0165 wt % max |
| Solids component of emulsion = | 45 wt % |
| Tote Contains = | 2200 lb emulsion |
| Emulsion Density = | 67.28 lb/ft ³ |
| No. of Totes = | 48 per month |
| Specific Volume = | 359.7 ft ³ /mol |
| Operating Time = | 8760 hr |

Emission Rates

Convert CD concentration to exclude the solids component

$$\begin{aligned}\text{CD component of emulsion} &= 0.099 / (1 - 0.45) \\ &= 0.180 \%\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction CD} &= 0.18 / 88.54 / [0.18 / 88.54 + (100 - 0.18) / 18] \\ &= 0.00037\end{aligned}$$

$$\begin{aligned}\text{Partial Pressure CD in Totes} &= 334.3 \times 0.00037 \\ &= 0.123 \text{ mm Hg}\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction CD in Vapor} &= 0.123 \text{ mm Hg} / 760 \\ &= 0.000161\end{aligned}$$



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Totes

TEMPO ID: EQT0213

Point Source ID No.: 1700-84B

Page 2 of 3

$$\begin{aligned}\text{Vapor Vented per Tote} &= 2200 \text{ lb/tote} / 67.284 \text{ lb/cu ft} \\ &= 32.70 \text{ ft}^3/\text{tote}\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 48 \text{ totes/month} \times 12 \text{ months/yr} \times 32.7 \text{ cu ft/tote} \times 0.000161 \\ &= 3.04 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 3.04 \text{ cu ft} \times 88.54 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.84 \text{ lb} \\ &= 0.0004 \text{ tpy} \\ &= 0.0001 \text{ lb/hr}\end{aligned}$$

Convert toluene concentration to exclude the solids component

$$\begin{aligned}\text{Toluene component of emulsion} &= 0.0165 / (1 - 0.45) \\ &= 0.030 \%\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction Toluene} &= 0.03 / 92.14 / [0.03 / 92.14 + (100 - 0.03) / 18] \\ &= 0.00006\end{aligned}$$

$$\begin{aligned}\text{Partial Pressure Toluene in Totes} &= 52 \times 0.00006 \\ &= 0.003 \text{ mm Hg}\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction Toluene in Vapor} &= 0.003 \text{ mm Hg} / 760 \\ &= 0.000004\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 48 \text{ totes/month} \times 12 \text{ months/yr} \times 32.7 \text{ cu ft/tote} \times 0.000004 \times 0.9 \\ &= 0.07 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 0.07 \text{ cu ft} \times 92.14 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.02 \text{ lb} \\ &= 0.00001 \text{ tpy} \\ &= 0.000002 \text{ lb/hr}\end{aligned}$$



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Totes

TEMPO ID: EQT0213

Point Source ID No.: 1700-84B

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|--------------------------------------|--------------------------------------|----------------------------|
| Total VOC | 0.86 | 0.0001 | 0.0001 | 0.0004 |
| Chloroprene | 0.84 | 0.0001 | 0.0001 | 0.0004 |
| Toluene | 0.02 | 0.000002 | 0.000002 | 0.00001 |
| Total HAPs | 0.86 | 0.0001 | 0.0001 | 0.0004 |
| Total TAPs | 0.86 | 0.0001 | 0.0001 | 0.0004 |



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85

Page 1 of 4

Basis:

65% of LD shipments will be by bulk carrier.

LD loaded from Emulsion Storage Tanks # 11, 12, 15, 16 into vendor tank trucks

| | |
|-----------------------------------|----------------------------|
| Total LD Shipped = | 15 MMlb/yr dry wt |
| Total LD-750 Shipped = | 3.7 MMlb/yr dry wt |
| Solids component = | 50 wt % |
| Total LD Shipments Bulk = | 65 % of total |
| Loading Temperature = | 35 C |
| Vapor pressure CD at 35 °C = | 334.3 mm Hg |
| Vapor pressure toluene at 35 °C = | 52 mm Hg |
| MW of CD = | 88.54 lb/lb-mol |
| MW of Toluene = | 92.14 lb/lb-mol |
| CD component of emulsion = | 0.099 wt % max |
| Toluene component of emulsion = | 0.008415 wt % (LD-750) |
| Weight of LD loaded per truck = | 46000 lb wet wt |
| Weight of LD loaded per tote = | 2200 lb wet wt |
| Weight of LD loaded per Railcar = | 180000 lb wet wt |
| LD Density = | 68.53 lb/ft ³ |
| Specific Volume = | 359.7 ft ³ /mol |
| Operating Time = | 8760 hr |

Emission Rates

Truck Loading

Convert CD concentration to exclude the solids component

$$\begin{aligned} \text{CD component of emulsion} &= 0.099 / (1 - 0.5) \\ &= 0.198 \% \end{aligned}$$

$$\begin{aligned} \text{Mole Fraction CD} &= 0.198 / 88.54 / [0.198 / 88.54 + (100 - 0.198) / 18] \\ &= 0.0004 \end{aligned}$$

$$\begin{aligned} \text{Partial Pressure CD} &= 334.3 \times 0.0004 \\ &= 0.135 \text{ mm Hg} \end{aligned}$$

$$\begin{aligned} \text{Mole Fraction CD in Vapor} &= 0.135 \text{ mm Hg} / 760 \\ &= 0.000177 \end{aligned}$$



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Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 17C0-85

Page 2 of 4

$$\begin{aligned}\text{Vapor Vented per Truck} &= 46000 \text{ lb/truck} / 68.53 \text{ lb/cu ft} \\ &= 671.24 \text{ ft}^3/\text{truck}\end{aligned}$$

$$\begin{aligned}\text{No. of Trucks} &= 15 \text{ MMlb/yr dry} / (1 - 0.5) \times 0.65 \times 1000000 / 46000 \text{ lb/truck} \\ &= 424 \text{ trucks}\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 424 \text{ trucks/yr} \times 671.24 \text{ cu ft/truck} \times 0.000177 \\ &= 50.48 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 50.48 \text{ cu ft} \times 88.54 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 14.02 \text{ lb} \\ &= 0.007 \text{ tpy} \\ &= 0.002 \text{ lb/hr}\end{aligned}$$

Convert toluene concentration to exclude the solids component

$$\begin{aligned}\text{Toluene component of emulsion} &= 0.008415 / (1 - 0.5) \\ &= 0.017 \%\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction Toluene} &= 0.01683 / 92.14 / [0.01683 / 92.14 + (100 - 0.01683) / 18] \\ &= 0.00003\end{aligned}$$

$$\begin{aligned}\text{Partial Pressure Toluene in Tank} &= 52 \times 0.00003 \\ &= 0.002 \text{ mm Hg}\end{aligned}$$

$$\begin{aligned}\text{Mole Fraction Toluene in Vapor} &= 0.002 \text{ mm Hg} / 760 \\ &= 0.000002\end{aligned}$$

$$\begin{aligned}\text{No. of Trucks} &= 3.7 \text{ MMlb/yr dry} / (1 - 0.5) \times 0.65 \times 1000000 / 46000 \text{ lb/truck} \\ &= 105 \text{ trucks}\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 105 \text{ trucks/yr} \times 671.24 \text{ cu ft/truck} \times 0.000002 \\ &= 0.16 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 0.16 \text{ cu ft} \times 92.14 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.05 \text{ lb} \\ &= 0.00002 \text{ tpy} \\ &= 0.000005 \text{ lb/hr}\end{aligned}$$



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85

Page 3 of 4

Tote Filling

Allow 25% for reworking off spec and returns

$$\begin{aligned}\text{Vapor Vented per Tote} &= 2200 \text{ lb/tote} / 68.53 \text{ lb/cu ft} \\ &= 32.10 \text{ ft}^3/\text{tote}\end{aligned}$$

$$\begin{aligned}\text{No. of Totes} &= 15 \text{ MMlb/yr dry} / (1 - 0.5) \times (1 - 0.65) \times 1000000 / 2200 \text{ lb/tote} \times 1.25 \\ &= 5966 \text{ totes}\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 5966 \text{ totes/yr} \times 32.1 \text{ cu ft/tote} \times 0.000177 \\ &= 33.97 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{CD Emitted} &= 33.97 \text{ cu ft} \times 88.54 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 9.43 \text{ lb} \\ &= 0.005 \text{ tpy} \\ &= 0.001 \text{ lb/hr}\end{aligned}$$

$$\begin{aligned}\text{No. of LD-750 Totes} &= 3.7 \text{ MMlb/yr dry} / (1 - 0.5) \times (1 - 0.65) \times 1000000 / 2200 \text{ lb/tote} \times 1.25 \\ &= 1472 \text{ totes}\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 1472 \text{ totes/yr} \times 32.1 \text{ cu ft/tote} \times 0.000002 \\ &= 0.11 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\text{Toluene Emitted} &= 0.11 \text{ cu ft} \times 92.14 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.03 \text{ lb} \\ &= 0.00002 \text{ tpy} \\ &= 0.000004 \text{ lb/hr}\end{aligned}$$

**RTP**

Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85

Page 4 of 4

Railcar Loading

A maximum of 50 railcars will be loaded per year.

No. of Railcars = 50 railcars

$$\begin{aligned}\text{Vapor Vented per Truck} &= 180000 \text{ lb/railcar} / 68.53 \text{ lb/cu ft} \\ &= 2626.59 \text{ ft}^3/\text{railcar}\end{aligned}$$
$$\begin{aligned}\text{CD Emitted} &= 50 \text{ railcars/yr} \times 2626.59 \text{ cu ft/railcar} \times 0.000177 \\ &= 23.29 \text{ ft}^3\end{aligned}$$
$$\begin{aligned}\text{CD Emitted} &= 23.29 \text{ cu ft} \times 88.54 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 6.47 \text{ lb} \\ &= 0.003 \text{ tpy} \\ &= 0.001 \text{ lb/hr}\end{aligned}$$
$$\begin{aligned}\text{Toluene Emitted} &= 50 \text{ railcars/yr} \times 2626.59 \text{ cu ft/railcar} \times 0.000002 \\ &= 0.30 \text{ ft}^3\end{aligned}$$
$$\begin{aligned}\text{Toluene Emitted} &= 0.3 \text{ cu ft} \times 92.14 \text{ lb/lb-mole} / [359.7 \text{ cu ft/mole} \times (273 / (273 + 35))] \\ &= 0.09 \text{ lb} \\ &= 0.00004 \text{ tpy} \\ &= 0.00001 \text{ lb/hr}\end{aligned}$$

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------|---------------------|-----------------------------------|-----------------------------------|-------------------------|
| Total VOC | 30.08 | 0.0034 | 0.0034 | 0.015 |
| Chloroprene | 29.92 | 0.0034 | 0.0034 | 0.015 |
| Toluene | 0.16 | 0.00002 | 0.00002 | 0.00008 |
| Total HAPs | 30.08 | 0.0034 | 0.0034 | 0.015 |
| Total TAPs | 30.08 | 0.0034 | 0.0034 | 0.015 |



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Fugitive Emissions - Neoprene Unt

TEMPO ID: FUG0004

Point Source ID No.: 1-93

Page 1 of 3

Basis:

Site specific emission factors are based on bagging studies performed at various DuPont-Dow facilities including the Pontchartrain Site and consider historical performance from monitoring.

Emissions are for those components located outside of the Poly Building. Fugitives from equipment components located in the Poly Building are covered by the various manhole vents and Poly Building wall fans.

Calculation basis provided by Ms. D. Grego, DuPont

Summary

| Equipment | Service | Total Component Count | Average Emission Rate lb/hr | Total Emissions lb/yr | Total Emissions tpy |
|------------|------------|-----------------------|-----------------------------|-----------------------|---------------------|
| Valves | Lt. Liquid | 314 | 0.1225 | 1073 | 0.54 |
| | Gas | 89 | 0.0320 | 281 | 0.14 |
| Pump Seals | Lt. Liquid | 14 | 0.0161 | 141 | 0.07 |
| Connectors | All | 1780 | 0.3204 | 2807 | 1.40 |
| PRVs | Gas | 29 | 0.0035 | 30 | 0.02 |
| Total: | | | 0.4945 | 4332 | 2.17 |

Maximum Emission Rate = 0.4945 lb/hr

Speciation

Chloroprene Emissions = 0.3657 lb/hr
Chloroprene Emissions = 3203 lb/yr
Chloroprene Emissions = 1.602 tpy

Toluene Emissions = 0.0501 lb/hr
Toluene Emissions = 439 lb/yr
Toluene Emissions = 0.219 tpy



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Fugitive Emissions - Neoprene Unt

TEMPO ID: FUG0004

Point Source ID No.: 1-93

Page 2 of 3

Components in Chloroprene Service

| Equipment | Service | Component Count | Dupont-Dow Factor lb/hr/src | Emission Rate lb/hr | Total Emissions lb/yr |
|------------|--------------|-----------------|--------------------------------|------------------------|--------------------------|
| Valves | Lt. Liq./Gas | 234 | 3.90E-04 | 0.0913 | 799 |
| | Gas | 66 | 3.60E-04 | 0.0238 | 208 |
| Pump Seals | Lt. Liquid | 9 | 1.15E-03 | 0.0104 | 91 |
| Connectors | All | 1335 | 1.80E-04 | 0.2403 | 2105 |
| PRVs | Gas | 21 | 1.20E-04 | 0.0025 | 22 |
| Total: | | | | 0.3657 | 3203 |

Components in Toluene Service

| Equipment | Service | Component Count | Dupont-Dow Factor lb/hr/src | Emission Rate lb/hr | Total Emissions lb/yr |
|------------|--------------|-----------------|--------------------------------|------------------------|--------------------------|
| Valves | Lt. Liq./Gas | 32 | 3.90E-04 | 0.0125 | 109 |
| | Gas | 9 | 3.60E-04 | 0.0032 | 28 |
| Pump Seals | Lt. Liquid | 2 | 1.15E-03 | 0.0023 | 20 |
| Connectors | All | 178 | 1.80E-04 | 0.0320 | 281 |
| PRVs | Gas | 3 | 1.20E-04 | 0.0004 | 3 |
| Total: | | | | 0.0501 | 439 |

Components in Acetic Acid Service

| Equipment | Service | Component Count | Dupont-Dow Factor lb/hr/src | Emission Rate lb/hr | Total Emissions lb/yr |
|------------|--------------|-----------------|--------------------------------|------------------------|--------------------------|
| Valves | Lt. Liq./Gas | 16 | 3.90E-04 | 0.0062 | 55 |
| | Gas | 5 | 3.60E-04 | 0.0018 | 16 |
| Pump Seals | Lt. Liquid | 1 | 1.15E-03 | 0.0012 | 10 |
| Connectors | All | 89 | 1.80E-04 | 0.0160 | 140 |
| PRVs | Gas | 2 | 1.20E-04 | 0.0002 | 2 |
| Total: | | | | 0.0252 | 221 |



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Fugitive Emissions - Neoprene Unit

TEMPO ID: FUG0004

Point Source ID No.: 1-93

Page 3 of 3

Components in Other VOC Service

| Equipment | Service | Component Count | Dupont-Dow Factor lb/hr/src | Emission Rate lb/hr | Total Emissions lb/yr |
|------------|--------------|-----------------|--------------------------------|------------------------|--------------------------|
| Valves | Lt. Liq./Gas | 32 | 3.90E-04 | 0.0125 | 109 |
| | Gas | 9 | 3.60E-04 | 0.0032 | 28 |
| Pump Seals | Lt. Liquid | 2 | 1.15E-03 | 0.0023 | 20 |
| Connectors | All | 178 | 1.80E-04 | 0.0320 | 281 |
| PRVs | Gas | 3 | 1.20E-04 | 0.0004 | 3 |
| Total: | | | | 0.0501 | 439 |



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Diversion Tank

TEMPO ID: EQT0202

Point Source ID No.: 3-95

Page 1 of 3

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation = 8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 2.056E-08 g/s
Emission Rate = 0.0000002 lb/hr
Emission Rate = 0.001 lb/yr
Emission Rate = 0.0000007 tpy

Chloroprene

Emission Rate = 3.16E-06 g/s
Emission Rate = 0.00003 lb/hr
Emission Rate = 0.2 lb/yr
Emission Rate = 0.0001 tpy

Toluene

Emission Rate = 1.666E-07 g/s
Emission Rate = 0.000001 lb/hr
Emission Rate = 0.01 lb/yr
Emission Rate = 0.000006 tpy

ACR

Emission Rate = 1.666E-07 g/s
Emission Rate = 0.000001 lb/hr
Emission Rate = 0.01 lb/yr
Emission Rate = 0.000006 tpy



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Diversion Tank

TEMPO ID: EQT0202

Point Source ID No.: 3-95

Page 2 of 3

1,2-Dichlorobenzene

Emission Rate = 1.60E-07 g/s
Emission Rate = 0.000001 lb/hr
Emission Rate = 0.01 lb/yr
Emission Rate = 0.000006 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 1.58E-07 g/s
Emission Rate = 0.000001 lb/hr

Chloroprene

Emission Rate = 1.37E-05 g/s
Emission Rate = 0.0001 lb/hr

Toluene

Emission Rate = 1.28E-06 g/s
Emission Rate = 0.00001 lb/hr

ACR

Emission Rate = 1.28E-06 g/s
Emission Rate = 0.00001 lb/hr

1,2-Dichlorobenzene

Emission Rate = 1.23E-06 g/s
Emission Rate = 0.00001 lb/hr



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Diversion Tank

TEMPO ID: EQT0202

Point Source ID No.: 3-95

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|---------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 0.3 | 0.00003 | 0.0001 | 0.0001 |
| Chloroprene | 0.2 | 0.00003 | 0.0001 | 0.0001 |
| 1,2-Dichlorobenzene | 0.01 | 0.000001 | 0.00001 | 0.000006 |
| Toluene | 0.01 | 0.000001 | 0.00001 | 0.000006 |
| Total HAPs | 0.2 | 0.00003 | 0.0001 | 0.0001 |
| Total TAPs | 0.2 | 0.00003 | 0.0001 | 0.0001 |



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 Aeration Tank

TEMPO ID: EQT0203

Point Source ID No.: 4-95

Page 1 of 3

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation = 8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 0.000005233 g/s
Emission Rate = 0.00004 lb/hr
Emission Rate = 0.4 lb/yr
Emission Rate = 0.0002 tpy

Chloroprene

Emission Rate = 0.062409 g/s
Emission Rate = 0.495 lb/hr
Emission Rate = 4339 lb/yr
Emission Rate = 2.170 tpy

Toluene

Emission Rate = 0.001774 g/s
Emission Rate = 0.014 lb/hr
Emission Rate = 123 lb/yr
Emission Rate = 0.062 tpy

ACR

Emission Rate = 0.001774 g/s
Emission Rate = 0.014 lb/hr
Emission Rate = 123 lb/yr
Emission Rate = 0.062 tpy



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 Aeration Tank

TEMPO ID: EQT0203

Point Source ID No.: 4-95

Page 2 of 3

1,2-Dichlorobenzene

Emission Rate = 0.00184 g/s
Emission Rate = 0.015 lb/hr
Emission Rate = 128 lb/yr
Emission Rate = 0.064 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 4.05E-05 g/s
Emission Rate = 0.0003 lb/hr

Chloroprene

Emission Rate = 0.27019 g/s
Emission Rate = 2.144 lb/hr

Toluene

Emission Rate = 0.013652 g/s
Emission Rate = 0.108 lb/hr

ACR

Emission Rate = 0.013652 g/s
Emission Rate = 0.108 lb/hr

1,2-Dichlorobenzene

Emission Rate = 0.014244 g/s
Emission Rate = 0.113 lb/hr



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 Aeration Tank

TEMPO ID: EQT0203

Point Source ID No.: 4-95

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|----------------------------|--------------------------------------|--------------------------------------|--------------------------------|
| Total VOC | 4586 | 0.524 | 2.361 | 2.293 |
| Chloroprene | 4339 | 0.495 | 2.144 | 2.170 |
| 1,2-Dichlorobenze | 128 | 0.014 | 0.113 | 0.064 |
| Toluene | 123 | 0.014 | 0.108 | 0.062 |
| Total HAPs | 4590 | 0.523 | 2.366 | 2.295 |
| Total TAPs | 4590 | 0.523 | 2.366 | 2.295 |



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.

Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 Aeration Tank

TEMPO ID: EQT0204

Point Source ID No.: 5-95

Page 1 of 3

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation = 8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 5.58E-07 g/s
Emission Rate = 0.000004 lb/hr
Emission Rate = 0.04 lb/yr
Emission Rate = 0.00002 tpy

Chloroprene

Emission Rate = 0.0007275 g/s
Emission Rate = 0.006 lb/hr
Emission Rate = 51 lb/yr
Emission Rate = 0.025 tpy

Toluene

Emission Rate = 0.00001718 g/s
Emission Rate = 0.0001 lb/hr
Emission Rate = 1 lb/yr
Emission Rate = 0.001 tpy

ACR

Emission Rate = 0.00001718 g/s
Emission Rate = 0.0001 lb/hr
Emission Rate = 1 lb/yr
Emission Rate = 0.001 tpy



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 Aeration Tank

TEMPO ID: EQT0204

Point Source ID No.: 5-95

Page 2 of 3

1,2-Dichlorobenzene

Emission Rate = 1.12E-04 g/s
Emission Rate = 0.0009 lb/hr
Emission Rate = 8 lb/yr
Emission Rate = 0.004 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 4.31E-06 g/s
Emission Rate = 0.00003 lb/hr

Chloroprene

Emission Rate = 0.00315 g/s
Emission Rate = 0.025 lb/hr

Toluene

Emission Rate = 1.32E-04 g/s
Emission Rate = 0.001 lb/hr

ACR

Emission Rate = 1.32E-04 g/s
Emission Rate = 0.001 lb/hr

1,2-Dichlorobenzene

Emission Rate = 8.70E-04 g/s
Emission Rate = 0.007 lb/hr



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 Aeration Tank

TEMPO ID: EQT0204

Point Source ID No.: 5-95

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|---------------------|--------------------------------|--------------------------------|-------------------------|
| Total VOC | 53 | 0.006 | 0.027 | 0.027 |
| Chloroprene | 51 | 0.006 | 0.025 | 0.025 |
| 1,2-Dichlorobenze | 8 | 0.001 | 0.007 | 0.004 |
| Toluene | 1 | 0.000 | 0.001 | 0.001 |
| Total HAPs | 60 | 0.007 | 0.033 | 0.030 |
| Total TAPs | 60 | 0.007 | 0.033 | 0.030 |



Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Clarifier

TEMPO ID:

Point Source ID No.: 6-95

Page 1 of 3

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation = 8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 4.74E-08 g/s
Emission Rate = 0.0000004 lb/hr
Emission Rate = 0.003 lb/yr
Emission Rate = 0.000002 tpy

Chloroprene

Emission Rate = 9.316E-06 g/s
Emission Rate = 0.00007 lb/hr
Emission Rate = 0.6 lb/yr
Emission Rate = 0.0003 tpy

Toluene

Emission Rate = 2.346E-07 g/s
Emission Rate = 0.000002 lb/hr
Emission Rate = 0.02 lb/yr
Emission Rate = 0.000008 tpy

ACR

Emission Rate = 2.346E-07 g/s
Emission Rate = 0.000002 lb/hr
Emission Rate = 0.02 lb/yr
Emission Rate = 0.000008 tpy



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Clarifier

TEMPO ID:

Point Source ID No.: 6-95

Page 2 of 3

1,2-Dichlorobenzene

Emission Rate = 2.04E-06 g/s
Emission Rate = 0.00002 lb/hr
Emission Rate = 0.1 lb/yr
Emission Rate = 0.00007 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 3.66E-07 g/s
Emission Rate = 0.00000 lb/hr

Chloroprene

Emission Rate = 4.03E-05 g/s
Emission Rate = 0.0003 lb/hr

Toluene

Emission Rate = 1.81E-06 g/s
Emission Rate = 0.00001 lb/hr

ACR

Emission Rate = 1.81E-06 g/s
Emission Rate = 0.00001 lb/hr

1,2-Dichlorobenzene

Emission Rate = 1.58E-05 g/s
Emission Rate = 0.0001 lb/hr



RTP
Environmental Associates, Inc.

Air Emissions Calculation Sheet

RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Clarifier

TEMPO ID:

Point Source ID No.: 6-95

Page 3 of 3

Summary

| Compound | Total Loss lb/yr | Average Emission Rate lb/hr | Maximum Emission Rate lb/hr | Annual Emissions tpy |
|-------------------|---------------------|-----------------------------------|-----------------------------------|-------------------------|
| Total VOC | 0.7 | 0.00008 | 0.0004 | 0.0003 |
| Chloroprene | 0.6 | 0.00007 | 0.0003 | 0.0003 |
| 1,2-Dichlorobenze | 0.1 | 0.00002 | 0.0001 | 0.00007 |
| Toluene | 0.02 | 0.000002 | 0.00001 | 0.000008 |
| Total HAPs | 0.8 | 0.00009 | 0.0005 | 0.0004 |
| Total TAPs | 0.8 | 0.00009 | 0.0005 | 0.0004 |

APPENDIX B

CERTIFICATION OF GOOD STANDING

Tom Schedler
Secretary of State

State of Louisiana
Secretary of State

COMMERCIAL DIVISION
225.925.4704



Fax Numbers
225.932.5317 (Admin. Services)
225.932.5314 (Corporations)
225.932.5318 (UCC)

| Name | Type | City | Status |
|--------------------------------------|--------------------------------------|------------|--------|
| E. I. DU PONT DE NEMOURS AND COMPANY | Business Corporation (Non-Louisiana) | WILMINGTON | Active |

Business: E. I. DU PONT DE NEMOURS AND COMPANY

Charter Number: 09302090F

Registration Date: 4/24/1919

State Of Origin:

Domicile Address

1007 MARKET STREET

WILMINGTON, DE 19898

Mailing Address

ATTENTION: TAX DIVISION, D-13039

1007 MARKET STREET

WILMINGTON, DE 19898

Principal Business Office

1007 MARKET STREET

WILMINGTON, DE 19898

Registered Office in Louisiana

5615 CORPORATE BLVD., STE. 400B

BATON ROUGE, LA 70808

Principal Business Establishment in Louisiana

PONTCHARTRAIN WORKS

LAPLACE, LA 70068

Status

Status: Active

Annual Report Status: In Good Standing

Qualified: 4/24/1919

Last Report Filed: 4/4/2012

Type: Business Corporation (Non-Louisiana)

Registered Agent(s)

| | |
|--------------------------|---------------------------------|
| Agent: | C T CORPORATION SYSTEM |
| Address 1: | 5615 CORPORATE BLVD., STE. 400B |
| City, State, Zip: | BATON ROUGE, LA 70808 |
| Appointment Date: | 12/12/1955 |

Officer(s)

Additional Officers: No

| | |
|-------------------|--------------------------|
| Officer: | NICHOLAS C. FANANDAKIS |
| Title: | Executive Vice-President |
| Address 1: | 1007 MARKET ST. |

| | |
|--------------------------|--------------------------|
| City, State, Zip: | WILMINGTON, DE 19898 |
| Officer: | THOMAS M. CONNELLY, JR. |
| Title: | Executive Vice-President |
| Address 1: | 1007 MARKET ST. |
| City, State, Zip: | WILMINGTON, DE 19898 |
| Officer: | MARY E. BOWLER |
| Title: | Secretary |
| Address 1: | 1007 MARKET ST. |
| City, State, Zip: | WILMINGTON, DE 19898 |
| Officer: | MARY P. VAN VEEN |
| Title: | Vice-President |
| Address 1: | 1007 MARKET ST. |
| City, State, Zip: | WILMINGTON, DE 19898 |
| Officer: | ELLEN J. KULLMAN |
| Title: | Officer, Director |
| Address 1: | 1007 MARKET ST. |
| City, State, Zip: | WILMINGTON, DE 19898 |

Mergers (4)

| Filed Date | Effective Date: | Type | Charter# | Chater Name | Role |
|------------|-----------------|-------|-----------|--------------------------------------|----------|
| 1/29/1973 | 1/29/1973 | MERGE | 09302090F | E. I. DU PONT DE NEMOURS AND COMPANY | SURVIVOR |
| 6/4/1973 | 6/4/1973 | MERGE | 09302090F | E. I. DU PONT DE NEMOURS AND COMPANY | SURVIVOR |
| 10/24/1977 | 10/24/1977 | MERGE | 09302090F | E. I. DU PONT DE NEMOURS AND COMPANY | SURVIVOR |
| 4/19/1982 | 4/19/1982 | MERGE | 09302090F | E. I. DU PONT DE NEMOURS AND COMPANY | SURVIVOR |

Amendments on File (35)

| Description | Date |
|-------------|------------|
| Amendment | 6/18/1923 |
| Amendment | 7/27/1925 |
| Amendment | 11/13/1926 |
| Amendment | 2/16/1929 |
| Amendment | 5/14/1934 |
| Amendment | 8/23/1937 |
| Amendment | 10/30/1939 |
| Amendment | 5/2/1940 |
| Amendment | 4/10/1942 |
| Amendment | 6/22/1946 |
| Amendment | 5/12/1947 |
| Amendment | 5/12/1947 |
| Amendment | 6/20/1949 |
| Amendment | 7/11/1955 |
| Amendment | 7/11/1955 |
| Amendment | 7/11/1955 |
| Amendment | 12/5/1957 |
| Amendment | 7/19/1963 |
| Amendment | 9/26/1966 |

| | |
|---------------------------------|------------|
| Amendment | 5/6/1968 |
| Amendment | 5/14/1970 |
| Merger | 1/29/1973 |
| Merger | 6/4/1973 |
| Amendment | 4/29/1974 |
| Merger | 10/24/1977 |
| Amendment | 10/24/1977 |
| Amendment | 4/20/1979 |
| Amendment | 4/20/1979 |
| Amendment | 4/25/1980 |
| Amendment | 8/21/1981 |
| Merger | 4/19/1982 |
| Stmt of Chg or Chg Prin Bus Off | 2/22/1985 |
| Stmt of Chg or Chg Prin Bus Off | 4/1/1986 |
| Stmt of Chg or Chg Prin Bus Off | 2/1/1993 |
| Stmt of Chg or Chg Prin Bus Off | 1/29/2008 |

[Print](#)

APPENDIX C

FUGITIVE EMISSIONS PROGRAM CONSOLIDATION NOTICE

**Louisiana Fugitive Emission Program Consolidation
Source Notice and Agreement
DuPont Pontchartrain Site, St. John the Baptist Parish
(Agency Interest Numbers 1101 and 38806)**

By this notice and agreement, E. I. du Pont de Nemours Co. (DuPont Pontchartrain Site) notifies the Louisiana DEQ (LDEQ) and the United States Environmental Protection Agency (EPA) of the consolidation of fugitive emission programs as indicated below, effective January 1, 2014. Semiannual reports will be submitted on August 15 and February 15, to cover the periods January 1 through June 30 and July 1 through December 31, respectively. DuPont Pontchartrain Site agrees to implement the consolidated program in accordance with the Louisiana Fugitive Emission Program Consolidation Guidelines attached, and accepts federal and state enforceability of the consolidated program by EPA and LDEQ. DuPont Pontchartrain Site further acknowledges that compliance with the consolidated program in accordance with the Guidelines will serve to comply with each of the fugitive emission programs being consolidated. In addition, DuPont Pontchartrain Site acknowledges that noncompliance with the consolidated program in accordance with the Guidelines may subject DuPont Pontchartrain Site to enforcement action for one or more of the fugitive emissions programs being consolidated. Unless successfully challenged or otherwise terminated, this agreement remains in effect until revised or replaced upon request by DuPont Pontchartrain Site, LDEQ, or EPA, or until the initial Part 70 permit is issued for DuPont Pontchartrain Site, whichever is earliest. If, at any time, the agreement is not in effect with the State, then it shall not be in effect with EPA.

While several units at the DuPont Pontchartrain Site are only subject to less stringent fugitive emission rules, the entire site will comply with the HON (40 CFR 63 Subpart H) as the most stringent and guiding fugitive rule in each unit at the site per table below. On the effective date the reporting, recordkeeping, and monitoring time period (schedule) will be readjusted for the entire site to coincide with the current Diamines, ACR, and HCL Recovery Unit's schedule which runs as a calendar year from January through December therefore making the entire site applicable to just one time period. Also from the effective date, leak rates will be consolidated and calculated for the entire site per HON guidelines. The DuPont Pontchartrain Site will continue the annual valve and biennial connector monitoring frequency for the plant site until percentage leak rates dictate altering the monitoring frequency.

| Unit or Plant Site | Programs being Consolidated | Stream Applicability | Overall Most Stringent Program |
|---------------------------|---|---|--------------------------------|
| DuPont Pontchartrain Site | 63 Sub H – HON 63 Sub FFFF 63 Sub U - P & R I LA Non-HON NSPS RCRA Sub BB LAC 33:III.2121 | 5% VOHAP 5% VOHAP 5% VOHAP 5% VOTAP 10% VOC 10% VOC 10% VOC | 63 Subpart H - HON MACT |

Signed

Walter Glenn
Walter Glenn, Plant Manager

This 18 day of November, 2013



The miracles of science™

DuPont
Pontchartrain Site
560 Highway 44
LaPlace, LA 70068-6908

November 18, 2013

Dept. of Environmental Quality
Office of Environmental Services, Air Permits Division
P. O. Box 4313
Baton Rouge, La 70821-4313

CERTIFIED MAIL NO. 7011 3500 0001 6350 0509

**Re: DuPont Pontchartrain Site Fugitive Emissions Program Consolidation
Source Notice and Agreement (AI# 1101 and AI# 38806)**

The DuPont Pontchartrain Site (DuPont) is requesting consolidation of all applicable site fugitive emission programs in accordance with the Louisiana Fugitive Emission Program Consolidation Guidelines and is hereby submitting the attached Source Notice and Agreement. DuPont will implement the consolidated program beginning January, 1, 2014.

While several units are only subject to less stringent fugitive emission rules, the entire site will comply with the HON (40 CFR 63 Subpart H) as the most stringent and guiding fugitive rule in each unit at the site. According to 40 CFR 63.162(g)(2) and 63.9(i) it is acceptable to adjust time periods upon mutual agreement between owner and Administrator. In addition to being regulatory acceptable, adjusting time periods is in keeping with the spirit of the consolidation agreement recordkeeping and report streamlining intention. DuPont is also requesting that the reporting, recordkeeping, and monitoring time period (schedule) be readjusted for the entire site to coincide with the current Diamines, ACR, and HCL Recovery Unit's schedule which runs as a calendar year from January through December therefore making the entire site applicable to one time period. Each unit at the site currently has a leak rate that allows for annual valve and biennial connector monitoring. From the effective date, leak rates will be consolidated and calculated for the entire site per HON guidelines. The DuPont Pontchartrain Site will continue the annual valve and biennial connector monitoring frequency for the plant site until percentage leak rates dictate altering the monitoring frequency.

The following paragraphs provide additional details relating to the fugitive programs being consolidated and how the fugitive program will be structured after the effective date.

The DuPont Pontchartrain Site currently has five units subject to various fugitive emissions regulations which have multiple overlapping applicable reporting and recordkeeping requirements. The recordkeeping requirements of these various regulations result in the same data being saved and summarized multiple times in the LDAR database. The current reporting requirements result in the submittal

of ten different reports with deadlines for these reports at different times throughout the year. These different reports often result in submitting data already reported in previous reports. In other words, multiple reports are due for different periods with some of these reports requiring and containing the same data or at least some of the same data. The *Fugitive Emissions Semi-annual Report Summary Table* below summarizes the program report and reporting time period information for each unit.

The following is a list of the units at the site with the most stringent applicable regulation in parenthesis: the Diamines Unit (HON), ACR Unit (MON), Chloroprene Unit (HON), the Neoprene Unit (Polymer & Resins I), and the HCL Recovery Unit (RCRA BB). The Diamines Unit which has always been owned by E. I. du Pont de Nemours Co. has already been consolidated by agreement dated October 15, 1996. The ACR, Chloroprene, HCL Recovery, and Neoprene Units were operated by DuPont Performance Elastomers, a separate entity, before 2013 and are not currently consolidated per Louisiana Fugitive Agreement. The entire facility (DuPont Pontchartrain Site) is now owned by E. I. du Pont de Nemours Co.

Fugitive Emissions Semi-annual Report Summary Table

| Unit | Program Report | Reporting Time Period before January 1, 2014 | Reporting Time Period beginning on January 1, 2014 |
|--------------|-----------------------|---|--|
| Diamines | HON Consolidated | January through June and July through December | January through June and July through December |
| Chloroprene | HON | April through September and October through March | January through June and July through December |
| Neoprene | Polymers and Resins I | August through January and February through July | January through June and July through December |
| ACR | MON | January through June and July through December | January through June and July through December |
| HCL Recovery | Chapter 21 | January through June and July through December | January through June and July through December |

Note: Chapter 21 report contains data from Chloroprene, Neoprene, and ACR Units also.

Consolidating all the units at the DuPont Pontchartrain Site and making HON the Guiding Regulation (most stringent rule) throughout the site, will reduce the recordkeeping and reporting requirements without reducing quality of data that was submitted in the multiple reports. All of the monitoring and leak data would still be reported, it will just be reported in two semi-annual reports instead of the current ten reports that result in multiple instances of data duplication. The site will also be complying with an overall more stringent fugitive emissions program

than by complying with various less stringent programs, therefore over time reducing fugitive emissions at the site. The DuPont Pontchartrain Site will continue to submit fugitive reports for the non-HON regulations until all data for the 2013 calendar year has been reported. After all 2013 data has been reported per non-HON fugitive requirements, the DuPont Pontchartrain Site will discontinue these non-HON fugitive reports and will only submit HON semi-annual reports twice a year for the entire site.

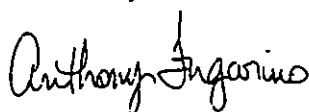
Each unit at the site currently has a leak rate that allows for annual valve and biennial connector monitoring. The DuPont Pontchartrain Site will continue this monitoring frequency (skip period frequency) for the plant site until percentage leak rates dictate altering the monitoring frequency. Leak rates will be calculated for the entire site per HON for periods that relate to calendar year of January through December beginning on the effective date.

In summary, on January 1, 2014, the effective date of the consolidated agreement, the DuPont Pontchartrain Site will streamline the recordkeeping, reporting, and monitoring requirements and readjust the recordkeeping, reporting, and monitoring requirements' annual time period to January through December to coincide with the current Diamines, ACR, and HCL Recovery Units' annual time period while keeping the current skip period monitoring frequency intact.

At the next opportunity for renewal or modification of each of the effective permits, DuPont will include a copy of the Fugitive Emissions Program Consolidation Source Notice and Agreement in each of the effective Title V operating permit applications. Current effective Permit Numbers are 3000-V3, 206-V1, 2249-V6, and 2090-V5.

If you have any questions or need additional information you can contact me at (985) 536-5438, or at Anthony.J.Fugarino@dupont.com.

Sincerely,



Anthony Fugarino
SHE Consultant

Enclosures

cc: US EPA Region 6
Compliance Assurance and Enforcement Division
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